

# **Specification for Validation of Wellhead Surface Safety Valves and Underwater Safety Valves for Offshore Service**

API SPECIFICATION 6AV1  
SECOND EDITION, FEBRUARY 2013



AMERICAN PETROLEUM INSTITUTE

## Special Notes

API publications necessarily address problems of a general nature. With respect to particular circumstances, local, state, and federal laws and regulations should be reviewed.

Neither API nor any of API's employees, subcontractors, consultants, committees, or other assignees make any warranty or representation, either express or implied, with respect to the accuracy, completeness, or usefulness of the information contained herein, or assume any liability or responsibility for any use, or the results of such use, of any information or process disclosed in this publication. Neither API nor any of API's employees, subcontractors, consultants, or other assignees represent that use of this publication would not infringe upon privately owned rights.

API publications may be used by anyone desiring to do so. Every effort has been made by the Institute to assure the accuracy and reliability of the data contained in them; however, the Institute makes no representation, warranty, or guarantee in connection with this publication and hereby expressly disclaims any liability or responsibility for loss or damage resulting from its use or for the violation of any authorities having jurisdiction with which this publication may conflict.

API publications are published to facilitate the broad availability of proven, sound engineering and operating practices. These publications are not intended to obviate the need for applying sound engineering judgment regarding when and where these publications should be utilized. The formulation and publication of API publications is not intended in any way to inhibit anyone from using any other practices.

Any manufacturer marking equipment or materials in conformance with the marking requirements of an API standard is solely responsible for complying with all the applicable requirements of that standard. API does not represent, warrant, or guarantee that such products do in fact conform to the applicable API standard.

All rights reserved. No part of this work may be reproduced, translated, stored in a retrieval system, or transmitted by any means, electronic, mechanical, photocopying, recording, or otherwise, without prior written permission from the publisher. Contact the Publisher, API Publishing Services, 1220 L Street, NW, Washington, DC 20005.

*Copyright © 2013 American Petroleum Institute*

## Foreword

Nothing contained in any API publication is to be construed as granting any right, by implication or otherwise, for the manufacture, sale, or use of any method, apparatus, or product covered by letters patent. Neither should anything contained in the publication be construed as insuring anyone against liability for infringement of letters patent.

Shall: As used in a standard, “shall” denotes a minimum requirement in order to conform to the specification.

Should: As used in a standard, “should” denotes a recommendation or that which is advised but not required in order to conform to the specification.

This document was produced under API standardization procedures that ensure appropriate notification and participation in the developmental process and is designated as an API standard. Questions concerning the interpretation of the content of this publication or comments and questions concerning the procedures under which this publication was developed should be directed in writing to the Director of Standards, American Petroleum Institute, 1220 L Street, NW, Washington, DC 20005. Requests for permission to reproduce or translate all or any part of the material published herein should also be addressed to the director.

Generally, API standards are reviewed and revised, reaffirmed, or withdrawn at least every five years. A one-time extension of up to two years may be added to this review cycle. Status of the publication can be ascertained from the API Standards Department, telephone (202) 682-8000. A catalog of API publications and materials is published annually by API, 1220 L Street, NW, Washington, DC 20005.

Suggested revisions are invited and should be submitted to the Standards Department, API, 1220 L Street, NW, Washington, DC 20005, [standards@api.org](mailto:standards@api.org).



## Contents

	Page
<b>1 Scope</b>	<b>1</b>
<b>2 Normative References</b>	<b>1</b>
<b>3 Definitions and Abbreviations</b>	<b>1</b>
3.1 Definitions	1
3.2 Abbreviations	2
<b>4 Validation</b>	<b>2</b>
4.1 General	2
4.2 Class II and Class III SSV/USV Valve Validation	3
4.3 Test Agency	3
4.4 Validation—Requirements	5
<b>5 Test Procedures</b>	<b>12</b>
5.1 Class II Validation Test Summary	12
5.2 Class II Test Procedure	13
5.3 Class III Validation Test Summary	13
5.4 Class III Test Procedure	17
<b>6 Scaling of Test Results</b>	<b>21</b>
6.1 Scaling of Class II Validation Results	21
6.2 Scaling of Class III Validation Results	21
<b>Annex A (informative) API Monogram Program</b>	<b>23</b>
<b>Bibliography</b>	<b>25</b>
<b>Figures</b>	
1 Example Piping Arrangement—Test Facility for Class II SSV/USV Valve Validation	5
2 Example SSV/USV Valve Validation Section Detail	6
3 Class II SSV/USV Validation Summary Flow Diagram	12
4 Class III Validation Summary Flow Diagram	13
<b>Tables</b>	
1 Example Application SSV/USV Valve Validation	8
2 Example Class II SSV/USV Valve Test Reporting Form	10
3 Example Class III SSV/USV Valve Test Reporting Form	11
4 Initial Leakage Test	14
5 Sand Slurry Flow Test	15
6 Sand Slurry Flow Test While Opening and Closing During Circulation	16
7 Initial Leakage Test	17
8 Class III Sand Slurry Flow Rates	18
9 Class III Sand Slurry Flow Test	19
10 Sand Slurry Flow Test While Opening and Closing During Circulation	20



# Specification for Validation of Wellhead Surface Safety Valves and Underwater Safety Valves for Offshore Service

## 1 Scope

This specification establishes design validation requirements for API 6A surface safety/underwater safety valves (SSV/USV) and associated valve bore sealing mechanism(s) for Class II and Class III. These classes are intended for use if substances such as sand can be expected to cause an SSV/USV valve failure. Class III adds requirements for the validation of the valve bonnet assembly inclusive of stem seals and may be selected by the user/purchaser. Validation to Class III also validates the same SSV/USV for Class II.

NOTE Previous editions of this document included reference to and requirements for verification to PR1, standard service (Class I).

## 2 Normative References

The following referenced documents are indispensable for the application of this specification. For dated references, only the edition cited applies. For undated references, the latest edition of the referenced document (including any amendments) applies.

*API Manual of Petroleum Measurement Standards (MPMS) Chapter 10.4, Determination of Sediment and Water in Crude Oil by the Centrifuge Method (Field Procedure)*

*API Specification 6A, Specification for Wellhead and Christmas Tree Equipment*

*API Recommended Practice 13B-1, Recommended Practice for Field Testing Water-based Drilling Fluids*

## 3 Definitions and Abbreviations

### 3.1 Definitions

The definitions below are related specifically to surface safety and underwater safety valves and are presented to define the terminology used in this specification.

#### 3.1.1

##### **failure**

Improper performance of a device or equipment item that prevents completion of its design function.

#### 3.1.2

##### **SSV/USV actuator**

Device that causes the SSV/USV valve to open when power is supplied and to automatically close when power is lost or released.

#### 3.1.3

##### **SSV/USV valve**

Subassembly of the SSV/USV that contains the wellstream and shuts off the flow when closed.

#### 3.1.4

##### **substantive change**

Change identified by the manufacturer that affects the performance of the product in the intended service.

**3.1.5****surface safety valve****SSV**

Automatic wellhead valve assembly that closes upon loss of power supply.

NOTE When used in this specification, the term is understood to include an SSV valve and SSV actuator.

**3.1.6****test agency**

Independent third party that provides a test facility and administers a testing program that meets the SSV/USV valve validation testing requirements of this specification.

**3.1.7****underwater safety valve****USV**

Automatic valve assembly installed at an underwater wellhead location that closes upon loss of power supply.

NOTE When used in this specification, the term is understood to include a USV valve and USV actuator.

**3.1.8****validation**

Confirmation, through the provision of objective evidence (data), that the requirements for a specific intended use or application have been fulfilled.

NOTE Previous editions referred to this term as verification test(ing).

**3.1.9****valve bonnet assembly**

Pressure containing subassembly of SSV/USV consisting of the valve bonnet, valve stem, stem seals, and body-to-bonnet seals.

**3.2 Abbreviations**

The following abbreviations are used in this specification.

bbl (m <sup>3</sup> )	barrels (cubic meters)
gpm (m <sup>3</sup> /min)	gallons per minute (cubic meters per minute)
PR	Performance Requirement
RWP	rated working pressure
SSV	surface safety valve
USV	underwater safety valve

**4 Validation****4.1 General**

This section includes the SSV/USV validation requirements for the two classes defined in Section 1 of this specification.

The validation requirements in this specification are not represented as duplicating actual well conditions.



