Liquid Ring Vacuum Pumps and Compressors for Petroleum, Chemical, and Gas Industry Services

API STANDARD 681 FIRST EDITION, FEBRUARY 1996



Document provided by IHS Licensee=Sincor Venezuela/5934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

Liquid Ring Vacuum Pumps and Compressors for Petroleum, Chemical, and Gas Industry Services

Manufacturing, Distribution and Marketing Department

API STANDARD 681 FIRST EDITION, FEBRUARY 1996



SPECIAL NOTES

1. API PUBLICATIONS NECESSARILY ADDRESS PROBLEMS OF A GENERAL NATURE. WITH RESPECT TO PARTICULAR CIRCUMSTANCES, LOCAL, STATE, AND FEDERAL LAWS AND REGULATIONS SHOULD BE REVIEWED.

2. API IS NOT UNDERTAKING TO MEET THE DUTIES OF EMPLOYERS, MANU-FACTURERS, OR SUPPLIERS TO WARN AND PROPERLY TRAIN AND EQUIP THEIR EMPLOYEES, AND OTHERS EXPOSED, CONCERNING HEALTH AND SAFETY RISKS AND PRECAUTIONS, NOR UNDERTAKING THEIR OBLIGATIONS UNDER LOCAL, STATE, OR FEDERAL LAWS.

3. INFORMATION CONCERNING SAFETY AND HEALTH RISKS AND PROPER PRECAUTIONS WITH RESPECT TO PARTICULAR MATERIALS AND CONDI-TIONS SHOULD BE OBTAINED FROM THE EMPLOYER, THE MANUFACTURER OR SUPPLIER OF THAT MATERIAL, OR THE MATERIAL SAFETY DATA SHEET.

4. NOTHING CONTAINED IN ANY API PUBLICATION IS TO BE CONSTRUED AS GRANTING ANY RIGHT, BY IMPLICATION OR OTHERWISE, FOR THE MANU-FACTURE, SALE, OR USE OF ANY METHOD, APPARATUS, OR PRODUCT COV-ERED BY LETTERS PATENT. NEITHER SHOULD ANYTHING CONTAINED IN THE PUBLICATION BE CONSTRUED AS INSURING ANYONE AGAINST LIABIL-ITY FOR INFRINGEMENT OF LETTERS PATENT.

5. GENERALLY, API STANDARDS ARE REVIEWED AND REVISED, REAF-FIRMED, OR WITHDRAWN AT LEAST EVERY FIVE YEARS. SOMETIMES A ONE-TIME EXTENSION OF UP TO TWO YEARS WILL BE ADDED TO THIS REVIEW CYCLE. THIS PUBLICATION WILL NO LONGER BE IN EFFECT FIVE YEARS AF-TER ITS PUBLICATION DATE AS AN OPERATIVE API STANDARD OR, WHERE AN EXTENSION HAS BEEN GRANTED, UPON REPUBLICATION. STATUS OF THE PUBLICATION CAN BE ASCERTAINED FROM THE API AUTHORING DEPART-MENT [TELEPHONE (202) 682-8000]. A CATALOG OF API PUBLICATIONS AND MATERIALS IS PUBLISHED ANNUALLY AND UPDATED QUARTERLY BY API, 1220 L STREET, N.W., WASHINGTON, D.C. 20005.

All rights reserved. No part of this work may be reproduced, stored in a retrieval system, or transmitted by any means, electronic, mechanical, photocopying, recording, or otherwise, without prior written permission from the publisher. Contact API Publications Manager, 1220 L Street, N.W., Washington, D.C. 20005.

Copyright © 1996 American Petroleum Institute

FOREWORD

This standard requires the purchaser to specify certain details and features. Although it is recognized that the purchaser may desire to modify, delete, or amplify sections of the standard, it is strongly recommended that such modifications, deletions, and amplifications be made by supplementing this standard rather than by rewriting or incorporating sections of this standard into another complete standard.

Suggested revisions are invited and should be submitted to the director of the Manufacturing, Distribution and Marketing Department, American Petroleum Institute, 1220 L Street, N.W., Washington, D.C. 20005. SECTION 1—GENERAL

CONTENTS

1.1 Scope

1.2 Alternative Designs

COPYRIGHT 2002; American Petroleum Institute

V
Document provided by IHS Licensee=Sincor Venezuela/5934214100, User≡, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

1.3	Conflicting Requirements	1
1.4	Definition of Terms	1
1.5	References	3
1.6	Unit Conversion	5
SEC	TION 2—BASIC DESIGN	
2.1	General	6
2.2	Casings	7
2.3	Casing Connections	7
2.4	External Forces and Moments	8
2.5	Rotating Elements	8
2.6	Mechanical Shaft Seals	9
2.7	Dynamics	9
2.8	Bearings, Bearing Housings, and Lubrication	11
2.9	Materials	12
2.10	Nameplate and Rotation Arrows	14
SEC	TION 3—SYSTEM DESIGN	
3.1	Ring Liquid System	15
3.2	Controls and Instrumentation	16
3.3	Drivers and Transmissions	19
3.4	Couplings and Guards	20
3.5	Belt Drives	20
3.6	Mounting Plates	21
3.7	Piping	22
3.8	Special Tools	23
SEC	TION 4—INSPECTION, TESTING, AND	
	PREPARATION FOR SHIPMENT	
4.1	General	23
4.2	Inspection	24
4.3	Testing	25
4.4	Preparation for Shipment	27
SEC	TION 5VENDOR'S DATA	
5.1	General	28
5.2	Proposals	29
5.3	Contract Data	30
APP	ENDIX A—LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEETS	31
APPI	ENDIX B—LIQUID RING VACUUM PUMP SCHEMATIC	57
	ENDIX C—SHAFT DEFLECTION SCHEMATIC	59
APP	ENDIX D—LIQUID RING VACUUM PUMP RING LIQUID FLOW SCHEMATICS	61
APP	ENDIX E—MECHANICAL SEAL AND PIPING ARRANGEMENT SCHEMATICS	65
APP	ENDIX F—MATERIAL LIST	69

Page

1

1

-

Page

APPENDIX GLIQUID RING VACUUM PUMPS AND COMPRESSORS VENDOR DRAWING AND DATA REQUIREMENTS	71
APPENDIX H—SYSTEM CONSIDERATIONS, OPERATING VARIABLES, AND TEST PERFORMANCE CONVERSION	75
Figure	
1—Illustration of Terms	2
2—Bearing-Housing Vibration Limits (Antifriction Bearings)	11
B-1—Liquid Ring Vacuum Pump Schematic	58
C-1—Shaft Deflection Schematic	60
D-1—Liquid Ring Vacuum Pump Ring Liquid Flow Schematics	62
E-1—Typical Mechanical Seal Arrangements	66
E-2—Piping for Single-Seal Arrangements and Primary Seals of	
Tandem Seal Arrangements	67
E-3—Piping for Throttle Bushing, Auxiliary Seal Device, Tandem	
Seals, or Double Seals	68
Tables	
1—Driver Trip Speeds	3
2-Cooling Water Design Parameters	6
3-Maximum Coupling End Floats	20
4-Maximum Severity of Defects in Castings	25
5—Performance Tolerances	27
F-1—Material List	70

Liquid Ring Vacuum Pumps and Compressors for Petroleum, Chemical, and Gas Industry Services

SECTION 1—GENERAL

1.1 Scope

1.1.1 This standard covers the minimum requirements for liquid ring vacuum pump and compressor systems for service in the petroleum, chemical, and gas industries. This includes both vacuum pump and compressor design and system design.

1.1.2 The design of the system is critical to the successful operation of the liquid ring vacuum pump or compressor. Close attention must be paid not only to the design of the ring liquid system but also to how it is integrated into the user's process.

1.1.3 Although this standard covers minimum requirements appropriate for petroleum refinery service, purchasers may wish to consider pumps, compressors, and systems that do not meet all the requirements of this standard, based on specific nonflammable, nontoxic service conditions.

Note: A bullet (\bullet) at the beginning of a paragraph indicates that a decision by the purchaser is required. These decisions should be indicated on the data sheet (see Appendix A); otherwise, they should be stated in the quotation request or in the order.

1.2 Alternative Designs

The vendor may offer alternative designs. Equivalent metric dimensions, fasteners, and flanges may be substituted as mutually agreed upon by the purchaser and the vendor.

1.3 Conflicting Requirements

In case of conflict between this standard and the inquiry, or order, the information included in the order shall govern.

1.4 Definition of Terms

Terms used in this standard are defined in 1.4.1 through 1.4.26 (refer to Figure 1).

1.4.1 The *alarm point* is a preset value of a parameter at which an alarm is actuated to warn of a condition that requires corrective action.

1.4.2 The *compressor rated point* is the point on the 100 percent speed curve at the highest capacity of any specified.

1.4.3 Hydrodynamic bearings are bearings that use the principles of hydrodynamic lubrication. Their surfaces are oriented so that relative motion forms an oil wedge to support the load without journal-to-bearing contact.

1.4.4 Inlet cubic feet per minute (ICFM) refers to the flow rate determined at the conditions of pressure, temperature, compressibility, and gas composition, including moisture, at the compressor inlet flange. Actual cubic feet per minute (ACFM) may be used to refer to flow at a number of locations and should therefore not be used interchangeably with inlet cubic feet per minute.

1.4.5 A liquid ring vacuum pump, or compressor, is a rotary positive-displacement machine in which gas compression is achieved by the action of a radially bladed impeller mounted in an eccentric or elliptical casing which is partially filled with liquid.

1.4.6 Maximum allowable differential pressure is the maximum differential pressure for which the manufacturer has designed the equipment for continuous operation.

1.4.7 *Maximum allowable speed* (revolutions per minute) is the highest speed at which the manufacturer's design will permit continuous operation.

1.4.8 Maximum allowable temperature is the maximum continuous temperature for which the manufacturer has designed the equipment (or any part to which the term is referred) when handling the specified fluid at the specified pressure.

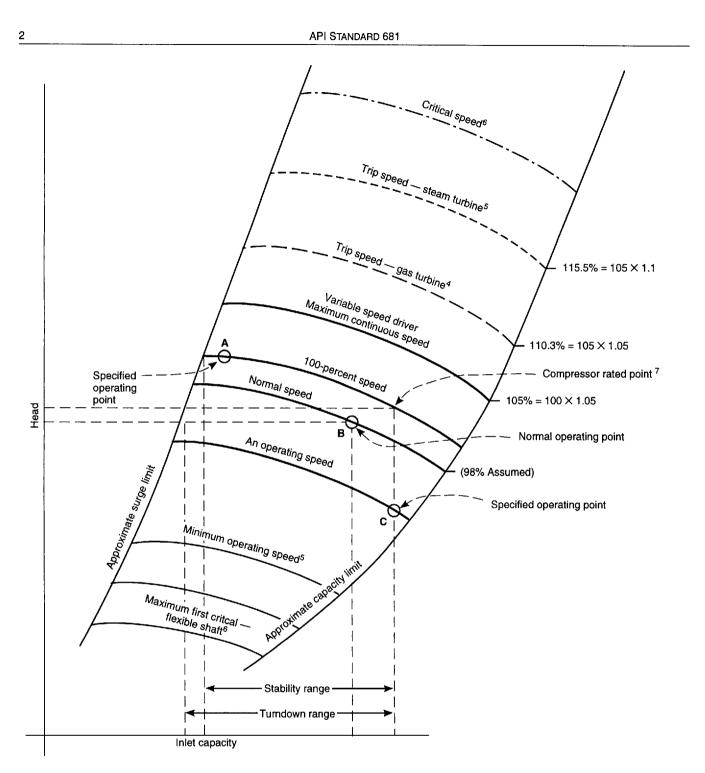
1.4.9 Maximum allowable vacuum is the maximum vacuum (minimum suction pressure) for which the manufacturer has designed the equipment, corrected for the vapor pressure of the seal liquid at the operating temperature.

1.4.10 Maximum allowable working pressure is the maximum continuous pressure for which the manufacturer has designed the equipment (or any part to which the term is referred) when handling the specified fluid at the specified temperature.

1.4.11 Maximum continuous speed (revolutions per minute) is the speed at least equal to 105 percent of the rated speed. Maximum continuous speed for constant-speed drivers shall be equal to the 100-percent speed.

1.4.12 Maximum differential pressure is the maximum discharge pressure minus the minimum suction pressure that the pump is able to develop when operating at the specified speed, specific gravity, and pumping temperature.

API STD*681 96 🗰 0732290 0550619 626 🖿



Notes:

1. Except where specific numerical relationships are stated, the relative values implied in this figure are assumed values for illustration only.

2. The 100 percent speed curve is determined from the operating point requiring the highest head; point A in the illustration.

3. The compressor rated point (CRP) is the intersection on the 100 percent speed line corresponding to the highest flow of any operating point; point C in the illustration.

4. The head-capacity curve at 100 percent speed shall extend to at least 115 percent of the capacity of the CRP. Head-capacity curves at other speeds shall be extended to equivalent capacity at each speed. For

example, the head-capacity curve at 105 percent speed shall be extended to at least 1.05 times 1.15 times the capacity of the CRP; the head-capacity curve at 90 percent speed shall be extended to at least 0.9 times 1.15 times capacity of the CRP; and so on. These points define the "approximate capacity limit" curve.

5. Refer to the applicable standard for the compressor driver such as API Standard 612 (Steam Turbine) or API Standard 616 (Gas Turbine) for trip speed and minimum operating speed limits.

6. Refer to 2.7 for allowable margins of critical speeds to operating speeds.

7. See 1.4.4.

Figure 1—Illustration of Terms

Document provided by IHS Licensee=Sincor Venezuela/S934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584. **1.4.13** Maximum discharge pressure is the maximum suction pressure plus the maximum differential pressure that the pump is able to develop when operating at the specified speed, specific gravity, and pumping temperature.

1.4.14 *Maximum sealing pressure* is the highest pressure expected at the seals during any specified static or operating condition and during start-up and shutdown.

1.4.15 *Minimum allowable temperature* is the minimum continuous temperature for which the manufacturer has designed the equipment (or any part to which the term is referred).

1.4.16 Normal operating point is the point at which usual operation is expected and optimum efficiency is desired.

1.4.17 The *casing* is the composite of all stationary pressure-containing parts of the unit, including all nozzles, seal glands, and other attached parts but excluding the stationary and rotating members of mechanical seals (see Figure E-1, Appendix E).

1.4.18 *Radially split* refers to casing joints that are transverse to the shaft centerline.

1.4.19 *Rated discharge pressure* is the highest pressure required to meet the conditions specified by the purchaser for the intended service.

1.4.20 The *rated operating point* is the point at which the vendor certifies that performance is within the tolerances stated in this standard. Performance includes the following factors: capacity, power, efficiency, rotative speed, and rated suction and discharge pressures.

1.4.21 The *shutdown point* is a preset value of a parameter at which automatic or manual shutdown of the system is required.

1.4.22 Standard flow is the flow rate expressed in volume flow rate. ISO standard flow rate is cubic meters per hour or minute $(m^3/h \text{ or } m^3/\min)$ at an absolute pressure of 1.013 bar [14.7 pounds per square inch (psi)] and a temperature of 0°C (32°F). Customary units are standard cubic feet per minute (SCFM) or million standard cubic feet per day (MMSCFD) at an absolute pressure of 14.7 pounds per square inch and a temperature of 60°F.

1.4.23 *Total indicated runout* (TIR), also known as total indicator reading, is the runout of a diameter or face determined by measurement with a dial indicator. The indicator reading implies an out-of-squareness equal to the reading or an eccentricity equal to half the reading.

1.4.24 *Trip speed* (revolutions per minute) is the speed at which the independent emergency overspeed device operates to shut down a variable speed prime mover (see Table 1).

Table 1—Driver Trip Speeds			
Driver Type	Trip Speed (% of Maximum Continuous Speed)		
Steam turbine			
NEMA Class A ^a	115		
NEMA Classes B, C, D ^a	110		
Gas turbine	105		
Variable speed motor	110		
Reciprocating engine	110		

3

^aIndicates governor class as specified in NEMA SM 23

1.4.25 Unit responsibility refers to the responsibility for coordinating the technical aspects of the equipment and all auxiliary systems included in the scope of the order. It includes responsibility for reviewing such factors as the power requirements, speed, rotation, general arrangement, couplings, dynamics, noise, lubrication, sealing system, material test reports, instrumentation, piping, and testing of components.

1.4.26 A *wet critical speed* is a rotor resonant frequency calculated considering the additional support and damping produced by the action of the pumped liquid within internal running clearances at the operating conditions and allowing for flexibility and damping within the bearings.

1.5 References

1.5.1 This standard makes reference to American standards; other international or national standards may be used as mutually agreed between purchaser and vendor provided it can be shown that these standards meet or exceed the American standards referenced.

1.5.2 The editions of the following standards, codes, and specifications that are in effect at the time of publication of this standard shall, to the extent specified herein, form a part of this standard. The applicability of changes in standards, codes, and specifications that occur after the inquiry shall be mutually agreed upon by the purchaser and the vendor.

AFBMA¹

Std 7 Shaft and Housing Fits for Metric Radial Ball and Roller Bearings (Except Tapered Roller Bearings) Conforming to Basic Boundary Plans

- Std 9 Load Ratings and Fatigue Life for Ball Bearings
- Std 19 Tapered Roller Bearings–Radial Inch Design

¹ Anti-Friction Bearing Manufacturers Association, 1235 Jefferson Davis Highway, Arlington, Virginia 22202.

API STD*681 96 🛲 0732290 0550621 284 🛲

4	API STAN	DARD 681		
Std 19.1	Tapered Roller Bearings–Radial Metric Design		RP 520	Sizing, Selection and Installation of Pressure Relieving Devices in Refin-
Std 20	Radial Bearings of Ball, Cylindrical			eries
	Roller and Spherical Roller Types,		Std 526	Flanged Steel Safety Relief Valves
	Metric Design: Conforming to Basic Boundary Plans: Boundary Dimen-		Std 550	Manual on Installation of Refinery Instruments and Control Systems (oop)
	sions, Tolerances and Identification Code.		Std 610	Centrifugal Pumps for General Refinery Service
AGMA ²			Std 611	General-Purpose Steam Turbines for Refinery Services
9000-C90(1990)	Flexible Couplings-Potential Unbal- ance Classification		Std 615	Sound Control of Mechanical Equip- ment for Refinery Services (00p)
9002	Bores and Keyways for Flexible Couplings (Inch Series)		Std 660	Shell-and-Tube Heat Exchangers for General Refinery Services
2			Std 670	Vibration, Axial-Position, and Bear-
AISC ³				ing-Temperature Monitoring Systems
Manual of Steel (Construction		Std 677	General Purpose Gear Units for Refinery Service
ANSI ⁴		Manua	l of Petrol	eum Measurement Standards, Chapter
B1.1	Unified Inch Screw Threads (UN and			15, "Guidelines for the Use of the
B1.20.1	UNR Thread Form) Pipe Threads, General Purpose (Inch)			International System of Units (SI) in the Petroleum and Allied Industries"
B1.20.1 B1.20.3	Dryseal Pipe Threads (Inch)			the Petroleum and Amed Industries
B16.1	Cast Iron Pipe Flanges and Flanged	ASME ⁵		
	Fittings, Class 25, 125, 250, and 800	110.012	B1.20.1	Pipe Threads, General Purpose (Inch)
B16.5	Pipe Flanges and Flanged Fittings,		B16.47	Large Diameter Steel Flanges: NPS
	Steel Nickel Alloy and Other Special			26 through NPS 60
	Alloys		B31.3	Chemical Plant and Petroleum Refin-
B16.11	Forged Steel Fittings, Socket-Welding and Threaded			ery Piping Boiler and Pressure Vessel Code, Section V, "Non-destructive
B16.42	Ductile Iron Pipe Flanges and Flanged Fitting, Class 150 and 300			Examination"; Section VIII, "Rules for Construction of Pressure Vessels";
B73.1	Specification for Horizontal End Suction Centrifugal Pumps for Chem- ical Processes			and Section IX, "Welding and Brazing Qualifications"
B73.2	Specification for Vertical In-line	ASTM ⁶		
			4 105	

- Specification for Carbon Steel Forg-A 105 ings for Piping Components
- A 106 Specification for Seamless Carbon Steel Pipe for High-Temperature Service
- A 120 Specification for Black and Hot-Dipped Zinc-Coated (Galvanized) Welded and Seamless Steel Pipe for Ordinary Uses
- A 153 Specification for Zinc Coating (Hot Dip) on Iron and Steel Hardware
- A 181 Specification for Carbon Steel Forgings for General Purpose Piping

9000-C90(1990)	Flexible	e Coi	uplings-Pot	ential	Unbal-
	ance Cl	assifi	cation		
9002	Bores	and	Keyways	for	Flexible

- Centrifugal Pumps for Chemical Services
- Mechanical Vibration-Balance Qual-S2.19 ity of Rigid Rotors-Part 1, Determination of Permissible Residual Unbalance

API

Specification for Line Pipe Spec 5L

RP 500A Classification of Locations for Electrical Installations in Petroleum Refineries

⁵ American Society of Mechanical Engineers, 345 East 47th Street, New York, New York 10017. ⁶ American Society for Testing and Materials, 1916 Race Street, Philadel-

phia, Pennsylvania 19103

COPYRIGHT 2002; American Petroleum Institute

² American Gear Manufacturers Association, 1500 King Street, Suite 201, Alexandria, Virginia 22314-2730. ³ American Institute of Steel Construction, 1 East Wacker Drive, Suite 3100,

Chicago, Illinois 60601-2001. ⁴ American National Standards Institute, 11 West 42nd Street, New York,

New York 10036.

5

- A 193 Specifications for Alloy-Steel and Stainless Steel Bolting Materials for High-Temperature Service
- A 194 Specification for Carbon and Alloy-Steel Nuts for Bolts for High-Pressure and High-Temperature Service.
- A 197 Specification for Cupola Malleable Iron
- A 247 Method for Evaluating the Microstructure of Graphite in Iron Castings
- A 269 Specification for Seamless and Welded Austenitic Stainless Steel Tubing for General Service
- A 278 Specification for Gray Iron Castings for Pressure Containing Parts for Temperatures up to 650°F
- A 338 Specification for Malleable Iron Flanges, Pipe Fittings, and Valve Parts for Railroad, Marine and Other Heavy Duty Service at Temperatures up to 650°F (345°C)
- A 395 Specification for Ferrite Ductile Iron Pressure-retaining Castings for Use at Elevated Temperatures
- A 515 Specification for Carbon Steel Pressure Vessel Plates for Intermediate and Higher-Temperature Service
- A 524 Specification for Seamless Carbon Steel Pipe for Atmospheric and Lower Temperatures
- A 536 Specification for Ductile Iron Castings
- E 94 Guides for Radiographic Testing
- E 125 Reference Photographs for Magnetic Particle Indications on Ferrous Castings
- E 142 Method for Controlling Quality of Radiographic Testing
- E 709 Practice for Magnetic Particle Examination

AWS⁷

D1.1 Structural Welding Code-Steel

EEMUA⁸

151 Liquid Ring Vacuum Pumps and Compressors

HEI9

Performance Standard for Liquid Ring Vacuum Pumps

NACE¹⁰

MR-01-75 Sulfide Stress Cracking Resistent Metallic Material For Oil Field Equipment

Corrosion Engineer's Reference Book

NEMA¹¹

SM 23 Steam Turbines for Mechanical Drive Service

NFPA¹²

- 70 National Electrical Code, Articles 500 and 501
- 496 Purged and Pressurized Enclosures for Electrical Equipment

OSHA13

29 Code of Federal Regulations Part 1910

PNEUROP 6612¹⁴

Acceptance Specification and Performance Tests for Liquid Ring Vacuum Pumps

SSPC¹⁵

SP 6 Commercial Blast Cleaning

TEMA¹⁶

Standard of Tubular Exchangers Manufacturers Association

1.5.3 The purchaser and the vendor shall mutually determine the measures that must be taken to comply with any governmental codes, regulations, ordinances, or rules that are applicable to the equipment.

1.5.4 It is the vendor's responsibility to invoke all applicable specifications to each subvendor.

1.6 Unit Conversion

The factors in Chapter 15 of the API Manual of Petroleum Measurement Standards were used to convert from customary to SI units; the resulting exact SI units were then rounded off.

⁷ American Welding Society, 550 N.W. LeJeume Road, PO. Box 351040, Miami, Florida 33135. ⁸ The Engineering Enging Engineering Enging Engineering E

⁸ The Engineering Equipment and Materials Users Association, 14-15 Belgrave Square, London, U.K. SWIX8PS.

⁹ Heat Exchange Institute, 1230 Keith Building, Cleveland, Ohio 44115.

¹⁰ NACE International, P.O Box 218340, Houston, Texas 77218-8340.

¹¹ National Electrical Manufacturers Association, 2101 L. Street, N.W., Washington, D.C. 20037.

¹² National Fire Protection Association, Batterymarch Park, Quincy, Massachusetts 02269.

¹³ Occupational Safety and Health Standards.

 ¹⁴ European Committee of Manufacturers of Compressors, Vacuum Pumps and Pneumatic Tools, c/o British Compressed Air Society, Leicestor House & Leicestor Street, London, U K. WCZH 7NN.
 ¹⁵ Steel Structures Painting Council, 4400 Fifth Avenue, Pittsburgh, Penn-

 ¹⁵ Steel Structures Painting Council, 4400 Fifth Avenue, Pittsburgh, Pennsylvania 15213-2683.
 ¹⁶ Tubular Evolution of Avenue, Manufacture, Man

¹⁶ Tubular Exchanger Manufacturers Association, 25 North Broadway, Tarrytown, New York 10591.

Document provided by IHS Licensee–Sincor Venezuela/5934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

API STANDARD 681

SECTION 2—BASIC DESIGN

2.1 General

6

2.1.1 The equipment (including auxiliaries) covered by this standard shall be designed and constructed for a minimum service life of 20 years and at least three years of uninterrupted operation. It is recognized that this is a design criterion.

2.1.2 The vendor shall assume unit responsibility of all the equipment and all auxiliary systems included in the scope of the order.

- 2.1.3 The purchaser will specify the equipment's normal and rated operating points on the data sheets. The purchaser will also specify any other anticipated operating conditions.
- 2.1.4 Control of the sound pressure level (SPL) of all equipment furnished shall be a joint effort of the purchaser and the vendor. The equipment furnished by the vendor shall conform to the maximum allowable sound pressure level specified by the purchaser.
- 2.1.5 Cooling water design conditions will be specified by the purchaser. Note that cooling water design parameters are particularly critical to the performance of liquid ring machines. The lowest available cooling water temperature will result in the best performance, namely, capacity and suction pressure. The conditions in Table 2 are suggested guidelines.

	Parameters			
Conditions	SI Units	English Units		
Velocity over heat exchange surfaces Maximum allowable working	1.5-2.5 m/s	5-8 ft/s		
pressure	$\geq 5.2 \text{ bar}^{a}$	75 psig		
Test pressure	≥15×MAWP	115 psig		
Maximum pressure drop	1bar	15 psi		
Maximum inlet temperature	30°C	90°F		
Maximum outlet temperature	50°C	120°F		
Maximum temperature rise	20K	30°F		
Minimum temperature rise ^b	10K	20°F		
Fouling factor on water side	0.35m ² K/kW	0.002 hr-ft ² °F/Btu		
Shell corrosion allowance	3.0 mm	0.125 in		

Note: The vendor shall notify the purchaser if the criteria for minimum temperature rise and velocity over heat exchange surfaces result in a conflicting design. The criterion for velocity over heat exchanger surfaces is intended to minimize water-side fouling, the criterion for minimum temperature rise is intended to minimize the use of cooling water. It is accepted that the specified minimum temperature rise may be too restrictive for vacuum pumps handling condensable vapors. The purchaser will approve the final selection

^a Gauge pressure

^bLower temperature rise may be necessary depending upon conditions and pending purchaser approval.

Provision shall be made for complete venting and draining of the system.

- 2.1.7 The arrangement of the equipment, including piping and auxiliaries, shall be developed jointly by the purchaser and the vendor. The arrangement shall provide adequate clearance areas and safe access for operation and maintenance. Any special clearance or safe access areas located on the skid will be specified by the purchaser.
- 2.1.8 Motors, electrical components, and electrical installations shall be suitable for the area classification (class, group, and division or zone) specified by the purchaser on the data sheets and shall meet the requirements of NFPA 70, Articles 500, 501, 502, and 504 as well as local codes specified and furnished by the purchaser.

2.1.9 Housings that enclose moving lubricated parts (such as bearings, shaft seals, highly polished parts, instruments, and control elements) shall be designed to minimize contamination by moisture, dust, and other foreign matter during periods of operation and idleness.

2.1.10 All equipment shall be designed to permit rapid and economic maintenance. Major parts such as casing components and bearing housings shall be designed (shouldered or cylindrically doweled) and manufactured to ensure accurate alignment on reassembly.

