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Natural gas — Calculation of methane number

Gaz naturel — Calcul de l'indice de méthane

Reference number
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Foreword

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The committee responsible for this document is ISO/TC 193, *Natural Gas*.

Natural gas — Calculation of methane number

1 Scope

This Technical Report describes methods for the calculation of the methane number (*MN*) of dry natural gas when the composition of the gas by mole fraction is known.

If the difference of *MN* between two calculation methods is more than 6, it is recommended to use a test method to determine *MN* for the gas.

The Gas Research Institute (GRI) methods are used to calculate methane number, *MN*, and motor octane number, *MON*, of gas; the linear relation is useful in determining and comparing the knock resistance of high methane content natural gas.

2 Terms and definitions

For the purposes of this document, the following terms and definitions apply.

2.1

methane number

MN

measure of resistance of a gas fuel to knock, which is assigned to a test fuel based upon operation in knock testing unit at the same standard knock intensity

Note 1 to entry: It is assigned that pure methane is used as the knock resistant reference fuel, that is, methane number of pure methane is 100, and pure hydrogen is used as the knock sensitive reference fuel, methane number of pure hydrogen is 0.

2.2

motor octane number

MON

numerical rating of knock resistance obtained by comparison of its knock intensity with that of primary reference fuels when both are tested in a standardized CFR engine operating under the specified conditions

3 Calculation methods of methane number

3.1 GRI methods

The GRI has applied the ASTM octane rating method to various natural gas fuels (see [Annex A](#)) to measure *MON*. Two mathematical relations were developed to estimate the *MON* rating of a natural gas fuel. The limitation of each component is shown in [Table A.2](#).

3.1.1 Linear coefficient relation

$$MON = 137,78_{x1} + 29,948_{x2} - 18,193_{x3} - 167,062_{x4} + 181,233_{x5} + 26,994_{x6} \quad (1)$$

where

x is the mole fraction of corresponding component.

The number of subscripts for each corresponding component is given as follow:

| number | 1 | 2 | 3 | 4 | 5 | 6 |
|-----------|-----------------|-------------------------------|-------------------------------|--------------------------------|-----------------|----------------|
| component | CH ₄ | C ₂ H ₆ | C ₃ H ₈ | C ₄ H ₁₀ | CO ₂ | N ₂ |

3.1.2 Hydrogen/carbon ratio relation

$$MON = -406,14 + 508,04 R - 173,55 R^2 + 20,17 R^3 \quad (2)$$

where

R is ratio of hydrogen atoms to carbon atoms.

NOTE In the original GRI composition data of gas fuels for octane test, the heaviest hydrocarbon is butane. In fact, real gas can contain C₆+ even C₈ hydrocarbons. If the gas contains hydrocarbons heavier than butane, take into account that the ratio of hydrogen atoms to carbon atoms could be different. All hydrocarbons are to be considered, not only those that are lighter than butane.

3.1.3 Correlation between MON and MN

$$MN = 1,445 MON - 103,42 \quad (3)$$

$$MON = 0,679 MN + 72,3 \quad (4)$$

NOTE The correlation is not quite linear, and as a result the formulae are not the inverse of each other.

3.2 AVL method

AVL Inc. also developed a method to calculate the methane number, but the exact algorithm is confidential and property of AVL Inc.

NOTE The AVL method is to be published in a CEN standard developed by CEN/TC 234/WG 11.

4 Express calculated MN

4.1 Mole fraction

If the mole fraction of a natural gas fuel is known, MN can be calculated. Since there are two formulae for MON, two MNs of the gas can be calculated. The two results should both be reported in the calculation report.

For the same gas, if the difference between the two MNs is more than 10, this is extraordinary. It means the composition of the gas is unusual. For example, the gas can be diluted by LPG gas, or the gas can contain more nitrogen or CO₂.

According to Reference [1], most European gases are in the MN range between 65 and 100. For the engines used in the tests, as a rule of thumb, a 10-point decrease in MN roughly results in a 1-point decrease in the knock-limited compression ratio. Also, a 10-point decrease in MN roughly results in a reduction in the knock-limited bemp.