Validations (previously known as verifications) for PR2 sandy service or Class II that have been completed in accordance with testing requirements of API 14D or previous editions of API 6AV1 during their validity shall satisfy the requirements of API 6AV1 Class II.

Validation to Class III also validates the same SSV/USV for Class II in accordance with the scaling limitations in 6.1.

**NOTE** In this edition of the specification, the term "Performance Requirement (PR)" has been replaced with "Class" (i.e. "PR2 sandy service" has now become "Class II"). This was done to ensure full alignment with the related terminology used in the reference document, API 6A. This is for alignment of the identification of the equipment only; no technical changes were made in the performance requirements for Class II.

## **4.2 Class II and Class III SSV/USV Valve Validation**

To qualify a specific SSV/USV valve design for Class II or Class III, the manufacturer shall submit an SSV/USV valve to a test agency that meets the requirements of this specification.

Any substantive change in the design or materials of construction that would affect the SSV/USV valve bore sealing mechanism shall require requalification by validation testing. A substantive change is a change identified by the manufacturer that affects the performance of the product in the intended service condition.

Additionally for Class III, any substantive change to the valve bonnet assembly shall require requalification by validation testing.

## **4.3 Test Agency**

### **4.3.1 General**

The test agency shall provide a facility, personnel, written procedures, and forms to assure conformance to the requirements of this specification. The test agency shall maintain literature that includes as a minimum:

- a) a description of the facility including any limitations on size or pressure rating of SSV/USV that may be tested;
- b) test procedures and forms actually used at the facility;
- c) basis for determining test scheduling priorities;
- d) procedures for making application for test, delivery of the SSV/USV, initial installation and checkout of the SSV/USV, and other pertinent information;
- e) any limitations on accessibility of the facility, although such limitations shall not preclude reasonable access to the facility for inspection by manufacturers or operators;
- f) any limitations on receipt of proprietary information; and
- g) any other information considered pertinent by the test agency.

The above literature shall be kept current and shall be furnished to manufacturers or user/purchasers or operators upon written request.

Test agencies shall be licensed by API in order to test SSV/USV equipment to the requirements of this specification. See Annex A of this specification for API licensing requirements.

## 4.3.2 Facility Requirements

### 4.3.2.1 General

An example piping arrangement and test section detail of a test facility are shown in Figure 1 and Figure 2.

### 4.3.2.2 Design Considerations

The test facility shall be designed to permit the validation to be made as detailed in 5.2 and 5.4 of this specification.

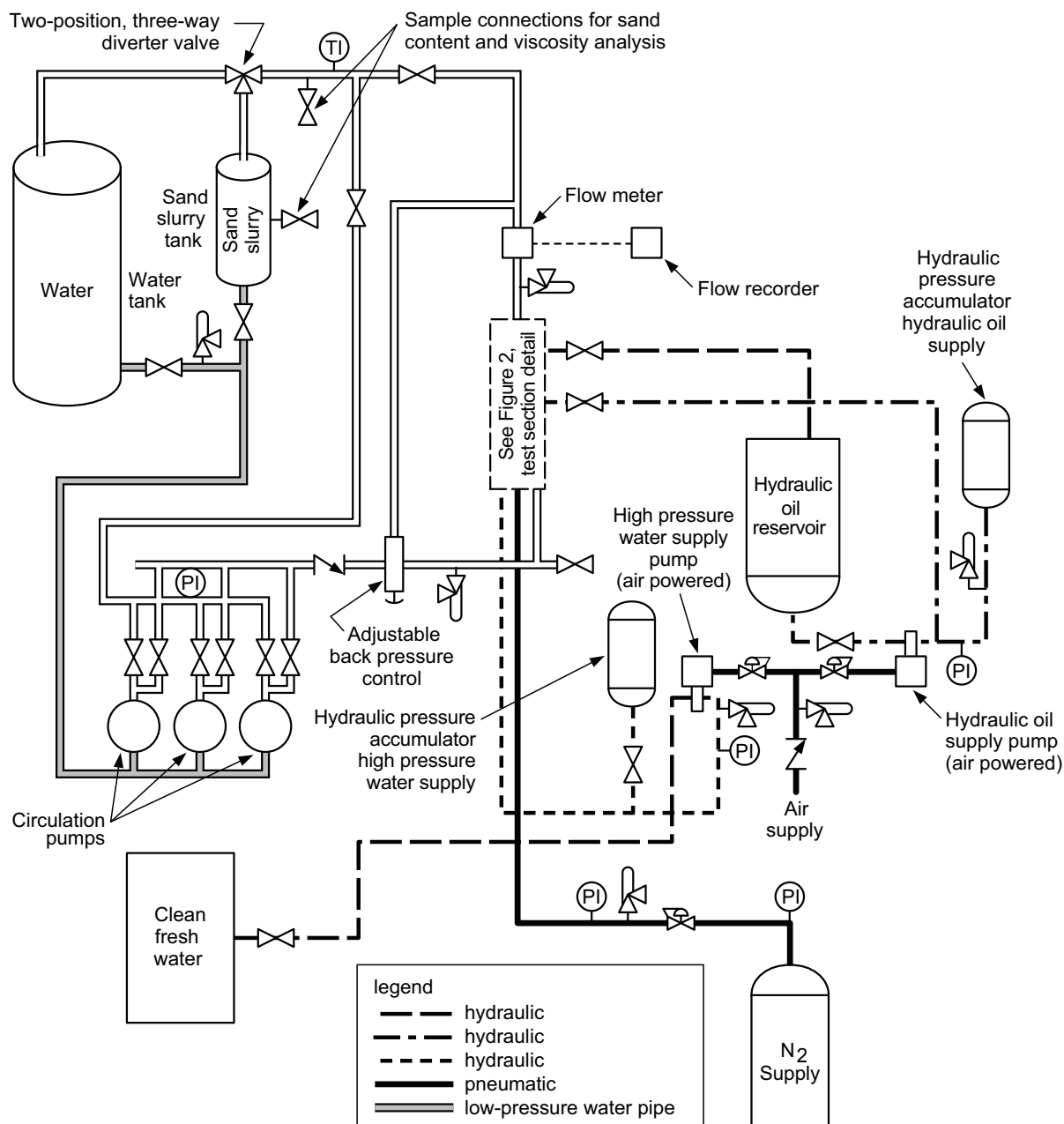
### 4.3.2.3 Circulation System Components

The test facility shall have the following circulation system components as a minimum.

- a) *Freshwater Tank*—A freshwater tank shall be provided with a minimum capacity of 5 bbl (0.8 m<sup>3</sup>).
- b) *Sand Slurry Tank and Associated Accessories*—A cone-bottom sand slurry tank with a minimum capacity of 5 bbl (0.8 m<sup>3</sup>) shall be provided. The tank shall be equipped with agitation as required to obtain proper slurry consistency. Sample connections shall be provided in the tank and in the return line to the tank so that representative sand content and viscosity analysis samples may be taken.
- c) *Circulating Pumps and Controls*—Circulating pumps with drivers and special equipment for pumping the sand slurry and freshwater at the required flow rates and pressures shall be installed. A means of flow control shall be provided.
- d) *Circulation Piping and Controls*—The circulation piping should be installed in an arrangement similar to that shown in Figure 1. Block valves should be provided as indicated in Figure 1 and Figure 2. The return piping to the sand slurry tank shall be installed in such a manner as to provide agitation to aid in preventing sand accumulation in the bottom of the tank. A device shall be installed between the circulation pumps and test section and shall be used to control SSV/USV differential pressure to 400 psi (2.8 MPa) during the cycling test (refer to 5.2.3 and 5.4.3).
- e) *Circulation Flow Meter*—The circulation flow meter shall be sized so that the flow rate to be measured falls within the flow meter's calibrated measurement range. This flow meter shall provide an output signal suitable for electronic data acquisition.
- f) *Instrumentation*—Pressure measuring devices shall meet the requirements of API 6A. Measurement instrumentation shall be provided to monitor the following data at a minimum:
  - circulation flow rate during all testing,
  - SSV/USV valve upstream test pressure during valve seat leakage test, and
  - differential pressure across SSV/USV valve being tested during closure test.
- g) *Data Acquisition System*—A data acquisition system shall be provided to gather electronic data from instrumentation on a time-based system.