2.1.11 The machine and its driver shall perform on the test stand and on their permanent foundation within the specified acceptance criteria. After installation, the performance of the combined units shall be the joint responsibility of the purchaser and the vendor who has unit responsibility.

2.1.12 In designing the liquid ring unit, the vendor shall take into account that many factors (such as piping loads, alignment at operating conditions, supporting structure, and handling during shipment and installation) may adversely affect site performance.

• 2.1.13 The purchaser will specify whether the installation is indoors (heated or unheated) or outdoors (with or without a roof), as well as the weather and environmental conditions in which the equipment must operate (including maximum and minimum temperatures, unusual humidity, and dusty or corrosive conditions). The unit and its auxiliaries shall be suitable for operation under these specified conditions. For purchaser's guidance, the vendor shall list in the proposal any special protection that the purchaser is required to supply.

2.1.14 All equipment shall be additionally suitable for running on air during commissioning. The vendor shall provide air performance curves, operating guidelines, and any additional features required.

Note: It may be necessary to use a different ring liquid to run on air.

2.1.15 Spare parts for the machine and all furnished auxiliaries shall meet the criteria of this standard.

• **2.1.16** When specified, the equipment feet shall be provided with vertical jackscrews and shall be drilled with pilot holes that are accessible for use in final doweling.

2.1.17 A guide to liquid ring vacuum pump and compressor nomenclature will be found in Appendix B.

2.2 Casings

2.2.1 The stress used in design for any given material shall not exceed the values given for that material in Section VIII, Division 1, of the ASME Code. For cast materials, the factor specified in the code shall be applied. Pressure casings of forged steel, rolled and welded plate, or seamless pipe with welded cover shall comply with the applicable rules of Section VIII, Division 1, of the ASME Code. Manufacturer's data report forms and stamping, as specified in the code, are not required.

2.2.2 The maximum allowable working pressure of the casing shall be at least equal to the specified relief valve setting.

2.2.3 Where more than one compression stage is incorporated within a single casing, the whole of that casing shall be designed for the maximum allowable working pressure of the higher pressure stage.

2.2.4 Casings and supports shall be designed to have sufficient strength and rigidity to limit any change of shaft alignment at the coupling flange, caused by the worst combination of allowable pressure, torque, and piping forces and moments, to 50 micrometers (0.002 inch) at static conditions. Under dynamic conditions, the calculated shaft deflection at the coupling flange shall not exceed 125 microinches (0.005 inch). Supports and alignment bolts shall be rigid enough to permit the machine to be moved by the use of its lateral and axial jackscrews (see Appendix C).

2.2.5 The use of tapped holes in vacuum and pressure parts shall be minimized. To prevent leakage in vacuum and pressure sections of casings, metal equal in thickness to at least half the nominal bolt diameter, in addition to the allowance for corrosion, shall be left around and below the bottom of drilled and tapped holes. The depth of the tapped holes shall be at least one and one half times the stud diameter.

2.2.6 Bolting shall be furnished as specified in 2.2.6.1 through 2.2.6.4.

2.2.6.1 The details of threading shall conform to ANSI B1.1.

• 2.2.6.2 Studs are preferred to cap screws and shall have the first one and one half threads removed at both ends. When specified, studs shall be supplied.

2.2.6.3 Material grade markings shall be located on the nut end of the exposed stud.

2.2.6.4 Adequate clearance shall be provided at bolting locations to permit the use of socket or box wrenches.

2.2.6.5 Slotted nut, or spanner-type bolting shall not be used unless specifically approved by the purchaser.

- 2.2.7 Jackscrews and cylindrical casing alignment dowels or shoulders shall be provided to facilitate disassembly and reassembly. When jackscrews are specified or required as a means of parting contacting faces, one of the faces shall be relieved (counterbored or recessed) to prevent a leaking joint or improper fit caused by marring of the face.
- **2.2.8** When specified, hold-down or foundation bolt holes shall be spot faced to a diameter three times that of the hole.

2.3 Casing Connections

2.3.1 Casings with double flow inlet or discharge connections shall, unless specified otherwise, be furnished with manifolds to a single terminal point connection. The manifolds shall be designed for the same vacuum and maximum allowable working pressure as the casing.

• 2.3.2 Inlet and outlet connections shall be flanged or machined and studded, oriented as specified on the data sheets, and suitable for the maximum allowable working pressure of the casing as defined in 1.4.10.

2.3.3 Casing openings for piping connections shall be at least NPS $\frac{1}{2}$ and for flammable or toxic service shall be flanged or machined and studded, or threaded and seal welded. When threaded connections are approved for nonflammable, nontoxic service, they shall comply with the requirements of 2.3.3.1 through 2.3.3.5.

2.3.3.1 Threaded connections shall be NPS $\frac{1}{2}$ through $\frac{1}{2}$ nominal pipe sizes only.

• 2.3.3.2 When specified, a pipe nipple, preferably not more than 150 millimeters (6 inches) long, shall be screwed into the threaded opening and shall comply with the requirements of 2.3.3.2.1 through 2.3.3.2.3. Additional fittings may be used if space is restricted.

2.3.3.2.1 The pipe nipple shall meet the minimum schedules listed in Table 3.

2.3.3.2.2 The pipe nipple shall be provided with a flange at its outer end.

2.3.3.2.3 The nipple and flange materials shall meet the requirements of 2.3.5.

2.3.3.3 Tapped openings and bosses for pipe threads shall conform to ANSI B16.5.

Document provided by IHS Licensee–Sincor Venezuela/5934214100, User=, 08/14/2022 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

2.3.3.4 Pipe threads shall be taper threads conforming to ANSI B1.20.1.

2.3.4 For flammable and toxic service the threaded connection shall be seal welded; however, seal welding is not permitted on cast iron equipment, for instrument connections, or where disassembly is required for maintenance. Seal-welded joints shall be in accordance with ASME B 31.3.

2.3.5 Connections welded to the casing shall meet the material requirements of the casing, including impact values, rather than the requirements of the connected piping (see 2.3.3.2.3 and 2.9.3.5).

2.3.6 Openings for NPS $1\frac{1}{4}$, $2\frac{1}{2}$, $3\frac{1}{2}$, 5, 7, and 9 shall not be used.

2.3.7 Tapped openings not connected to piping shall be plugged with solid plugs furnished in accordance with ASME B16.11. As a minimum, these plugs shall meet the material requirements of the casing. Plugs that may later require removal shall be of corrosion resistant material. A lubricant that meets the proper temperature specification shall be used on all threaded connections. Tape shall not be applied to threads of plugs inserted into oil passages. Plastic plugs are not permitted.

2.3.8 Flanges shall conform to ASME B16.1, B 16.5, or B 16.42 as applicable, except as specified in 2.3.8.1 through 2.3.8.4.

2.3.8.1 Cast iron flanges shall be flat-faced.

2.3.8.2 Flat-faced flanges with full raised-face thickness are acceptable on casings other than cast iron.

2.3.8.3 Flanges that are thicker or have a larger outside diameter than that required by ASME B16.5 or B16.47 Series "B" are acceptable.

2.3.8.4 Connections other than those covered by ASME B16.5, B16.47 Series "B" require the purchaser's approval. Unless otherwise specified, mating parts for these nonstandard flanges shall be furnished by the vendor.

2.3.9 Machined and studded connections shall conform to the facing and drilling requirements of ASME B16.1, B16.5, or B16.42. Studs and nuts shall be furnished installed. The first one and one half threads at both ends of each stud shall be removed. Connections larger than those covered by ASME shall meet the requirements of 2.3.8.4.

2.3.10 All of the purchaser's connections shall be accessible for disassembly without the machine being moved.

2.3.11 Casings shall be provided with a vent connection unless they are self-venting by the arrangement of the piping.

2.3.12 Casings shall be provided with sufficient drains to ensure complete drainage.

2.3.13 Welded branches of one inch nominal size or less shall be reinforced by gusset plates or otherwise adequately supported to avoid a fatigue failure at the point of attachment, particularly where a valve or other mass is supported from the branch.

2.4 External Forces and Moments

The manufacturer shall specify the maximum allowable external forces and moments that the compressor or vacuum pump casing will withstand. These shall be at least equal to the values calculated in accordance with NEMA SM-23. The allowable forces and moments shall be shown on the outline drawing.

2.5 Rotating Elements

2.5.1 Rotating assemblies shall be designed to be stiff enough to prevent contact between the rotor and the casing when operating at the maximum allowable differential pressure for all possible operating conditions. Calculated deflection of the shaft at the seals shall not exceed 50 micrometers (0.002 inches).

2.5.2 The impeller shall be either secured to the shaft by an interference fit or keyed, and be capable of transmitting a torque not less than 2.5 times that required for any specified duty, and provided with an arrangement for positive axial location.

2.5.3 Solid rotors are preferred. Hollow rotors will be acceptable only if furnished in compliance with one of the requirements specified in 2.5.3.1 or 2.5.3.2.

2.5.3.1 The rotor is continuously self-venting.

2.5.3.2 The rotor is provided with a plug to allow complete venting of any accumulated gas before beginning any maintenance activity.

2.5.4 Shafts shall be made of one piece, forged steel or hot rolled bar stock and be of ample size to transmit the maximum torque required under any specified operating conditions and to withstand continuously all stresses resulting from supported weights, thrusts, and starting, including direct-on-line motor starting.

2.5.5 Shafts shall be provided with renewable shaft sleeves (that are removable without machining) in the shaft sealing areas. The sleeves shall be of wear-, corrosion-, and erosion-resistant material. Sleeves shall be ground and polished on their outside surface or finished for the specific seal application. Sleeves shall be positively located on the shaft and shall be not less than 2.5 millimeters (0.1 inches) thick.

2.5.6 With the purchaser's approval, sleeves may be omitted provided the proposal so states and the shaft is constructed of an equivalent material and has equal finish to that of a sleeve. Shafts or stub shafts shall include centers to permit refinishing.

8

Document provided by IHS Licensee=Sincor Venezuela/5934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

LIQUID RING VACUUM PUMPS AND COMPRESSORS FOR PETROLEUM, CHEMICAL, AND GAS INDUSTRY SERVICES

2.5.7 For shafts that require sleeve gaskets to pass over threads, the threads shall be at least 2 millimeters ($\frac{1}{6}$ inches) less than the internal diameter of the gasket, and the diameter transition shall be chamfered 15-20 degrees to avoid damage to the gasket.

2.5.8 Shaft sleeves shall be sealed at one end, and the shaft-sleeve assembly shall extend at least 3 millimeters ($\frac{1}{8}$ inches) beyond the outer face of the seal end plate. Leakage between the shaft and the sleeve thus cannot be confused with leakage through the mechanical seal faces.

2.5.9 Shafts shall be machined and properly finished throughout their length so that there is no more than 25 micrometers (0.001 inches) total indicated run-out. Shaft sleeves shall have no more than 50 micrometers (0.002 inches) total indicated run-out on the outside diameter.

2.6 Mechanical Shaft Seals

• **2.6.1** Mechanical seals shall be furnished. When specified, cartridge type seals shall be furnished.

2.6.2 The mechanical seal shall minimize leakage from or into the vacuum pump or compressor over the entire range of specified operating conditions, during shut-down, start-up and periods of idleness and shall also be suitable for operation of the machine on air.

2.6.3 Seals shall withstand the maximum vacuum and maximum allowable working pressure. Component parts of the seals shall be suitable for the specified service conditions.

• 2.6.4 Where seal face leakage must be contained, dual seals or single seals plus auxiliary shaft sealing devices may be specified by the purchaser. Venting, flushing, or blanketing the space between the primary mechanical seal and the auxiliary sealing device, or between mechanical seals, shall be accomplished by means of tapped openings of the appropriate size but not less than NPS ½, unless agreed to by the purchaser. The arrangement of seal fluid piping shall be approved by the purchaser.

2.6.5 Seals shall be removable without removing the vacuum pump or compressor end housing, inlet or discharge piping, or disturbing the driver.

2.6.6 Mechanical seal materials shall be proposed by the vendor and approved by the purchaser.

2.6.7 The seal end plate component parts shall be satisfactory for at least the maximum design vacuum or maximum allowable working pressure and operating temperature and shall have sufficient rigidity to avoid any distortion that would impair seal operation, including distortion that may occur during tightening of the bolts to set gasketing. Provisions shall be made for centering the seal end plate stuffing box bore with either an inside diameter or an outside diameter register fit. A minimum of 3-millimeter (0.125-inch) thick

shoulder shall be provided to prevent axial movement of the mechanical seal seat as a result of chamber under or over pressure. Seal end plate bolting shall be based on specified operating temperature and maximum allowable working pressure and shall be in accordance with Section VIII, Division I, of the ASME Code, except that no fewer than four bolts shall be used.

9

2.6.8 Gland plate connections shall be identified by stamping on the seal end plate the seal fluid inlet and outlet and vent and drain connections. When required by seal design, direction of rotation shall be shown on each gland plate.

- 2.6.9 The vendor shall furnish all mechanical seal piping and accessories as specified by the purchaser. See Appendix E for typical seal flush plans. The seal piping system, including pipe, tubing, fittings, valves, strainers, orifices, and separators, etc., shall be as specified in 3.7. The seal manufacturer and the vacuum pump or compressor vendor shall jointly establish the seal chamber circulation rate and shall advise the purchaser of the condition required in the seal chamber to ensure proper seal operation. In vacuum service, the seal design shall be suitable to seal against atmospheric pressure when the pump is not operating.
- **2.6.10** When specified for flammable fluids, a non-sparking throttle bushing shall be provided to minimize leakage in the event of a complete seal failure. The diametral clearance at the bushing bore shall not be more than 650 micrometers (0.025 inches).
- 2.6.11 When specified or required, the seal gland plate mating joint shall incorporate a fully confined gasket.

2.7 Dynamics

2.7.1 CRITICAL SPEEDS

2.7.1.1 Critical speeds correspond to resonant frequencies of the rotating assembly/bearing support system. The basic identification of critical speeds is made from the natural frequencies of the system and the forcing phenomena. If the frequency of any harmonic component of a periodic forcing phenomenon is equal to, or approximates, the frequency of any mode of the rotating assembly vibration, a condition of resonance may exist. If resonance exists at a finite speed, that speed is called a critical speed.

2.7.1.2 A rotor-bearing support system in resonance will have its normal vibration displacement amplified. The magnitude of amplification and the rate of phase angle change are related to the amount of damping in the system and the mode shape taken by the rotor.

Note: Lateral critical speeds are not usually a matter of concern for liquid ring compressors and vacuum pumps, as their first lateral critical speed (dry) is usually above their operating speed **2.7.1.3** An exciting frequency may be less than, equal to, or greater than the rotational speed of the rotating assembly. Potential exciting frequencies that are to be considered in the design of rotor-bearing systems shall include, but are not limited to, the following sources:

- a. Unbalance in the rotating assembly system.
- b. Internal rubs.

10

- c. Blade or vane, passing frequencies.
- d. Gear-tooth meshing and side bands.
- e. Coupling misalignment.
- f. Loose rotating assembly system components.
- g. Ball and race frequencies of antifriction bearings.

2.7.1.4 Resonance of structural support may adversely affect the rotor vibration amplitude. Resonance of support systems within the vendor's scope of supply shall not occur at the operating speed of a fixed speed machine or at any speed within the operating range of a variable speed machine.

2.7.1.5 The vendor who is specified to have unit responsibility shall assure that the drive-train (turbine, gear, motor, and the like) critical speeds (rotating assembly lateral, system torsional, impeller blade modes, and the like) will not excite any critical speed of the machinery being supplied and that the entire train is suitable for the specified operating speed range, including any starting-speed detent (hold-point) requirements of the train. A list of all undesirable speeds from zero to trip shall be submitted to the purchaser for his review and included in the instruction manual for his guidance.

2.7.1.6 Rotating assemblies shall be designed such that their first dry critical speed is at least 120 percent of the maximum continuous or trip speed (whichever is greater).

Note Wet critical speeds are not of a concern since they occur at speeds higher than dry critical speeds.

• 2.7.1.7 When specified, the equipment vendor shall make a lateral critical speed analysis to determine that the critical speeds of the driver and compressor/vacuum pump are compatible and to assure acceptable amplitudes of vibration at any speed from zero to trip. When mutually agreed to between the vendor and purchaser, a typical lateral critical speed analysis may be provided for the selection being offered.

2.7.1.8 Excitations of undamped torsional natural frequencies may come from many sources, which should be considered in the analysis. These sources may include, but are not limited to, the following:

a. Gear effects such as pitch line runout.

b. Start-up conditions such as speed detents (under inertial impedances) and other torsional oscillations.

c. Torsional transients such as start-ups of synchronous electric motors.

d. Torsional excitation from drivers such as electric motors and reciprocating engines.

e. Hydraulic governor and electronic feedback and control loop resonances from variable-frequency motors.

f. Unbalance.

2.7.1.9 The undamped torsional natural frequencies of the complete train shall be at least 10 percent above or 10 percent below any possible excitation frequency at the operating speed of a fixed speed machine or within the operating speed range of a variable speed machine.

2.7.1.10 In addition to multiples of running speeds, torsional excitations that are not a function of operating speeds or that are nonsynchronous in nature shall be considered in the torsional analysis when applicable and shall be shown to have no adverse effect. Identification of these frequencies shall be the mutual responsibility of the purchaser and the vendor.

2.7.1.11 When torsional resonances are calculated to fall within the margin specified in 2.7.1.9, (and the purchaser and vendor have agreed that all efforts to remove the critical from within the limiting frequency range have been exhausted) a stress analysis shall be performed to demonstrate that the resonances have no adverse effect on the complete train. The acceptance criteria for this analysis shall be mutually agreed upon by the purchaser and the vendor.

• 2.7.1.12 When specified, the vendor shall perform a torsional vibration analysis of the complete coupled train and shall be responsible for directing the modifications necessary to meet the requirements of 2.7.1.8 through 2.7.1.11.

2.7.2 VIBRATION AND BALANCING

2.7.2.1 Rotating components shall be statically or dynamically balanced in accordance with vendor's standard requirements.

2.7.2.2 The unfiltered vibration for all anti-friction bearing vacuum pumps and compressors, measured in any direction on the bearing housing during the shop test and field operation at rated speed and specified operating pressures, shall not exceed the velocity or displacement values, whichever are more restrictive, shown in Figure 2. Filtered vibration shall be measured at running-speed frequency, vane passing frequency or frequencies, and any other frequencies specified by the purchaser.

• 2.7.2.3 When specified by the purchaser, the vendor shall demonstrate that the vacuum pump or compressor can operate at the quoted maximum and minimum pressure ratios and capacity without exceeding the limits specified in 2.7.2.2.

LIQUID RING VACUUM PUMPS AND COMPRESSORS FOR PETROLEUM, CHEMICAL, AND GAS INDUSTRY SERVICES

2.8 Bearings, Bearing Housings, and Lubrication

2.8.1 BEARINGS

2.8.1.1 Both radial and thrust bearings shall be the vendor's standard antifriction design (ball or roller).

2.8.1.2 Antifriction bearings shall be selected to give a minimum L_{10} life of 50,000 hours in continuous operation at normal operating duty but not less than 32,000 hours at maximum axial and radial loads and normal speed. (The L_{10} life is the number of hours at the rated bearing load and speed that 90 percent of a group of identical bearings will complete or exceed before the first evidence of failure.)

2.8.1.3 Bearings shall be sized for continuous operation under the most adverse specified operating conditions. Calculations of the loads shall include, but shall not be limited to, the following factors:

a. Fouling and variation in clearances up to twice the design internal clearances.

- b. Step thrust from all diameter changes.
- c. Stage differential pressure.

- d. Variations in inlet and discharge pressure.
- e. External loads from the driving equipment.

2.8.1.4 Thrust bearings shall be arranged to allow axial positioning of each rotor relative to the casing and setting of the bearings' clearance or preload.

11

2.8.1.5 Antifriction bearings shall be retained on the shaft and fitted into housings in accordance with the requirements of AFBMA Standard 7; however, the device used to lock ball thrust bearings to the shaft shall be restricted by a nut with a tongue-type lock washer, for example, Series W.

2.8.1.6 Unless otherwise specified or required, non-angular contact type antifriction bearings with AFBMA symbol 3 internal clearances (C3) shall be provided.

Single or double row bearings shall be of the Conrad type (no filling slots). Pumps or compressors using other than C3 clearance bearings shall have a stainless steel plate on each bearing housing, clearly showing the bearing identification and the AFBMA internal clearance symbol.

Note: Bearings with AFBMA symbol 0 (normal) internal clearance (C0) may be required to maintain proper rotor axial position relative to the casing to prevent metal to metal contact.

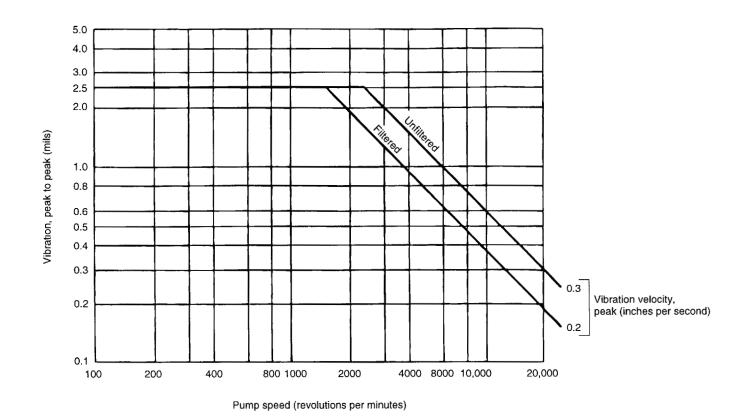


Figure 2—Bearing-Housing Vibration Limits (Antifriction Bearings)

API STANDARD 681

2.8.2 BEARING HOUSINGS

2.8.2.1 Bearing housings shall be equipped with labyrinth-type seals or lip-type seals where the shaft passes through the housing.

2.8.2.2 Bearing housings for grease lubricated bearings shall be provided with stainless steel pressure type grease fittings for filling while operating and a visible discharge port for observing the displaced grease.

2.8.2.3 Where the gas or liquid is flammable or toxic, cantilevered shaft support structures bolted to steel cases shall also be steel.

- 2.8.2.4 When specified, bearing housings for oil-lubricated non-pressure-fed bearings shall be provided with tapped and plugged fill and drain openings at least 1/2 inch National Pipe Thread (NPT) in size. Tape shall not be applied to threads of plugs inserted into oil passages. The housings shall be equipped with constant-level sight-feed oilers at least 0.1 liters (4 ounces) in size, with a positive level positioner (not a set screw), heat resistant containers (not subject to sunlight-or heat induced opacity or deterioration), and protective wire cages. When specified, the oilers shall meet the purchaser's preference. A permanent indication of the proper oil level shall be accurately located and clearly marked on the outside of the bearing housing with permanent metal tags, marks inscribed in the castings or other durable means.
- 2.8.2.5 When specified, bearing housings shall be equipped with replaceable labyrinth-type end seals and deflectors shall be provided. The seals and deflectors shall be made of nonsparking materials. The design of the seals and deflectors shall effectively retain oil in the housing and prevent entry of foreign material into the housing.
- **2.8.2.6** When specified, provisions shall be made for mounting one radial vibration transducer in each bearing housing. The transducer location shall be as specified in API Standard 670 (see 3.2.4.6).
- **2.8.2.7** When specified, thrust bearings and radial bearings shall be fitted with bearing-metal temperature sensors installed in accordance with API Standard 670.

2.8.3 LUBRICATION

2.8.3.1 Unless otherwise specified, bearings and bearing housings shall be arranged for grease lubrication.

• **2.8.3.2** When specified, bearings and bearing housings shall be arranged for hydrocarbon oil lubrication.

2.8.3.3 Any points that require grease lubrication shall have suitable extension lines to permit access during operation.

• **2.8.3.4** When specified, provisions shall be made for a circulating or an oil mist system. The system design and arrangement shall be agreed upon by the purchaser and the vendor.

2.9 Materials

2.9.1 GENERAL

2.9.1.1 Materials of construction shall be the manufacturer's standard for the specified operating conditions, except as required or prohibited by the data sheets or this standard (see 3.7 for requirements for piping material). See Appendix F for typical materials. The metallurgy of all major components shall be clearly stated in the vendor's proposal.

2.9.1.2 Pressure retaining parts of machines that are in flammable or toxic services shall be steel.

2.9.1.3 Materials shall be identified in the proposal with their applicable ASTM, AISI, ASME, or SAE¹ numbers, including the material grade (see Appendix F). When no such designation is available, the vendor's material specification, giving physical properties, chemical composition, and test requirements shall be included in the proposal.

2.9.1.4 The vendor shall specify the ASTM optional tests and inspection procedures that may be necessary to ensure that materials are satisfactory for the service. Such tests and inspections shall be listed in the proposal. The purchaser may consider specifying additional tests and inspections, especially for materials used in critical components (see 5.2.3, Item i).

2.9.1.5 Minor parts that are not identified (such as nuts, springs, washers, gaskets, and keys) shall have corrosion resistance at least equal to that of specified parts in the same environment.

• 2.9.1.6 The purchaser will specify any corrosive agents present in the gas and ring liquid and in the environment, including constituents that may cause stress corrosion cracking.

2.9.1.7 If parts exposed to conditions that promote intergranular corrosion are to be fabricated, hard faced, overlaid, or repaired by welding, they shall be made of low carbon or stabilized grades of austenitic stainless steels.

Note. Overlays or hard surfaces that contain more than 0.10 percent carbon can sensitize both low-carbon and stabilized grades of austenitic stainless steel, unless a buffer layer that is not sensitive to intergranular corrosion is applied.

2.9.1.8 Where mating parts such as studs and nuts of AISI Standard Type 300 stainless steel or materials with similar

¹ Society of Automotive Engineers, 400 Commonwealth Drive, Warrendale, Pennsylvania 15096.

Document provided by IHS Licensee=Sincor Venezuela/5934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-4511584.

LIQUID RING VACUUM PUMPS AND COMPRESSORS FOR PETROLEUM, CHEMICAL, AND GAS INDUSTRY SERVICES

galling tendencies are used, they shall be lubricated with an antiseizure compound of the proper temperature specification and be compatible with the gas.

Note. Torque loading values will be considerably different with and without antiseizing compound.

• 2.9.1.9 Materials exposed to a sour environment (wet H_2S) as defined by NACE MR-01-75 shall be in accordance with the requirements of that standard. Ferrous materials not covered by NACE MR-01-75 shall be limited to a yield strength not exceeding 6200 bar (90,000 pounds per square inch) and a hardness not exceeding Rockwell C22.

Components that are fabricated by welding shall be post-weld heat treated, if required, so that both welds and heat-affected zones meet the yield strength and hardness requirements. The purchaser will specify on the data sheets the presence of H_2S in the process gas.

• **2.9.1.10** When dissimilar materials with significantly different electrical potentials are placed in contact in the presence of an electrolytic solution, galvanic couples that can result in serious corrosion of the less noble material may be created. If such conditions exist, the purchaser and the vendor should select materials in accordance with the NACE *Corrosion Engineer's Reference Book*.

2.9.1.11 Materials, casting factors, and the quality of any welding shall be equal to those required by Section VIII, Division 1, of the ASME Code. The manufacturer's data report forms, as specified in the code, are not required.

2.9.1.12 The use of ASTM A 515 steel is prohibited. Low carbon steels can be notch sensitive and susceptible to brittle fracture at ambient or low temperatures. Therefore, only fully killed, normalized steels made to fine grain practice are acceptable.

• 2.9.1.13 Copper and copper alloys (excluding Monel or its equivalent, bearing babbitt, and precipitation hardened stainless steels) shall not be used for parts of vacuum pumps, compressors or auxiliaries in contact with corrosive gas or with gases capable of forming explosive copper compounds. It will be the responsibility of the purchaser to note such gas characteristics on the inquiry data sheets.

2.9.2 CASTINGS

2.9.2.1 Castings shall be sound and free from porosity, hot tears, shrink holes, blow holes, cracks, scale, blisters, and similar injurious defects. Surfaces of castings shall be cleaned by sandblasting, shotblasting, chemical cleaning, or any other standard method. Mold-parting fins and remains of gates and risers shall be chipped, filed, or ground flush.

2.9.2.2 The use of chaplets in pressure castings shall be held to a minimum. The chaplets shall be clean and corrosion

free (plating permitted) and of a composition compatible with the casting.

13

2.9.2.3 Ferrous castings shall not be repaired by welding, peening, plugging, burning in, or impregnating, except as specified in 2.9.2.3.1 and 2.9.2.3.2.

2.9.2.3.1 Weldable grades of steel castings may be repaired by welding, using a qualified welding procedure based on the requirements of Section VIII, Division 1 and Section IX of the ASME Code.

2.9.2.3.2 Cast gray iron or nodular iron may be repaired by plugging within the limits specified in ASTM A 278, A 395, or A 536. The holes drilled for plugs shall be carefully examined, using liquid penetrant, to ensure that all defective material has been removed. All repairs that are not covered by ASTM specifications shall be subject to the purchaser's approval.