If the difference between the two MN results is more than 6, the user should consider that the two MNs are in doubt, then, a test method rather than the calculations of this technical report should be used.

Annex A (informative)

GRI original composition data of gas fuels for octane test

Table A.1 — GRI original composition data of gas fuels for octane test

| Blend % | Metane % | Ethane % | Propane % | Butane % | CO ₂ % | Nitrogen % | H/C % |
|---------|----------|----------|-----------|----------|-------------------|------------|-------|
| 1 | 100 | - | - | - | - | - | 4,0 |
| 2 | 95,0 | 3,0 | 0,5 | 0,5 | 0,2 | 0,8 | 3,89 |
| 3 | 90,1 | 6,0 | 0,7 | 0,8 | 0,7 | 1,7 | 3,82 |
| 4 | 85,0 | 6,5 | 3,0 | 1,0 | 1,0 | 3,5 | 3,72 |
| 5 | 88,3 | 7,8 | 1,2 | 0,3 | 1,8 | 0,6 | 3,80 |
| 6 | 84,2 | 8,5 | 3,7 | - | 1,0 | 2,5 | 3,72 |
| 7 | 84,2 | 8,6 | 3,7 | - | 1,0 | 2,5 | 3,72 |
| 8 | 82,1 | 14,0 | 1,2 | - | 0,7 | 2,0 | 3,71 |
| 9 | 75,0 | - | 25,0 | - | - | - | 3,33 |
| 10 | 82,5 | - | 17,5 | - | - | - | 3,48 |
| 11 | 88,9 | - | 11,1 | - | - | - | 3,64 |
| 12 | 92,5 | 3,5 | 1,0 | 0,5 | 1,0 | 1,5 | 3,87 |

From John Kubesh[2].

Table A.2 — The concentration limitation of each component for octane test of GRI

| No. | Component | Limitation, mole fraction % |
|-----|-----------------|-----------------------------|
| 1 | Methane | ≥75 |
| 2 | Ethane | ≤14 |
| 3 | Propane | ≤25 |
| 4 | Butane+ | ≤1,0 |
| 5 | CO ₂ | ≤1,8 |
| 6 | Nitrogen | ≤3,5 |

Annex B

(informative)

The calculated *MNs* of some typical natural gas mixtures

There are 36 European and 30 Chinese and Thai natural gas mixtures, the calculated *MNs* are listed in [Tables B.1](#) and [B.2](#). The causes for *MN* difference of more than 6 are listed in [Tables B.3](#) and [B.4](#), and the composition of the gas is listed in [Tables B.5](#) and [B.6](#).