### 4.3.2.4 Utility Systems

The manufacturer and test agency shall agree on the utility systems required to operate the SSV/USV and any other associated operating mechanisms.



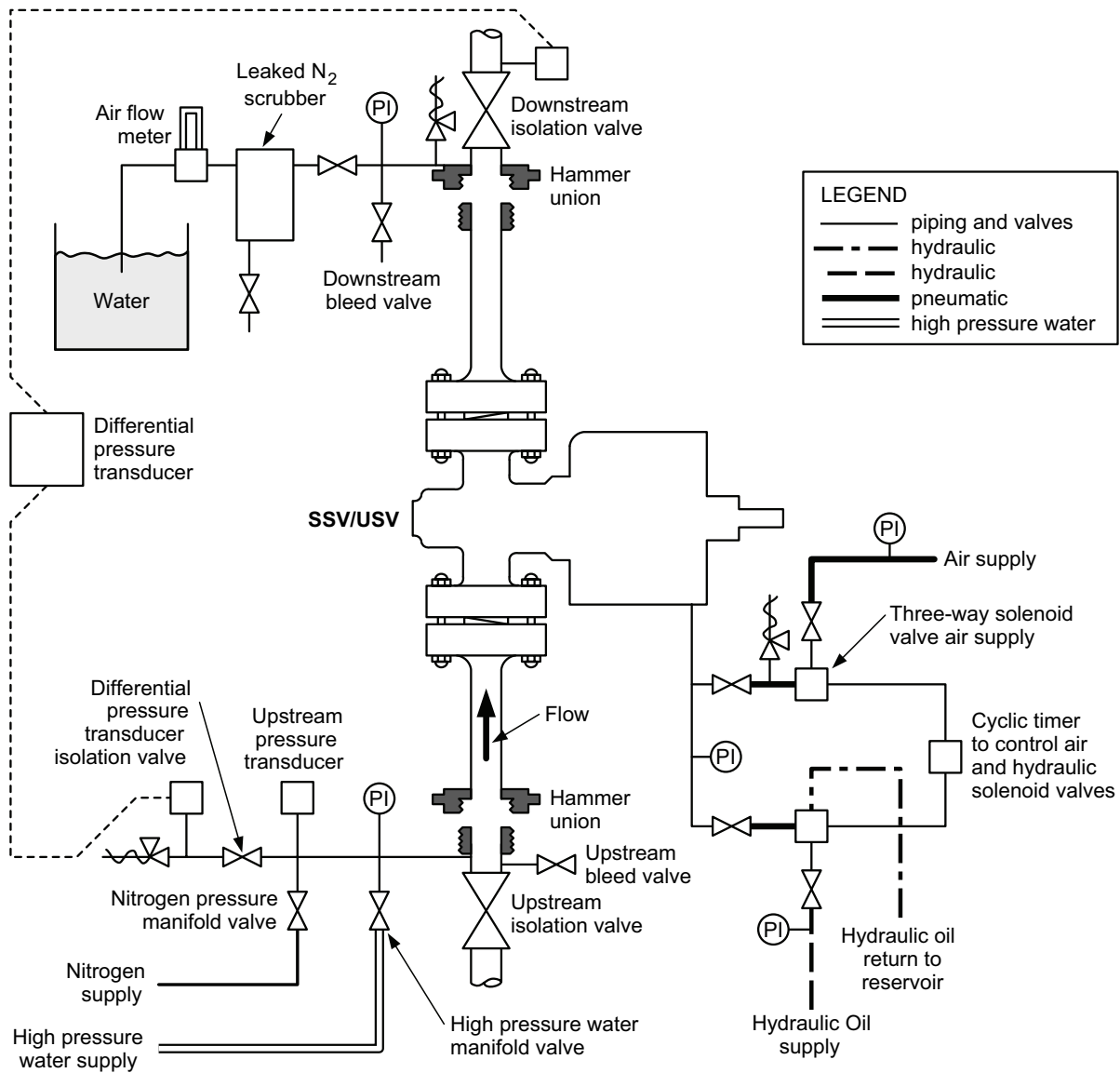
**Figure 1—Example Piping Arrangement—Test Facility for Class II SSV/USV Valve Validation**

## 4.4 Validation—Requirements

### 4.4.1 Class II Requirements for SSV/USV Valve

Unless otherwise noted on the SSV/USV valve manufacturer's application, a 2<sup>1</sup>/<sub>16</sub> in. (52 mm), 5000 psi (34.5 MPa) rated working pressure (RWP) SSV/USV valve shall be used for the validation test.

The SSV/USV valve manufacturer shall provide the test agency with one SSV/USV valve that meets the requirements of and has been tested to API 6A, PSL2, in exact accordance with the data supplied with the



**Figure 2—Example SSV/USV Valve Validation Section Detail**

manufacturer's test application. It shall be completely assembled with an SSV/USV actuator of the SSV/USV valve manufacturer's choice. The SSV/USV shall be furnished with an appropriate operating manual.

If other than a flanged, 2<sup>1</sup>/<sub>16</sub> in. (52 mm) 5000 psi (34.5 MPa) RWP valve, manufacturer shall also furnish to the test agency all piping components necessary to install the SSV/USV in the facility test loop, unless the manufacturer has made other arrangements with the test agency. The test valve may be either a prototype representative of the production model or actual production model.

#### 4.4.2 Class III Requirements for SSV/USV Valve

The SSV/USV valve manufacturer shall provide the test agency with one SSV/USV that meets the requirements of and has been tested to API 6A, PSL3G, in accordance with the data supplied with the manufacturer's test application. It shall

be completely assembled with an SSV/USV actuator of the SSV/USV valve manufacturer's choice. The SSV/USV shall be furnished with an appropriate operating manual.

If other than a flanged, 2<sup>1</sup>/<sub>16</sub> in. (52 mm) 5000 psi (34.5 MPa) RWP valve, manufacturer shall also furnish to the test agency all piping components necessary to install the SSV/USV in the facility test loop, unless the manufacturer has made other arrangements with the test agency. The test valve may be either a prototype representative of the production model or actual production model.

The SSV/USV valve shall be equipped with a provision to monitor stem seal leakage during the testing.

#### 4.4.3 Test Application

The SSV/USV valve manufacturer shall declare that a SSV/USV valve of a specific design and materials of construction is being submitted for the validation test by submitting a formal application to the test agency. The application form shall contain the minimum information shown below. An example of an application form is shown in Table 1.

- Manufacturer's name, address, representative, and contact information.
- Designation of retest or initial test and class of test (Class II or Class III).

SSV/USV Valve Data	SSV/USV Actuator Data
— Manufacturer	— Manufacturer
— Model or catalog number	— Model or catalog number
— Part number	— Part number
— Serial number	— Serial number
— Size and RWP	— Actuator type (pneumatic, hydraulic, other)
— End connections	— RWP
— Special considerations	— Special considerations

- a) If a particular SSV/USV valve has design or operational features that are incompatible with the test facility and test procedures required by this specification, the manufacturer shall advise the test agency of the nature of the incompatibility and shall request and fully describe on the test application, or attachment thereto, any nonspecified equipment or procedures required to test the SSV/USV valve. Responsibility for furnishing and installing nonspecified equipment shall be by agreement between the test agency and the manufacturer. The manufacturer shall document that such nonspecified equipment or procedures are not less stringent than requirements of this specification.
- b) The test agency shall conduct the test as specified on the SSV/USV valve manufacturer's test application. Any variation from the test requirements of this specification shall be prominently recorded in the test report generated by the test agency.

#### 4.4.4 Testing

Conduct the Class II test according to the procedures in 5.2.

Conduct the Class III test according to the procedures in 5.4.