2.9.2.4 Fully enclosed cored voids, including voids closed by plugging, are prohibited.

• 2.9.2.5 When specified, nodular iron castings shall be produced in accordance with ASTM A 395. The production of the castings shall also conform to the conditions specified in 2.9.2.5.1 through 2.9.2.5.5.

2.9.2.5.1 A minimum of one set (three samples) of Charpy V-notch impact specimens at one third the thickness of the test block shall be made from the material adjacent to the tensile specimen on each keel or Y block. These specimens shall have a minimum impact value of 14.0 joules (10 foot pounds) at room temperature.

2.9.2.5.2 The Keel or Y block cast at the end of the pour shall be at least as thick as the thickest section of the main casting.

2.9.2.5.3 Integrally cast test bosses, preferably at least 25 millimeters (1 inch) in height and diameter, shall be provided for all critical areas of the casting for subsequent removal for the purposes of hardness testing and microscopic examination. Critical areas are typically heavy sections, section changes, high stress points, flanges, and other points agreed upon by the purchaser and the vendor. Classification of graphite nodules shall be in accordance with ASTM A 247.

2.9.2.5.4 An as-cast sample from each ladle shall be chemically analyzed.

2.9.2.5.5 Brinell hardness readings shall be made on the actual casting at feasible locations including section changes and flanges. Sufficient surface material shall be removed before hardness readings are made to eliminate any skin effect. Readings shall also be made at the extremities of the casting at locations that represent the section poured first and last. These shall be made in addition to Brinell readings on the keel or Y blocks.

API STANDARD 681

2.9.3 WELDING

2.9.3.1 Welding of piping and pressure containing parts, as well as any dissimilar metal welds and weld repairs, shall be performed and inspected by personnel and procedures qualified in accordance with Section VIII, Division 1 and Section IX of the ASME Code.

2.9.3.2 The vendor shall be responsible for the review of all repairs and repair welds to ensure that they are properly heat treated and nondestructively examined for soundness and compliance with the applicable qualified procedures (see 2.9.1.11). Repair welds shall be nondestructively tested by the same method used to detect the original flaw. As a minimum, the inspection shall be by the magnetic particle method, in accordance with 4.2.2.4 for magnetic material and by the liquid penetrant method in accordance with 4.2.2.5 for nonmagnetic material.

2.9.3.3 Unless otherwise specified, all welding other than that covered by Section VIII, Division 1, of the ASME Code and ASME B31.3, such as welding on base-plates, non-pressure ducting, lagging, and control panels, shall be performed in accordance with AWS D1.1.

• **2.9.3.4** When specified, pressure containing casings made of wrought materials or combinations of wrought and cast materials shall conform to the conditions specified in 2.9.3.4.1 through 2.9.3.4.4.

2.9.3.4.1 Plate edges shall be inspected by magnetic particle or liquid penetrant examination as required by Section VIII, Division 1, UG-93 (d)(3), of the ASME Code.

2.9.3.4.2 Accessible surfaces of welds shall be inspected by magnetic particle or liquid penetrant examination after back chipping or gouging and again after post-weld heat treatment.

2.9.3.4.3 Pressure-containing welds, including welds of the case to horizontal- and vertical-joint flanges, shall be full-penetration welds.

2.9.3.4.4 Casings fabricated from materials that, according to Section VIII, Division 1, of the ASME code, require post-weld heat treatment shall be heat treated regardless of thickness.

- **2.9.3.5** When specified, connections welded to pressure casings shall be installed as specified in 2.9.3.5.1 through 2.9.3.5.5.
- **2.9.3.5.1** In addition to the requirements of 2.9.3.1, the purchaser may specify that magnetic particle inspection or liquid penetrant inspection of welds is required.

2.9.3.5.2 Auxiliary piping welded to chromium-molybdenum alloy steel or 12 percent chrome steel components shall be of the same material, except that chromium-molybdenum alloy steel pipe may be substituted for 12 percent chrome steel pipe.

2.9.3.5.3 When heat treatment is required, piping welds shall be made before the component is heat treated.

• **2.9.3.5.4** When specified, proposed connection designs shall be submitted to the purchaser for approval before fabrication. The drawings shall show weld designs, size, material, and pre- and post-weld heat treatments.

2.9.3.5.5 All welds shall be heat treated in accordance with Section VIII, Division 1, UW-10 and UW-40, of the ASME Code.

• 2.9.4 LOW TEMPERATURE

For operating temperatures below $-30^{\circ}C$ ($-20^{\circ}F$) or when specified for other low ambient temperatures, steels shall have, at the lowest specified temperature, an impact strength sufficient to qualify under the minimum Charpy V-notch impact energy requirements of Section VIII, Division 1, UG-84, of the ASME code. For materials and thicknesses not covered by the code, the purchaser will specify the requirements on the data sheets.

2.10 Nameplate and Rotation Arrows

2.10.1 A nameplate shall be securely attached at a readily visible location on the equipment and on any other major piece of auxiliary equipment.

2.10.2 Rotation arrows shall be cast in or attached to each major item of rotating equipment at a readily visible location. Nameplates and rotation arrows (if attached) shall be of AISI Standard Type 300 stainless steel or nickel-copper alloy (Monel or its equivalent). Attachment pins shall be of the same material. Welding is not permitted.

• 2.10.3 The purchaser's item number, the vendor's name, the machine's serial number, and the machine's size and type, as well as its minimum and maximum allowable design limits and rating data (including pressures, temperatures, speeds, and power), maximum allowable working pressures and temperatures, hydrostatic test pressures, and critical speeds, shall appear on the machine's nameplate or data plate. The purchaser will specify on the data sheets whether customary or SI units are to be shown.

14

SECTION 3—SYSTEM DESIGN

3.1 Ring Liquid System

3.1.1 GENERAL

• **3.1.1.1** Unless otherwise specified, a system shall be furnished to supply the ring liquid at a suitable pressure and temperature to the vacuum pump or compressor. Typical systems are shown in Appendix D. The purchaser will specify the system required.

Note: A liquid ring pump or compressor requires a ring liquid to operate. Typically, the system required to provide this liquid is furnished by the vendor. The extent of the vendor's scope of supply depends upon how the vacuum pump or compressor is integrated into the user's process.

3.1.1.2 The ring liquid system may include, but need not be limited to the following components, as specified or required (see 3.1.2 through 3.1.8):

a. Separator to disengage the ring liquid from the discharge gas stream. This separator may also serve as a storage vessel.b. Cooler.

- c. Strainer or filter.
- d. Ring liquid pump.
- e. Interconnecting piping.
- f. Check valves.
- g. Ring liquid purge system.

3.1.1.3 The ring liquid used shall be mutually agreed upon by the purchaser and the vendor. Purchaser will provide composition and properties of the ring liquid.

3.1.1.4 The system shall be designed to supply the required quantity of ring liquid for all specified operating conditions including start up and "run-in" on air. The system shall be designed and arranged to insure correct ring liquid level during start-up and operation.

• **3.1.1.5** The purchaser will specify whether the ring liquid components are to be mounted on the machine base or on a separate skid.

3.1.1.6 Unless otherwise specified, the ring liquid system, its arrangement (see 2.1.7), and controls shall be subject to purchaser review.

• **3.1.1.7** Coolers, filters, separators, drain traps, and other pressure vessels within the scope of Section VIII, Division 1, of the ASME Code shall conform to the code and, if specified by the purchaser, shall be code stamped.

3.1.2 RING LIQUID SEPARATOR

• **3.1.2.1** If a separator is specified, it shall be designed to separate the discharge gas from the ring liquid. Vendor shall advise the actual gas velocity in the separator vapor space.

• **3.1.2.2** When specified, the vendor shall state the quantity of the ring liquid which will remain entrained in the gas delivered from the separator at each specified operating condition. The purchaser will specify any limitations on liquid carryover from the system.

Note: Transient conditions such as start-up and shutdown may cause unusual carryover conditions.

• **3.1.2.3** When liquid-liquid separation is specified, the system shall be designed to separate condensed process vapors from the ring liquid and allow their removal. The purchaser shall advise the separation time.

Note: Liquid-liquid separation is usually accomplished in a vessel designed for this purpose or in the same vessel used for liquid-gas separation.

3.1.2.4 Unless otherwise specified, an anti-vortex device shall be installed in the draw-off nozzle for the ring liquid that is recycled to the machine.

• **3.1.2.5** The purchaser will provide the vendor with sufficient data to estimate the extent to which the vapor may be expected to condense within the machine. The vendor shall account for this in the design of the machine and separator and, if necessary, provide facilities for the removal of condensate. The purchaser will specify the pressure in the system into which the condensate is to be discharged.

3.1.3 RING LIQUID COOLER

3.1.3.1 Unless otherwise specified, the cooler shall be a water-cooled, shell-and-tube type, with cooling water on the tube side.

3.1.3.2 Unless otherwise specified, coolers shall be constructed and arranged to allow removal of the tube bundles without dismantling piping or machine components.

3.1.3.3 A removable-bundle design is required for coolers with more than 0.45 square meters (5 square feet) of surface, unless otherwise specified. Removable-bundle coolers shall be in accordance with TEMA Class C and shall be constructed with a removable channel cover. Tubes shall not have an outside diameter of less than 15 millimeters (5% inch), and the tube wall shall not have a thickness of less than 1.25 millimeters [18 BWG (0.0049 inch)]. U-bend tubes are not permitted. Coolers shall be equipped with vent and drain connections on their shell and tube sides.

3.1.3.4 The vendor shall include in the proposal complete details of any proposed air-cooled heat exchanger.

• 3.1.3.5 When specified, water-cooled shell-and-tube coolers shall be designed and constructed in accordance with TEMA Class C or R, as specified. When TEMA Class R is

Document provided by IHS Licensee=Sincor Venezuela/5934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

specified, the heat exchanger shall be in accordance with API Standard 660.

3.1.4 RING LIQUID FILTER

3.1.4.1 The ring liquid system shall contain as a minimum a Y-type strainer with a 40-mesh (or finer) screen.

- **3.1.4.2** When specified, or when recommended by the vendor, a ring liquid filter shall be supplied, designed to remove solid particles down to the stated size.
- **3.1.4.3** When specified, the filter shall be the replaceable cartridge, duplex type arranged for online, uninterrupted changeover.

3.1.5 RING LIQUID PUMPS

3.1.5.1 If a ring liquid pump is required, it shall be centrifugal and in accordance with ANSI B73.1 or B73.2, unless otherwise specified.

• **3.1.5.2** The purchaser may specify a pump in accordance with API 610.

3.1.6 RING LIQUID PIPING

3.1.6.1 Ring liquid piping shall be in accordance with the requirements of 3.7.

• **3.1.6.2** When specified by the purchaser, the vendor shall make provision for manual or automatic makeup and draining of the ring liquid while the equipment is operating.

3.1.7 CHECK VALVES

• **3.1.7.1** A check valve is required at the inlet to the vacuum pump or compressor. The purchaser will specify if the valve is to be provided by the vendor.

Note: Low-pressure-drop check valves are required for proper operation of the system.

3.1.7.2 Alternate designs, such as a quick acting isolating valve activated on loss of driver power, may be provided as mutually agreed upon by the purchaser and the vendor.

• **3.1.7.3** When specified, the vendor shall provide a discharge check valve and pressure relief valve.

3.1.8 RING LIQUID PURGE SYSTEM

A ring liquid purge system shall be provided when specified or when required to reduce dissolved solids, gases, or condensed vapors to an acceptable level.

3.2 Controls and Instrumentation

3.2.1 GENERAL

3.2.1.2 Unless otherwise specified, controls and instrumentation shall be suitable for outdoor installation.

• **3.2.1.3** The vendor shall provide sufficient performance data for the vacuum pump/compressor to enable the purchaser to design a control system for startup and for all specified operating conditions. When specified, the vendor shall review the purchaser's overall control system for compatibility with vendor furnished control equipment.

3.2.2 CONTROL SYSTEMS

- **3.2.2.1** The purchaser will specify the method of control, the source of the control signal, its sensitivity and range, and the equipment to be furnished by the vendor.
- **3.2.2.2** Unless specified otherwise, controlled recycle bypass from discharge to suction is required. When specified, this shall be supplied by the vendor.

Note: Bypass control can be used for suction pressure control, start-up, and pump protection from cavitation For certain applications, a vacuum relief valve may be acceptable.

3.2.2.3 For a variable-speed drive, the control signal shall act to adjust the set point of the driver's speed-control system. Unless otherwise specified, the control range shall be from 105 percent of the speed required to maintain ring liquid stability (at the specified control parameter conditions) to maximum continuous speed. Vendor shall advise the minimum speed required to maintain ring liquid stability.

Note. A combination of control modes may be required on drives with a limited speed range and on multiservice or multistream applications.

3.2.2.4 For a variable-speed drive, the equipment and control system shall be equipped with an overspeed trip device independent of the speed control system.

3.2.2.5 The full range of the specified control signal shall correspond to the required operating range of the driven equipment. Unless otherwise specified, the maximum control signal shall correspond to the maximum continuous speed or the maximum flow.

3.2.2.6 Actuation of the control signal or failure of the signal or actuator shall neither prevent the speed control system from limiting the speed to the maximum continuous speed nor prevent manual regulation with the hand speed changer.

3.2.3 INSTRUMENT AND CONTROL PANELS

• **3.2.3.1** When specified, a panel shall be provided and shall include all panel-mounted instruments for the driven equipment and the driver. Such panels shall be designed and

LIQUID RING VACUUM PUMPS AND COMPRESSORS FOR PETROLEUM, CHEMICAL, AND GAS INDUSTRY SERVICES

fabricated in accordance with the purchaser's specification. The purchaser will specify whether the panel is to be freestanding, located on the base of the unit, or in another location. The instruments on the panel shall be clearly visible to the operator from the driver control point. A lamp test push button shall be provided. The instruments to be mounted on the panel shall be specified on the data sheets.

3.2.3.2 Panels shall be completely assembled, requiring only connection to the purchaser's external piping and wiring circuits. When more than one wiring point is required on a unit for control or instrumentation, the wiring to each switch or instrument shall be provided from a single terminal box with terminal posts, mounted on the unit (or its base, if any). Wiring shall be installed in metal conduits or enclosures. All leads and posts on terminal strips, switches, and instruments shall be tagged for identification.

3.2.4 INSTRUMENTATION

3.2.4.1 Minimum Instrumentation

Vendor shall submit his recommendations for instrumentation to ensure safe and reliable operation. The following, as a minimum, shall be included. Refer to Appendix D.

- a. Gas inlet pressure.
- b. Gas inlet temperature.
- c. Ring liquid/gas outlet pressure.
- d. Ring liquid/gas outlet temperature.
- e. Ring liquid supply temperature.
- f. Ring liquid level in separator (not required for oncethrough or partial recirculation systems).

g. Ring liquid supply pressure, or flow.

3.2.4.2 Temperature Gauges

3.2.4.2.1 Dial-type temperature gauges shall be heavy duty and corrosion resistant. They shall be at least 125 millimeters (5 inches) in diameter and bimetallic type or liquid filled. Black printing on a white background is standard for gauges.

3.2.4.2.2 The sensing elements of temperature gauges shall be in the flowing fluid.

Note: This is particularly important for lines that may run partially full

3.2.4.3 Thermowells

Temperature sensing devices that are in contact with flammable or toxic fluids or that are located in pressurized or flooded lines shall be furnished with NPS ¾ AISI Standard Type 300 stainless steel separable solid-bar thermowells.

3.2.4.4 Thermocouples and Resistance Temperature Detectors

Where practical, the design and location of thermocouples and resistance temperature detectors shall permit replacement while the unit is operating. The lead wires of thermocouples and resistance temperature detectors shall be installed as continuous leads between the thermowell or detector and the terminal box. Conduit runs from thermocouple heads to a pull box or boxes located on the baseplate shall be provided.

• 3.2.4.5 Pressure Gauges

Pressure gauges (excluding built-in instrument air gauges) shall be furnished with Type 316 stainless steel Bourdon tubes and stainless steel movements, 110-millimeter (4½-inch) dials and NPS ½-inch male alloy steel connections. Black printing on a white background is standard for gauges. When specified, liquid-filled gauges shall be furnished in locations subject to vibration. Gauge ranges shall preferably be selected so that the normal operating pressure is in the middle *third* of the gauge's range. In no case, however, shall the maximum reading on the dial be less than the applicable relief valve setting plus 10 percent. Each pressure gauge shall be provided with a device such as a disc insert or blow-out back designed to relieve excess case pressure.

3.2.4.6 Vibration Detectors

- **3.2.4.6.1** When specified, accelerometers shall be supplied, installed, and calibrated in accordance with API Standard 670.
- **3.2.4.6.2** When specified, monitors shall be supplied, installed, and calibrated in accordance with API Standard 670.

3.2.4.7 Solenoid Valves

3.2.4.7.1 Direct solenoid-operated valves shall be used only in clean, dry instrument-air service, shall have Class F insulation or better, and shall have a continuous service rating. When required for other services, the solenoid shall act as a pilot valve.

3.2.4.7.2 Solenoid valves shall not be used in continuous services that may affect normal operations. They may be used in intermittent instrument services.

3.2.4.8 Pressure Relief Valves

3.2.4.8.1 The vendor shall furnish the relief valves that are to be installed on equipment or in piping that the vendor is supplying Other relief valves will be furnished by the purchaser. Relief valves for all operating equipment shall meet

17

the limiting relief valve requirements defined in API Recommended Practice 520, Parts I and II, and in API Standard 526. The vendor shall determine the size and set pressure of all relief valves related to the equipment for the purchaser's approval. The vendor's quotation shall list all relief valves and shall clearly indicate those to be furnished by the vendor. Relief valve settings, including accumulation, shall take into consideration all possible types of equipment failure and the protection of piping systems (see 5.2.3, Item j).

3.2.4.8.2 Unless otherwise specified, relief valves shall have steel bodies.

• **3.2.4.8.3** When specified, thermal relief valves shall be provided for components that may be blocked in by isolation valves.

3.2.5 ALARMS AND SHUTDOWNS

• 3.2.5.1 General

Switches, control devices, and annunciator display units shall be furnished and mounted by the vendor as specified and may include those listed below. The alarm setting shall precede the shutdown setting.

- a. High gas outlet temperature.
- b. High gas outlet pressure.
- c. High ring liquid outlet temperature.
- d. Low ring liquid flow.
- e. Low ring liquid level in separator.
- f. High ring liquid level separator.
- g. High bearing housing vibration.
- h. Low mechanical seal fluid pressure.

3.2.5.2 Annunciator

The vendor shall furnish a first-out annunciator when an annunciator system is specified. The annunciator shall contain approximately 25 percent spare points and, when specified, shall be arranged for purging. Connections shall be provided for actuation of a remote signal when any function alarms or trips. The sequence of operation shall be as specified in 3.2.5.2.1 through 3.2.5.2.3.

3.2.5.2.1 Alarm indication shall consist of the flashing of a light and the sounding of an audible device.

3.2.5.2.2 The alarm condition shall be acknowledged by operating an alarm-silencing button common to all alarm functions.

3.2.5.2.3 When the alarm is acknowledged, the audible device shall be silenced, but the light shall remain steadily lit as long as the alarm condition exists. The annunciator shall be capable of indicating a new alarm (with a flashing light and sounding horn) if another function reaches an alarm

condition, even if the previous alarm condition has been acknowledged but still exists.

3.2.5.3 Alarm and Trip Switches

3.2.5.3.1 Each alarm switch and each shutdown switch shall be furnished in a separate housing located to facilitate inspection and maintenance. Hermetically sealed, single-pole, double-throw switches with a minimum capacity of 5 amperes at 120 volts AC and $\frac{1}{2}$ ampere at 120 volts DC shall be used. Mercury switches shall not be used.

3.2.5.3.2 Unless otherwise specified, electric switches that open (de-energize) to alarm and close (energize) to trip shall be furnished by the vendor.

3.2.5.3.3 Alarm and trip switch settings shall not be adjustable from outside the housing. Alarm and trip switches shall be arranged to permit testing of the control circuit, including, when possible, the actuating element, without interfering with normal operation of the equipment. The vendor shall provide a clearly visible light on the panel to indicate when trip circuits are in a test bypass mode. Unless otherwise specified, shutdown systems shall be provided with switches or another suitable means to permit testing without shutting down the unit.

3.2.5.3.4 The vendor shall furnish with the proposal a complete description of the alarm and shutdown facilities to be provided (see 5.2.3, Item j).

3.2.5.3.5 Pressure-sensing elements shall be of AISI Standard Type 300 stainless steel. Low pressure alarms, which are activated by falling pressure, shall be equipped with a valved bleed or vent connection to allow controlled depressuring so that the operator can note the alarm set pressure on the associated pressure gauge. High pressure alarms, which are activated by rising pressure, shall be equipped with valved test connections so that a portable test pump can be used to raise the pressure.

• 3.2.5.4 Replacement of Instruments and Controls

When specified, all instruments and controls other than shutdown sensing devices shall be installed with sufficient valving to permit their replacement while the system is in operation. When shutoff valves are specified for shutdown sensing devices, the vendor shall provide a means of locking the valves in the open position.

3.2.5.5 Housings for Arcing–Type Switches

Particular attention is called to the requirements of 2.1.8 concerning the characteristics of housings for arcing-type switches outlined in the applicable codes.

COPYRIGHT 2002; American Petroleum Institute

18

3.2.6 ELECTRICAL SYSTEMS

- **3.2.6.1** The characteristics of electrical power supplies for motors, heaters, and instrumentation shall be specified. A pilot light shall be provided on the incoming side of each supply circuit to indicate that the circuit is energized. The pilot lights shall be installed on the control panels.
- **3.2.6.2** Electrical equipment located on the unit or on any separate panel shall be suitable for the hazard classification specified. Electrical starting and supervisory controls may be either AC or DC.

3.2.6.3 Power and control wiring within the confines of the baseplate shall be resistant to oil, heat, moisture, and abrasion. Stranded conductors shall be used within the confines of the baseplate and in other areas subject to vibration. Measurement and remote-control panel wiring may be solid conductor. Thermoplastic insulation shall be used and shall be covered by a Neoprene or equal sheath for abrasion protection. Wiring shall be suitable for the environmental temperatures specified.

3.2.6.4 Unless otherwise specified, all leads on terminal strips, switches and instruments shall be permanently tagged for identification. All terminal boards in junction boxes and control panels shall have at least 20 percent spare terminal points.

3.2.6.5 To facilitate maintenance, liberal clearances shall be provided for all energized parts (such as terminal blocks and relays) on equipment. The clearances required for 600-volt service shall also be provided for lower voltages. To guard against accidental contact, enclosures shall be provided for all energized parts.

 3.2.6.6 Electrical materials, including insulation, shall be corrosion resistant and non-hygroscopic insofar as is possible. When specified for tropical location, materials shall be given the treatments specified in 3.5.6.6.1 and 3.5.6.6.2.

3.2.6.6.1 Parts (such as coils and windings) shall be protected from fungus attack.

3.2.6.6.2 Unpainted surfaces shall be protected from corrosion by plating or another suitable coating.

3.2.6.7 Control, instrumentation, and power wiring (including temperature element leads) within the confines of the baseplate shall be installed in rigid metallic conduits and boxes, properly bracketed to minimize vibration, and isolated or shielded to prevent interference between voltage levels. Conduits may terminate (and in the case of temperature element heads, shall terminate) with a flexible metallic conduit long enough to permit access to the unit for maintenance without removal of the conduit. If temperature element heads will be exposed to temperatures above $60^{\circ}C$ ($140^{\circ}F$), a

19-millimeter (¾-inch) bronze hose with four-wall interlocking construction and joints with packed-on (heatproof) couplings shall be used.

3.2.6.8 For Division 2 locations, flexible metallic conduits shall have a liquid tight thermosetting or thermoplastic outer jacket and approved fittings. For Division 1 locations, an NFPA-approved connector shall be provided.

3.2.6.9 AC and DC circuits shall be clearly labeled, connected to separate terminal blocks, and isolated from each other.

3.3 Drivers and Transmissions

- **3.3.1** The type of driver shall be specified. The driver shall be sized to meet the maximum specified operating conditions, including external transmission losses, and shall be in accordance with applicable specifications, as stated in the inquiry and order. The driver shall be suitable for satisfactory operation under the utility and site conditions specified by the purchaser.
- **3.3.2** Anticipated process variations that may affect the sizing of the driver (such as changes in the pressure, temperature, or properties of the fluid handled, as well as special plant start-up conditions) shall be specified.
- **3.3.3** The starting conditions for the driven equipment shall be specified, and the starting method shall be mutually agreed upon by the purchaser and the vendor. The driver's starting-torque capabilities shall exceed the speed-torque requirements of the driven equipment. Particular attention shall be given to starting conditions when the machine is used as a vacuum pump and may be required to start with the suction at atmospheric pressure.

3.3.4 For motor driven units, the motor nameplate rating (exclusive of the service factor) shall be at least 110 percent of the maximum power required (including gear and coupling losses) for any of the specified operating conditions. Consideration shall be given to starting conditions. Equipment driven by induction motors shall be rated at the actual motor speed for the rated load condition.

- **3.3.5** In the case of electric motor drives, the purchaser will specify the type of motor and its characteristics and accessories, including the following:
 - a. Electrical characteristics.

b. Starting conditions (including the expected voltage drop on starting).

- c. Type of enclosure.
- d. Maximum allowable sound pressure level.
- e. Area classification.
- f. Type of insulation.

API STANDARD 681

20

g. Required service factor.

h. Ambient temperature and elevation above sea level.

i. Transmission losses.

j. Temperature detectors, vibration sensors, and heaters, if these are required.

k. Auxiliaries (such as a ventilation blower and instrumentation).

• 3.3.6 The motor's starting-torque requirements shall be met at a specified reduced voltage, and the motor shall accelerate to full speed within a period of time agreed upon by the purchaser and the vendor.

Note: For most applications, the starting voltage is typically 80 percent of the normal voltage, and the time required to accelerate to full speed is generally less than 15 seconds.

3.3.7 Steam turbine drivers shall conform to API 611. Steam turbine drivers shall be sized to deliver continuously 110 percent of the maximum power required for the purchaser's specified conditions while operating at a corresponding speed of the specified steam conditions. Consideration shall be given to starting conditions.

3.3.8 Gears shall conform to API Standard 677.

3.3.9 For drivers that weigh more than 450 kilograms (1000 pounds), the driver feet shall be provided with vertical jackscrews.

3.4 Couplings and Guards

3.4.1 Unless otherwise specified, flexible couplings and guards between drivers and driven equipment shall be supplied by the manufacturer of the driven equipment.

• 3.4.2 Coupling hubs shall be steel. Flexible-disc types shall have discs of corrosion-resistant material. The make, model, materials, service factor, and mounting arrangement of couplings will be specified by the purchaser. A spacer coupling shall be used unless otherwise specified. The spacer shall have a nominal length of at least 125 millimeters (5 inches) and shall permit removal of the coupling, bearings, and seals without disturbing the driver or the suction and discharge piping.

Note: When flexible-element couplings are specified, consideration should be given to designs that will retain the spacer if a flexible element ruptures.

3.4.3 Information on shafts, keyway dimensions (if any), and shaft end movements due to end play and thermal effects shall be furnished to the vendor supplying the coupling.

3.4.4 Couplings and coupling-to-shaft junctures shall be rated for at least the maximum driver power, including any motor service factor.

3.4.5 Couplings shall be keyed. Keys, keyways, and fits shall conform to AGMA 9002. Coupling hubs shall be

furnished with tapped puller holes at least 3% inch (10 millimeters) in size to aid removal.

- **3.4.6** When specified, the coupling surfaces normally used for checking alignment shall be concentric with the axis of coupling hub rotation within the following limits: 0.5 micrometers total indicated runout per millimeter of shaft diameter (0.0005 inch per inch), with a maximum of 100 micrometers (0.003 inches) total indicated runout. All other diameters not used for location, registration, or alignment shall be to the coupling manufacturer's standard, provided balance requirements are met.
- **3.4.7** When specified, couplings shall be manufactured to meet the balance requirements of AGMA 9000, Class 8. When specified by the purchaser or recommended by the vendor, couplings shall be dynamically balanced in accordance with AGMA 9000. For dynamic balancing, the AGMA balance class shall be mutually agreed upon by the purchaser and the vendor.
- **3.4.8** When specified, limited-end-float couplings with maximum coupling end floats as specified in Table 3 shall be supplied with horizontal-sleeve-bearing motors to prevent the motor rotor from rubbing stationary motor parts.

Note: Couplings with axial elastic centering forces are usually satisfactory without these precautions.

3.4.9 When the vendor is not required to mount the driver, he shall deliver the fully machined half-coupling to the driver manufacturer's plant or any other designated location, together with the necessary instructions for mounting the half-coupling on the driver shaft.

3.4.10 Removable coupling guards shall be furnished and shall be in accordance with the Occupational Safety and Health Administration's requirements for coupling guards.