Table B.1 — Calculated *MN* of 36 Euro natural gas mixtures by two GRI methods

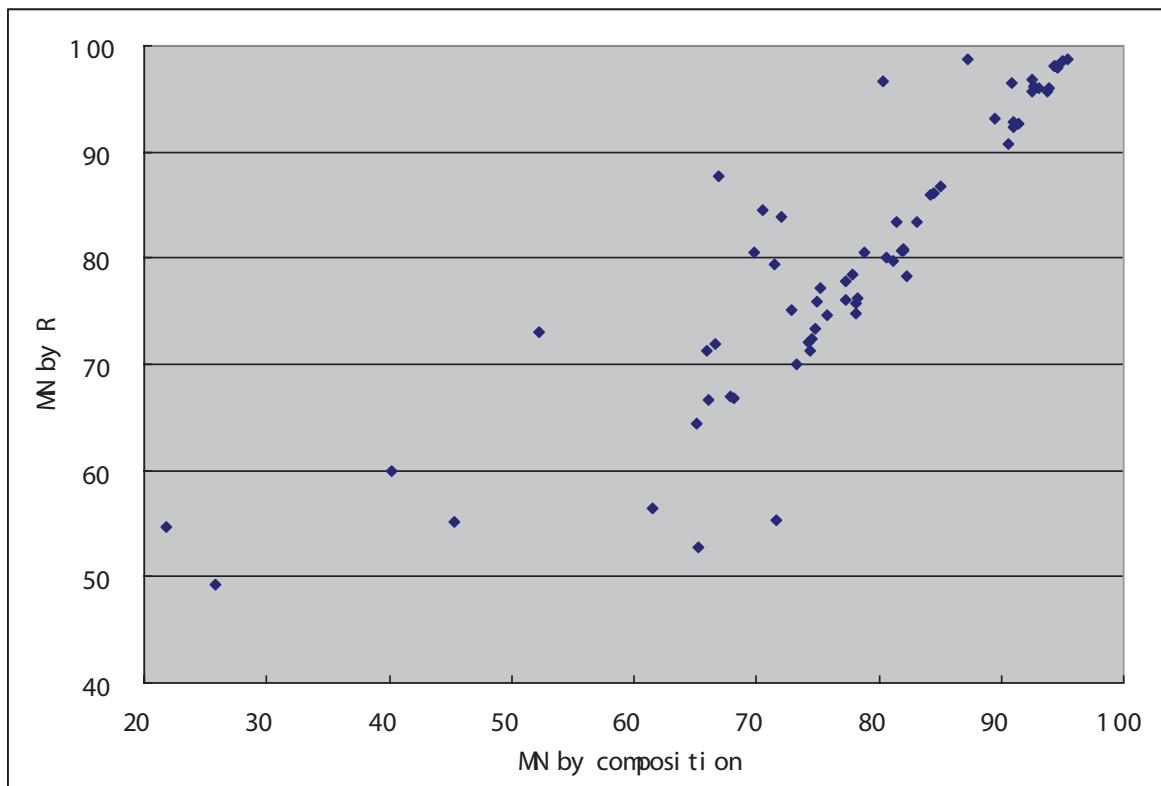
| No. | Content method | HC ratio method | Difference (absolute) |
|-----|----------------|-----------------|-----------------------|
| 1 | 84,18 | 85,90 | 1,72 |
| 2 | 71,48 | 79,39 | 7,91 |
| 3 | 85,08 | 86,83 | 1,75 |
| 4 | 78,10 | 74,74 | 3,36 |
| 5 | 73,23 | 70,04 | 3,19 |
| 6 | 81,50 | 83,36 | 1,86 |
| 7 | 66,05 | 66,61 | 0,56 |
| 8 | 74,78 | 73,29 | 1,49 |
| 9 | 78,81 | 80,52 | 1,71 |
| 10 | 80,58 | 80,01 | 0,57 |
| 11 | 70,56 | 84,60 | 14,04 |
| 12 | 91,03 | 92,38 | 1,35 |
| 13 | 89,53 | 93,13 | 3,60 |
| 14 | 68,20 | 66,77 | 1,43 |
| 15 | 67,83 | 66,97 | 0,86 |
| 16 | 66,97 | 87,72 | 20,75 |
| 17 | 75,24 | 77,26 | 2,02 |
| 18 | 69,81 | 80,54 | 10,73 |
| 19 | 95,06 | 98,57 | 3,51 |
| 20 | 92,73 | 96,21 | 3,48 |
| 21 | 84,48 | 86,08 | 1,60 |
| 22 | 66,66 | 71,86 | 5,20 |
| 23 | 74,41 | 71,24 | 3,17 |
| 24 | 77,35 | 76,07 | 1,28 |
| 25 | 83,11 | 83,40 | 0,29 |
| 26 | 75,78 | 74,56 | 1,22 |
| 27 | 91,05 | 92,77 | 1,72 |
| 28 | 66,00 | 71,32 | 5,32 |
| 29 | 80,34 | 96,62 | 16,28 |
| 30 | 72,07 | 83,88 | 11,81 |
| 31 | 74,26 | 72,15 | 2,11 |

Table B.1 (continued)

| No. | Content method | HC ratio method | Difference (absolute) |
|-----|----------------|-----------------|-----------------------|
| 32 | 92,54 | 95,68 | 3,14 |
| 33 | 74,99 | 75,90 | 0,91 |
| 34 | 18,04 | 53,15 | 35,11 |
| 35 | 40,14 | 59,89 | 19,75 |
| 36 | 21,84 | 54,67 | 32,83 |