**Table 1—Example Application SSV/USV Valve Validation**

Test Agency \_\_\_\_\_ Manufacturer \_\_\_\_\_  
Address \_\_\_\_\_ Representative \_\_\_\_\_  
\_\_\_\_\_ Address \_\_\_\_\_  
\_\_\_\_\_ Telephone \_\_\_\_\_  
\_\_\_\_\_ Date \_\_\_\_\_

Application for:

Official Qualification Test (Class II or Class III) \_\_\_\_\_ Retest \_\_\_\_\_

**SSV/USV to be Tested****SSV/USV Valve Data:**

Manufacturer \_\_\_\_\_ Model or Cat. No. \_\_\_\_\_ Part Number \_\_\_\_\_  
Serial No. \_\_\_\_\_ Size \_\_\_\_\_ RWP \_\_\_\_\_  
End Connections \_\_\_\_\_  
Special Considerations \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

**SSV/USV Actuator Data:**

Manufacturer \_\_\_\_\_ Model or Cat. No. \_\_\_\_\_ Part Number \_\_\_\_\_  
Serial No. \_\_\_\_\_ RWP \_\_\_\_\_  
Type: Pneumatic \_\_\_\_\_ Hydraulic \_\_\_\_\_ Other \_\_\_\_\_  
Special Considerations \_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_  
\_\_\_\_\_

#### 4.4.5 Test Reporting

The test agency shall record the results of the validation test on forms that contain the minimum data specified below:

- 1) identification of product manufacturer (company name, location/address, etc.);
- 2) if retest, reference to previous test number;
- 3) nonstandard equipment required for testing;
- 4) deviations to the test facility procedures;
- 5) equipment type, model, part number, serial number, size, and RWP;
- 6) test results:
  - a) dates and times at the start and end of all pressure holds and flow rates;
  - b) test pressures applied and notes on leakage;
  - c) person(s) performing the tests;
  - d) sand slurry flow rates;
  - e) sand slurry sand concentration, temperatures, and viscosities at the start and end of tests;
  - f) differential test pressures applied during opening/closing cycles;
  - g) number of opening/closing cycles completed and average cycles per minute;
  - h) type and frequency of preventive maintenance applied;
  - i) notes on any testing problems or difficulties; and
  - j) assessment of test results (pass/fail).

Example forms are shown in Table 2 and Table 3. The results shall be retained by the manufacturer and by the test agency and shall be available to the operator upon request to the manufacturer. Results shall be confidential to the party requesting the test and the test agency.

#### 4.4.6 Assessment

The SSV/USV valve being tested shall successfully complete all steps of the validation test procedure within the limits specified. The validation test cannot continue if the SSV/USV valve fails to perform within specified limits of any step, except when such failures are determined to be a result of actions by the test agency of a malfunction or failure within the test facility. The basis for terminating the validation test, and any unusual conditions observed at or prior to the time of termination, shall be noted on the test data form by the test agency; however, the manufacturer shall be responsible for determining the cause of valve failure.

If an SSV/USV valve fails to meet the requirements of this section, that SSV/USV, or any other SSV/USV valve of the same basic design and materials of construction, shall not be submitted for retest until the SSV/USV valve manufacturer has determined and documented both the need for corrective action and the corrective action taken as specified in API 6A. Such information shall be placed in the manufacturer's test file before that SSV/USV valve is submitted for retest.

**Table 2—Example Class II SSV/USV Valve Test Reporting Form**

Test Report Number \_\_\_\_\_

**I. Tested SSV/USV Valve and SSV/USV Actuator Verification**

	<b>Manufacturer</b>	<b>Model</b>	<b>Type</b>	<b>Part No.</b>	<b>Serial No.</b>	<b>Size</b>	<b>RWP</b>
SSV/USV Valve	_____	_____	_____	_____	_____	_____	_____
SSV/USV Actuator	_____	_____	_____	_____	_____	_____	_____

**II. Initial SSV/USV Valve Seat Leakage Test (Refer to 5.2.1)**

Date \_\_\_\_\_ Time \_\_\_\_\_

Test Performed by \_\_\_\_\_

## 1) Liquid SSV/USV valve seat leakage test

Test Pressure \_\_\_\_\_ psi    Leaked    Yes \_\_\_\_\_    No \_\_\_\_\_

## 2) Nitrogen leakage test

Test Pressure \_\_\_\_\_ psi    Leaked    Yes \_\_\_\_\_    No \_\_\_\_\_

**III. Sand Slurry Flow Test (Refer to 5.2.2)**

Date \_\_\_\_\_ Time \_\_\_\_\_

Test Performed by \_\_\_\_\_

1) \_\_\_\_\_ gpm (m<sup>3</sup>/min) circulation rate of sand slurry.

2) \_\_\_\_\_ % by volume of 40 to 60 US mesh sand in circulating sand slurry.

3) \_\_\_\_\_ seconds, viscosity determined by Marsh funnel viscometer.

4) \_\_\_\_\_ °F (°C) slurry temperature.

5) \_\_\_\_\_ hours of sand slurry circulation.

## 6) a. \_\_\_\_\_ Liquid SSV/USV valve seat leakage test

Test Pressure \_\_\_\_\_ psi    Leaked    Yes \_\_\_\_\_    No \_\_\_\_\_

## b. Nitrogen leakage test

Test Pressure \_\_\_\_\_ psi    Leaked    Yes \_\_\_\_\_    No \_\_\_\_\_

**IV. Sand Slurry Flow Test While Opening and Closing During Circulation (Refer to 5.2.3)**

Date \_\_\_\_\_ Time \_\_\_\_\_

Test Performed by \_\_\_\_\_

1) \_\_\_\_\_ gpm (m<sup>3</sup>/min) circulation rate of sand slurry.

2) \_\_\_\_\_ % by volume of 40 to 60 US mesh sand in circulating sand slurry.

3) \_\_\_\_\_ seconds, viscosity determined by Marsh funnel viscometer.

4) \_\_\_\_\_ °F (°C) slurry temperature.

5) \_\_\_\_\_ psi differential pressure across SSV/USV valve when opened.

6) \_\_\_\_\_ seconds, time for one complete cycle.

7) \_\_\_\_\_ number of SSV/USV cycles.

## 8) a. Liquid SSV/USV valve seat leakage test

Test Pressure \_\_\_\_\_ psi    Leaked    Yes \_\_\_\_\_    No \_\_\_\_\_

## b. Nitrogen leakage test

Test Pressure \_\_\_\_\_ psi    Leaked    Yes \_\_\_\_\_    No \_\_\_\_\_

## 9) a. Type and frequency of preventive maintenance. Describe in detail.

b. Number of cycles completed at last preventive maintenance operation.

**V. SSV/USV Valve Performance Test Certification (to be completed by person performing the test or by test facility designated certifying officer). Remarks—Note any testing problem or difficulties.**

SSV/USV valve qualified for Class II (Yes, No) \_\_\_\_\_

Certified: \_\_\_\_\_

Date: \_\_\_\_\_



**Table 3—Example Class III SSV/USV Valve Test Reporting Form**

Test Report Number \_\_\_\_\_

**I. Tested SSV/USV Valve and SSV/USV Actuator Verification**

	<b>Manufacturer</b>	<b>Model</b>	<b>Type</b>	<b>Part No.</b>	<b>Serial No.</b>	<b>Size</b>	<b>RWP</b>
SSV/USV Valve	_____	_____	_____	_____	_____	_____	_____
SSV/USV Actuator	_____	_____	_____	_____	_____	_____	_____

**II. Initial SSV/USV Valve Seat Leakage Test (Refer to 5.4.1)**

Date \_\_\_\_\_ Time \_\_\_\_\_

Test Performed by \_\_\_\_\_

## 1) Liquid SSV/USV valve seat leakage test

Test Pressure \_\_\_\_\_ psi Leaked Yes \_\_\_\_\_ No \_\_\_\_\_

## 2) Nitrogen leakage test

Test Pressure \_\_\_\_\_ psi Leaked Yes \_\_\_\_\_ No \_\_\_\_\_

**III. Sand Slurry Flow Test (Refer to 5.4.2)**

Date \_\_\_\_\_ Time \_\_\_\_\_

Test Performed by \_\_\_\_\_

1) \_\_\_\_\_ gpm (m<sup>3</sup>/min) circulation rate of sand slurry.

2) \_\_\_\_\_ % by volume of 40 to 60 US mesh sand in circulating sand slurry.

3) \_\_\_\_\_ seconds, viscosity determined by Marsh funnel viscometer.

4) \_\_\_\_\_ °F (°C) slurry temperature.

5) \_\_\_\_\_ hours of sand slurry circulation.

## 6) a. \_\_\_\_\_ Liquid SSV/USV valve seat leakage test

Test Pressure \_\_\_\_\_ psi Leaked Yes \_\_\_\_\_ No \_\_\_\_\_

## b. Nitrogen leakage test

Test Pressure \_\_\_\_\_ psi Leaked Yes \_\_\_\_\_ No \_\_\_\_\_

**IV. Sand Slurry Flow Test While Opening and Closing During Circulation (Refer to 5.4.3)**

Date \_\_\_\_\_ Time \_\_\_\_\_

Test Performed by \_\_\_\_\_

1) \_\_\_\_\_ gpm (m<sup>3</sup>/min) circulation rate of sand slurry.