3.5 Belt Drives

3.5.1 Belt drives shall only be used for equipment of 150 kilowatts (200 brake horsepower) or less and, unless otherwise specified, shall employ multiple-V belts or positive drive belts. Multiple V-belts shall be furnished in either matched sets or banded multi-V designs. All belts shall be oil resistant (that is, they shall have a core of Neoprene or an equivalent material) and shall be of the static-conducting type. The service factor shall not be less than 1.75 times the driver nameplate power rating.

Minimum Motor Rotor End Float		Maximum Coupling End Float	
Millimeters	Inches	Millimeters	Inches
6	0 250	2	0.090
13	0.500	5	0 190

3.5.2 The vendor shall provide a positive belt-tensioning device on all belt drives. This device shall incorporate a lateral adjustable base with guides and hold-down bolts, two belt-tensioning screws, and locking bolts.

3.5.3 The vendor who has unit responsibility shall inform the manufacturer of the connected equipment when a belt drive is to be used. The driver manufacturer shall be provided with the belt drive's radial-load. These characteristics shall be taken into account when the driver is selected.

3.5.4 Belt drives shall meet the requirements of 3.5.4.1 through 3.5.4.7.

3.5.4.1 The distance between the centers of the sheaves shall not be less than 1.5 times the diameter of the large sheave.

3.5.4.2 The belt wrap (contact) angle on the small sheave shall not be less than 140 degrees.

3.5.4.3 The shaft length on which the sheave hub is fitted shall be greater than or equal to the width of the sheave hub.

3.5.4.4 The length of a shaft key fitting used to mount a sheave shall not be less than the length of the sheave bore.

3.5.4.5 The sheave shall be mounted on a tapered adapter bushing.

3.5.4.6 To reduce bearing moment loading (belt tension), the sheave overhang distance shall be minimized.

• **3.5.4.7** When specified, sheaves shall meet the balance requirements of ANSI S2.19, Grade 6.3.

3.5.5 Removable guards shall be furnished and shall be in accordance with the Occupational Safety and Health Administrations requirements for guards.

3.6 Mounting Plates

3.6.1 GENERAL

• **3.6.1.1** The equipment shall be furnished with soleplate or a baseplate as specified on the data sheets. The vendor shall mount and align the driver and transmission on the mounting plate prior to shipment. The purchaser will specify either continuously grouted or column mounting (see 3.6.1.2.4 and 3.6.2.4).

3.6.1.2 In 3.6.1.2.1 through 3.6.1.2.11, the term *mounting plate* refers to both baseplate and soleplates.

3.6.1.2.1 The upper surfaces of mounting plates used for mounting the equipment shall be machined parallel. The maximum surface finish shall be 3 micrometers (125 micro-inches) Ra.

3.6.1.2.2 Mounting plates shall be equipped with vertical jackscrews.

3.6.1.2.3 Unless otherwise specified, alignment positioning screws shall be provided for each driver and gearbox that weighs 225 kg (500 lb) or more to facilitate longitudinal and transverse horizontal adjustment. The lugs holding these jackscrews shall be attached to the mounting plates so that they do not interfere with the installation or removal of the drive element or shims.

3.6.1.2.4 Machinery supports shall be designed to limit a change of alignment to 50 micrometers (0.002 inches) at the coupling flange, in addition to that allowed in 2.2.4 (see 2.4 for allowable piping forces).

• 3.6.1.2.5 When epoxy grout is specified, the vendor shall commercially sandblast, in accordance with SSPC SP 6, all the grouting surfaces of the mounting plates and shall precoat these surfaces with a catalyzed epoxy primer. The epoxy primer shall be compatible with epoxy grout. The vendor shall submit to the purchaser instructions for field preparation of the epoxy primer.

Note: Epoxy primers have a limited life after application. The grout manufacturer should be consulted to ensure proper field preparation of the mounting plate for satisfactory bonding of the grout.

3.6.1.2.6 Anchor bolts shall not be used to fasten machinery to the mounting plates.

3.6.1.2.7 Mounting plates shall not be drilled for equipment to be mounted by others. The outside corners of the mounting plates in contact with the grout shall have at least 50 millimeters (2 inch) radii in the plan view.

3.6.1.2.8 Machined mounting surfaces shall extend at least 25 millimeters (1 inch) beyond the outer three sides of equipment feet to facilitate alignment at installation.

3.6.1.2.9 All pads for drivers and gearboxes shall be machined to allow for the installation of shims at least 3 millimeters ($\frac{1}{8}$ inch) thick under each component. When the vendor mounts the components, a set of stainless steel shims at least 3 millimeters ($\frac{1}{8}$ inch) thick shall be furnished. All shim packs shall straddle the hold down bolts and any vertical jackscrews.

3.6.1.2.10 Anchor bolts will be furnished by the purchaser.

3.6.2 BASEPLATE

• **3.6.2.1** When a baseplate or skid is specified, the data sheets will indicate the major equipment items to be mounted on it. A baseplate shall be a single unit of fabricated steel construction.

3.6.2.2 Unless otherwise specified, the baseplate shall extend under the pump, driver, and gear.

• **3.6.2.3** When specified, baseplates or skids shall be provided with levelling pads or targets protected by remov-

Document provided by IHS Licensee=Sincor Venezuela/5934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1:800-451-1584.

API STD*681 96 🎟 0732290 0550639 414 🛙

API STANDARD 681

22_____

able covers. The pads or targets shall be accessible for field levelling after installation, with the equipment mounted and the baseplate on the foundations.

• **3.6.2.4** When column mounting is specified, the baseplate shall be of sufficient rigidity to be supported at the specified points without continuous grouting under structural members. The baseplate design shall be mutually agreed upon by the purchaser and the vendor.

3.6.2.5 Unless otherwise specified, fabricated baseplates shall be designed in accordance with AISC *Manual of Steel Construction*, Part 5, Specifications and Codes.

• **3.6.2.6** Single-piece drain-rim or drain-pan baseplates shall be furnished. The rim or pan of the baseplate shall be sloped at least 1:120 toward the pump end, where a tapped drain opening at least 1 inch NPT in size shall be located to affect complete drainage. As a minimum, the drain-rim or drain-pan shall extend underneath the pump or compressor to collect leakage. When specified, more extensive leakage collection shall be provided.

3.6.2.7 The baseplate shall be provided with lifting lugs for at least a four-point lift. Lifting the baseplate complete with all equipment mounted shall not permanently distort or otherwise damage the baseplate or machinery mounted on it.

3.6.2.8 The bottom of the baseplate between structural members shall be open. When the baseplate is installed on a concrete foundation, it shall be provided with at least one grout hole having a clear area of at least 100 square centimeters (19 square inches) and no dimension less than 75 millimeters (3 inches) in each bulkhead section. These holes shall be located to permit grouting under all load-carrying structural members. Where practical, holes shall be accessible for grouting with equipment installed. The holes shall have 13-millimeter (½-inch) raised-lip edges, and if located in an area where liquids could impinge on the exposed grout, metallic covers with a minimum thickness of 16 gauge shall be provided. Vent holes at least 13 millimeters (½ inch) in size shall be provided at the highest point in each bulkhead section of the baseplate.

- **3.6.2.9** When specified, mounting pads on the bottom of the baseplate shall be provided and shall be in one plane to permit use of a single-level foundation.
- **3.6.2.10** When specified, nonskid metal decking covering all walk and work areas shall be provided on baseplate top.
- **3.6.2.11** When specified, the baseplate mounting pads shall be machined after the baseplate is fabricated.

3.7 Piping

3.7.1 GENERAL

3.7.1.1 Piping design and joint fabrication, examination, and inspection shall be in accordance with ANSI B31.3.

3.7.1.2 Piping systems are defined as follows:

- a. Group I:
 - 1. Vapor piping.
 - 2. Ring liquid.
 - 3. Mechanical seal flushing fluid.
 - 4. Drains and vents.

b. Group II:

- 1. Cooling water.
- 2. Cooling water drains and vents.
- 3. Instrument air.

Systems shall comply with the requirements of Table 4.

Note: Casing connections are discussed in 2.3

3.7.1.3 Piping systems shall include piping, isolating valves, control valves, relief valves, pressure reducers, orifices, temperature gauges and thermowells, pressure gauges, sight flow indicators, and all related vents and drains.

3.7.1.4 The vendor shall furnish all piping systems, including mounted appurtenances, located within the confines of the main unit's base area, or any auxiliary base area. The piping shall terminate with flanged connections at the edge of the base. The purchaser will furnish only interconnecting piping between equipment groupings and off-base facilities (see 3.7.2.2).

3.7.1.5 The design of piping systems shall achieve the following:

a. Proper support and protection to prevent damage from vibration or from shipment, operation, and maintenance.

b. Proper flexibility and normal accessibility for operation, maintenance, and thorough cleaning.

c. Installation in a neat and orderly arrangement adapted to the contour of the machine without obstruction of access openings.

d. Elimination of air pockets by the use of valved vents or nonaccumulating piping arrangements.

e. Complete drainage through low points without disassembly of piping.

3.7.1.6 The use of flanges and fittings shall be minimized. Piping shall preferably be fabricated by bending and welding to minimize the use of flanges and fittings. Welded flanges are permitted only at equipment connections, at the edge of any base, and for ease of maintenance. The use of flanges at other points is permitted only with the purchaser's specific

LIQUID RING VACUUM PUMPS AND COMPRESSORS FOR PETROLEUM, CHEMICAL, AND GAS INDUSTRY SERVICES

approval. Other than tees and reducers, welded fittings are permitted only to facilitate pipe layout in congested areas. Pipe bushings shall not be used. Threaded connections shall be held to a minimum.

3.7.1.7 Pipe threads shall be taper threads in accordance with ASME B 1.20.1. Flanges shall be in accordance with ANSI B 16.5. Slip-on flanges are permitted only with the purchaser's specific approval. Unless otherwise specified, for socket-welded construction, a 1.6-millimeter ($\frac{1}{16}$ -inch) gap shall be left between the pipe end and the bottom of the socket.

3.7.1.8 Connections, piping, valves, and fittings that are 30 millimeters ($1\frac{1}{4}$ inches), 65 millimeters ($2\frac{1}{2}$ inches), 90 millimeters ($3\frac{1}{2}$ inches), 125 millimeters (5 inches), 175 millimeters (7 inches), or 225 millimeters (9 inches) in size shall not be used.

3.7.1.9 Where space does not permit the use of NPS $\frac{1}{2}$, $\frac{3}{4}$, or 1 pipe, seamless tubing may be furnished in accordance with Table 3. The make and model of fittings shall be subject to purchaser's approval.

3.7.1.10 The minimum size of any connection shall be NPS ¹/₂ nominal pipe size.

3.7.1.11 Piping systems furnished by the vendor shall be fabricated, installed in the shop, and properly supported. Bolt holes for flanged connections shall straddle lines parallel to the main horizontal or vertical centerline of the equipment.

3.7.1.12 Welding shall be performed by operators and procedures qualified in accordance with Section IX of the ASME code.

3.7.1.13 Pipe plugs shall be in accordance with 2.3.7.

• **3.7.1.14** The extent of and requirements for process piping to be supplied by the vendor shall be specified.

• 3.7.1.15 When specified, the vendor shall review all piping, appurtenances, and vessels immediately upstream and downstream of the equipment and supports. The purchaser and the vendor shall mutually agree on the scope of this review.

3.7.2 INSTRUMENT PIPING

3.7.2.1 The vendor shall supply all necessary piping, valves, and fittings for instruments and instrument panels (see 3.2.3.2).

3.7.2.2 Connections on equipment and piping for pressure instruments and test points shall conform to 3.7.1.4. Beyond the initial $\frac{3}{4}$ -inch isolating valve, NPS $\frac{1}{2}$ piping, valves, and fittings may be used. Where convenient, a common connection may be used for remotely mounted instruments that measure the same pressure. Separate secondary $\frac{1}{2}$ -inch isolating valves are required for each instrument on a common connection. Where a pressure gauge is to be used for testing pressure alarm or shutdown switches, common connections are required for pressure gauge and switches.

3.8 Special Tools

3.8.1 When special tools and fixtures are required to disassemble, assemble, or maintain the unit, they shall be included in the quotation and furnished as part of the initial supply of the machine. For multi-unit installations, the requirements for quantities of special tools and fixtures shall be mutually agreed upon by the purchaser and the vendor. These or similar tools shall be used during shop assembly and post-test disassembly of the equipment.

3.8.2 When special tools are provided, they shall be packaged in a separate, rugged metal box or boxes and shall be marked "special tools for (Tag/Item Number)." Each tool shall be stamped or tagged to indicate its intended use.

SECTION 4—INSPECTION, TESTING, AND PREPARATION FOR SHIPMENT

4.1 General

4.1.1 After advance notification of the vendor by the purchaser, the purchaser's representative shall have entry to all vendor and subvendor plants where manufacturing, testing, or inspection of the equipment is in progress.

4.1.2 The vendor shall notify subvendors of the purchaser's inspection and testing requirements.

4.1.3 The vendor shall provide sufficient advance notice (see 4.3.1.3) to the purchaser before conducting any inspection or test that the purchaser has specified to be witnessed or observed.

• **4.1.4** The purchaser will specify the extent of participation in the inspection and testing and the amount of advance notification required.

4.1.4.1 When shop inspection and testing have been specified by the purchaser, purchaser and vendor shall meet to coordinate manufacturing hold points and inspectors' visits.

4.1.4.2 Witnessed means that a hold shall be applied to the production schedule and that the inspection or test shall be carried out with the purchaser or his representative in attendance. For mechanical running or performance test, this requires written notification of a successful preliminary test.

API STANDARD 681

4.1.4.3 Observed means that the purchaser shall be notified of the timing of the inspection or test; however, the inspection or test shall be performed as scheduled, and if the purchaser or his representative is not present, the vendor shall proceed to the next step. (The purchaser should expect to be in the factory longer than for a witnessed test.)

4.1.5 Equipment for the specified inspection and tests shall be provided by the vendor.

4.1.6 The purchaser's representative shall have access to the vendor's quality program for review.

4.2 Inspection

4.2.1 GENERAL

4.2.1.1 The vendor shall keep the following data available for at least five years for examination or reproduction by the purchaser or his representative upon request:

a. Necessary certification of materials, such as mill test reports.

b. Test data to verify that the requirements of the specification have been met.

c. Results of documented tests and inspections, including fully identified records of all heat treatment and radiography.

• d. When specified, final assembly maintenance and running clearances.

4.2.1.2 Pressure-containing parts shall not be painted until the specified inspection of the parts is completed.

• **4.2.1.3** In addition to the requirements of 2.9.3.1, the purchaser may specify the following:

a. Parts that shall be subjected to surface and subsurface examination.

b. The type of examination required, such as magnetic particle, liquid penetrant, radiographic, and ultrasonic examination.

4.2.2 MATERIAL INSPECTION

4.2.2.1 General

4.2.2.1.1 When radiographic, ultrasonic, magnetic particle, or liquid penetrant inspection of welds or materials is required or specified, the criteria in 4.2.2.2 to 4.2.2.5 shall apply unless other criteria are specified by the purchaser. Cast iron may be inspected in accordance with 4.2.2.4 and 4.2.2.5. Welds, cast steel, and wrought material may be inspected in accordance with 4.2.2.5.

4.2.2.1.2 It shall be the vendor's responsibility to review the design limits of all components in the event that more stringent requirements are necessary. Defects that exceed the

limits imposed in 4.2.2 shall be removed to meet the quality standards cited, as determined by the Inspection Method specified.

4.2.2.2 Radiography

4.2.2.2.1 Radiography shall be in accordance with ASTM E 94 and ASTM E 142.

4.2.2.2.2 The acceptance standard used for welded fabrications shall be Section VIII, Division 1, UW-52, of the ASME Code. The acceptance standard used for castings shall be Section VIII, Division 1, Appendix 7, of the ASME Code.

4.2.2.3 Ultrasonic Inspection

4.2.2.3.1 Ultrasonic inspection shall be in accordance with Section V, Articles 5 and 23 of the ASME Code.

4.2.2.3.2 The acceptance standard used for welded fabrications shall be Section VIII, Division 1, Appendix 12, of the ASME Code. The acceptance standard used for castings shall be Section VIII, Division 1, Appendix 7, of the ASME Code.

4.2.2.4 Magnetic Particle Inspection

4.2.2.4.1 Both wet and dry methods of magnetic particle inspection shall be in accordance with ASTM E 709.

4.2.2.4.2 The acceptance standard used for welded fabrications shall be Section VIII, Division 1, Appendix 6 and Section V, Article 25, of the ASME Code. The acceptability of defects in castings shall be based on a comparison with the photographs in ASTM E 125. For each type of defect, the degree of severity shall not exceed the limits specified in Table 4.

4.2.2.5 Liquid Penetrant Inspection

4.2.2.5.1 Liquid penetrant inspection shall be in accordance with Section V, Article 6, of the ASME Code.

4.2.2.5.2 The acceptance standard used for welded fabrications shall be Section VIII, Division 1, Appendix 8 and Section V, Article 24, of the ASME Code. The acceptance standard used for castings shall be Section VIII, Division 1, Appendix 7, of the ASME Code.

4.2.3 MECHANICAL INSPECTION

4.2.3.1 During assembly of the system and before testing, each component (including cast-in passages of these components) and all piping and appurtenances shall be cleaned chemically or by another appropriate method to remove foreign materials, corrosion products, and mill scale.

- **4.2.3.2** When specified, the purchaser may inspect for cleanliness the equipment and all piping and appurtenances furnished by or through the vendor before heads are welded to vessels, openings in vessel or exchangers are closed, or piping is finally assembled.
- **4.2.3.3** When specified, the hardness of parts, welds, and heat-affected zones shall be verified as being within the allowable values by testing of the parts, welds, or heat-affected zones. The method, extent, documentation, and witnessing of the testing shall be mutually agreed upon by the purchaser and the vendor.

4.3 Testing

4.3.1 GENERAL

4.3.1.1 Equipment shall be tested in accordance with 4.3.2 and 4.3.3. Other tests that may be specified by the purchaser are described in 4.3.4 and 4.3.5.

4.3.1.2 At least six weeks before the first scheduled running test, the vendor shall submit to the purchaser, for his review and comment, detailed procedures for the mechanical running test and all specified running optional tests, including acceptance criteria for all monitored parameters.

4.3.1.3 The vendor shall notify the purchaser not less than five working days before the date the equipment will be ready for testing. If the testing is rescheduled, the vendor shall notify the purchaser not less than five working days before the new test date.

4.3.2 HYDROSTATIC TEST

4.3.2.1 Pressure-containing parts (including auxiliaries) shall be tested hydrostatically with liquid at a minimum of 1.5 times the maximum allowable working pressure but not less than 1.5 bar gauge (20 pounds per square inch gauge). The test liquid shall be at a higher temperature than the nil-ductility transition temperature of the material being tested.

4.3.2.2 If the part tested is to operate at a temperature at which the strength of a material is below the strength of that material at room temperature, the hydrostatic test pressure shall be multiplied by a factor obtained by dividing the allowable working stress for the material at room temperature by that at operating temperature. The stress values used shall conform to those given in ASME B31.3 for piping or in Section VIII, Division 1, of the ASME Code for vessels. The pressure thus obtained shall then be the minimum pressure at which the hydrostatic test shall be performed. The data sheets shall list actual hydrostatic test pressures.

10010	maximum correnty or bolicoto in ouclinge				
Туре	Defect	Maximum Severity Level			
I	Liner discontinuities	1			
11	Shrinkage	2			
III	Inclusions	2			
IV	Chills and chaplets	1			
v	Porosity	1			
VI	Welds	1			

4.3.2.3 Where applicable, tests shall be in accordance with the ASME Code. In the event that a discrepancy exists between the code test pressure and the test pressure in this standard, the higher pressure shall govern.

4.3.2.4 The chloride content of liquids used to test austenitic stainless steel materials shall not exceed 50 parts per million. To prevent deposition of chlorides as a result of evaporative drying, all residual liquid shall be removed, and tested parts shall be dried at the conclusion of the test.

4.3.2.5 Tests shall be maintained for a sufficient period of time to permit complete examination of parts under pressure. The hydrostatic test shall be considered satisfactory when neither leaks nor seepage through the casing or casing joint is observed for a minimum of 30 minutes. Large, heavy castings may require a longer testing period—to be agreed upon by the purchaser and the vendor. Seepage past internal closures required for testing of segmented cases and operation of a test pump to maintain pressure are acceptable.

4.3.3 MECHANICAL RUNNING TEST

4.3.3.1 The requirements of 4.3.3.1.1 through 4.3.3.1.3 shall be met before the mechanical running test is performed.

4.3.3.1.1 The contract shaft seals and bearings shall be used in the machine for the mechanical running test.

4.3.3.1.2 All joints and connections shall be checked for tightness, and any leaks shall be corrected.

4.3.3.1.3 All warning, protective, and control devices used during the test shall be checked, and adjustments shall be made as required.

4.3.3.2 The vendor's standard mechanical running test of the machine shall be conducted at normal speed for a minimum of one hour, and correct operation of the control system, if furnished, shall be demonstrated.

4.3.3.3 The requirements of 4.3.3.3.1 to 4.3.3.3.3 shall be met during the mechanical running test.

4.3.3.3.1 During the mechanical running test, the mechanical operation of all equipment being tested and the operation of the test instrumentation shall be satisfactory. The measured unfiltered vibration shall not exceed the limits of 2.7.2.2 and shall be recorded throughout the operating speed range.

25

- **4.3.3.3.2** When specified while the equipment is operating at maximum continuous speed, and at all other speeds that may have been specified in the test agenda, sweeps shall be made for vibration amplitudes at frequencies other than synchronous speed. As a minimum, these sweeps shall cover a frequency range from 0.25 to 20 times the maximum continuous speed but not more than 3000 hertz (180,000 cycles per minute). If the amplitude of any discrete, nonsynchronous vibration exceeds 20 percent of the allowable vibration as defined in 2.7.2.2 the purchaser and the vendor shall mutually agree on requirements for any additional testing and on the equipment's suitability for shipment.
- **4.3.3.3.3** When specified, recordings shall be made of all real-time vibration data. When specified, a copy of the recordings shall be given to the purchaser.

4.3.3.3.4 If replacement or modification of bearings or seals or dismantling of the case to replace or modify other parts is required to correct mechanical or performance deficiencies, the initial test will not be acceptable, and the shop tests shall be run after these replacements or corrections are made.

• **4.3.3.4** When specified, any of the requirements of 4.3.3.4.1 through 4.3.3.4.7 shall be met during the mechanical running test.

4.3.3.4.1 All purchased vibration probes, transducers, and accelerometers shall be in use during the test. If vibration probes are not furnished by the equipment vendor or if the purchased probes are not compatible with shop readout facilities, then shop probes and readouts that meet the accuracy requirements of API Standard 670 shall be used.

4.3.3.4.2 Shop test facilities shall include instrumentation with the capability of continuously monitoring and plotting rotational speed, vibration amplitude, and phase angle revolutions per minute, peak-to-peak displacement and phase angle (x-y-y'). Presentation of vibration displacement and phase marker shall be by oscilloscope.

4.3.3.4.3 The vibration characteristics determined by the use of the instrumentation specified in 4.3.3.4.1 and 4.3.3.4.2 shall serve as the basis for acceptance or rejection of the machine.

• **4.3.3.4.4** When seismic test values are specified, vibration data (minimum and maximum values) shall be recorded and located (clock angle) in a radial plane transverse to each bearing centerline (if possible), using shop instrumentation during the test.

4.3.3.4.5 Testing with the contract coupling is preferred.

4.3.3.4.6 The mechanical running test shall verify that the operating speed range is free of critical speeds.

4.3.3.4.7 The mechanical running test of a fixed speed machine shall be conducted at normal speed for a minimum

4.3.4 GAS LEAK TEST

4.3.4.1 Each completely assembled vacuum pump or compressor casing intended for toxic, hazardous, flammable, or hydrogen-rich service shall be tested as specified in 4.3.4.2.

4.3.4.2 Unless otherwise specified, the casing (with the end seals installed) shall be pressurized to the rated discharge pressure, or in the case of vacuum pumps to 1 bar g (15 psig), held at this pressure for a minimum of 30 minutes, and subjected to a soap-bubble test or another approved test to check for gas leaks.

4.3.5 PERFORMANCE TEST

4.3.5.1 Liquid ring vacuum pumps shall be tested in accordance with HEI *Performance Standards for Liquid Ring Vacuum Pumps*, or PNEUROP 6612 standards, or as mutually agreed to between purchaser and vendor.

• **4.3.5.2** When specified, the compressor, together with it's ring liquid system, shall be subjected to a performance test, the extent of which, and the applicable test methods, shall be agreed to between purchaser and vendor.

4.3.5.3 Unless otherwise specified the machine shall be tested on dry air and water.

4.3.5.4 The performance test may be combined with the mechanical running test.

4.3.5.5 For vacuum pumps, test data shall be recorded at one speed at five suction pressures varying from atmospheric pressures to maximum vacuum. For compressors, test data shall be recorded at one speed from minimum discharge pressure to maximum discharge pressure. The points are subject to negotiation between purchaser and vendor.

4.3.5.6 The dry air and water performance shall be within the tolerances given in Table 5.

4.3.5.7 Performance at the rated operating point shall be calculated from test data in accordance with the vendor's standard procedures, or as otherwise specified. Where the test is to be performed under different conditions or with different fluids from those specified, the method of converting the test results to the specified conditions shall also be agreed upon (see Appendix H).

4.3.5.8 If it is necessary to dismantle a pump or compressor for a correction, such as improvement of efficiency, the initial test will not be acceptable, and the final hydrotest, gas

Document provided by IHS Licensee=Sincor Venezuela/S934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

leak test, and performance test shall be repeated after the correction is made.

4.3.5.9 The performance test shall be conducted using only one contract rotor, unless otherwise specified.

4.3.5.10 The vendor shall maintain a complete, detailed log of all final tests and shall prepare the required number of copies, including test curves and data, certified for correctness. All preliminary tests and mechanical checks shall be completed by the vendor before the purchaser's witnessed performance test.

• **4.3.5.11** The requirements of 4.3.5.11.1 through 4.3.5.11.6 shall be met before the performance test is performed. These items apply only to machines with oil lubricated bearings.

4.3.5.11.1 The contract shaft seals and bearings shall be used in the machine for the performance test. At the vendor's request, the purchaser may approve the use of substitute seals for reasons such as incompatibility of the contract seals with the test fluid. The acceptable level of leakage during testing shall be mutually agreed upon by the purchaser and the vendor.

4.3.5.11.2 All lubricating-oil and liquid-sealant pressures, viscosities, and temperatures shall be within the range of operating values recommended in the vendor's operating instructions for the specified unit being tested. For circulating lubrication systems, oil flow rates for each bearing housing shall be measured.

4.3.5.11.3 For circulating lubrication systems, test-stand oil filtration shall be 10 microns nominal or better. Oil system components downstream of the filters shall be cleaned prior to the test in accordance with the vendor's criteria for field installation.

4.3.5.11.4 Bearings used in oil mist lubrication systems shall be prelubricated.

4.3.5.11.5 All joints and connections shall be checked for tightness, and any leaks shall be corrected.

4.3.5.11.6 All warning, protective, and control devices used during the test shall be checked, and adjustments shall be made as required.

• 4.3.6 OPTIONAL TESTS

The purchaser will specify in the inquiry or in the order whether any of the shop tests specified in 4.3.6.1 to 4.3.6.5 shall be performed.

4.3.6.1 Complete–Unit Test

Such components as compressors, gears, drivers, ring liquid system, and auxiliaries that make up a complete unit may be tested together as a complete unit. A separate auxilNote: Standard industry tolerances are in accordance with HEI performance standards for liquid ring vacuum pumps. These are more liberal than the tolerances shown in Table 6, and if used could result in the selection of a smaller machine

Table 5—Performance Tolerances

iary test may be performed with the purchaser's approval. When specified, torsional vibration measurements shall be made to verify the vendor's analysis. By agreement the complete-unit test may be combined with the mechanical running test of one or more of the individual components specified by the purchaser.

4.3.6.2 Gear Test

The gear shall be tested with the machine unit during the mechanical running test.

4.3.6.3 Sound–Level Test

The sound-level test shall be performed in accordance with purchaser requirements.

4.3.6.4 Ring Stability Test

For variable speed machines a test agreed to between the purchaser and the vendor shall be conducted to establish the operating limits of liquid ring stability.

• 4.3.6.5 Auxiliary–Equipment Test

Auxiliary equipment such as control systems shall be tested in the vendor's shop. Details of the auxiliary equipment tests shall be developed jointly by the purchaser and the vendor.

4.4 Preparation for Shipment

• 4.4.1 Equipment shall be suitably prepared for the type of shipment specified. The preparation shall make the equipment capable of withstanding six months of outdoor storage from the time of shipment, with no disassembly required before operation, except for inspection of bearings and seals. If storage for a longer period is contemplated, the purchaser will consult with the vendor regarding the recommended procedures to be followed.

4.4.2 The equipment shall be prepared for shipment after all testing and inspection have been completed and the equipment has been released by the purchaser. The preparation shall include that specified in 4.4.2.1 through 4.4.2.11.