Table B.2 — Calculated MN of 24 Chinese natural gas mixtures by two GRI methods

| No. | Content method | HC ratio method | Differences (absolute) |
|-----|----------------|-----------------|------------------------|
| 1 | 82,01 | 80,71 | 1,30 |
| 2 | 74,53 | 72,38 | 2,15 |
| 3 | 78,16 | 75,76 | 2,40 |
| 4 | 82,00 | 80,89 | 1,11 |
| 5 | 91,46 | 92,65 | 1,19 |
| 6 | 93,73 | 95,77 | 2,04 |
| 7 | 93,87 | 96,03 | 2,16 |
| 8 | 90,58 | 90,76 | 0,18 |
| 9 | 93,07 | 96,06 | 2,99 |
| 10 | 78,33 | 76,30 | 2,03 |
| 11 | 87,24 | 98,74 | 11,50 |
| 12 | 95,43 | 98,67 | 3,24 |
| 13 | 72,88 | 75,03 | 2,15 |
| 14 | 77,87 | 78,46 | 0,59 |
| 15 | 77,35 | 77,81 | 0,46 |
| 16 | 52,20 | 73,11 | 20,91 |
| 17 | 81,93 | 80,63 | 1,30 |
| 18 | 81,13 | 79,77 | 1,36 |
| 19 | 65,12 | 64,48 | 0,64 |
| 20 | 45,34 | 55,08 | 9,74 |
| 21 | 82,31 | 78,33 | 3,98 |
| 22 | 94,37 | 98,01 | 3,64 |
| 23 | 94,57 | 97,91 | 3,34 |
| 24 | 94,49 | 98,11 | 3,62 |
| 25 | 61,56 | 56,36 | 5,20 |
| 26 | 71,68 | 55,38 | 16,30 |
| 27 | 65,32 | 52,84 | 12,48 |
| 28 | 90,89 | 96,47 | 5,58 |
| 29 | 25,87 | 49,30 | 23,43 |
| 30 | 92,46 | 96,77 | 4,31 |

**Figure B.1 — MNs from two methods**

The [Figure B.1](#) represents the results of [Tables B.1](#) and [B.2](#). It shows the relationship between the methane number calculated from composition and the one calculated from HC ratio. It is apparent that while a certain degree of consistency exists for high methane numbers, below MN 85, both methods are giving inconsistent results. For instance, a gas with a methane value around 70 when calculated with composition will have a methane value between 65 and 80 according to the HC method.

Table B.3 — Causes for MN difference is more than 6 (Euro gas)

| No. of sample | MN difference | Causes |
|---------------|-----------------|---|
| No.11 | 13,59 | N_2 : 10,8 % |
| No.16 | 20,21 | N_2 : 14,351 % |
| No.18 | 9,83 | N_2 : 11,001 %; CO_2 : 4,184 % |
| No.29 | 16,20 | N_2 : 9,58 % |
| No.30 | 11,16 | N_2 : 9,85 % |
| No.34 | 34,73 | O_2 : 3,39 %; N_2 : 13,53 %; nC_4 : 10,77 % |
| No.35 | 19,39 | O_2 : 3,39 %; N_2 : 13,77 % |
| No.36 | 32,54 | O_2 : 2,14%; N_2 : 16,57%; nC_4 : 8,48% |

Table B.4 — Causes for MN difference is more than 6 (Chinese and Tahiland's gas)

| No. of sample | MN difference | Causes |
|---------------|-----------------|--------------------------------|
| No. 11 | 6,18 | N_2 : 6,39%; CO_2 : 3,71 % |
| No. 16 | 17,95 | N_2 : 17,24 % |
| No. 20 | 6,51 | C_4 : 6,45 % |

Table B.4 (continued)

| No. of sample | MN difference | Causes |
|---------------|---------------|---------------------------|
| No. 25 | 13,52 | CO ₂ : 22,34 % |
| No. 26 | | CO ₂ : 23,46 % |
| No. 29 | | C ₄ : 6,966 % |