2) \_\_\_\_\_ % by volume of 40 to 60 US mesh sand in circulating sand slurry.

3) \_\_\_\_\_ seconds, viscosity determined by Marsh funnel viscometer.

4) \_\_\_\_\_ °F (°C) slurry temperature.

5) \_\_\_\_\_ psi differential pressure across SSV/USV valve when opened.

6) \_\_\_\_\_ seconds, time for one complete cycle.

7) \_\_\_\_\_ number of SSV/USV cycles.

## 8) a. Liquid SSV/USV valve seat leakage test

Test Pressure \_\_\_\_\_ psi Leaked Yes \_\_\_\_\_ No \_\_\_\_\_

## b. Nitrogen leakage test

Test Pressure \_\_\_\_\_ psi Leaked Yes \_\_\_\_\_ No \_\_\_\_\_

## 9) a. Type and frequency of preventive maintenance. Describe in detail.

b. Number of cycles completed at last preventive maintenance operation.

V. SSV/USV Valve Performance Test Certification (to be completed by person performing the test or by test facility designated certifying officer). Remarks—Note any testing problem or difficulties.

SSV/USV valve qualified for Class II (Yes, No) \_\_\_\_\_

Certified: \_\_\_\_\_

Date: \_\_\_\_\_

#### 4.4.7 Records

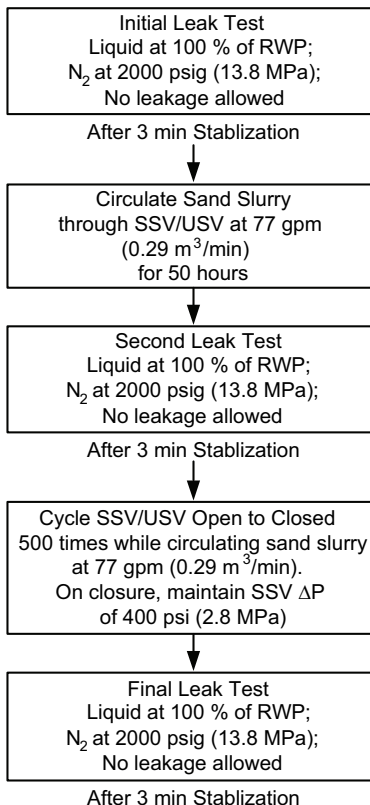
The manufacturer shall maintain a validation file on each test, including any retest that may have been required to qualify a particular SSV/USV valve design and materials of construction. This file shall be available to the operator for inspection upon request and shall be retained by the SSV/USV valve manufacturer for a period of at least 10 years after SSV/USV valves of that design and materials of construction are discontinued from the manufacturer's product line. As a minimum, this file shall contain sufficient documentation to identify and permit retrieval of the following:

- a) all detailed dimensional drawings and material specifications applicable to the tested SSV/USV valve at the time that particular SSV/USV valve was manufactured;
- b) all applications for official test or retest;
- c) all design and material modifications or other justification for retests of SSV/USV valves that did not pass any validation;
- d) all test data specified in this specification; and
- e) model numbers and other pertinent identifying data on all other sizes and RWP of SSV/USV valves of the same basic design and materials of construction that were qualified for Class II or Class III by the validation of this particular SSV/USV valve.

## 5 Test Procedures

### 5.1 Class II Validation Test Summary

The following procedures describe the general requirements for Class II SSV/USV valve validation. Figure 3 summarizes the test in flow diagram format.



**Figure 3—Class II SSV/USV Validation Summary Flow Diagram**

## 5.2 Class II Test Procedure

### 5.2.1 Initial Leakage Test

Perform the initial leakage test per Table 4.

**Warning—High-pressure gas testing involves potential hazards. Appropriate safety precautions should be taken.**

### 5.2.2 Sand Slurry Flow Test

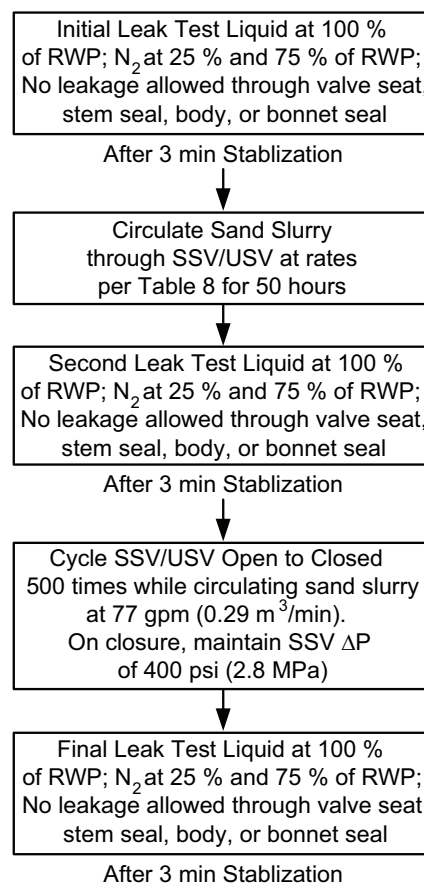
Perform the sand slurry flow test per Table 5 to check for erosion and fouling.

### 5.2.3 Sand Slurry Flow Test While Opening and Closing During Circulation

Perform the sand slurry flow test while opening and closing during circulation per Table 6.

## 5.3 Class III Validation Test Summary

The following procedures describe the general requirements for Class III SSV/USV valve validation. Figure 4 summarizes the test in flow diagram format.



**Figure 4—Class III Validation Summary Flow Diagram**

Table 4—Initial Leakage Test

Step	Procedure Step and Acceptance Criteria	Data to be Recorded
0)	Verify the identification (model and serial number) of the valve and actuator before starting the test.	<ul style="list-style-type: none"> <li>— Valve mfg.</li> <li>— Valve model</li> <li>— Valve part number</li> <li>— Valve serial number</li> <li>— Valve size</li> <li>— Valve RWP</li> <li>— Actuator mfg.</li> <li>— Actuator model</li> <li>— Actuator part number</li> <li>— Actuator serial number</li> <li>— Actuator type</li> <li>— Actuator RWP</li> </ul>
1)	Install SSV/USV in the test section.	
2)	<p>Check SSV/USV valve for leakage with liquid:</p> <p>a) circulate freshwater at a minimum flow rate of 77 gpm (0.29 m<sup>3</sup>/min) but no more than 90 gpm (0.34 m<sup>3</sup>/min) for at least 10 minutes with SSV/USV valve fully open;</p> <p>b) close SSV/USV by releasing actuator power;</p> <p>c) close isolation valves upstream and downstream from SSV/USV;</p> <p>d) open downstream liquid leak detection valve;</p> <p>e) apply water pressure upstream of the SSV/USV equal to 95 % to 105 % of the RWP of the SSV/USV valve; and</p> <p>f) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for SSV/USV valve seat leakage from the downstream leak detection valve for a period of 5 minutes minimum.</p> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<ul style="list-style-type: none"> <li>— Date (month/day/year)</li> <li>— Person performing test</li> </ul> <p><b>Flow Period</b></p> <ul style="list-style-type: none"> <li>— Test start time of flow</li> <li>— Flow rate</li> <li>— Test end time of flow</li> </ul> <p><b>Pressure Holding</b></p> <ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Test passed (yes/no)</li> </ul>
3)	<p>Check SSV/USV valve for leakage with nitrogen pressure:</p> <p>a) close upstream and downstream block valves;</p> <p>b) bleed all pressure and drain water on both sides of SSV/USV valve (open and close SSV/USV valve three times while draining water);</p> <p>c) close SSV/USV;</p> <p>d) with bleed valve open, immerse the end of a flexible tube connected thereto in a container of water;</p> <p>e) apply 2000 psi (13.8 MPa) ±5 % nitrogen on upstream side of SSV/USV valve; and</p> <p>f) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for valve seat leakage by observing for gas bubbles for a period of 5 minutes minimum.</p> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Test passed (yes/no)</li> </ul>