4.4.2.1 Exterior surfaces, except for corrosion resistant materials and machined surfaces, shall be given at least one

Document provided by IHS Licensee=Sincor Venezuela/9334214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

coat of the manufacturer's standard non-lead and nonchromate paint.

4.4.2.2 Exterior machined surfaces, except for corrosion resistant materials, shall be coated with a suitable rust preventative.

4.4.2.3 Exposed shafts and shaft couplings shall be wrapped with waterproof, moldable waxed cloth or vapor-phase-inhibitor paper. The seams shall be sealed with oil-proof adhesive tape.

4.4.2.4 Bearing assemblies shall be fully protected from the entry of moisture and dirt. If vapor-phase-inhibitor crystals in bags are installed in large cavities to absorb moisture, the bags must be attached in an accessible area for ease of removal. Where applicable, bags shall be installed in wire cages attached to flanged covers, and bag locations shall be indicated by corrosion-resistant tags attached with stainless steel wire.

4.4.2.5 The interior of the equipment shall be clean; free from scale, welding spatter, and foreign objects; and sprayed or flushed with a suitable rust preventative that can be removed with solvent. The rust preventative shall be applied through all openings while the machine is slow-rolled.

4.4.2.6 Flanged openings shall be provided with metal closures at least 5 millimeters ($\frac{3}{6}$ inch) thick, with elastomer gaskets, and at least four full-diameter bolts. For studded openings, all nuts needed for the intended service shall be used to secure closures.

4.4.2.7 Threaded openings shall be provided with steel caps or round-head steel plugs. In no case shall nonmetallic (such as plastic) caps or plugs be used.

Note: These are shipping plugs; permanent plugs are covered in 2.3.7.

• 4.4.2.8 When a spare rotor is purchased, it shall be prepared for unheated indoor storage for a period of at least three years. The rotor shall be treated with a rust preventative and shall be housed in a vapor-barrier envelope with a slow-release volatile-corrosion inhibitor. The rotor shall be crated for domestic or export shipment, as specified. A purchaser-approved resilient material 3.0 millimeters (½ inch) thick [not Tetrafluoroethylene (TFE) or Polytetrafluoroethylene (PTFE)] shall be used between the rotor and the cradle at the support areas. The rotor shall not be supported at journals.

4.4.2.9 Internal steel areas of bearing housings and carbon steel oil systems' auxiliary equipment such as reservoirs, vessels, and piping shall be coated with a suitable oil-soluble rust preventive.

4.4.2.10 Lifting points and lifting lugs shall be clearly identified on the equipment or equipment package. The recommended lifting arrangement shall be identified on boxed equipment.

4.4.2.11 The equipment shall be identified with item and serial numbers. Material shipped separately shall be identified with securely affixed, corrosion-resistant metal tags indicating the item and serial number of the equipment for which it is intended. In addition, crated equipment shall be shipped with duplicate packing lists, one inside and one on the outside of the shipping container.

4.4.3 The vendor shall provide the purchaser with the instructions necessary to preserve the integrity of the storage preparation after the equipment arrives at the job site and before startup.

4.4.4 Auxiliary piping connections furnished on the purchased equipment shall be impression stamped or permanently tagged to agree with the vendor's connection table or general arrangement drawing. Service and connection designations shall be indicated.

4.4.5 One copy of the manufacturer's installation instructions shall be packed and shipped with the equipment.

4.4.6 Openings that have been beveled for welding shall be provided with closures designed to prevent entrance of foreign materials and damage to the bevel.

SECTION 5-VENDOR'S DATA

5.1 General

5.1.1 The information to be furnished by the vendor is specified in 5.2 and 5.3. The vendor shall complete and forward the Vendor Drawing and Data Requirements form (see Appendix G) to the addresses noted on the inquiry or order. This form shall detail the schedule for transmission of drawings, curves, and data as agreed to at the time of the proposal or order, as well as the number and type of copies required by the purchaser.

5.1.2 The data shall be identified on transmittal (cover) letters and in title blocks or title pages with the following information:

- a. Purchaser/user's corporate name.
- b. Job/project number.
- c. Equipment item number and service name.
- d. The inquiry or purchase order number.

e. Any other identification specified in the inquiry or purchase order.

Document provided by IHS Licensee=Sincor Venezuela/5934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

LIQUID RING VACUUM PUMPS AND COMPRESSORS FOR PETROLEUM, CHEMICAL, AND GAS INDUSTRY SERVICES

f. Vendor's identifying proposal number, shop order number, serial number, or other reference required to identify return correspondence completely.

• 5.1.3 When specified, a coordination meeting shall be held, preferably at the vendor's plant, within four to six weeks after the purchase commitment. Unless otherwise specified, the vendor shall prepare and distribute an agenda prior to this meeting which, as a minimum, will include review of the following items:

a. Purchase order, scope of supply, unit responsibility, and subvendor items.

b. Data sheets.

c. Applicable specifications and previously agreed upon exceptions.

d. Schedules for transmittal of data, production, and testing.

e. Quality assurance program and procedures.

f. Inspection, expediting, and testing.

g. Schematics and bills of material for auxiliary systems.

h. The physical orientation of the equipment, piping, and auxiliary systems.

i. Coupling and seal selections.

j. Bearing life.

k. Sizing criteria for auxiliary equipment.

5.2 Proposals

5.2.1 GENERAL

The vendor shall forward the original and the specified number of copies of the proposal to the addressee specified in the inquiry documents. As a minimum, the proposal shall include the data specified in 5.2.2 through 5.2.4 and a specific statement that the system and all its components are in strict accordance with this standard. If the system and components are not in strict accordance, the vendor shall include a list that details and explains each deviation. The vendor shall provide details to enable the purchaser to evaluate any alternative designs proposed. All correspondence shall be clearly identified in accordance with 5.1.2.

5.2.2 DRAWINGS

5.2.2.1 The drawings described on the Vendor Drawing and Data Requirements form (see Appendix G) shall be included. As a minimum, the following preliminary data shall be furnished:

a. A general arrangement or outline drawing for each major skid or system showing estimated overall dimensions, and

b. Cross-sectional drawings showing details of the proposed equipment.

c. Piping and instrumentation diagrams (P&IDs) and lists of major components and instrumentation.

5.2.2.2 If "typical" drawings, schematics, and bills of material are used, they shall be marked up to show estimated

weight and dimension data and to reflect the equipment and scope proposed.

5.2.3 TECHNICAL DATA

The following data shall be included in the proposal:

a. The purchaser's data sheet with complete vendor's information entered thereon and literature to fully describe details of the offering.

b. Completed purchaser's noise data sheet or the form from the appendix of API Standard 615.

c. The Vendor Drawing and Data Requirements form (see Appendix G) indicating the schedule according to which the vendor agrees to transmit all the data specified as part of the contract.

d. A schedule for shipment of the equipment, in weeks after receipt of the order.

e. A list of recommended spare parts for start-up and normal maintenance purposes.

f. A list of the special tools furnished for maintenance. The vendor shall state if metric items are included in the offering. g. A statement of any special protection required for startup, operation, and periods of idleness under the site conditions specified on the data sheets. The list shall show the protection to be furnished by the purchaser, as well as that included in the vendor's scope of supply.

h. A complete tabulation of utility requirements, such as steam, water, electricity, air, and the nameplate power rating and operating power requirements of auxiliary drivers. (Approximate data shall be defined and clearly identified as such.)

i. A description of the tests and inspection procedures for materials, as required by 2.9.1.4.

j. A description of special requirements, specified in the purchaser's inquiry and as outlined in 2.9.1.3, 3.1.2.1, 3.1.2.2, 3.1.3.4, 3.1.4.2, 3.2.1.3, 3.2.4.1, 3.2.4.8.1, and 3.2.5.3.4.

k. A list of similar machines installed and operating under conditions analogous to those specified in the proposal.

1. Any startup, shutdown, or operating restrictions required to protect the integrity of the equipment.

m. List of vendor's proposed manufacturers for auxiliary equipment and instruments.

n. A description of proposed alarm and shutdown systems, when included in vendor's scope of supply.

o. Method of calculation used to convert from performance conditions on dry air and water to the specified operating conditions.

5.2.4 CURVES

5.2.4.1 The vendor shall provide performance curves to encompass the map of operations, with any limitations indicated thereon. Curves shall show volumetric capacity and required power as a function of discharge pressure (compres-

Document provided by IHS Licensee–Sincor Venezuela/5934214100, User=, 08/14/2002 13:03:08 MDT Questions or comments about this message: please call the Document Policy Management Group at 1-800-451-1584.

sors) or inlet pressure (vacuum pumps). Curves shall be based on dry air at 20°C (68°F) with water at 15°C (60°F) as the ring liquid. For variable speed applications, curves shall show the full range of operation from minimum speed to maximum continuous speed.

5.2.4.2 Estimated performance curves based on the specified conditions for the process gas and ring liquid shall be provided.

5.3 Contract Data

5.3.1 GENERAL

5.3.1.1 The contract information to be furnished by the vendor is specified in Appendix G. Each drawing, bill of material, and data sheet shall have a title block in the lower right hand corner that shows the date of certification, the reference to all identification data specified in 5.1.2, the revision number and date, and the title (see 5.3.2 and 5.3.3).

5.3.1.2 The purchaser will promptly review the vendor's data when he receives them; however, this review shall not constitute permission to deviate from any requirements in the order unless specifically agreed upon in writing. After the data have been reviewed, the vendor shall furnish certified copies in the quantity specified.

5.3.1.3 A complete list of vendor data shall be included with the first issue of major drawings. This list shall contain titles, drawing numbers, and a schedule for transmission of all data the vendor will furnish (see Appendix G).

5.3.2 DRAWINGS

The drawings furnished shall contain sufficient information so that with the drawings and the manuals specified in 5.3.6, the purchaser can properly install, operate, and maintain the ordered equipment. Drawings shall be clearly legible and shall be identified in accordance with 5.3.1.1. As a minimum, each drawing shall include the details for that drawing listed in Appendix G.

5.3.3 TECHNICAL DATA

Data shall be submitted in accordance with Appendix G and identified in accordance with 5.3.1.1. If any drawing comments or specification revisions necessitate a change to the data sheets, the vendor shall provide revised data which will be used by the purchaser to correct the data sheets for reissue as part of the order specifications.

5.3.4 PROGRESS REPORTS

The vendor shall submit progress reports to the purchaser at the interval specified on the Vendor Drawing and Data Requirements form (see Appendix G).

• 5.3.5 PARTS LISTS AND RECOMMENDED SPARES

5.3.5.1 The vendor shall submit complete parts lists for all equipment and accessories supplied. The lists shall include manufacturer's unique part numbers, materials of construction, and delivery times. Materials shall be identified as specified in 2.9.1.3. Each part shall be completely identified and shown on cross-sectional or assembly-type drawings so that the purchaser may determine the interchangeability of the part with other equipment. Parts that have been modified from standard dimensions and/or finish to satisfy specific performance requirements shall be uniquely identified by part number for interchangeability and future duplication purposes. Standard purchased items shall be identified by the original manufacturer's name and part number.

5.3.5.2 The vendor shall indicate on the above parts lists which parts are recommended spares for startup and which parts are recommended for normal maintenance (see 5.2.3, Item f). The vendor shall forward the lists to the purchaser promptly after receipt of the reviewed drawings and in time to permit order and delivery of the parts before field start-up. The transmittal letter shall be identified with the data specified in 5.1.2.

5.3.6 INSTALLATION, OPERATION, AND MAINTENANCE MANUALS

5.3.6.1 The vendor shall provide sufficient written instructions and a list of all drawings to enable the purchaser to correctly install, operate, and maintain all of the equipment ordered. When specified, this information shall be compiled in a manual with a cover sheet containing all reference-identifying data required in 5.1.2, an index sheet that contains section titles, and a complete list of referenced and enclosed drawings by title and drawing number. When specified, the manual shall be prepared for the specified installation; a typical manual is not acceptable.

5.3.6.2 Any special information required for proper installation design (such as special piping, foundation, and grouting procedures) that is not on the drawings shall be provided separate from the operating and maintenance instructions. This information shall be forwarded at a time mutually agreed upon in the order, but not later than the final issue of prints. This information shall also be included in the Installation, Operation, and Maintenance Manual.

• 5.3.6.3 Manuals shall be forwarded no more than two weeks after all of the specified tests have been successfully completed. When specified, manuals shall include a section that provides special instructions for operation at specified extreme environmental conditions, such as temperatures. As a minimum, the manual contents described in Appendix G shall also be included.

30

API STD*681 96 🔳 0732290 0550648 427 🖿

APPENDIX A—LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEETS

ļ

API	SID*687	96	0732290	0550649	363	
	0.0.00					

		Page1 of
	Job No	Item No
LIQUID RING VACUUM	Purch, Order No.	Date
PUMP AND COMPRESSOR	Inquiry No	Ву
SYSTEM DATA SHEET	Revision	Date

-

1							SPECIFICATION		
2				ED: O BY PI				BY PURCH	ASER OR MFR.
3		to: O Prop	oosal ()		As Built	Servi			
4	For:	. <u>.</u>			Unit:		Site		
5		ns Required:			e, No. Stage	s:	Mode		
6	Manufactur	er:		Vendor:				al No.:	
7			VAC		OR COMPRE	ESSOR DATA	GENERAL		
8	No. Require	ed:		Motor Item No			Turbine Item		
9	Item No.:			Motor Provide	ed by:		Turbine Provi	ded by:	
10	No. Motor D	Driven:		Motor Mounte	ed by:		Turbine Mour	nted by:	
11	No. Turbine			Driver Data S	heet Nos.:		Turbine Data	Sheet Nos.:	
12		SYST	TEM DESC	RIPTION			RING	LIQUID	
13	O Liquid R	ing Vacuum	Pump C) Liquid Ring (Compressor	O Type/Nam	e of Liquid:		
14	LIG	UID RING S	YSTEM (Appendix D)		O Supply Te			· · · · · · · · · · · · · · · · · · ·
15	O Once Th	rough Syste	m			Normal:		Mi	n: (°C)
16		lecirculation				O Supply Pre			(kPa)
17		circulation S				O Vapor Pre			(kPa abs)
18		Continuou		nittent Starts	s/Day:		ravity @ Max. T	emperature:	(
19		tem Volume			(m ³)	O Specific H			(kJ/kg °C)
20		d Evacuation			(min)			cP @	(* C)
21		SITE AND U		ТА	(sity @ Min Tem		(cP)
1	Location:						Erosive Agent:		(01 /
22	O Indoo	or O He	ated	O Under Roo	nf	O Chloride C	v	· · · · · · · · · · · · · · · · · · ·	(ppm)
23	O Outd	-	heated	O Partial Sid		O H ₂ S Conce			(ppm)
24	O Grad	-	zzanine	01 ania 310				ole O Other	(3.5.2.11)
25		Area Classifi		<u> </u>			d Purge System		(0.5.2.11)
26	Class		aroup:	Div:		Circulation		(3.1.6).	(m ³ /hr)
27		ation Reqd.		opicalization R	load	☐ Make-up F			(m ³ /hr)
28						System Vo			(m ³)
29	Steam		/ers		ating		esign Pressure:		(kPa)
30	Conditions	Pless(KFa)	Temp (°C	;) Press(kPa)	Temp (°C)			The results are set	
31 32	Min				<u> </u>		ility in Ring Liq.		mmH₂O&°C
33	Max		. <u> </u>		<u> </u>	0.4	NOISE SPEC	FICATION	
	Electricity		Llasting	Control	Chudulaum		e to Machine:		
34	Electricity	Drivers	Heating	Control	Shutdown				
35 36	Voltage		ļ		<u> </u>	O Applicable	e to Neighborh	1000:	
- 1	Phase				<u> </u>			<u> </u>	
37	Hertz			_ <u>_</u>			ousing: O Yes		
38	O Elevatio		(m); Bai		(kPa abs)			SPECIFICATIO	
39		t Temp. Ran		Min:	(°C)			m Pump and Co	mpressor
40		Humidity (%		· · · · · · · · · · · · · · · · · · ·	lin:		Refinery Servic		
41		onditions - (· · · · · · · · · · · · · · · · · · ·	O Fumes		O Governin	g Specification	(If Different):	
42		osive Due to							
43	¥	ter Temp I		Norm:	(°C)		PAINTING	· ·	
44	Min:	Max	<u> </u>	Max Return:	(°C)		urer's Standard		
45	O Pressur			Design:	(kPa)	and a second sec	ystem Supplier	's Standard:	
46	the second se	Min Return:	ł	Max Allow DP:	(kPa)	O Other:			
47	O Water S	··						AENT (4.4)	
48	Instrument	Air Press I	Max:	Min:	(kPa)	O Domestic			loxing Reqd.
49 🛛						O Outdoor S	Storage More TI	han Six Months (4.4.1)
50									
51								_	

_

32

API S	SID*P87	96 🔳	0732290	0550650	085 🔳
-------	---------	------	---------	---------	-------

Job No.

Revision ____

Page	2	of	
ltem No.			
Date			
Ву			

LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEET

1				OPER/	ATING		DITIO	NS				
2				NOD		D 4 7		OTADT		OTHER	CONDITIONS	
3	(All Data On Per Unit Bas	sis)		NOR		RAT	ED	START		Α	В	
4	O Gas Handled											
5	O m ³ /hr (1.013 bar 8	& 0 °C drv)										
6	O Mass Flow (kg/min) (v											
7	INLET CONDITIONS -											
8	O Pressure (kPa)		·							-		1
9	O Temperature (°C)						-					
10	O Relative Humidity (%)							<u> </u>				
11	O Molecular Weight (%)											
12	Cp/Cv (K ₁) or (Zavg)			· · · ·		·						1
13	\Box Compressibility (Z ₁) c	or (Zave)							<u> </u>			
14	☐ Inlet Volume Flow (m ²)		<i>/</i>)					<u> </u>				
14			0	ł				†				1
15 16	O Pressure (kPa)											1
16 17	O Temperature (°C)							<u> </u>	†``			1
17 18	Cp/Cv (K1) or (Kavg)	·		<u> </u>			<u> </u>					1
18 19	Compressibility (Z1) o	r (Zava)						<u> </u>				1
19 20	KW Required (All Los)									
	KW Required (All Loss		2									
21	Speed (rpm)						<u></u>			1.		
22	O Guarantee Point											
23 24	Performance Curve N	lo.		<u> </u>				1		<u> </u>		
	Gas Characteristics:		O Flar	nmable	[) Othe	r:					,
25 26	Gas Analysis:			<u> </u>		X			Othe	r Cond.		
26 27	O mol % O	MW	NORM	IAL	RA	TED	STA	RTUP A B			Remarks (2.9	9.1.13)
	Air	28.966								†		· · · ·
28 29	Oxygen	32.000					1		• • •	1		
29 30	Nitrogen	28.015								1		
30 31	Water Vapor	18.016										
32	Carbon Monoxide	28.010					<u> </u>					
33	Carbon Dioxide	44.010										
34	Hydrogen Sulfide	34.076										
35	Hydrogen	2.016					1				(2.9.1.6) (2.9	9.1.9)
36	Methane	16.042									· · · · · · · · · · · · · · · · · · ·	· · · · · · · · · · · · · · · · · · ·
37	Ethylene	28.062										
38	Ethane	30.068					1			1		
39	Propylene	42.078					1					
40	Propane	44.094										
41	i - Butane	58.120										
42	n - Butane	58.120					1	-		1		
43	i - Pentane	72.146					<u> </u>				1	
44	n - Pentane	72.146					1					-14*
45	Hexane Plus		<u> </u>						·	1		
46										1		
47	Total						1			1		
48	Avg. Mol Wt.	1								1		
49			··									
4 9 50		<u> </u>					+	···		1	t	
51			ļ				1			-		
52		+								1		

API	ЅТ♪∗⊦₽Ъ	96		0732290	0550651	Tľľ
-----	---------	----	--	---------	---------	-----

LIQUID RING VACUUM
PUMP AND COMPRESSOR
SYSTEM DATA SHEET

Page <u>3</u> of _____ Item No. _____ Date _____ By _____

Job No. _____

Revision _____

1		ONSTRUCTION FEATURES
2	SPEEDS	SHAFT
3	Rotation, Viewed from Driven End	□ Material:
4	☐ Max. Continuous: ☐ Trip: rpm	□ Dia @ Rotor: @ Coupling: (mm)
5	Minimum Stable Speed: rpm	Shaft End: 🛛 Tapered 🛛 Cylindrical
6	Lateral (Damped) Critical Speeds - rpm	SHAFT SLEEVES (2.5.5)
7	First: rpm: mode	At Shaft Seals - Material:
8	O Typical Lateral Analysis Required (2.7.1.7)	BEARING HOUSINGS
9	O Undamped Stiffness Map Required	Cast Iron Ductile Iron Steel
10	O Train Torsional Analysis Reqd (2.7.1.12)	Seals: O Lip Type O Labyrinth (2.8.2.5)
11	First Torsional Critical Speed: rpm	O Vibration Probe Provisions (2.8.2.6)
12	Vibration- Allowable Test Level (mils):	BEARINGS AND LUBRICATION
13	MATERIALS INSPECTION REQUIREMENTS (4.2.2)	Bearings - Type No. Clearance
14	O Charpy Testing (2.9.4)	🗌 Radial
15		Thrust
16		Lubrication:
17	O Liquid Penetrant Required for:	Grease Flood O Ring Oil
18	CASING	Flinger Purge Oil Mist Oil Mist
19	Model: Casing Split:	O Constant Level Oiler O Pressure
20	□ Material (2.9.2.5):	O 1 1/2 NPS Minimum Oil Fill & Drain (2.8.2.4)
21	Thickness: (mm); Corr. Allow.: (mm)	
22	Manifold Material:	O Oil Heater - O Electric O Steam
23	Port Plate/Cone Material: Max. Working Pressure: kPa	
24	□ Max. Working Pressure: kPa □ Max. Design Pressure: kPa	VIBRATION DETECTORS O See Attached API-670 Data Sht
25	□ Test Press. (kPa) - Helium: Hydro:	O Type: O API 670 O Mfr: □ Model:
26		O No. at each Shaft Bearing: ; Total No.:
27	□ Oper. Temp. (*C) - Max: Min: □ Max. Casing Capacity: m ³	O Oscillator - Detectors Supplied by:
28	O Casing Studs Required (2.2.6.2)	O Mfr.: □ Model:
29 30		Monitor Supplied by (3.2.4.6.):
30		O Location: Enclosure:
32		O Mfr: □ Model:
33		□ Scale Range □ Alarm Set @ µm
34	O System Relief Valve Set Pt. (2.2.2): kPa	O Shutdown - ☐ Set @ µmOTime Delay: sec
35	ROTORS	AXIAL POSITION DETECTOR O See Attached API-670 Data Sht
36		O Type: O No. Required:
37	Diameters (mm):	O Mfr: D Model:
38	No. Vanes Per Rotor:	O Oscillator - Demodulator Supplied by:
39	Type: Open Closed Other:	O Manufacturer: D Model:
40	Type Fabrication:	O Monitor Supplied by (3.2.4.6.):
41	Material:	O Location: Enclosure:
42		
43	□ Brinnel Hardness - Max: Min:	🗌 Scale Range 🛛 Alarm Set @ 🛛 🛛 🖉
44		OShutdown - ⊡Set @ µm O Time Delay sec
45		
46		
47		
48		
49		
50		·····
51		
52		

API STD*681 96 🖿 0732290 0550652 958 🖿

Page _____ of _____

Item No.	
----------	--

LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEET

R Revision

Ву _____

Date ____

1													
2	Connection	[□ No.	🗆 Siz	e 🗆	Facing		Rating	Position	Flange Studd	ed or	⊃Ma	ating Ring Gasket
3 4										Threa (2.3)	ded	by	Gasket Vendor 2.3.8.4)
5	System Inlet									(2.3)			2.3.0.4)
6	System Discharge												
7	Machine Inlet												
8	Machine Discharge												
9	Machine Drain												
10	Cooling Water												
11	Ring Liquid Inlet												
12	Vents									••••••			
13													
14	ALLOW. FORCE	S AND	MOME	NTS O	N LIQ.	RING	MACH.			(kgs)			
15			nlet		harge			Liquid Ring	g Machine:	Driv	ver:		
16		Force	Mom't	Force	Mom't	Force	Mom't	Separator:					
17		Ν	N-M	Ν	N-M	N	N-M	Complete					
18	Axial							Max. Main	tenance:				
19	Vertical							Total Ship					
20	Horiz. 90°							S	PACE REQUIR				
21										Length	Width	<u>ا</u>	Height
22			Mom't										
23		N	N-M	N	N-M	N	N-M		achine & Driver				
24	Axial							Separator	Vessel				
25	Vertical												
26	Horiz. 90°								20				
27	O. I. Turner					COUPL	INGS						
28	Coupling - Type:								ached API - 671 [Requirements:	Jata Sheet			
29	Mfr/Model No.: Furnished by:				±1			O Non-Lub		O Other			
30 31	□ Spacer Length:		R	atina (k	W/1000) rpm).		Belt Driv					
32		t Regi				/ ipinj.		Belt Typ					
	Guard Type: OFul				-Open		n-spark						
34	Furnished by:	. <u>,</u>				•			vice Factor (3.5.	1):			
35		alf Cou	uplina						ade 6.3 Sheave I		.4.7)		
36										· · · ·			
37													
38						MC	UNTIN	G PLATES					
39	O Baseplates furni	shed b	oy (3.6.1	.1):					es furnished by:				
40	O Machine and Dr	iver	\bigcirc Co	omplete	e Syste	m		-	Machine 🔿 Driv	er 🔿 Othe	r:		
41	O Drip Rim (3.6.2.	6)	O Mac	hine &	Driver			Thickne				n	nillimeters
42			⊖ For					-	e Plates Require				
43	O Column Mountir								(Chock) Blocks				
44	O Continuously G				eveling				s Steel Shim Thi			n	nillimeters
45	Stainless Steel				4.6.5	mil	limeters		or Epoxy Grout F	Required (3.0	5.1.2.5)		11-7-1-1-
46	O Primer for Epox	y Grou	t Requi	red (3.6	5.1.2.5)			Type:					
47	Type:			0.0									
48	O Machined Mour			.2.9)									
49	0	ng (3.6	5.2.10)					l					
50									· · · · · · · · · · · · · · · · · · ·				
51	······································												
52	1												

Job No. _____

API STD*681 96 🎟 0732290 0550653 894	API	SID*P97	96		0732290	0550653	894	
--------------------------------------	-----	---------	----	--	---------	---------	-----	--

Job No.