Table B.5 — Composition of 36 Euro gas mixtures

| Component | 1 | 2 | 3 | 4 | 5 | 6 |
|------------------|-------|-------|-------|--------|--------|--------|
| N ₂ | 2,04 | 7,19 | 2,14 | 0,9 | 0,97 | 2,79 |
| CO ₂ | 0,33 | 0,43 | 0,86 | 2,28 | 2,63 | 0,78 |
| C ₁ | 93,3 | 86,04 | 93,05 | 87,44 | 85,27 | 91,27 |
| C ₂ | 3,24 | 4,46 | 2,96 | 6,69 | 7,24 | 3,73 |
| C ₃ | 0,66 | 1,06 | 0,59 | 2,19 | 2,73 | 0,89 |
| i-C ₄ | 0,13 | 0,25 | 0,12 | 0,22 | 0,46 | 0,175 |
| n-C ₄ | 0,13 | 0,25 | 0,12 | 0,22 | 0,46 | 0,175 |
| i-C ₅ | 0,04 | 0,1 | 0,035 | 0,025 | 0,1 | 0,05 |
| n-C ₅ | 0,04 | 0,1 | 0,035 | 0,025 | 0,1 | 0,05 |
| C ₆ | 0,05 | 0,08 | 0,05 | 0,01 | 0,03 | 0,04 |
| C ₇ | 0,03 | 0,03 | 0,03 | 0 | 0,01 | 0,04 |
| C ₈ | 0,01 | 0,01 | 0,01 | 0 | 0 | 0,01 |
| Sum | 100 | 100 | 100 | 100 | 100 | 100 |
| Component | 7 | 8 | 9 | 10 | 11 | 12 |
| N ₂ | 0,05 | 0,6 | 3,36 | 1 | 10,8 | 0,3 |
| CO ₂ | 0 | 0 | 1,4 | 0 | 1,1 | 0 |
| C ₁ | 82,07 | 88,6 | 88,72 | 91,2 | 83,5 | 97,3 |
| C ₂ | 15,86 | 8,2 | 4,9 | 6,5 | 3,6 | 2,1 |
| C ₃ | 1,89 | 2 | 1,12 | 1,1 | 0,7 | 0,2 |
| i-C ₄ | 0,07 | 0,25 | 0,14 | 0,1 | 0,1 | 0,05 |
| n-C ₄ | 0,06 | 0,35 | 0,21 | 0,1 | 0,1 | 0,05 |
| i-C ₅ | 0 | 0 | 0,04 | 0 | 0,1 | 0 |
| n-C ₅ | 0 | 0 | 0 | 0 | 0 | 0 |
| C ₆ | 0 | 0 | 0,11 | 0 | 0 | 0 |
| C ₇ | 0 | 0 | 0 | 0 | 0 | 0 |
| C ₈ | 0 | 0 | 0 | 0 | 0 | 0 |
| Sum | 100 | 100 | 100 | 100 | 100 | 100 |
| Component | 13 | 14 | 15 | 16 | 17 | 18 |
| N ₂ | 1,8 | 0,4 | 0,4 | 14,351 | 3,904 | 11,001 |
| CO ₂ | 0,26 | 0 | 0 | 0,89 | 1,325 | 4,184 |
| C ₁ | 96,24 | 88 | 85,9 | 81,309 | 86,692 | 78,99 |
| C ₂ | 1,17 | 5,5 | 9 | 2,85 | 6,012 | 4,314 |
| C ₃ | 0,34 | 4 | 3,5 | 0,37 | 1,607 | 1,161 |
| i-C ₄ | 0,05 | 1 | 0,6 | 0,07 | 0,155 | 0,095 |
| n-C ₄ | 0,08 | 1 | 0,6 | 0,07 | 0,155 | 0,095 |