**Table 5—Sand Slurry Flow Test**

Step	Procedure Step and Acceptance Criteria	Data to be Recorded
1)	Circulate sand slurry at a minimum flow rate of 77 gpm (0.29 m <sup>3</sup> /min) while bypassing the test section until slurry viscosity and sand content stabilize with slurry agitator on.	— Date (month/day/year) — Person performing test
2)	Determine sand content of slurry by filling two oil gaugers' 100 ml sample tubes with slurry sample and centrifuge with oil gaugers' centrifuge according to API MPMS Ch. 10.4. The use of solvents and temperature controls are not required. Adjust sand content of circulating fluid to 2 % (1½ % to 2½ % acceptable) by adding 40 to 60 US mesh sand or diluting mixture with freshwater.	— Sand concentration (%)
3)	Determine viscosity of sand slurry sample with Marsh funnel viscometer according to API 13B-1. Adjust viscosity to 100 sec (120 sec maximum and 90 sec minimum) by adding polymer viscosifier or diluting mixture with freshwater.	— Slurry viscosity (sec)
4)	If dilution or strengthening was necessary in Step 3, return to procedure in Step 1.	
5)	Adjust flow rate to a minimum of 77 gpm (0.29 m <sup>3</sup> /min).	— Flow rate at start of circulation period — Slurry viscosity (sec) — Sand concentration (%)
6)	Pump sand slurry through SSV/USV valve for 25 hours (±1 hour).	— Time at start of slurry circulation through valve — Time at end of slurry circulation through valve
7)	Check sand content and viscosity of slurry as before in Step 2 and Step 3; adjust as required.	— Slurry viscosity (sec) — Sand concentration (%)
8)	Pump sand slurry through SSV/USV valve for an additional 25 hours (±1 hour) at a minimum flow rate of 77 gpm (0.29 m <sup>3</sup> /min). The total duration of the flow periods in Step 6 and Step 8 shall be a minimum of 50 hours.	— Time at start of slurry circulation through valve — Flow rate at start of circulation period — Time at end of slurry circulation through valve
9)	Check SSV/USV valve for leakage with liquid: a) close SSV/USV by releasing actuator power; b) close isolation valves upstream and downstream from SSV/USV; c) open downstream liquid leak detection valve; d) apply water pressure upstream of the SSV/USV equal to 95 % to 105 % of the RWP of the SSV/USV valve; and e) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for SSV/USV valve seat leakage from the downstream leak detection valve for a period of 5 minutes minimum. <b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.	— Date (month/day/year) — Person performing test <b>Pressure Holding</b> — Test start time of pressure monitoring — Test end time of pressure monitoring — Pressure at start of test — Pressure at end of test — Test passed (yes/no)
10)	Check SSV/USV valve for leakage with nitrogen pressure: a) close upstream and downstream block valves; b) bleed all pressure and drain water on both sides of SSV/USV valve (open and close SSV/USV valve three times while draining water); c) close SSV/USV; d) with bleed valve open, immerse the end of a flexible tube connected thereto in a container of water; e) apply 2000 psi (13.8 MPa) ±5 % nitrogen on upstream side of SSV/USV valve; and f) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for valve seat leakage by observing for gas bubbles for a period of 5 minutes minimum. <b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.	— Test start time of pressure monitoring — Test end time of pressure monitoring — Pressure at start of test — Pressure at end of test — Test passed (yes/no)

**Table 6—Sand Slurry Flow Test While Opening and Closing During Circulation**

Step	Procedure Step and Acceptance Criteria	Data to be Recorded
1)	Circulate sand slurry at a minimum flow rate of 77 gpm (0.29 m <sup>3</sup> /min) while bypassing the test section until slurry viscosity and sand content stabilize with slurry agitator on.	<ul style="list-style-type: none"> <li>— Date (month/day/year)</li> <li>— Person performing test</li> </ul>
2)	Determine sand content of slurry by filling two oil gauger's, 100 ml sample tubes with slurry samples. Centrifuge with oil gauger's centrifuge according to API MPMS Ch.10.4. The use of solvents and temperature controls are not required. Adjust sand content to 2 % (1.5 % to 2.5 % acceptable) by adding 40 to 60 US mesh sand or diluting mixture with freshwater.	<ul style="list-style-type: none"> <li>— Sand concentration (%)</li> </ul>
3)	Determine viscosity of slurry sample with Marsh funnel viscometer according to API 13B-1. Adjust viscosity to 100 sec (120 sec maximum, 90 sec minimum) by adding polymer viscosifier or diluting mixture with freshwater.	<ul style="list-style-type: none"> <li>— Slurry viscosity (sec)</li> </ul>
4)	If dilution or strengthening was necessary in Step 3, return to procedure in Step 1.	
5)	Adjust flow rate to a minimum of 77 gpm (0.29 m <sup>3</sup> /min).	<ul style="list-style-type: none"> <li>— Flow rate at start of circulation period</li> <li>— Slurry viscosity (sec)</li> <li>— Sand concentration (%)</li> </ul>
6)	Cycle SSV/USV valve from fully opened to fully closed at a maximum rate of 7 cycles per minute.	
7)	Adjust choke (or equivalent) upstream from SSV/USV valve to provide a differential pressure of 400 psi (2.8 MPa) $\pm$ 10 % across the SSV/USV valve when closed.	<ul style="list-style-type: none"> <li>— Differential pressure across valve when closed (psi)</li> </ul>
8)	Open and close SSV/USV a minimum of 500 cycles but no more than 510 cycles. During this phase of testing, normal preventive maintenance procedures, if any, as prescribed in the manufacturer's operating manual, shall be performed except that no preventive maintenance shall be allowed during the last 100 cycles of operation in the test and during Step 9 and Step 10.	<ul style="list-style-type: none"> <li>— Number of cycles</li> <li>— Cycles per minute (nominal)</li> <li>— Type and frequency of maintenance performed (list)</li> </ul>
9)	<p>Check SSV/USV valve for leakage with fresh water:</p> <ul style="list-style-type: none"> <li>a) close SSV/USV by releasing actuator power;</li> <li>b) close isolation valves upstream and downstream from SSV/USV;</li> <li>c) open downstream liquid leak detection valve;</li> <li>d) apply water pressure upstream of the SSV/USV equal to 95 % to 105 % of the RWP of the SSV/USV valve; and</li> <li>e) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for SSV/USV valve seat leakage from the downstream leak detection valve for a period of 5 minutes minimum.</li> </ul> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<ul style="list-style-type: none"> <li>— Date (month/day/year)</li> <li>— Person performing test</li> </ul> <p><b>Pressure Holding</b></p> <ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Test passed (yes/no)</li> </ul>
10)	<p>Check SSV/USV valve for leakage with nitrogen pressure:</p> <ul style="list-style-type: none"> <li>a) close upstream and downstream block valves;</li> <li>b) bleed all pressure and drain water on both sides of SSV/USV valve (open and close SSV/USV valve three times while draining water);</li> <li>c) close SSV/USV;</li> <li>d) with bleed valve open, immerse the end of a flexible tube connected thereto in a container of water;</li> <li>e) apply 2000 psi (13.8 MPa) <math>\pm</math>5 % nitrogen on upstream side of SSV/USV valve; and</li> <li>f) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for valve seat leakage by observing for gas bubbles for a period of 5 minutes minimum.</li> </ul> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Test passed (yes/no)</li> </ul>

## 5.4 Class III Test Procedure

### 5.4.1 Initial Leakage Test

Perform the initial leakage test per Table 7.