Revision ____

Page 5	of
ltem No.	
Date	· · · · · · · · · · · · · · · · · · ·
Ву	

LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEET

1	MECHANIC	AL S	EAL/PA	CKING					
2	Seal Data -		Seal Co	onstruction	•				
3	O Special Data Sheet:	O No Sleeve							
4	API Material Class Code (Table H-4):	O Pumping Ring							
	Manufacturer:		O Cart	ridge Mount					
6	Size and Type:		O Hool	ked Sleeve o	r Non-Cartridge	e			
7	Manufacturer Code:		Slee	ve Material:					
8	Packing Data -		🗌 Glan	d Material:					
9	Manufacturer:		O Auxi	liary Seal De	vice:				
	🖸 Туре:		🖸 Jack	et Required					
11	Size and No. Rings:		Gland 1	aps:					
	Packing Injection Required			F)lush	🖸 (D)rain	🖸 (B)arrie	er		
		Pa)		C)ooling	(V)ent				
14[Lantern Ring:			H)eating	(Q)uench				
15	Max. Sealing Pressure: (k	Pa)	D Fully	Confined G	and Plate Gasl	ket (2.6.11)			
16	SEALI	NG F	LUIDS D	ATA					
17	Seal Fluids-		Quenct	n Fluid -					
18	Note: If flush liquid is pumpage liquid (as in flush piping p	lans	🔿 Nam	e of Fluid:					
19	11 to 41), following flush liquid data is not required.		O Flow	Rate:			(m ³ /hr)		
20	○ Temperature (°C) -		Barrier	Fluid -					
21	Supply: Min: Max:		🔿 Tem	perature (°C)) -				
22	O Specific Gravity: @	•C		Supply:	Min:	Max:			
23	O Name of Fluid:			cific Gravity:		@	°C		
24	O Specific Heat: Kj/k	ς°C	🔿 Nam	e of Fluid:					
25			or Pressure:		a abs @	°C			
26	○ Toxic ○ Flammable ○ Other:		c 🔿 Flamn		er:				
27		Flow Rate (m ³ /hr)- Max: Min:							
28			Required Press. (kPa) - Max: Min:						
29	Required Temp. (°C) - Max: Min:		Required Temp. (°C) - Max: Min:						
30			SH PIPI						
	Plan: O Tubing O Carbon Stee			Tube Fitting					
32	O Pipe O Stainless Ste			Indicator (P					
33	Auxiliary Plan: O Tubing O Carbon Stee	_	O Heat Exchanger (Plan 52/53)						
34	O Pipe O Stainless Ste			sure Switch					
	Piping Assembly: O Threaded O Seal Welded			sure Guage					
36	O Unions O Flanged O Socket Weld	_			cator (Plans 21	, 22, 23, 32, 4	1)		
37			ATER PI						
	Cooling Water Plan:					Flow (m ³ /hr)	Temp (°C)		
	O Galvanized Piping Required O Inlet Valve			cket/Bearing	<u> </u>				
40				at Exchange	er				
41	O Stainless Steel Tubing Req'd O Sight Flow Indicate	ors	Ring Liquid Cooler						
42				ooling Water					
43			TEMS (3						
44				O Ring Liq					
45	O Pressure Control Valve O Check Valve C	Bloc	CK Valve		atic Shut-off Va				
46	O Check Valve O Ejector O Relief Valve:				up Control Valv		-up Piping		
47 ⊿o	O Block Valve Set Press.		kPa		Piping O Drai				
48 40					Ige Type Filter				
49 50	O SS O Other: O SS O Other			U Materi	al: O Steel (er:		
50									
51 52					·····				
321									

API	ZID*F97	96	0732290	0550654	720 🔳

Job No. _

Revision ____

LIQUID RING VACUUM
PUMP AND COMPRESSOR
SYSTEM DATA SHEET

Page _____ of _____ Item No. _____ Date _____

By _

1			SEPARA	TOR (3.1.2)						
2	O Inspection (O Spot Radiograph		CONNECTIONS						
3		O Surface O Ot			No.	Size	Dati	ng/Facing/Ty	20	
4	O ASME Design wit	th Stamp O ASM	E Design w/o Stamp		NO.	0120	Hati	ng/racing/ry		
5	O Other:			Inlet						
6	O Corrosion Allowa			Outlet						
7) Vertical		Vent						
8	O Max. Allowable L		ppm	Drain						
9	O Separator Liquid	drain to	at kPa	Instruments						
10				Relief Valve						
11	SEP	ARATOR MATERIA								
12		Description	ASTM Number	All connections 38	mm an	d larger	shall be	flanged.		
13	O Shell									
14				Diameter (mm):			🗆 Lenç	gth (mm):		
15				□ Thickness - She						
16				Clean Pressure I			Flange)	(kPa):		
17				Gas Vertical Velo						
18	O Internals			Max. Allowable V				kPa @	°C	
19	O Gaskets			Minimum Design			ture:	°C @	kPa	
20				Hydrotest Pressu						
21				Support Method:		egs L] Skirt	Saddles		
22	Remarks:									
23	nemaria.			194 ⁴						
24										
25										
26	1000 - 1000 - 111 - 1									
27										
28 29										
30		······								
31										
32										
33										
34										
35										
36										
37										
38										
39										
40										
41										
42										
43										
44										
45				- Network						
46										
47										
48										
49										
50							A. 6.171			
51										
52										

	АРІ ЅТ⊅∗68Ъ	96 🔳 0	732290	05506	55 G	67 🔜			
							_	-	
							Page	<u>/</u> of	
	QUID RING VACU	IM ·	Job No.				Item No.		
Р	UMP AND COMPRI	ESSOR	Revision				_ Date		
S	YSTEM DATA SHE	ET					Ву		
							<i>by</i>		
	[
2	O Process Control Metho			INSTRUM					
23	O Suction Throttling		to	LD+	Sign				
4	O Speed Variation fr		to to	kPa%	Туре	Electronic, Ra O Pneumatic:	inge	to	mA
5	O Discharge Blowoff		10	/0		O Other:			kPa
6	O Bypass from Disch				Instr	ument Mounting:			
7	C Dypadd Helli Diddi	laige to mot					mote Panel		
8						cally (On Pipe or Equ		l ocal Gar	e Board)
9				NSTRUMEN				<u>-oou</u> aug	je Dourdy
10		Ma	nufacturer		1	Size		Туре	
11	Pressure Gages								
12	Temperature Gages								
13	Level Gages								
14	Diff. Pressure Gages								
15	Pressure Switches								
16	Diff. Pressure Switches								
17	Temperature Switches								
18	Level Switches								
19	Control Valves								
20	Pressure Relief Valves								
21	Thermal Relief Valves								
22	Sight Flow Indicators								
23	Flow Switches								
24	Vibration Equipment								
25	Constant Level Oilers								
26	Solenoid Valves			<u>.</u>					
27	Annunciator				$- \bot$	No. Points:			
28	PRESSURE G			Deserts		TEMPERATUR			
29		Locally Mounted	Local Panel	Remote Panel			Locally	Local	Remote
30 31	1st Stage Inlet				1 of 1	Stage Inlet	Mounted	Panel	Panel
32	2nd Stage Inlet					Stage Inlet			
33	1st Stage Discharge					Stage Discharge			
34	2nd Stage Discharge					Stage Discharge			
35	1st Stage Liq. Ring Inlet					Stage Liq. Ring Inlet			
36	2nd Stage Liq. Ring Inle		00	00	•	Stage Liq. Ring Inlet	00		
37	Other:	00	00	- ŏ 🗖	Oth		<u> </u>	00	
38									
39		ALAR	M & SHUT	DOWN SW	ITCHE	S (3.2.5.1) (TABLE 2)	}		
40		Pre-A	larm	Shutdown			Pre-A	arm S	Shutdown
41	O High Gas Discharge T	Temp ()	0	Он	igh Ring Liquid Level	C)	0
42	O High Liq. Ring Outlet	Temp C)	0		igh Vibration	C		0
43	High Gas Outlet Press)	0	OL	ow Mech. Seal Fluid F			0
44	O Low Ring Liquid Flow			0	OP	anel Purge Failure	C		0
45	O Low Ring Liquid Level)	0			C)	0
46	Remarks:								
47									
48									
49									
50									
51									

- -

- --

			Page	8	_ of	
L		····	Item N	lo		
	UMP AND COMPRESSOR Revision		Date			
S	YSTEM DATA SHEET		By			
1		IENTATION (Con't)				
2	Switch Closures:		<u> </u>			
3					De-Ener	
4	Shutdown Contacts Shall: O Open O Close to Trip an) Energiz	ed () De-Ener	gized
5 6	Note: Normal Condition is when Compressor is in Operation	<u></u>				
7	MISC. INSTRUMENTATION	NODEOT		71110		
8		INSPECTI	UN & TES	-	14.0	
- 1	O Ring Liquid Level Gage	Ohan Inon-stian		Req'd	Witness.	
10		Shop Inspection Cleanliness (4.2.3.2)				0
11		QC Program Review (4.1.7	7)			0
1	O Vibration & Shaft Position Readout Equipment	Hydrostatic)	0		0
	Vibration Readout Location:	Mech. Run-LR Machine				$-\Theta$
14		Contract I Idling		Jin Pres	s. Ratio (2	723
	O Annunciator System		O Max/			
	Q Panel & Annunciator Purge	Contract Shop		0		0
	O Instrument Block Valves (Except Shutdown Instruments)	Probes Probes		ŏ	-0	ŏ
	O Instrument Block Valves for Shutdowns	Vibration Spectrum Plot (4	3332)	ŏ	ŏ	ŏ
	O Liquid Filled Pressure Gages	Vibration Recording (4.3.3		<u> </u>	<u>ŏ</u>	0
	O Alarm Horn & Acknowledgement Switch	Cont. Plots of Speed, Vibra		ŏ	<u> </u>	ŏ
	O Test Lamp Pushbutton	Phase, Angle (4.3.3.5.2)				
22	O Permissive Start with Pilot Light	Seismic Vibration Data (4.3		0	0	0
	O Pilot Light Incoming Circuits	Critical Speed Verification			0	Ŏ
24	O Start-Stop Switches	4 Hr. Mech. Run (4.3.3.5.7	· · · · · · · · · · · · · · · · · · ·	0	Õ	Õ
	O Bearing Metal Temp. Sensors (2.8.2.7)	Mech. Run Spare Rotor	<u> </u>	0	0	0
26	O Radial - Number: O Axial - Number:	Ring Stability Test (4.3.6.4)	0	0	0
27	O Pre-Alarm & Shutdown Switches Shall be Separate	Panel Functional Test		0	0	0
28	O Electrical & Instrument Connections within the Confines	Gas Leak Test Disch. Pres	s. (4.3.4)	0	0	0
29	of the Base Shall be Brought out to Terminal Boxes	O Before O After	Mechani	cal Run		
30	MISCELLANEOUS	Performance Test		0	0	0
31		Contract Liquid Ring Syste		0	0	0
32		Complete Unit Test (4.2.3.	3)		0	0
33		Hardness Tests (4.2.3.3)		0		0
34	O Ring Liquid Level Control Valve	Gear Test (4.3.6.2)		0		0
35		Sound Level Test (4.3.6.3)		0	0	0
36		O Advance Notice Req'd:			(4.3.1.3)	
37	O Dynamic Rotor Balancing (ISO Grade:)	O Inspection Checklist Re				
38	O Special Skid Clearances or Safe Access Areas (2.1.7):		TY CONS	JMPTIO		
39		Cooling Water:				n ³ /hr
40 41		Steam, Normal:				kg/hr
41 42	O Spare Rotor Required (4.4.2.8)	Steam, Max.:				kg/hr
42 43	O Units of Measure (Dwgs., Nameplates, etc.) (2.10.3):	Instrument Air:				m ³ /hr
	C 5 Vr. Botoption of Final Accomply Clearanaes (4.2.1.1.e)	kW (Driver):	··			<w <w< td=""></w<></w
44 45	 5 Yr. Retention of Final Assembly Clearances (4.2.1.1.e) Coordination Meeting Required (5.1.3) 	kW (Auxiliaries):				
45 46	Coordination Meeting Required (5.1.3)	Heaters:				⟨W m ³ /hr
	Pomorko:	Purge (Air or Nitrogen):			r	<u>n°/nr</u>
47 48	Remarks:					
40 49						
4 9 50		······				
50 51						
52		······································				

API STD*681 96 🖿 0732290 0550656 5T3 🖿

 -	_	 	 -	_	_	

API STD*681 96 🎟 0732290 0550657 43T 🖿

Job No.

Revision ____

LIQUID RING VACUUM
PUMP AND COMPRESSOR
SYSTEM DATA SHEET

Page	9	of	
ltem	No		
Date			
Ву			

1				RING LIQUID	COOLER	1				
2	Duty:		Ŵ		Cooler Item Number:					
3	Supplier:				No. Units Required:					
4	Model Number:			· · · · · · · · · · · · · · · · · · ·	Type:					
5				OPERATING		ONS				
6	· · · · · · · · · · · · · · · · · · ·			Sh	ell Side	-			Tube Side	
7	O Fluid									
8	Total Flow (kg/hr)									
9	Specific Gravity				@		'c		@	°C
10		ity (Ki/ka	$x m^2 x C$		@		'c		@	°C
11	Specific Heat (Kj/kg				@		°C		Q	°C
12		<u> </u>			@		°C		@	°C
13		atures (°C	C)	IN	OUT		1	1	OUT	
14	Inlet Pressure (k		/				_			
15	Inlet Velocity (m/									
16				ALLOW	CAL	C	A	LLOW	CALC	
17	Design Temperatur									
18	Pressure (kPa)			MIN	TEST		- N	IIN	TEST	
19	Foul Resistance	(m ² x hr	x °C / kJ)							
20						· · · ·				
21	Number of Passes	<u> </u>								
22				CONSTRUCT	TION DET	AILS				
23	Total Area (1) (Sq.	Meters)	:		Shell	No. x ID		x	mm	
24		ć			Tube	s - No. pe	r Shell:			<u>.</u>
25						.D. x Leng		(mm) x	(mm)
26		an):				auge - BW			(Avg., Min. Wall)	
27						ube Pitch:			mm)∆ O □	
28		e:	· · · · · · · · · · · · · · · · · · ·		Removable Tube Bu				Yes No	
29			SME O	TEMA:	00	ode Stam	p:	[] Yes 🗌 No	
30		Each Bun	dle:	Bundle &	Shell:			Full of	Water:	
31					LE SIZES	S				
32			Sh	ell Side				Τι	ube Side	
33		No.	Size	Rating & Fac	ing	No.	Size		Rating & Facing	
34	Inlet									
35	Outlet									
36	Drain									
37	Vent									
38					ERIALS					
39	Tubes:				Baffles					
40	Tube Sheets:		Chann							
41	Shell:			el Flanges						
42	Shell Flanges:					el Nozzle	Flanges			
43				uding area in tube sl						
44				e stamp shell have l	ongitudina	l weld sea	ms spo	exam	ined per Para. UW-	52 of
45	AS	ME code								
46										_
47										
48										
49										
50								·····		
51										
52										

API STD*681 96 🖿 0732290 0550658 376 🎟

LIQUID RING VACUUM
PUMP AND COMPRESSOR
SYSTEM DATA SHEET

Job. No. _____

Revision _____

Item No.

Page_10_of _____

Date _____

By _____

1	Pump Size and Model:	Brg. Frame:		Service:
2	O No. Pumps Req'd: No. Motors Req'd:		No. T	urbines Req'd: Item No.:
3		NS - EACH PUMP		PERFORMANCE
4	Liquid/Slurry:			Performance Curve No.:
	PT °C Norm: Max: m ³ /h at Norm:	Rated:		RPM: NPSH (water):
6	Sp. Gr. at Norm PT: Total Head, m	Rated:		Eff.: % BkW Rated:
7	Vap. Press. at Norm. PT (kPa abs): Suct. P	ress. (kPa) Max: Rated:		Max. kW Rated Impeller:
8	Vis. at Norm. PT Pa s: NPSHA, m	:		Max. Head Rated:
9	Corr./Eros. caused by: Ph:	Hyd. kW:		Max. Discharge Pressure (kPa):
10	Driver kw to be selected for Max. S.G.:	& Max. Viscosity:		Min. Continuous m ³ /h:
11				SHOP TESTS
12				O Nonwit. Perf. O Wit. Perf.
13	CONSTRUCTION: O ASME B73.1M	O ASME B73.2M		O Nonwit. Hydro. O Wit. Hydro.
14	O OTHER:			O Nonwit. NPSH O Wit. NPSH
15	Pump Type: O Horiz. O Vert. In-Line	O Coupled Motor Shaft		O Nonwit. Vibration O Wit. Vibr.
16	O Cradled Mnt.			O Dismantle & Inspect After Test
17	Case Horizontal Mount:	Centerline		O Other:
18	Vert. Mount: 🔲 Motor Shaft 📋 Rigid C	oupling 🔲 Other:		
19	Split: 🔲 Radial 🛛 Axial Type Volut	e: 🗌 Single 🔄 Double		PUMP MATERIALS
20	Press: 🔲 Max. Allow. (kPa)	(°C) Hydro Test (kPa)		Casing:
21	Connect: O Drain O Gauge Suc	ction () Gauge Discharge		Impeller:
22	Impeller Dia. Rated: Max.:	impeller Type:		Wear Rings:
23	Bearings Type: Radial: Three	ust:		Shaft/Sleeve:
24	Lube: Oil Oil Mist Gre	ase 🔲 Grease for Life		Gland:
25	Coupling: Mfr.: Model: Gua	ard: Oiler:		Gaskets:
26	Driver Half Mtd. By: O Pump Mfr.	O Driver Mfr. O Purchas	er	Baseplate:
27	Stuffing Box Cover: 🔲 Standard 🔲	Jacketed 🔲 Seal Only		Coupling Guard:
28	O Packing: D Mfr. & Type:	Size/No. of Rings:		Other:
29	Lantern Rings: 🔲 Yes 📋 No			
30	O Mech. Seal: Mfr. & Model	Material Code:		INSPECTION: O Not Required
31	Balanced Dubalanced	🗌 Single 🔄 Inside		O In Process O Final
32	Double Back to Back	Tandem 🗌 Outside		Days Notification Required:
33	Cartridge Face to Face			SOUND SPECIFICATION
34	AUXILIARY PIPING (see Figs	s. A2 and A3 for Code)		REQUIREMENTS
35	Stuf. Box Plan No.:	/. Piping Plan No.:		
36	Total Cooling Water Req'd., m ³ /h:	O Sight F.I. Req'd.		
37	Packing Cooling Injection Req'd., Total m ³			
38		(kPa)		
39				ADDITIONAL REQUIREMENTS/
		er, provided by:		COMMENTS
		Volts/Phase/Hertz:		
	Mfr.: Bearings: Service Fa			
	Type: Insulation: Amps:			
	Lube: Temp. Rise (°C): End			L
	Inlet Press.: Exhaust Press	s.: Steam Temp.:		Water Rate:
	Other:	Customer/User:		
47				
48		· · · · · · · · · · · · · · · · · · ·		
49	1 +			
50		Items No(s).:		Equip. No(s).:
51		Factory Order No(s).:		Pump Serial No(s).:
	the American Society of Mechanical	Issued By:		Date:
53	Engineers, ASME B73.2M–1991	Rev.:		Date:

API STD*681 96 📟 0732290 0550659 202 📟

LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEET

Job. No. _____

Revision _____

Page <u>11</u> of	
Item No.	
Date	
By	

1		MOTOR DESIGN DATA (CONTINUED)
2	APPLICABLE SPECIFICATIONS:	VIBRATION:
3	O NEMA	O NEMA Standard O
4	0	NOISE:
5	0	O NEMA Standard O
6	SITE DATA:	
7	Area: O Class Gr. Div. O Non-Hazardous	
8	O Alt. (m) O Ambient Temp: Max. (°C) Min. (°C)	ACCESSORY EQUIPMENT
9	Unusual Conditions: O Dust O Fumes	O Baseplate O Soleplate O Stator Shift
10		O Mfr. Std Fans O Non-sparking Fans
11	DRIVE SYSTEM: O Direct Connected	O D.C. EXCITATION
12) Gear	kW Req'd.: Volts:
13		By: O Purchaser O Manufacturer
14	TYPE OF MOTOR:	Description:
15	O Squirrel Cage Induction O NEMA Design	O ENCLOSED COLLECTOR RINGS:
16		O Purged: Medium Press. (kPa)
17	O Power Factor Req'd.:	O Explosion-Resistant Non-purged
18		O Forced Ventilation
19		\square m ³ /h Press. Drop (mm) H ₂ O
20	O Wound Rotor Induction	O BEARING TEMP. DEVICES:
21	0	Location:
22	ENCLOSURE:	Description:
23	O Class Group Div.	Set @ (°C) for Alarm (°C) for Shutdown
24	O TEFC, Severe Duty O Exp. Proof	O SPACE HEATERS:
25	O Weather Protected, Type:	☐ kW
26		O Volts Phase Hertz
27	O Double Wall Carbon Steel Tubes	O Max. Sheath Temp.: (°C)
28	O Water Supply: Press.: (kPa) Temp.: (°C)	WINDING TEMPERATURE DETECTOR:
29		O Thermistors: No/Phase:
30	O Water Side Min. Corr. Allow. (mm)	Type: O Pos. Temp. Coeff.
31	and Foul Factor:	O Neg. Temp. Coeff.
32		Temperature Switch: O Yes O No
33		O Resistance Temp. Detectors: No/Phase
34		O Resistance Material
35		O Ohms
36		Selector Switch & Indicator by:
37		O Purchaser
	BASIC DATA:	O Manufacturer
39		Max. Stator Winding Temperatures:
40		(°C) for Alarm (°C) for Shutdown
41		WINDING TEMP. DETECTOR & SPACE HEATER LEADS:
42		O In Same Conduit Box
43		O In Separate Conduit Boxes
	STARTING: O Full Voltage O Reduced Voltage %	PROTECTION:
45	<u> </u>	O Self-Balance Primary-Current Method
46		O C.T. Description:
47 48		O Extended Leads Length (m)
48 49		
49 50		
50		

Job. No. _____

-			
Re	/1S	inn	
1.0			-

Page <u>12</u> of	
Item No.	
Date	
Ву	

1		MANUFACTURER'S DATA (CONTINUED)
	O SURGE CAPACITORS:	Limit End Float to:
3	O LIGHTNING ARRESTERS	Curves Req'd Based on Mtr. Saturation & Rated Volt:
4	O C.T. FOR AMMETER	O Speed vs Torque @ 100%, 90% & 80% rated Voltage:
5	O Description:	O Speed vs. Current @ 100%, 90% & 80% rated Voltage:
6	MAIN CONDUIT BOX SIZED FOR:	
7	O Main Motor Leads O Type	WEIGHT (kg) [.]
8	O Insulated O Non-Insulated	Net Weight: Shipping Weight:
9	O C.T.'s for Diff. Protection (mounted by)	Rotor Weight: Max. Erection Wt.:
10	O Surge Capacitors (mounted by):	Max. Maint. Wt. (Identify):
11	O Lightning Arresters (mounted by):	DIMENSIONS (m):
12	O C.T. for Ammeter (mounted by):	L: W: H:
13	O Space for Stress Cones:	
14	O AIR FILTERS.	
15	Mfr.: Type:	
16		SHOP INSPECTION AND TESTS
17	MANUFACTURER'S DATA	Reg'd. <u>Witness</u>
18	Manufacturer:	Shop Inspection: O O
19	Frame No.: Full Load RPM (Ind.):	Testing per NEMA: O O
20	Efficiency: F L. 3/4L 1/2L	Mfr. Std. Shop Tests: O O
21	Pwr. Factor (Ind.) F.L. 3/4F 1/2L	Immersion Test: O O
22	Curr. (Rated Volt.): Full Load Locked Rotor:	Special Tests (list below): O O
23	Locked Rotor Power Factor:	0 0
24	Locked Rotor w/Stand Time (cold start):	0 0
25	Locked Rotor w/Stand Time (hot start).	0 0
26	Torques (FtLb.). Full Load:	0 0
27	Locked Rotor: Starting (Syn):	
28	Pull-Up (Ind.): Pull-In (Syn.):	PAINTING:
29	Breakdown (Ind.). Pull-Out (Syn.):	O Manufacturer's Standard
30		0
31	Open Circuit Time Constant (Sec.):	0
32	Symmetrical Contribution to 3 Phase Terminal Fault:	
33	at 1/2 Cycle. at 3 Cycles:	SHIPMENT:
34	Reactances: Sub-Transient (X"D)	O Domestic O Export O Export Boxing Req'd.
35		O Outdoor Storage Over 3 Months
	A.C. Stator Resistance. Ohms @ (°C)	0
	Rated kVA:	0
	kVA Inrush @ Full Volt. & Locked Rotor (Syn.): %	
	kVA @ Full Voltage & 95% Speed %	REMARKS:
40	Max. Line Curr in Stator on 1st Slip Cyc & Pull-Out (Syn.):	
41		
	Acceleration Time (Mtr. only & Rated Volt.): Sec.	
	Accel. Time (Mtr. & Load & 85% Rated Volt.). Sec.	
	Rotor/Field Wk ² & Mtr. Shaft (kg-m ²)	
	No of Starts per Hour:	
	Bearing. Type Lubr	
	Lube Oil Required m ³ /h & (kPa)	
48	3 Total Shaft End Float.	
49		
50	D	

COPYRIGHT 2002; American Petroleum Institute

.

API STD*681 96 🔳 0732290 0550661 960 🔳

		Page <u>1</u> of
	Job No	Item No
LIQUID RING VACUUM	Purch. Order No.	Date
PUMP AND COMPRESSOR	Inquiry No	Ву
SYSTEM DATA SHEET	Revision	

1 2 3 4 5 6 7	INFORMAT Applicable For:	ION TO BE (OMPLET	ED: OBY PL	JRCHASER		SPECIFICATION		ASER OR MFR.
3 4 5 6	Applicable For:						IUFACTURER	L BY PURCH	ASER OR MFR.
4 5 6	For:	io: O Prop		INFORMATION TO BE COMPLETED: O BY PURCHASEF					
5 6) As Built	Service:			
6					Unit:		Site		
	No. System				e, No. Stage	s:	Mode		
7	Manufactur	er:		Vendor:				al No.:	
-						SSOR DATA			
8	No. Require	ed:		Motor Item No		Turbine Item No.:			
9	Item No.:		Motor Provided by:				Turbine Provi		
10	No. Motor Driven: Motor Mounted by: No. Turbine Driven: Driver Data Sheet Nos.;					Turbine Mour			
11				· · · · · · · · · · · · · · · · · · ·	Turbine Data				
12								LIQUID	
13		ng Vacuum) Liquid Ring C	ompressor		ne of Liquid:		
14				Appendix D)			emperature-		
15		rough Syste				Norma		M	in: (°F)
16		ecirculation				O Supply P			(psig)
17	O Total Re	circulation S	ystem	without Ot- t	(Dav <i>i</i>)	O Vapor Pr			(psig)
18	Service: O Continuous O Intermittent Starts/Day:					Gravity @ Max. T	emperature:	(DA	
19	O Inlet System Volume: (ft ³) O Required Evacuation Time: (min)				O Specific I		cP @	(Btu/Lb °F)	
20				T A	(min)	· · · · ·			(° F)
21	Location:	SITE AND UT	ILITY DA				osity @ Min Tem	iperature:	(cP)
22	O Indoo	or O He	atod				e/Erosive Agent:		(222)
23	O Indoc O Outd	-	heated	O Under Roc O Partial Sid			Concentration:		(ppm)
24	O Grad		zzanine	O Partial Sid	es	O H ₂ S Concentration: (ppm) O Toxic O Flammable O Other (3.5.2.11)			
25		Area Classifi		0			id Purge System		(3.5.2.11)
26	Class		aroup:	Div:				1 (3.1.6).	(gpm)
27		ation Reqd.		opicalization R	and	☐ Make-up Rate: (gpm)			
28	Steam	Driv			ating	System V			(gpin) (gal)
29 30	Conditions		Temp (°F		Temp (°F)		Design Pressure:		(gai)
30	Min	r ress(psig)		/ riess(psig)			bility in Ring Liq.		"H ₂ O & °F
32	Max				<u> </u>		NOISE SPEC		1120 0 1
33	- Max						ble to Machine:		
34	Electricity	Drivers	Heating	Control	Shutdown				
35	Voltage						ble to Neighbort	nood:	
36	Phase								
37	Hertz					Acoustic H	lousing: O Yes	O No	
38	O Elevatio	n:	(ft); Ba	rometer:	(psia)			SPECIFICATIO	ONS
39		t Temp. Ran		Min:	(•F)		quid Ring Vacuu		
40		Humidity (%					r Refinery Servic		
41	Unusual Co		O Dust	O Fumes		O Governing Specification (If Different):			
42						<u> </u>	,,		
43		ter Temp		Norm:	(*F)	PAINTING (4.4.2)			
44	Min:	Max		Max Return:	(°F)	O Manufad	cturer's Standard		<u></u>
45		e- Normal:		Design:	(psig)	O Unified,	System Supplier	's Standard:	
46		Min Return:		Max Allow DP		O Other:	<u></u>		18 Harris
47	O Water S						SHIP	MENT (4.4)	
48	Instrument	Air Press (Max:	Min:	(psig)	O Domest			Boxing Reqd.
49							Storage More T		
50									
51									

Job No.