Table B.5 (continued)

| | | | | | | |
|------------------|-----------|-----------|-----------|-----------|-----------|-----------|
| i-C ₅ | 0,02 | 0,1 | 0 | 0,02 | 0,04 | 0,025 |
| i-C ₅ | 0,02 | 0,1 | 0 | 0,02 | 0,04 | 0,025 |
| n-C ₅ | 0 | 0 | 0 | 0,02 | 0,04 | 0,025 |
| C ₆ | 0,04 | 0 | 0 | 0,05 | 0,07 | 0,11 |
| C ₇ | 0 | 0 | 0 | 0 | 0 | 0 |
| C ₈ | 0 | 0 | 0 | 0 | 0 | 0 |
| Sum | 100 | 100 | 100 | 100 | 100 | 100 |
| No. | 19 | 20 | 21 | 22 | 23 | 24 |
| N ₂ | 0,24 | 0,87 | 2,28 | 5,41 | 0,325 | 0,439 |
| CO ₂ | 0,03 | 0,08 | 0,89 | 0,2 | 1,15 | 0 |
| C ₁ | 99,62 | 98,26 | 92,69 | 83,8 | 88,27 | 89,123 |
| C ₂ | 0,06 | 0,54 | 2,95 | 7,72 | 6,25 | 9,119 |
| C ₃ | 0,03 | 0,16 | 0,81 | 1,95 | 2,75 | 1,114 |
| i-C ₄ | 0,01 | 0,03 | 0,11 | 0,28 | 0,39 | 0,088 |
| n-C ₄ | 0 | 0,03 | 0,16 | 0,41 | 0,59 | 0,11 |
| i-C ₅ | 0 | 0,01 | 0,03 | 0,08 | 0,116 | 0,004 |
| n-C ₅ | 0 | 0,01 | 0,03 | 0,08 | 0,09 | 0,003 |
| C ₆ | 0,01 | 0,01 | 0,05 | 0,07 | 0,069 | 0 |
| C ₇ | 0 | 0 | 0 | 0 | 0 | 0 |
| C ₈ | 0 | 0 | 0 | 0 | 0 | 0 |
| Sum | 100 | 100 | 100 | 100 | 100 | 100 |
| No. | 25 | 26 | 27 | 28 | 29 | 30 |
| N ₂ | 1,072 | 0,527 | 0,423 | 5,513 | 9,58 | 9,85 |
| CO ₂ | 0,005 | 0 | 0,003 | 0,255 | 2,06 | 1,45 |
| C ₁ | 92,356 | 88,374 | 97,426 | 83,656 | 87,61 | 84,3 |
| C ₂ | 5,923 | 9,425 | 1,855 | 7,47 | 0,67 | 3,43 |
| C ₃ | 0,565 | 1,399 | 0,111 | 2,007 | 0,05 | 0,63 |
| i-C ₄ | 0,036 | 0,113 | 0,085 | 0,301 | 0,01 | 0,2 |
| n-C ₄ | 0,043 | 0,15 | 0,091 | 0,477 | 0,01 | 0,22 |
| i-C ₅ | 0 | 0,007 | 0,003 | 0,102 | 0 | 0,03 |
| n-C ₅ | 0 | 0,005 | 0,003 | 0,12 | 0 | 0,03 |
| C ₆ | 0 | 0 | 0 | 0,099 | 0,01 | 0,06 |
| C ₇ | 0 | 0 | 0 | 0 | 0 | 0 |
| C ₈ | 0 | 0 | 0 | 0 | 0 | 0 |
| Sum | 100 | 100 | 100 | 100 | 100 | 100,2 |
| No. | 31 | 32 | 33 | 34 | 35 | 36 |
| N ₂ | 1,03 | 0,86 | 3,03 | 13,53 | 13,77 | 16,57 |
| CO ₂ | 1,27 | 0,1 | 1,27 | 0,09 | 0,06 | 1,05 |
| C ₁ | 86,92 | 98,2 | 86,75 | 71,34 | 70,88 | 68,11 |
| C ₂ | 8,16 | 0,55 | 6,85 | 0,64 | 0,51 | 2,97 |
| C ₃ | 1,94 | 0,19 | 1,53 | 0,19 | 11,18 | 0,59 |
| i-C ₄ | 0,2 | 0,03 | 0,2 | 0 | 0 | 0 |