**Warning—High-pressure gas testing involves potential hazards. Appropriate safety precautions should be taken.**

**Table 7—Initial Leakage Test**

Step	Procedure Step and Acceptance Criteria	Data to be Recorded
0)	Verify the identification (model and serial number) of the valve and actuator before starting the test.	<ul style="list-style-type: none"> <li>— Valve mfg.</li> <li>— Valve model</li> <li>— Valve part number</li> <li>— Valve serial number</li> <li>— Valve size</li> <li>— Valve RWP</li> <li>— Actuator mfg.</li> <li>— Actuator model</li> <li>— Actuator part number</li> <li>— Actuator serial number</li> <li>— Actuator type</li> <li>— Actuator RWP</li> </ul>
1)	Install SSV/USV in the test section.	
2)	<p>Check SSV/USV valve for leakage with liquid:</p> <ul style="list-style-type: none"> <li>a) circulate freshwater at a minimum flow rate of 77 gpm (0.29 m<sup>3</sup>/min) but no more than 90 gpm (0.34 m<sup>3</sup>/min) for at least 10 minutes with SSV/USV valve fully open;</li> <li>b) close SSV/USV by releasing actuator power;</li> <li>c) close isolation valves upstream and downstream from SSV/USV;</li> <li>d) open downstream liquid leak detection valve;</li> <li>e) apply water pressure upstream of the SSV/USV equal to 95 % to 105 % of the RWP of the SSV/USV valve; and</li> <li>f) after the pressure has stabilized within the specified range for 3 minutes minimum, check for SSV/USV valve seat, stem seal, body, and bonnet seal leakage for a period of 5 minutes minimum.</li> </ul> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<ul style="list-style-type: none"> <li>— Validation test number</li> <li>— Date (month/day/year)</li> </ul> <p><b>Flow Period</b></p> <ul style="list-style-type: none"> <li>— Test start time of flow</li> <li>— Flow rate</li> <li>— Test end time of flow</li> </ul> <p><b>Pressure Holding</b></p> <ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Leakage location (if any)</li> <li>— Test passed (yes/no)</li> </ul>
3)	<p>Check SSV/USV valve for leakage with nitrogen pressure:</p> <ul style="list-style-type: none"> <li>a) close upstream and downstream block valves;</li> <li>b) bleed all pressure and drain water on both sides of SSV/USV valve (open and close SSV/USV valve three times while draining water);</li> <li>c) close SSV/USV;</li> <li>d) with bleed valve open, immerse the end of a flexible tube connected thereto in a container of water;</li> <li>e) apply 25 % of RWP <math>\pm</math> 5 % using nitrogen on upstream side of SSV/USV valve; and</li> <li>f) after the pressure has stabilized within the specified range for 3 minutes minimum, check for valve seat, stem seal, body, and bonnet seal leakage by observing for gas bubbles for a period of 5 minutes minimum.</li> </ul> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p> <ul style="list-style-type: none"> <li>g) apply 75 % of RWP <math>\pm</math> 5 % using nitrogen on upstream side of SSV/USV valve; and</li> <li>h) after the pressure has stabilized within the specified range for 3 minutes minimum, check for valve seat stem seal, body, and bonnet seal leakage by observing for gas bubbles for a period of 5 minutes minimum.</li> </ul> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<p><b>25 % RWP Test</b></p> <ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Leakage location (if any)</li> <li>— Test passed (yes/no)</li> </ul> <p><b>75 % RWP Test</b></p> <ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Leakage location (if any)</li> <li>— Test passed (yes/no)</li> </ul>

## 5.4.2 Sand Slurry Flow Test

### 5.4.2.1 Sand slurry composition

The sand slurry composition for the Class III test shall meet the following requirements:

- 1) sand content of 1.5 % to 2.5 % by volume and
- 2) sand mixture shall be equal quantities by volume of 20/40, 40/60, and 80/100 US mesh sand.

### 5.4.2.2 Sand Slurry flow rate

The Class III sand slurry flow rate shall obtain a flow velocity greater than or equal to the flow velocity through a  $2^{1/16}$  valve at 77 gpm (7.4 ft/sec). Based on a flow rate of 77 gpm for a  $2^{1/16}$  valve size, Table 8 lists the minimum flow rates for other common valve sizes.

**Table 8—Class III Sand Slurry Flow Rates**

Valve Size (nominal ID)	Slurry Flow Rate (gpm)	Slurry Flow Rate (bpm)
2.06	77	1.8
2.56	119	2.8
3.12	177	4.2
3.19	185	4.4
4.06	299	7.1
4.12	308	7.3
4.25	328	7.8
5.12	476	11.3
6.00	653	15.6
6.12	680	16.2
6.38	739	17.6
6.62	795	18.9
7.06	904	21.5
7.12	920	21.9
9.00	1470	35.0



### 5.4.2.3 Test Method

Perform the sand slurry flow test per Table 9.

**Table 9—Class III Sand Slurry Flow Test**

Step	Procedure Step and Acceptance Criteria	Data to be Recorded
1)	Circulate sand slurry while bypassing the test section until slurry viscosity and sand content stabilize with slurry agitator on.	— Date (month/day/year) — Person performing test
2)	Determine sand content of slurry by filling two oil gaugers' 100 ml sample tubes with slurry sample and centrifuge with oil gaugers' centrifuge according to API MPMS Ch. 10.4. The use of solvents and temperature controls are not required. Adjust sand content of circulating fluid to 2 % (1½ % to 2½ % acceptable) by adding sand mixture or diluting slurry with freshwater.	— Sand concentration (%)
3)	Determine viscosity of sand slurry sample with Marsh funnel viscometer according to API 13B-1. Adjust viscosity to 70 sec (75 sec maximum and 65 sec minimum) by adding polymer viscosifier or diluting slurry with freshwater.	— Slurry viscosity (sec)
4)	If dilution or strengthening was necessary in Step 3, return to procedure in Step 1.	
5)	Adjust flow rate to a minimum per Table 8 corresponding to valve size.	— Flow rate at start of circulation period — Slurry viscosity (sec) — Sand concentration (%)
6)	Pump sand slurry through SSV/USV valve for 25 hours (±1 hour).	— Time at start of slurry circulation through valve — Time at end of slurry circulation through valve
7)	Check sand content and viscosity of slurry as before in Step 2 and Step 3; adjust as required.	— Slurry viscosity (sec) — Sand concentration (%)
8)	Pump sand slurry through SSV/USV valve for an additional 25 hours (±1 hour) at a minimum flow rate per Table 8 corresponding to valve size. The total duration of the flow periods in Step 6 and Step 8 shall be a minimum of 50 hours.	— Time at start of slurry circulation through valve — Flow rate at start of circulation period — Time at end of slurry circulation through valve
9)	Check SSV/USV valve for leakage with fresh water: a) close SSV/USV by releasing actuator power; b) close isolation valves upstream and downstream from SSV/USV; c) open downstream liquid leak detection valve; d) apply water pressure upstream of the SSV/USV equal to 95 % to 105 % of the RWP of the SSV/USV valve; and e) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for SSV/USV valve seat, stem seal, body, and bonnet seal leakage for a period of 5 minutes minimum.  <b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.	— Validation test number — Date (month/day/year)  <b>Pressure Holding</b> — Test start time of pressure monitoring — Test end time of pressure monitoring — Pressure at start of test — Pressure at end of test — Leakage location (if any) — Test passed (yes/no)

**Table 9—Class III Sand Slurry Flow Test (Continued)**

Step	Procedure Step and Acceptance Criteria	Data to be Recorded
10)	<p>Check SSV/USV valve for leakage with nitrogen pressure:</p> <p>a) close upstream and downstream block valves;</p> <p>b) bleed all pressure and drain water on both sides of SSV/USV valve (open and close SSV/USV valve three times while draining water);</p> <p>c) close SSV/USV;</p> <p>d) with bleed valve open, immerse the end of a flexible tube connected thereto in a container of water;</p> <p>e) apply 25 % of RWP <math>\pm 5</math> % using nitrogen on upstream side of SSV/USV valve; and</p> <p>f) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for valve seat, stem seal, body, and bonnet seal leakage by observing for gas bubbles for a period of 5 minutes minimum.</p> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p> <p>g) apply 75 % of RWP <math>\pm 5</math> % using nitrogen on upstream side of SSV/USV valve; and</p> <p>h) after the pressure has stabilized for 3 minutes minimum, check for valve seat, stem seal, body, and bonnet seal leakage by observing for gas bubbles for a period of 5 minutes minimum.</p> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<p><b>25 % RWP Test</b></p> <ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Leakage location (if any)</li> <li>— Test passed (yes/no)</li> </ul> <p><b>75 % RWP Test</b></p> <ul style="list-style-type: none"> <li>— Test start time of pressure monitoring</li> <li>— Test end time of pressure monitoring</li> <li>— Pressure at start of test</li> <li>— Pressure at end of test</li> <li>— Leakage location (if any)</li> <li>— Test passed (yes/no)</li> </ul>

#### 5.4.3 Sand Slurry Flow Test While Opening and Closing During Circulation

Perform the sand slurry flow test while opening and closing during circulation per Table 10.