Revision ____

.____

Page	2	_ of _	
item No.	<u></u>		
Date			
Ву			

LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEET

1				OPE	RATING	G CONI		NS				
2				NO				START UP		OTHER CONDITIONS		
3	(All Data On Per Unit Ba	sis)		NORMAL		RAT	ED	STAR	ן ייט י	Α	В	
4	O Gas Handled											
5	O SCFM (14.7 psia &	8 60 °F dry)										
6	O Mass Flow (Lb/min) (-			
7	INLET CONDITIONS -	.				•••						
8	O Pressure (psia)											
9	O Temperature (°F)				·							
10	O Relative Humidity (%)	}					-					
11	O Molecular Weight (%)											
12	Cp/Cv (K1) or (Zavg)											
13	Compressibility (Z1) o	or (Zavg)								······		
14	Inlet Volume Flow (cfr											
15	DISCHARGE CONDITIC											
16	O Pressure (psia)											
17	O Temperature (°F)											
18	Cp/Cv (K1) or (Kavg)			Ľ								
19	Compressibility (Z1) o	r (Zavg)										
20	BHP Required (All Lo	sses Include	ed)									
21	BHP Required at RV											
22	Speed (rpm)											
23	O Guarantee Point											
24	Performance Curve N	lo.										
25	Gas Characteristics:	OToxic	O Flar	nmabl	<u>e (</u>) Othe	r:					
26	Gas Analysis:	мw	NORM	101	RA	TED			Othe	r Cond.	Remarks (2.9	1 12)
27	Omol% O						STA	RT UP	Α	В		. 1. 13)
28	Air	28.966										
29	Oxygen	32.000										
30	Nitrogen	28.015										
31	Water Vapor	18.016										
32	Carbon Monoxide	28.010										
33	Carbon Dioxide	44.010										
34	Hydrogen Sulfide	34.076								_		
35 26	Hydrogen	2.016								+	(2.9.1.6) (2.9.	1.9)
36	Methane	16.042	ļ								***	
37 38	Ethylene	28.062								+		
30 39	Ethane	30.068				• •						····
39 40	Propylene	42.078										
40 41	Propane	44.094					 					
42	i - Butane	58.120		-						+		
42	n - Butane i - Pentane	58.120					-			+		
43		72.146										
44 45	n - Pentane Hexane Plus	12.140					 			+		
45 46	FIEXALLE FIUS		1				+					191891 - 1
40	Total	1										
48	Avg. Mol Wt.						+					
49							+			-		
49 50		1			<u> </u>		+					
51												
52							+					
52		1	L		1		<u> </u>			1		

API	SID*P87	96		0732290	0550663	733 🛛
-----	---------	----	--	---------	---------	-------

Revision _____

Job No. _____

Page _____ of _____ Item No. _____ Date _____ Ву _____

4		
1	LIQUID RING MACHINE C	CONSTRUCTION FEATURES
2	SPEEDS	SHAFT
3	Rotation, Viewed from Driven End	Material:
4	□ Max. Continuous: □ Trip: rpm	Dia @ Rotor: @ Coupling: (in.)
5	Minimum Stable Speed: rpm	Shaft End: Tapered Cylindrical
6	Lateral (Damped) Critical Speeds - rpm	SHAFT SLEEVES (2.5.5)
7	First: rpm: mode	At Shaft Seals - Material:
8	O Typical Lateral Analysis Required (2.7.1.7)	BEARING HOUSINGS
9	O Undamped Stiffness Map Required	Cast Iron Ductile Iron Steel
10		Seals: O Lip Type O Labyrinth (2.8.2.5)
11	First Torsional Critical Speed: rpm	O Vibration Probe Provisions (2.8.2.6)
12		BEARINGS AND LUBRICATION
13		Bearings - Type No. Clearance
	O Charpy Testing (2.9.4)	
	O Radiography Required for:	
	O Magnetic Particle Required for:	Lubrication:
17		Grease Flood O Ring Oil
18	CASING	□ Flinger □ Purge Oil Mist ○ Oil Mist
19		O Constant Level Oiler O Pressure
20		O 1/2 NPS Minimum Oil Fill & Drain (2.8.2.4)
21	□ Thickness: (in.); Corr. Allow.: (in.)	O Oil Viscosity ISO Grade:
22	□ Manifold Material:	O Oil Heater - O Electric O Steam
22	Port Plate/Cone Material:	O Oil Pressure to be Greater than Coolant Pressure
23 24		VIBRATION DETECTORS O September 2010
24 25	□ Max. Design Pressure: psig	O Type: O API 670 Data Sht
		O Mfr: O Model:
26 27	Oper. Temp. (°F) - Max: Min:	O No. at each Shaft Bearing: ; Total No.:
28		O Oscillator - Detectors Supplied by:
29		
	O Casing Disassembly Jackscrews (2.2.7)	Monitor Supplied by (3.2.4.6.):
	O Spot Faced Mounting Holes (2.2.8)	O Location: Enclosure:
	O Casing Vertical Jackscrews and Dowel Pilot Holes (2.2.9)	
	□ Radiography Quality	☐ Scale Range ☐ Alarm Set @ mils
34		
35		O Shutdown - ☐ Set @ milsO Time Delay: sec AXIAL POSITION DETECTOR O See Attached API-670 Data Sht
		O Type: O No. Required:
	Diameters (in.):	O No. Required. O Mfr: □ Model:
	□ No. Vanes Per Rotor:	O Oscillator - Demodulator Supplied by:
	Type: Open Closed Other:	O Manufacturer: ☐ Model:
	Type Fabrication:	O Monitor Supplied by (3.2.4.6.):
41	□ Material:	O Location: Enclosure:
42	☐ Max. Yield Strength: psi	O Mfr: Dodel:
43		☐ Scale Range ☐ Alarm Set @ mils
44		
45		OShutdown - Set @ mils O Time Delay sec
46		
47		
48		
49		-
50		
51		
52		

API STD*681 96 📰 0732290 0550664 677 📰

Page _____ of _____ Item No. _____

LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEET

Revision _____ Date _____

Ву _____

1													
2	Connection	Г	No.	📋 Siz		Facing		Rating	Position	Flange Studd	ed	⊖ Ma	ating Ring
3			-			3		Ĵ		Threa	ea or ded	& by	Gašket Vendor
4 5	System Inlet									(2.3)		(2	2.3.8.4)
6	System Discharge												
7	Machine Inlet												
8	Machine Discharge												
9	Machine Drain												
10	Cooling Water			• • • • • • • • •									
11													
12	Vents												
13													
14						MACH.			(Lbs)				
15		In	let	Disc	harge			Liquid Ring	Machine:	Driv	ver:		
16		Force	Mom't	Force	Mom't	Force	Mom't	Separator:					
17		Lb	Ft-Lb	Lb	Ft-Lb	Lb	Ft-Lb	Complete I	Unit:				
18	Axial							Max. Maint	enance:				
19	Vertical							Total Ship	oing:				
20	Horiz. 90°							□ S	PACE REQUIRE				
21										Length	Widt	h	Height
22			Mom't					Complete L					
23	Autol	Lb	Ft-Lb	Lb	Ft-Lb	Lb	Ft-Lb		lachine & Driver				
24	Axial							Separator	Vessel				
25	Vertical Horiz, 90 °												
26	Horiz. 90°				1		INICO		De				
27	Coupling Trees					LOUPL	INGS /	AND GUAR					
28	Coupling - Type:							See Attached API - 671 Data Sheet Lubricating Requirements:					
29	Mfr/Model No.: Furnished by:							Non-Lube Grease Other					
30	□ Spacer Length:		R	atina (H	lp/100 ı			Belt Drive					
	Limited End Floa	t Reau				<u>F)</u> .		Belt Type/No.:					
	Guard Type: O Ful				-Open	O No	n-spark						
34							1	Belt Service Factor (3.5.1):					
	O Vendor Mount H	alf Cou	pling					O ISO Grade 6.3 Sheave Balance (3.5.4.7)					
36										· · ·			
37			· · · ·										
38 MOUNTING PLATES													
39	9 O Baseplates furnished by (3.6.1.1):							es furnished by:					
40	Machine and Driver O Complete System							Machine 🔿 Driv	er 🔿 Othe	r:			
41						Thickne					inches		
42							e Plates Require						
43	9,,9						(Chock) Blocks	<u> </u>		-,			
44	, , , , , , , , , , , , , , , , , , ,						s Steel Shim Thi				inches		
45						or Epoxy Grout F	Required (3.0	6.1.2.5)				
46 47		y Grou	i Hequi	red (3.6	p. 1.2.5)			Type:					
	Type:	ting D	ada (2.0	2.0									
48 49	•		<u> </u>	o.2.9)									
49 50		ng (3.6	o.2.10)										
51													
52													
52	1												

Job No. _____

	API	ZID*P97	96 📖	0732290	0550665	506 🔳	
--	-----	---------	------	---------	---------	-------	--

Job No. _

Page 5	of
Item No.	
Date	
Ву	

LIQUID RING VACUUM
PUMP AND COMPRESSOR
SYSTEM DATA SHEET

MECHANICAL	SEAL/PA	CKING					
Seal Data -	Seal Co	onstruction -	•				
O Special Data Sheet:	O No Sleeve						
API Material Class Code (Table H-4):	O Pum	O Pumping Ring					
Manufacturer:	O Cart	ridge Mount					
Size and Type:	O Hoo	ked Sleeve o	r Non-Cartridge				
Manufacturer Code:		ve Material:					
Packing Data -	Glar	nd Material:					
Manufacturer:	O Aux	O Auxiliary Seal Device:					
🖸 Туре:	🖸 Jaci	ket Required					
Size and No. Rings:	Gland T	Gland Taps:					
Packing Injection Required		F)lush	D (D)rain	🖸 (B)arrie	er		
Flow: (gpm) @ (psig		C)ooling	(V)ent				
Lantern Ring:		H)eating	(Q)uench				
Max. Sealing Pressure: (psig) 🖸 Fully	Confined Gl	and Plate Gask	et (2.6.11)			
SEALING	FLUIDS D	ΑΤΑ					
Seal Fluids-		h Fluid -					
Note: If flush liquid is pumpage liquid (as in flush piping plan	s 🔿 Nam	ne of Fluid:					
11 to 41), following flush liquid data is not required.	O Flow	/ Rate:			(gpm)		
O Temperature (°F) -	Barrier	Fluid -					
Supply: Min: Max:	⊖ Terr	perature (°F)	-				
O Specific Gravity: @ *F	:	Supply:	Min:	Max:			
O Name of Fluid:		cific Gravity:		Q	°F		
O Specific Heat: Btu/Lb*		ne of Fluid:					
O Vapor Pressure: (psia) @ *F		or Pressure:		a @	•F		
O Toxic O Flammable O Other:	O Tox	c 🔿 Flamm	nable O Othe	r:			
Flow Rate (gpm) - Max: Min:	🗌 Flow	Flow Rate (gpm) - Max: Min:					
Required Press. (psig) - Max: Min:	Required Press. (psig) - Max: Min:						
Required Temp. (°F) - Max: Min:	Required Temp. (°F) - Max: Min:						
	USH PIPI						
Plan: O Tubing O Carbon Steel		e Tube Fitting					
O Pipe O Stainless Steel		Indicator (Pl					
Auxiliary Plan: O Tubing O Carbon Steel		t Exchanger (
O Pipe O Stainless Steel		sure Switch	· · · · · · · · · · · · · · · · · · ·				
Piping Assembly: O Threaded O Seal Welded	-	O Pressure Guage (Plan 52/53)					
O Unions O Flanged O Socket Welded		-	cator (Plans 21	, 22, 23, 32, 4	1)		
COOLING							
O Cooling Water Plan:				Flow (gpm)	Temp (°F)		
O Galvanized Piping Required O Inlet Valve		cket/Bearing					
O Copper Tubing Required O Outlet Valve		eat Exchange	r		· · · · · · · · · · · · · · · · · · ·		
○ Stainless Steel Tubing Req'd ○ Sight Flow Indicators		quid Cooler					
· · · · · · · · · · · · · · · · · · ·		ooling Water					
PIPING SY	· · ·						
O Vapor Inlet Piping (3.7.1.14) O LRVP Discharge Pip		O Ring Liq					
O Pressure Control Valve O Check Valve O B	ock Valve		atic Shut-off Va				
O Check Valve O Ejector O Relief Valve:			up Control Valv		-up Piping		
O Block Valve Set Press.	psig		Piping O Drair				
O Material: O Steel O Material: O Steel			lge Type Filter				
O SS O Other: O SS O Other:		O Materi	al: O Steel () SS () Oth	er:		

API SI	Ր♪*681	96		0732290	0550666	442	
--------	--------	----	--	---------	---------	-----	--

Page <u>6</u>	of
Item No	
Date	······································

Job No. _ Revision ____

By

1			SEPARA	TOR (3.1.2)					
2		O Spot Radiography			CONN	IECTION	NS		
3		O Surface O Oth			No.	Size	Batin	g/Facing/Ty	pe
4	O ASME Design wit	h Stamp O ASMI	E Design w/o Stamp			0.20		igr doing i y	
5	O Other:	('		Inlet					
6	O Corrosion Allowa			Outlet					
7		Vertical		Vent					
8	O Max. Allowable L		ppm	Drain Instruments					
9 10	O Separator Liquid	drain to	at psig	Relief Valve					
11	eed	ARATOR MATERIA		Heller valve					
12	367	Description	ASTM Number	All connections 1-1	1/0" and	lorgor o		mand	
13	O Shell	Description	ASTIVI NUMBER	All connections 1-	1/2 and	larger s	inali de lla	angea.	
14	O Heads			Diameter (in.):			Leng	th (in):	
15	O Demister			☐ Thickness - She	l / Hea	d (in.):			
16	O Nozzles			Clean Pressure			Flange)	(psi):	
17	O Flanges			Gas Vertical Vel			3-1		
18	O Internals			Max. Allowable V			re:	psig @	°F
19	O Gaskets			🔲 Minimum Design	Metal	Tempera	ture:	F @	psig
20				Hydrotest Pressu	ure (psig	g):			
21				Support Method:		egs [∃ Skirt	Saddles	;
22									
23	Remarks:					_			
24									
25									
26									
27		· · · · · · · · · · · · · · · · · · ·							
28			·····						
29									
30 31									
32									
33									
34					• •			· · · · · · · · · · · · · · · · · · ·	
35									
36									
37									
38									
39									
40									
41									
42									
43									
44									
45 46			an and the second s						
47									
48									
49					·				
50							·····		
51									
52									
			-						

							Page7	7 of	
		ı .(ob No.						
	QUID RING VACUUM								
P	UMP AND COMPRES	SOR H	evision .	. <u></u>			_ Date		<u></u>
S	YSTEM DATA SHEET	-					Ву		
1				INSTRUME	ENTA	TION			
2	O Process Control Method:			· · · · · · · · · · · · · · · · · · ·	Sig	nal- Source:			
3	O Suction Throttling from	n	to	psia	Тур		ange te	0	mA
4	 O Speed Variation from O Discharge Blowoff to 		to	%		O Pneumatic:			psig
6	O Bypass from Discharg	e to inlet			inet	Other: rument Mounting:			
7	O Dypuss nom Discharg						mote Panel		
8						ocally (On Pipe or Equ		ocal Gag	e Board)
9				NSTRUMEN	IT SU	PPLIERS			
10		Mar	ufacturer			Size		Туре	
11			"	·····				<u> </u>	
	Temperature Gages Level Gages		·····						
	Diff. Pressure Gages								
15	Pressure Switches	· · · · · · · · · · · · · · · · · · ·							
16	Diff. Pressure Switches			······································			······································		
17	Temperature Switches								
18	Level Switches		_						
	Control Valves								
20	Pressure Relief Valves Thermal Relief Valves								
21	Sight Flow Indicators								
22 23	Flow Switches								
24	Vibration Equipment								
25	Constant Level Oilers								
26	Solenoid Valves								
27	Annunciator				ı —	No. Points:			
28	PRESSURE GAG		• • • • • • • • • • • • • • • • • • • •	Remote		TEMPERATUR			Remote
29 30		Locally Mounted	Local Panel	Panel	┝		Locally Mounted	Local Panel	
31	1st Stage Inlet	00	00	00	1s	t Stage Inlet	00	00	00
32	2nd Stage Inlet	00	00	00	2r	d Stage Inlet	00	00	00
33	1st Stage Discharge	00	00	00		t Stage Discharge	00	00	0
34	2nd Stage Discharge	<u><u><u>o</u></u></u>		<u>_0</u>		d Stage Discharge	<u> 0 </u>		
35 36	1st Stage Liq. Ring Inlet 2nd Stage Lig. Ring Inlet					t Stage Liq. Ring Inlet Id Stage Liq. Ring Inlet			
37	Other:				+	her:			
38									
39		ALAR	A & SHU	TDOWN SW	птсн	ES (3.2.5.1) (TABLE 2	2)		
40		Pre-A		Shutdown			Pre-Al	arm	Shutdown
41	O High Gas Discharge Ten			0		High Ring Liquid Leve			0
42	O High Liq. Ring Outlet Ter					High Vibration	0		0
43 44	<u> </u>	<u> </u>			- <u> </u>	Low Mech. Seal Fluid Panel Purge Failure			<u> </u>
45	O Low Ring Liquid Level				0	raner urgeranure	0		0
46			<u> </u>				0		
47	·····								
48									
49							····		
50	· · · · · · · · · · · · · · · · · · ·								
51 52						······································			

COPYRIGHT 2002; American Petroleum Institute

API	ЅТД∗⊦₽Ъ	96 🔳	0732290	0550668	215	

Page ____8 ___ of _____

Date _____

LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEET

Revision _____

Job No. _____

Ву _____

1	INSTRUM	ENTATION (Con't)				
2	Switch Closures:	·				
3		Alarm and be Normally:	O Energize	d (De-Ener	gized
4	Shutdown Contacts Shall: O Open O Close to Trip ar		O Energize		De-Ener	
5	Note: Normal Condition is when Compressor is in Operation					
6						
7	MISC. INSTRUMENTATION	INSPECT	ION & TEST	ING		
8	O Ring Liquid Sight Flow Indicator			Req'd	Witness.	Obs.
9	O Ring Liquid Level Gage	Shop Inspection		0	0	0
10	O Vibration & Shaft Position Probes &	Cleanliness (4.2.3.2)		Ŏ	0	ŏ
11	Oscillator-Demodulators	QC Program Review (4.1.	7)	Õ	0	0
12	O Vibration & Shaft Position Readout Equipment	Hydrostatic		Õ	Õ	Ŏ
13	Vibration Readout Location:	Mech. Run-LR Machine		0	0	0
14	Local Panel Separate Panel Control Room	Contract Ildling	⊖Max/M	in Pre	ss. Ratio (2	.7.2.3)
15	O Annunciator System	Coupling Adaptor(s) () Max/M	in Cap	acity (2.7.2	2.3)
	O Panel & Annunciator Purge	Contract Shop		0	0	0
	O Instrument Block Valves (Except Shutdown Instruments)	Probes Probes		0	0	0
18	O Instrument Block Valves for Shutdowns	Vibration Spectrum Plot (4	4.3.3.3.2)	Ö	0	0
19	O Liquid Filled Pressure Gages	Vibration Recording (4.3.3		0	0	0
	O Alarm Horn & Acknowledgement Switch	Cont. Plots of Speed, Vib		0	0	0
21	O Test Lamp Pushbutton	Phase, Angle (4.3.3.5.2				
22	O Permissive Start with Pilot Light	Seismic Vibration Data (4		0	0	0
23	O Pilot Light Incoming Circuits	Critical Speed Verification		0	0	0
- 1	O Start-Stop Switches	4 Hr. Mech. Run (4.3.3.5.	7)	0	0	0
25	O Bearing Metal Temp. Sensors (2.8.2.7)	Mech. Run Spare Rotor		0	0	0
26	O Radial - Number: O Axial - Number:	Ring Stability Test (4.3.6.4	4)	0	0	0
27	O Pre-Alarm & Shutdown Switches Shall be Separate	Panel Functional Test		0	0	0
28	O Electrical & Instrument Connections within the Confines	Gas Leak Test Disch. Pre		0	0	_0
29	of the Base Shall be Brought out to Terminal Boxes	O Before O After	Mechanic	~		
30	MISCELLANEOUS	Performance Test		0	<u> </u>	0
31	O Anti-Fungal Protection & Corrosion Resistant Coatings	Contract Liquid Ring Syst		<u>0</u>	0	0
32	for Electrical Materials (3.2.6.6)	Complete Unit Test (4.2.3	.3)	0		0
	O Thermal Relief Valves	Hardness Tests (4.2.3.3)		0	0	0
	O Ring Liquid Level Control Valve	Gear Test (4.3.6.2))\	$\frac{0}{0}$	0	0
	O Review of Purchaser's Piping (3.7.1.15) & Foundation	Sound Level Test (4.3.6.3	,			
	Review of Purchaser's Control System	O Advance Notice Req'o O Inspection Checklist F		(+.1.4)	(4.3.1.3)	
38	O Dynamic Rotor Balancing (ISO Grade:) O Special Skid Clearances or Safe Access Areas (2.1.7):			MDTI	ON	
39	O Special Skill Glearances of Sale Access Areas (2.1.7):	Cooling Water:		ant'i N		mm
40	O Air Run-in Required (2.1.14)	Steam, Normal:				gpm _bs/Hr
41	O Spare Rotor Required (2.1.14)	Steam, Max.:				_bs/Hr
42	O Units of Measure (Dwgs., Nameplates, etc.) (2.10.3):	Instrument Air:				scfm
43	O onito of medoure (Dwys., Maniepiates, etc.) (2.10.5).	Hp (Driver):				Чр
44	○ 5 Yr. Retention of Final Assembly Clearances (4.2.1.1.e)	Hp (Auxiliaries):				Hp
45	O Coordination Meeting Required (5.1.3)	Heaters:				<w< td=""></w<>
46		Purge (Air or Nitrogen):				scfm
47	Remarks:	1				
48						
49						_
50						
51						
52		······································				

Job No.

Revision _____

Page	9	of	
Item No.			
Date			
Ву			

LIQUID RING VACUUM PUMP AND COMPRESSOR SYSTEM DATA SHEET

1	RING LIQUID COOLER							
2	Duty: Btu/hr Cooler Item Number:							
3	Supplier: No. Units Required:							
4	Model Number: Type:							
5	OPERATING CONDITIONS							
6		She	ell Side			Tube	e Side	
7	O Fluid					······		
8	Total Flow (Lbs/hr)							
9	Specific Gravity		Ø	۴F			0	•F
10	Thermal Conductivity (Btu/hr x Sq. Ft. x °F)		Q	•F	1		@	•F
11	Specific Heat (Btu/lb x °F)		Q	•F			8	•F
12	Viscosity - SSU		Ø	•F			0	•F
13	Operating Temperatures (°F)	IN	OUT		IN		OUT	
14	Inlet Pressure (psig)							
15	Inlet Velocity (ft/sec)							
16	O Pressure Drop (psi)	ALLOW	CAL	.C	ALLC	W	CALC	
17	Design Temperatures (°F)				1			
18	Pressure (psig)	MIN	TEST		MIN		TEST	
19	Foul Resistance (ft ² x hr x °F/Btu)				1			
20	O Min. Corrosion Allowance (inches)			~~~				
21	Number of Passes per Shell							
22		CONSTRUCT	TION DET	AILS				
23			Shell:	No. x ID.		x	Inches	
24	LMTD:	Tubes - No. per Shell:						
25	Corrected MTD:	O.D. x Length (In.) x				(ln.)		
26	Transfer Rate (Clean):			auge - BWG		the second s	lin. Wall)	
27	Transfer Rate (Service):]	ube Pitch:		(ln.) 🛆		
28				vable Tube	Bundle	🗌 Yes		
29	O Code Requirements: O ASME O TEM.			ode Stamp:				
30	Weights (lbs) - Each Bundle:	Bundle &			Full	of Water:		
31			LE SIZES	3		T 1 2 1 1		
32	Shell Si			NI. 1	0:	Tube Side		
33	No. Size	Rating & Faci	ing	No.	Size	Hati	ng & Facing	9
34		· ·				· · · ·		
35 36	Outlet							
30	Drain Vent							
37 38			ERIALS					
39	Tubes:		Baffles	,				
40	Tubes.		Channe				···· · · · · · · · · · · · · · · · · ·	
41	Shell:			el Flanges:				
42	Shell Flanges:	<u></u>	2	el Nozzie Fla	naes:			
43	REMARKS: 1) Outside tube area excluding	area in tube s	L					
44	1) Units exempt from code stat			l weld seam	s spot ex	amined ne	r Para LIW	-52 of
45	ASME code.				- 0001 68	anniou pe	1 414. 01	<u> </u>
46								
47	······································							
48								
49					······································			
50								
51		·	- <u> </u>					<u></u>
52								
							· · · · · · · · · · · · · · · · · · ·	

Job. No. _____

Revision

Page <u>10</u> of	
Item No.	
Date	
Ву	

_			
	Pump Size and Model:	Brg. Frame:	Service:
	O No. Pumps Req'd: No. Motors Req'd:		urbines Req'd: Item No.:
3	O OPERATING CONDITIO	NS - EACH PUMP	PERFORMANCE
	Liquid/Slurry:		Performance Curve No.:
	PT °F Norm: Max: US GPM at No		RPM: NPSH (water):
	Sp. Gr. at Norm PT: Total Head, Ft.	. Rated:	Eff.: % BHP Rated:
7		ress. (psig) Max: Rated:	Max. BHP Rated Impeller:
	Vis. at Norm. PT cP: NPSHA, Fi		Max. Head Rated:
	Corr./Eros. caused by: Ph:	Hyd. Hp:	Max. Discharge Pressure psig:
10	Driver Hp to be selected for Max. S.G.:	& Max. Viscosity:	Min. Continuous gpm:
11			SHOP TESTS
12			O Nonwit. Perf. O Wit. Perf.
13	CONSTRUCTION: O ASME B73.1M	O ASME B73.2M	O Nonwit. Hydro. O Wit. Hydro.
14	O OTHER:		O Nonwit. NPSH O Wit. NPSH
15	Pump Type: O Horiz. O Vert. In-Line	O Coupled Motor Shaft	O Nonwit. Vibration O Wit. Vibr.
16	O Cradled Mnt.		O Dismantle & Inspect After Test
	Case Horizontal Mount: D Foot	Centerline	O Other:
18		oupling 🔲 Other:	
19		e: 🗌 Single 🗌 Double	PUMP MATERIALS
20	Press: 🔲 Max. Allow. (psig)	(°F) Hydro Test (psig)	Casing:
21		ction O Gauge Discharge	Impeller:
		Impeller Type:	Wear Rings:
	Bearings Type: Radial: Thr		Shaft/Sleeve:
24	Lube: 🗌 Oil 🔲 Oil Mist 🗌 Gre	ase 🔲 Grease for Life	Gland:
	Coupling: Mfr.: Model: Gua		Gaskets:
26		O Driver Mfr. O Purchaser	Baseplate:
		Jacketed Seal Only	Coupling Guard:
	•	Size/No. of Rings:	Other:
29	Lantern Rings: Yes No		
	🔿 Mech. Seal: 📋 Mfr. & Model	Material Code:	INSPECTION: O Not Required
31	Balanced Unbalanced	🗋 Single 📋 Inside	O In Process O Final
32	Double Back to Back	Tandem 🔲 Outside	Days Notification Required:
33	Cartridge Face to Face		SOUND SPECIFICATION
34	AUXILIARY PIPING (see Fig	s. A2 and A3 for Code)	REQUIREMENTS
35	Stuf. Box Plan No.:	V. Piping Plan No.:	
36			
37	Packing Cooling Injection Req'd., Total (gpr		
38	External Seal Flush Fluid (gpm)	(psig)	
39	Seal Quench Plan: Seal Quen	ch Fluid:	ADDITIONAL REQUIREMENTS/
		ner, provided by:	COMMENTS
		Volts/Phase/Hertz:	
42	Mfr. Bearings: Service Fa	actor:	
43	Type: Insulation: Amps:	FL LR	
44	Lube: Temp. Rise (°F): En		
45	Inlet Press.: Exhaust Press	s.: Steam Temp.:	Water Rate:
46	Other:		
47		Customer/User:	
48		Location:	
49		Customer P.O. No.:	
50		Items No(s).:	Equip. No(s).:
51	This data sheet is provided courtesy of	Factory Order No(s).:	Pump Serial No(s).:
52	the American Society of Mechanical	Issued By:	Date:
53	Engineers, ASME B73.2M-1991	Rev.:	Date:

Job No. _____

Page_11_of _____ Item No. Date _____ Ву _____

Revision	
Revision	

1	MOTOR DESIGN DATA	MOTOR DESIGN DATA (CONTINUED)
2	APPLICABLE SPECIFICATIONS:	VIBRATION:
3		O NEMA Standard O
4	0	NOISE:
5		O NEMA Standard O
	SITE DATA	
7	Area: O Class Gr. Div. O Non-Hazardous	
8		ACCESSORY EQUIPMENT
9	Unusual Conditions: O Dust O Fumes	O Baseplate O Soleplate O Stator Shift
10		O Mfr. Std Fans O Non-sparking Fans
	DRIVE SYSTEM: O Direct Connected	O D.C. EXCITATION
12		kW Reg'd.: Volts:
13		By: O Purchaser O Manufacturer
	TYPE OF MOTOR:	Description:
15		O ENCLOSED COLLECTOR RINGS:
16		O Purged: Medium Press. (psig)
17	O Power Factor Reg'd.:	O Explosion-Resistant Non-purged
18	Excitation: O Brushless O Slip Ring	O Forced Ventilation
19		☐ cfm Press. Drop In. H ₂ O
20	O Wound Rotor Induction	O BEARING TEMP. DEVICES:
21	0	
	ENCLOSURE:	Description:
23	O Class Group Div.	Set @ (°F) for Alarm (°F) for Shutdown
24	O TEFC, Severe Duty O Exp. Proof	O SPACE HEATERS:
25	O Weather Protected, Type:	
26	O TEWAC O TEIGF, Using Gas	O Volts Phase Hertz
27	O Double Wall Carbon Steel Tubes	O Max. Sheath Temp.: (°F)
28	O Water Supply: Press.: (psig) Temp.: (°F)	WINDING TEMPERATURE DETECTOR:
29	□ O Water Allow △ P (psi) & Temp., Rise: (°F)	O Thermistors: No/Phase:
30	O Water Side Min. Corr. Allow (In)	Type O Pos. Temp. Coeff.
31	and Foul Factor:	O Neg. Temp. Coeff.
32	O (Air) (Gas) Supply Press. (psig)	Temperature Switch: O Yes O No
33	O Forced Ventilated	O Resistance Temp. Detectors: No/Phase
34	O Open-Drip Proof	O Resistance Material
35	O Open	O Ohms
36		Selector Switch & Indicator by:
37	0	O Purchaser
	BASIC DATA:	O Manufacturer
39		Max. Stator Winding Temperatures:
40		(°F) for Alarm (°F) for Shutdown
41		WINDING TEMP. DETECTOR & SPACE HEATER LEADS:
42		O In Same Conduit Box
43		
	STARTING: O Full Voltage O Reduced Voltage %	O MOTOR ARRANGED FOR DIFFERENTIAL
45		PROTECTION:
46 47	O Loaded O Unloaded	O Self-Balance Primary-Current Method O C.T. Description:
47 48		O Extended Leads Length (Ft.)
49		
50		