Table B.5 (continued)

| | | | | | | |
|------------------|-------|--------|------|--------|-------|------|
| n-C ₄ | 0,53 | 0,04 | 0,24 | 10,77 | 0,04 | 8,48 |
| i-C ₅ | 0 | 0 | 0 | 0,06 | 0,05 | 0 |
| n-C ₅ | 0,1 | 0,02 | 0,08 | 0,07 | 0,06 | 0,05 |
| C ₆ | 0,05 | 0,05 | 0,05 | 0 | 0 | 0,04 |
| C ₇ | 0 | 0 | 0 | 0 | 0 | 0 |
| C ₈ | 0 | 0 | 0 | 0 | 0 | 0 |
| O ₂ | 0 | 0 | 0 | 3,39 | 3,39 | 2,14 |
| Sum | 100,2 | 100,04 | 100 | 100,08 | 99,94 | 100 |

NOTE For some gas mixtures, the sum of original data is not exactly 100 %.

Table B.6 — Composition of 30 Chinese and Thailand's gas mixtures

| No. | 1 | 2 | 3 | 4 | 5 | 6 |
|-----------------|--------|--------|--------|--------|--------|--------|
| He | 0,02 | 0,02 | 0,02 | 0,03 | 0,02 | 0,03 |
| H ₂ | 0,00 | 0,00 | 0,00 | 0,00 | 0,00 | 0,00 |
| N ₂ | 0,49 | 0,38 | 0,29 | 0,6 | 0,51 | 0,59 |
| CO ₂ | 0,05 | 0,4 | 0,43 | 0,05 | 0,86 | 1,45 |
| C ₁ | 92,9 | 89,33 | 90,88 | 92,88 | 96,38 | 96,94 |
| C ₂ | 4,88 | 6,43 | 5,71 | 4,79 | 1,9 | 0,74 |
| C ₃ | 0,95 | 2,06 | 1,57 | 0,95 | 0,24 | 0,19 |
| iC ₄ | 0,16 | 0,35 | 0,33 | 0,16 | 0,05 | 0,03 |
| nC ₄ | 0,18 | 0,47 | 0,31 | 0,18 | 0,04 | 0,03 |
| iC ₅ | 0,06 | 0,14 | 0,12 | 0,06 | 0,00 | 0,00 |
| nC ₅ | 0,05 | 0,12 | 0,07 | 0,05 | 0,00 | 0,00 |
| C ₆₊ | 0,26 | 0,30 | 0,27 | 0,25 | 0,00 | 0,00 |
| sum | 100,00 | 100,00 | 100,00 | 100,00 | 100,00 | 100,00 |
| No. | 7 | 8 | 9 | 10 | 11 | 12 |
| He | 0,03 | 0,03 | 0,03 | 0,03 | 0,18 | 0,00 |
| H ₂ | 0,00 | 0,00 | 0,01 | 0,01 | 0,01 | 0,00 |
| N ₂ | 0,62 | 0,57 | 0,91 | 0,61 | 6,39 | 0,08 |
| CO ₂ | 1,50 | 1,31 | 0,98 | 0,56 | 3,71 | 0,12 |
| C ₁ | 96,93 | 95,66 | 97,17 | 91,09 | 89,61 | 99,69 |
| C ₂ | 0,70 | 1,66 | 0,68 | 4,96 | 0,10 | 0,08 |
| C ₃ | 0,17 | 0,48 | 0,16 | 1,47 | 0,00 | 0,03 |
| iC ₄ | 0,03 | 0,09 | 0,03 | 0,34 | 0,00 | 0,00 |
| nC ₄ | 0,02 | 0,09 | 0,03 | 0,31 | 0,00 | 0,00 |
| iC ₅ | 0,00 | 0,04 | 0,00 | 0,15 | 0,00 | 0,00 |
| nC ₅ | 0,00 | 0,02 | 0,00 | 0,08 | 0,00 | 0,00 |
| C ₆₊ | 0,00 | 0,05 | 0,00 | 0,39 | 0,00 | 0,00 |
| sum | 100,00 | 100,00 | 100,00 | 100,00 | 100,00 | 100,00 |
| No. | 13 | 14 | 15 | 16 | 17 | 18 |
| He | 0,02 | 0,01 | 0,01 | 0,10 | 0,00 | 0,00 |

Table B.6 (continued)

| | | | | | | |
|-----------------|-----------|-----------|-----------|-----------|-----------|-----------|
| H ₂ | 0,00 | 0,02 | 0,00 | 0,00 | 0,02 | 0,02 |
| N ₂ | 2,34 | 2,41 | 2,09 | 17,24 | 0,48 | 0,51 |
| CO ₂ | 0,04 | 0,53 | 0,01 | 0,79 | 0,04 | 0,05 |
| C ₁ | 85,63 | 90,48 | 91,48 | 74,11 | 92,86 | 92,54 |
| C ₂ | 11,51 | 4,09 | 3,65 | 4,81 | 4,95 | 5,08 |
| C ₃ | 0,43 | 1,39 | 1,34 | 2,01 | 0,94 | 0,99 |
| iC ₄ | 0,02 | 0,36 | 0,35 | 0,35 | 0,16 | 0,17 |
| nC ₄ | 0,01 | 0,36 | 0,45 | 0,48 | 0,16 | 0,19 |
| iC ₅ | 0,00 | 0,10 | 0,15 | 0,06 | 0,05 | 0,06 |
| nC ₅ | 0,00 | 0,10 | 0,17 | 0,05 | 0,04 | 0,04 |
| C ₆₊ | 0,00 | 0,15 | 0,30 | 0,00 | 0,30 | 0,35 |
| sum | 100,00 | 100,00 | 100,00 | 100,00 | 100,00 | 100,00 |
| No. | 19 | 20 | 21 | 22 | 23 | 24 |
| N ₂ | 0,8 | 0,41 | 0,42 | 0,52 | 0,43 | 0,51 |
| CO ₂ | 0,81 | 1,78 | 3,22 | 0,24 | 0,44 | 0,31 |
| C ₁ | 83,81 | 79,23 | 87,63 | 98,84 | 98,69 | 98,82 |
| C ₂ | 8,51 | 8,46 | 7,48 | 0,40 | 0,44 | 0,36 |
| C ₃ | 4,75 | 3,24 | 1,14 | 0,00 | 0,00 | 0,00 |
| iC ₄ | 0,64 | 5,69 | 0,02 | 0,00 | 0,00 | 0,00 |
| nC ₄ | 0,58 | 0,76 | 0,04 | 0,00 | 0,00 | 0,00 |
| iC ₅ | 0,03 | 0,26 | 0,02 | 0,00 | 0,00 | 0,00 |
| nC ₅ | 0,01 | 0,16 | 0,03 | 0,00 | 0,00 | 0,00 |
| C ₆₊ | 0,06 | 0,01 | 0,00 | 0,00 | 0,00 | 0,00 |
| sum | 100,00 | 100,00 | 100,00 | 100,00 | 100,00 | 100,00 |
| No. | 25 | 26 | 27 | 28 | 29 | 30 |
| N ₂ | 1,66 | 1,87 | 0,42 | 3,48 | 0,69 | 2,34 |
| CO ₂ | 0,496 | 1,88 | 0,90 | 15,33 | 22,34 | 23,46 |
| C ₁ | 96,70 | 95,45 | 70,69 | 64,67 | 61,89 | 56,74 |
| C ₂ | 0,409 | 0,65 | 12,06 | 8,33 | 7,50 | 7,66 |
| C ₃ | 0,107 | 0,07 | 9,04 | 4,85 | 4,60 | 6,41 |
| C ₄₊ | 0,128 | 0,028 | 6,966 | 3,15 | 3,70 | 3,40 |
| Sum | 99,5 | 99,948 | 100,076 | 99,81 | 100,72 | 100,01 |

NOTE The original data of No. 25 to No. 30 from Thailand are not normalized.

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- [1] KLIMSTRA Jacob, & QUINTO Vittorio et al. Classification methods for the knock resistance of gaseous fuels — an attempt towards unification.
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