API	SID*P97	96 🔳	0732290	0550672	746 I	

Job. No. _____

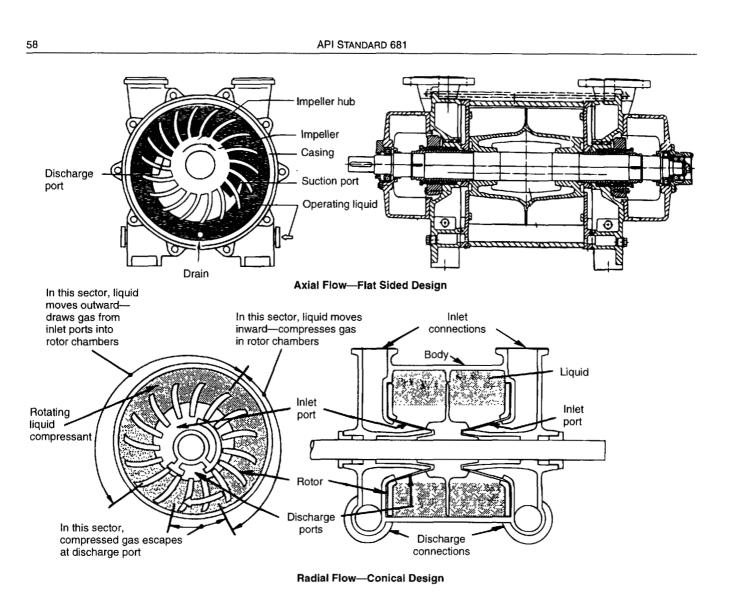
Page <u>12</u> of	
Item No.	
Date	
By	

Revision _____

1	ACCESSORY EQUIPMENT (CONTINUED)	MANUFACTURER'S DATA (CONTINUED)
2	O SURGE CAPACITORS:	Limit End Float to:
3	O LIGHTNING ARRESTERS	Curves Req'd Based on Mtr. Saturation & Rated Volt:
4	O C.T. FOR AMMETER	O Speed vs. Torque @ 100%, 90% & 80% rated Voltage:
5	O Description:	O Speed vs. Current @ 100%, 90% & 80% rated Voltage:
6	MAIN CONDUIT BOX SIZED FOR:	
7	O Main Motor Leads O Type:	WEIGHT (Lb.):
8	O Insulated O Non-Insulated	Net Weight: Shipping Weight:
9	O C.T.'s for Diff. Protection (mounted by):	Rotor Weight: Max. Erection Wt.:
10	O Surge Capacitors (mounted by):	Max. Maint. Wt. (Identify):
1	<u> </u>	DIMENSIONS (Feet & Inches):
	O C.T. for Ammeter (mounted by):	L: W: H:
13	O Space for Stress Cones:	
	O AIR FILTERS:	
15	Mfr _ Type:	
16		SHOP INSPECTION AND TESTS
17	MANUFACTURER'S DATA	Req'd. Witness
	Manufacturer:	Shop Inspection: O O
19	Frame No.: Full Load RPM (Ind.):	Testing per NEMA O O
1	Efficiency: F.L. 3/4L 1/2L	Mfr. Std. Shop Tests: O O
21	Pwr Factor (Ind.): F.L. 3/4F 1/2L	Immersion Test: O O
22	Curr. (Rated Volt.): Full Load: Locked Rotor:	Special Tests (list below): O O
23	Locked Rotor Power Factor:	0 0
24	Locked Rotor w/Stand Time (cold start)	0 0
25	Locked Rotor w/Stand Time (hot start):	0 0
26	Torques (FtLb.): Full Load:	0 0
27	Locked Rotor Starting (Syn.):	
28	Pull-Up (Ind.). Pull-In (Syn.):	PAINTING:
29	Breakdown (Ind.) Pull-Out (Syn.):	O Manufacturer's Standard
30		0
	Open Circuit Time Constant (Sec.):	0
32	Symmetrical Contribution to 3 Phase Terminal Fault	
33		SHIPMENT
34	Reactances: Sub-Transient (X"D)	O Domestic O Export O Export Boxing Req'd
	Transient (X'D): Synchronous (XD):	O Outdoor Storage Over 3 Months
	A.C Stator Resistance: Ohms @ (°F)	0
	Rated kVA:	0
	kVA Inrush @ Full Volt. & Locked Rotor (Syn.) %	
	kVA @ Full Voltage & 95% Speed: %	REMARKS:
	Max. Line Curr. in Stator on 1st Slip Cyc. & Pull-Out (Syn.):	
41		
	Acceleration Time (Mtr only & Rated Volt.) Sec.	
	Accel Time (Mtr. & Load & 85% Rated Volt): Sec	
	Rotor/Field Wk ² & Mtr. Shaft (Lb -Ft ²)	
	No. of Starts per Hour:	
	Bearing: Type: Lubr	
	Lube Oil Required: (gpm) & (psig)	
	Total Shaft End Float:	
49 5 0		
50		

API STD*681 96 🖿 0732290 0550673 682 🎟

APPENDIX B-LIQUID RING VACUUM PUMP SCHEMATIC



The Liquid Ring Pumping Action

The rotor propels a band of ring liquid that rotates inside the cylindrical body The rotor axis is offset from the body axis. As centrifugal force forms the ring of liquid inside the body, it almost fills, then almost empties, each rotor chamber during a single revolution. This sets up the piston action. Vacuum inlet ports and atmospheric discharge ports provide flow paths at

the inner edges of the rotor chambers for the gas mixture being handled.

Rotor Imbalance

As can be seen in the above diagrams and the previous paragraphs, the liquid ring rotates at the same speed as the rotor but is offset from the axis of the rotor.

If, for example, the rotor has twenty chambers, twenty liquid pistons complete an outward inlet and an inward discharge stroke for each revolution of the rotor. The frequency of this imbalanced piston would be twenty times the rotational or equal to the vane passing frequency.

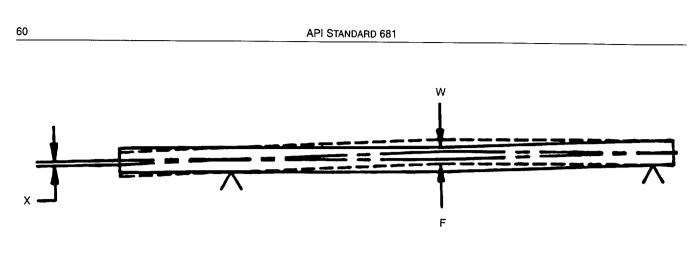
Because of the large mass and higher frequency of the liquid piston, the rotor imbalance becomes a minor factor, and the liquid piston imbalance becomes a major factor in the vibration characteristics of the entire system.

Figure B-1—Liquid Ring Vacuum Pump Schematic

API STD*681 96 🔳 0732290 0550675 455 🔳

APPENDIX C—SHAFT DEFLECTION SCHEMATIC

.



Notes:

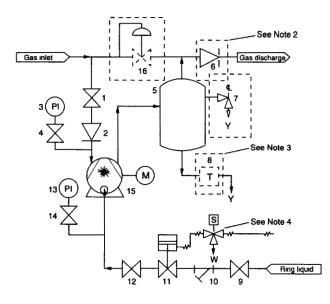
1. As in any machine, the static weight "W" of the liquid ring pump shaft and rotor will deflect the shaft downward. This results in an upward deflection of the shaft extension. 2. Due to the operational characteristics of the liquid ring pump, a pressure differential exists between the inlet and discharge of the pump. This pressure difference "F" will deflect the shaft extension. This change in deflection at the extension "X" may be as much as 0.005 inch and will vary directly with differential pressure.

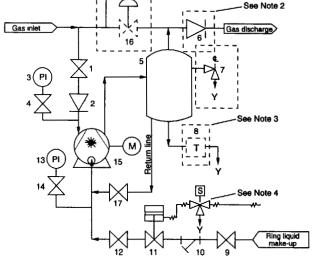
Figure C-1—Shaft Deflection Schematic

API STD*681 96 🖿 0732290 0550677 228 🖿

APPENDIX D—LIQUID RING VACUUM PUMP RING LIQUID FLOW SCHEMATICS

API STANDARD 681





See Note 1

Figure A—LRVP Once Through System

Figure B—LRVP Partial Recirculation System

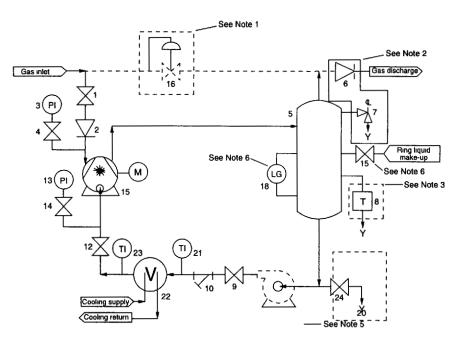


Figure C-LRVP Total Recirculation System

Figure D-1—Liquid Ring Vacuum Pump Ring Liquid Flow Schematics

LIQUID RING VACUUM PUMPS AND COMPRESSORS FOR PETROLEUM, CHEMICAL, AND GAS INDUSTRY SERVICES

Key to Parts

Figures A & B

- 1. Inlet isolating valve.
- 2. Inlet check valve.
- 3. Inlet pressure gauge.
- 4. Gauge isolation valve.
- 5. Gas/ring liquid separator.
- 6. Discharge check valve (see Note 2).
- 7. Pressure relief valve (see Note 2).
- 8. Ring liquid drain trap (see Note 3).
- 9. Inlet isolating valve.
- 10. Y Strainer.
- 11. Pilot operated automatic valve (see Note 4).
- 12. Flow regulating valve or orifice.
- 13. Ring liquid pressure gauge.
- 14. Gauge isolating valve.
- 15. Liquid ring pump and drive.
- 16. Inlet pressure control (see Note 1).
- 17. Partial ring liquid recirculation valve (Figure B only).

Figure C-Additions

- 18. Level gauge.
- 19. Make-up valve.
- 20. Optional ring liquid recirculation pump.
- 21. Temperature gauge.
- 22. Heat exchanger.
- 23. Temperature gauge.
- 24. Drain valve.

Notes

1. Optional inlet pressure control valve.

2. Optional pressurized discharge check valve and pressure relief valve. (Required on liquid ring compressors or vacuum pumps with positive discharge to a contained system.)

3. Optional pressurized discharge ring liquid drain system. (Required for compressors.)

4. Pilot operated isolating valve. Direct acting solenoid may be substituted at purchaser's discretion for small sizes.

5. Recirculation pump optional based on purchaser's requirements or application details.

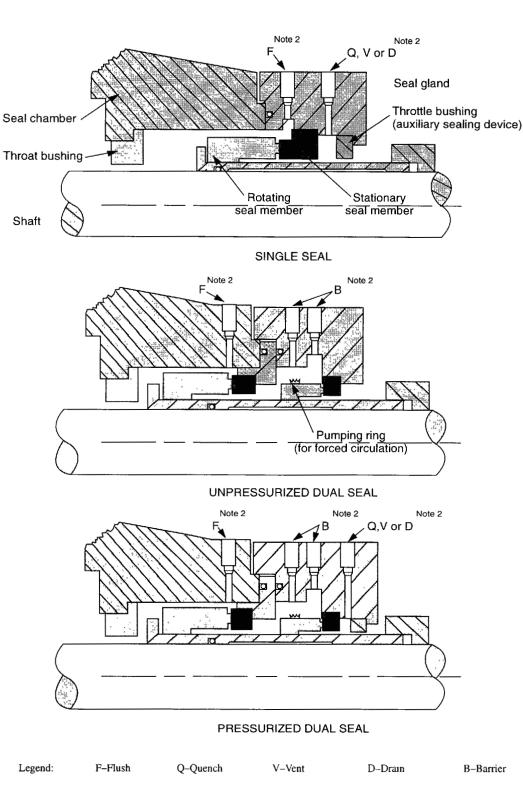
6. Optional level controls may be specified by purchaser.

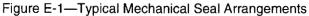
API STD*681 96 🔳 0732290 0550680 812 🔳

APPENDIX E-MECHANICAL SEAL AND PIPING ARRANGEMENT SCHEMATICS

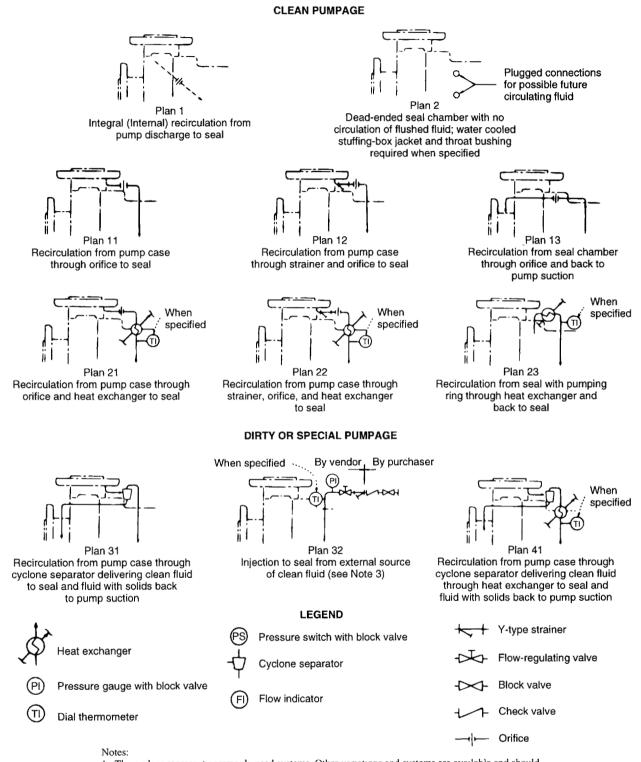
API STANDARD 681







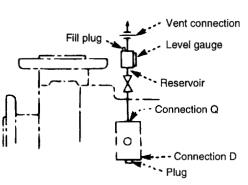
67



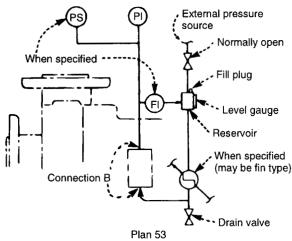
 These plans represent commonly used systems. Other variations and systems are available and should be specified in detail by the purchaser or mutually agreed upon by the purchaser and the vendor.
 These plans are for use with Connection F on the single- and tandem-seal arrangements shown in Figure E-1.

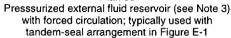
3. For Plan 32, the purchaser will specify the fluid characteristics, and the vendor shall specify the volume, pressure, and temperature required.

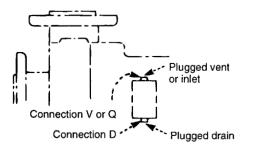
Figure E-2—Piping for Single-Seal Arrangements and Primary Seals of Tandem-Seal Arrangements



Plan 51 Dead-ended blanket (usually methanol, see Note 3); typically used with auxiliary sealing device (single- or double-seal arrangement in Figure E-1)



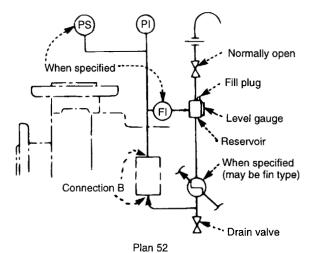




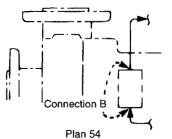
Plan 61

Tapped connections for purchaser's use; Note 3 applies when purchaser is to supply fluid (steam, gas, water, etc.) to auxiliary sealing device (single- or double-seal arrangement in Figure E-1)

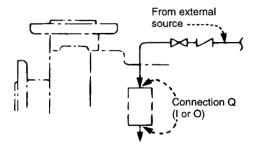
Notes:



Nonpresssurized external fluid reservoir (see Note 3) with forced circulation; typically used with tandem-seal arrangement in Figure E-1



Circulation of clean fluid from external system (see Note 3); typically used with double-seal arrangement in Figure E-1



Plan 62 External fluid quench (steam, gas, water, etc.; see Note 3); typically used with throttle bushing or auxiliary sealing device (single- or double-seal arrangement in Figure E-1)

1 These plans represent commonly used systems. Other variations and systems are available and should

- be specified in detail by the purchaser or mutually agreed upon by the purchaser and the vendor.
- 2. See Figure E-2 for explanation of symbols not specified here.
- 3. When supplemental seal fluid is provided, the purchaser will specify the fluid characteristics. The
- vendor shall specify the volume, pressure, and temperature required, where these are factors.

Figure E-3—Piping for Throttle Bushing, Auxiliary Seal Device, Tandem Seals, or Double Seals

APPENDIX F-MATERIAL LIST

•

_	^
	()

API STANDARD 681

Major Part Location	Material	Specification	Grade
Cast parts- casings and internals	Grey iron	ASTM A48 AS 1830 DIN 1691 SIS 0115 BS 1452	Class 20 min. Grade T150 min. GG10 min. MNC 705 min. Grade 150 min.
	Ductile iron	ASTM A536 ASTM A395 DIN 1693 SIS 1407 BS 2789	60-45-12 min. 60-40-18 min.
	Austenitic ductile iron	ASTM A439 BS 3468	
	Carbon steel	ASTM A216	WCA min.
	Stainless steel	ASTM A351, A743 or A744 DIN 17445 SIS 2343 or 2353 BS 1504	CF3, CF3M, CF8, CF8M, CA6NM, or CN7M 1.4581, 1.44406, 1.4410
	Nickle & nickle alloys	Hastelloy B Hastelloy C ASTM A494	Hastelloy B Hastelloy C-4 CW-2M, CQ-7M or N12
Fabricated parts- casings and internals	Steel	ASTM A36, A53, A203 or A516 DIN 17100 BS 3100	Al
	Stainless steel	ASTM A240 or A276 DIN 17440 BS 970	304, 304L, 316, 316L or 316TL
	Nickle & nickle alloys	Hastelloy B Hastelloy C ASTM B333 ASTM B575	Hastelloy B-2 Hastelloy C-276 N10001 min. N10276
Shafts	Steel	ASTM A29 or A576 DIN 17440	1045
	Martensitic stainless steel	ASTM A276 DIN 17440	420 or 431 1.4021
	Austenitic stainless steel	ASTM A276 DIN 17440	303, 304, 316 or 329 1.4401
	Duplex stainless steel	ASTM A572 DIN 17440	65 1.0080
	Nickle & nickle alloys	Hastelloy B Hastelloy C ASTM B335 ASTM B574	Hastelloy B Hastelloy C-276 N10001 min. N10276
Shaft sleeves	Martensitic stainless steel	ASTM A276 DIN 17440	420 1.4021
	Austenitic stainless steel	ASTM A276 DIN 17440	304 or 316 1.4401
	Nickle & nickle alloys	Hastelloy B Hastelloy C ASTM B335 ASTM B574	Hastelloy B Hastelloy C-276 N10001 min. N10276

Note: Temperature limitation -40°F to 250°F

APPENDIX G—LIQUID RING VACUUM PUMPS AND COMPRESSORS VENDOR DRAWING AND DATA REQUIREMENTS

LIQUID RING VACUUM PUMPS AND COMPRESSORS VENDOR DRAWING AND DATA REQUIREMENTS

JOB NO	ITEM NO	
PURCHASE ORDER NO.	DATE	
REQUISITION NO.	DATE	
INQUIRY NO	DATE	
PAGE <u>1</u> OF <u>2</u>	_ BY	<u>_</u>
REVISION		
UNIT		

SITE	 	 	
SERVICE	 		

FOR

NO. REQUIRED	

Bidder shall furnish _____ copies of data for all items indicated by an X. Proposal^a Vendor shall furnish ______ copies and _____ transparencies of drawings and data indicated. Review^b Vendor shall furnish ______ copies and ______ transparencies of drawings and data indicated. Final^b Vendor shall furnish _____ operating and maintenance manuals. Final—Received from vendor Due from vendor^c Review-Returned to vendor ___ Review---Received from vendor Review—Due from vendor^c LIQUID RING PUMP OR COMPRESSOR 1. Certified dimensional outline drawing and list of connections. 2. Cross-sectional drawings and bill of materials. 3. Shaft seal drawing and bill of materials.

Coupling assembly drawing and bill of materials.				
5. Ring liquid schematic and bill of materials.				
6. Cooling water schematic and bill of materials.				
7. Ring liquid system arrangement drawing and list of connections.				
8. Ring liquid component drawings and data.				
9. Electrical and instrumentation schematics and bill of materials.			_	
10. Electrical and instrumentation arrangement drawing and list of connections.				
11. Performance curves.				
12. Vibration analysis data.	 			
13. Lateral critical speed analysis.				
14. Torsional critical speed analysis.				
15. Certified hydrostatic test data.		1		
16. Progress reports.				
17. Weld procedures.				
18. Performance test data.				
19. Certified rotor balance data.				
20. As-built data sheets.				
21. As-built clearances.				
22. Installation, operation, and maintenance manuals.				
23. Spare parts recommendations.				
24. List of drawings.				
25. List of special tools furnished for maintenance.				
26. Material safety data sheets.				
27. Relief valve calculations.				

^aProposal drawings and data do not have to be certified or as-built.

^bPurchaser will indicate in this column the time frame for submission of materials using the nomenclature given at the end of the form. ^cBidder shall complete these two columns to reflect his actual distribution schedule and include this form with his proposal.

			JOB NO				ITEM NO)		
	LIQU	ID RING VACUUM PUMPS	PAGE	2	OF	2	BY			
		AND COMPRESSORS	DATE			REV.	NO.			
VEN		WING AND DATA REQUIREMENTS								
	Ducasala	Bidder shall furnish cop	ion of data for all it	omo indi	iootod by c	n V	<u>.</u>			
_	Proposala					ui A.				
Review ^b		Vendor shall furnish o	opies and	_ transp	arencies c	of drawin	igs and da	ata indio	cated.	
		Vendor shall furnish	copies and	trans	parencies	of drawir	ngs and d	lata indi	icated.	
Final ^b		Vendor shall furnish	operating and mai	ntenanc	e manuals		-			
			from vandar							<u> </u>
			from vendor							
			ed to vendor							
			ed from vendor							
			m vendor ^c							
]			
V	¥ ¥	MOTO	DR			,	• •	V	↓	•
		28. Certified dimensional outline drawing.								
		29. Cross-sectional drawing and bill of materials.							· · ·	
		30. As-built data sheets.								
		31. Performance data.		-						
		32. Certified drawings of auxiliary systems.								
		33. Installation, operation, and maintenance mar	nuals							
		34. Spare parts recommendations.								
		GEA	R							
		35. Certified dimensional outline drawings and li	st of connections					_		
		36. Cross-sectional drawing and bill of materials								+
		37 As-built data sheets.							+	\square
		38. Mechanical running test log.							1	
		39 Gear manufacturer's standard test logs			• • • • • • •	· · · · ·				
	1	40 Optional test data and reports.							+	
		41 Installation, operation, and maintenance mai	uals.						1	
		42. Spare parts recommendations.								

^aProposal drawings and data do not have to be certified or as-built.

^bPurchaser will indicate in this column the time frame for submission of materials using the nomenclature given at the end of the form.

^cBidder shall complete these two columns to reflect his actual distribution schedule and include this form with his proposal.

Notes:

1. Send all drawings and data to ____

2. All drawings and data must show project, appropriation, purchase order, and item numbers in addition to the plant location and unit. In addition to the copies specified above, one set of the drawings/instructions necessary for field installation must be forwarded with the shipment.

3. See expanded description of specified in items below.

Nomenclature:

	S-number of weeks prior to shipment.
	F—number of weeks after firm order.
	Dnumber of weeks after receipt of approved drawings.
Vendor	
Date	Vendor Reference

Signature _____

(Signature acknowledges receipt of all instructions)

API STD*681 96 🔳 0732290 0550689 T4T 🖿

APPENDIX H—SYSTEM CONSIDERATIONS, OPERATING VARIABLES, AND TEST PERFORMANCE CONVERSION

H.1 System Consideration—Factors Affecting Performance and Selection of Liquid Ring Vacuum Pump and Compressor Systems

Liquid ring vacuum pump and compressor performance in the user's process is significantly influenced by process variables. Process variables which must be considered during process development, design, and specification may include:

H.1.1 VARIABLES FOR GAS INLET TO PUMPING (OR COMPRESSING) EQUIPMENT

H.1.1.1 Temperature, pressure, mass flows, and molecular weights.

H.1.1.2 Saturation conditions and heats of vaporization and condensation.

H.1.1.3 Solubility of gases in the ring liquid fluid.

H.1.1.4 Presence of liquid or solid carryover, and particle size if applicable.

H.1.1.5 Variations with time in process gas specification (that is, batch processes).

H.1.1.6 Pump-up or pump-down time limitations.

H.1.1.7 Reactivity of the gas, or effects of the gas on the ring liquid.

H.1.2 VARIABLES FOR GAS DISCHARGED TO PROCESS OR VENT SYSTEM

H.1.2.1 Maximum (allowable) temperatures.

H.1.2.2 Pressures, including maximum allowable.

H.1.2.3 Gas mass flows required or desired downstream.

H.1.2.4 Permitted (or allowable) liquid carryover from the system.

H.1.2.5 Permitted (or allowable) vapor carryover from the system.

H.1.3 VARIABLES FOR RING LIQUID SYSTEM

H.1.3.1 Temperatures and pressures at the inlet to the system.

H.1.3.2 Temperatures and pressures required (or desired) at the discharge from the system.

H.1.3.3 Vapor pressure under equilibrium conditions at the pump or compressor suction and discharge within the operating range.

H.1.3.4 Specific gravity in the operating range.

H.1.3.5 Viscosity in the operating range.

H.1.3.6 Reactivity with the gas stream, if applicable.

H.1.3.7 Miscibility/solubility with inlet liquids or condensed vapors.

H.1.3.8 Fouling potential.

H.1.3.9 Specific heat and thermal conductivity within the operating ranges.

H.2 Operating Variables—Checklist

H.2.1 Inlet mixture may be cooled in pump increasing net capacity.

H.2.2 Inlet mixture may or may not be saturated with condensable vapors.

H.2.3 Inlet condensables may be miscible or immiscible with other or with service liquid.

H.2.4 Inlet condensables may be partially condensed in pump increasing net capacity.

H.2.5 Cooler service liquid temperature may increase net capacity and lower effective vapor pressure of service liquid.

H.2.6 Lower service liquid effective vapor pressure may increase net capacity.

H.2.7 Condensing vapors may increase service liquid temperature rise and increase heat load to optional heat exchanger.

H.2.8 Service liquid specific heat lower than water may increase temperature rise.

H.2.9 Service liquid specific gravity lower than water may affect performance.

H.2.10 Service liquid specific viscosity lower than water may decrease BHP and, in turn, reduce service liquid temperature rise.

H.2.11 Solubility of inlet gas in service liquid may reduce net capacity.

H.2.12 Inlet vapors may condense and contaminate the service liquid modifying its characteristics. Miscible condensables may accumulate in service liquid and become a dominant factor in determining net effective vapor pressure. Immiscible condensables with lower specific gravity than service liquid may collect at gas/liquid interface and

76

become dominant factors in determining net effective vapor pressure.

H.2.13 Net performance is generally determined by vapor pressure at effective service liquid temperature. For two stage pumps, the latter is the interstage temperature.

H.2.14 Higher service liquid rate may reduce temperature rise and increase net capacity at rated conditions.

H.2.15 Service liquid type may determine effective service liquid temperature and performance.

Once-through generally provides lowest service liquid temperature with higher effective service liquid temperature.

Full recirculation permits use of separate coolant medium-generally with higher effective service liquid temperature. A minimal service liquid purge flow should be used to control service liquid contamination.

H.2.16 Back pressures other than standard will affect performance.

H.3 Conversion of Standard Test Performance to Specified Operating Conditions

H.3.1 Since operating conditions with respect to inlet gases, condensable vapors, service liquid, and other field conditions are often different from those of the Standard Test, a conversion must be carried out. Conversions of this kind shall be based upon the manufacturer's standard method and shall be agreed upon before-hand by the parties involved.

H.3.2 A check list of operating variables will provide the user with a better understanding of conversions to be made. **H.3.3** It should be noted that a rigorous mathematical solution or conversion is generally not practicle. The equipment selection procedure is usually a reiteration of a series of approximations. The latter are based upon a combination of user and manufacturer field experience, vendor laboratory tests, and similarity. API STD*681 96 🖿 0732290 0550691 6T8 📟

ADDITIONAL COPIES AVAILABLE FROM PUBLICATIONS AND DISTRIBUTION (202) 682-8375



1220 L Street, Northwest Washington, D.C. 20005-4070 202-682-8000

Order No.C68101