**Table 10—Sand Slurry Flow Test While Opening and Closing During Circulation**

Step	Procedure Step and Acceptance Criteria	Data to be Recorded
1)	Circulate sand slurry while bypassing the test section until slurry viscosity and sand content stabilize with slurry agitator on.	<ul style="list-style-type: none"> <li>— Date (month/day/year)</li> <li>— Person performing test</li> </ul>
2)	Determine sand content of slurry by filling two oil gauger's, 100 ml sample tubes with slurry samples. Centrifuge with oil gauger's centrifuge according to API MPMS Ch. 10.4. The use of solvents and temperature controls are not required. Adjust sand content to 2 % (1.5 % to 2.5 % acceptable) by adding sand mixture or diluting slurry with freshwater.	<ul style="list-style-type: none"> <li>— Sand concentration (%)</li> </ul>
3)	Determine viscosity of slurry sample with Marsh funnel viscometer according to API 13B-1. Adjust viscosity to 70 sec (75 sec maximum, 65 sec minimum) by adding polymer viscosifier or diluting mixture with freshwater.	<ul style="list-style-type: none"> <li>— Slurry viscosity (sec)</li> </ul>
4)	If dilution or strengthening was necessary in Step 3, return to procedure in Step 1.	
5)	Adjust flow rate to a minimum of 77 gpm (0.29 m <sup>3</sup> /min).	<ul style="list-style-type: none"> <li>— Flow rate at start of circulation period</li> <li>— Slurry viscosity (sec)</li> <li>— Sand concentration (%)</li> </ul>
6)	Cycle SSV/USV valve from fully opened to fully closed at a maximum rate of 7 cycles per minute.	
7)	Adjust choke (or equivalent) upstream from SSV/USV valve to provide a differential pressure of 400 psi (2.8 MPa) $\pm 10$ % across the SSV/USV valve when closed.	<ul style="list-style-type: none"> <li>— Differential pressure across valve when closed (psi)</li> </ul>
8)	Open and close SSV/USV a minimum of 500 cycles but no more than 510 cycles. During this phase of testing, normal preventive maintenance procedures, if any, as prescribed in the manufacturer's operating manual, shall be performed except that no preventive maintenance shall be allowed during the last 100 cycles of operation in the test and during Step 9 and Step 10.	<ul style="list-style-type: none"> <li>— Number of cycles</li> <li>— Cycles per minute (nominal)</li> <li>— Type and frequency of maintenance performed (list)</li> </ul>

**Table 10—Sand Slurry Flow Test While Opening and Closing During Circulation (Continued)**

Step	Procedure Step and Acceptance Criteria	Data to be Recorded
9)	<p>Check SSV/USV valve for leakage with fresh water:</p> <p>a) close SSV/USV by releasing actuator power;</p> <p>b) close isolation valves upstream and downstream from SSV/USV;</p> <p>c) open downstream liquid leak detection valve;</p> <p>d) apply water pressure upstream of the SSV/USV equal to 95 % to 105 % of the RWP of the SSV/USV valve; and</p> <p>e) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for SSV/USV valve seat, stem seal, body, and bonnet seal leakage for a period of 5 minutes minimum.</p> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<p>— Validation test number</p> <p>— Date (month/day/year)</p> <p><b>Pressure Holding</b></p> <p>— Test start time of pressure monitoring</p> <p>— Test end time of pressure monitoring</p> <p>— Pressure at start of test</p> <p>— Pressure at end of test</p> <p>— Leakage location (if any)</p> <p>— Test passed (yes/no)</p>
10)	<p>Check SSV/USV valve for leakage with nitrogen pressure:</p> <p>a) close upstream and downstream block valves;</p> <p>b) bleed all pressure and drain water on both sides of SSV/USV valve (open and close SSV/USV valve three times while draining water);</p> <p>c) close SSV/USV;</p> <p>d) with bleed valve open, immerse the end of a flexible tube connected thereto in a container of water;</p> <p>e) apply 25 % of RWP <math>\pm 5</math> % using nitrogen on upstream side of SSV/USV valve; and</p> <p>f) after the pressure has stabilized within the acceptable range for 3 minutes minimum, check for valve seat, stem seal, body, and bonnet seal leakage by observing for gas bubbles for a period of 5 minutes minimum.</p> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p> <p>g) apply 75 % of RWP <math>\pm 5</math> % using nitrogen on upstream side of SSV/USV valve; and</p> <p>h) after the pressure has stabilized for 3 minutes minimum, check for valve seat, stem seal, body, and bonnet seal leakage by observing for gas bubbles for a period of 5 minutes minimum.</p> <p><b>Acceptance Criteria:</b> No visible leakage shall occur during the 5 minute hold period.</p>	<p><b>25 % RWP Test</b></p> <p>— Test start time of pressure monitoring</p> <p>— Test end time of pressure monitoring</p> <p>— Pressure at start of test</p> <p>— Pressure at end of test</p> <p>— Leakage location (if any)</p> <p>— Test passed (yes/no)</p> <p><b>75 % RWP Test</b></p> <p>— Test start time of pressure monitoring</p> <p>— Test end time of pressure monitoring</p> <p>— Pressure at start of test</p> <p>— Pressure at end of test</p> <p>— Leakage location (if any)</p> <p>— Test passed (yes/no)</p>

## 6 Scaling of Test Results

### 6.1 Scaling of Class II Validation Results

Successful completion of the validation test on a 2<sup>1</sup>/<sub>16</sub> in. (52 mm), 5000 psi (34.5 MPa) RWP SSV/USV valve shall qualify all sizes and all pressure ratings of that manufacturer's SSV/USV valves of the same basic design and materials of construction for Class II service.

Successful completion of the validation test on a size or pressure rating other than 2<sup>1</sup>/<sub>16</sub> in. (52 mm), 5000 psi (34.5 MPa) RWP SSV/USV valve shall qualify that size and larger for all pressure ratings of that manufacturer's SSV/USV valves of the same basic design and materials of construction for Class II service.

Any substantive change in the design or materials of construction that would affect the SSV/USV valve bore sealing mechanism shall require requalification by validation testing.

### 6.2 Scaling of Class III Validation Results

#### 6.2.1 General

Scaling may be used to validate the members of a product family in accordance with the requirements and limitations described in this section.

NOTE The intent of this section is to limit scaling due to the uncertainties associated with solids deposition and throttling flow during cycling of the valve.

### **6.2.2 Product Family**

A product family shall meet the following design requirements.

- The design principles of physical configuration and functional operation are the same.
- The allowable design stress levels in relation to material mechanical properties are based on the same criteria.

### **6.2.3 Limitations of Scaling**

#### **6.2.3.1 Design Validation by Pressure Rating**

The test product may be used to validate products of the same product family having equal or lower pressure ratings.

#### **6.2.3.2 Design Validation by Size**

Testing of one size of a product family shall validate products one nominal size larger and one nominal size smaller than the tested size. Testing of two sizes of a product family also validates all nominal sizes between the two sizes tested and the sizes one nominal size larger and one nominal size smaller than the tested size (if applicable). The valve nominal size shall be defined as the nominal size of the end connections, as defined in API 6A. For valves of the same product family, the  $1^{13/16}$  and  $2^{1/16}$  sizes (46 mm and 52 mm) may be considered as one size for scaling purposes.

### **6.2.4 Design Validation by PSL**

Validation of equipment is independent of the PSL of the production equipment.

## **Annex A** **(informative)**

### **API Monogram Program**

#### **A.1 Scope**

The API Monogram® is a registered certification mark owned by the American Petroleum Institute (API) and authorized for licensing by the API Board of Directors. Through the API Monogram Program, API licenses product manufacturers to apply the API Monogram to products which comply with product specifications and have been manufactured under a quality management system that meets the requirements of API Q1. API maintains a complete, searchable list of all Monogram licensees on the API Composite List website ([www.api.org/compositelist](http://www.api.org/compositelist)).

The application of the API Monogram and license number on products constitutes a representation and warranty by the licensee to API and to purchasers of the products that, as of the date indicated, the products were manufactured under a quality management system conforming to the requirements of API Q1 and that the product conforms in every detail with the applicable standard(s) or product specification(s). API Monogram program licenses are issued only after an on-site audit has verified that an organization has implemented and continually maintained a quality management system that meets the requirements of API Q1 and that the resulting products satisfy the requirements of the applicable API product specification(s) and/or standard(s). Although any manufacturer may claim that its products meet API product requirements without monogramming them, only manufacturers with a license from API can apply the API Monogram to their products.

Together with the requirements of the API Monogram license agreement, this annex establishes the requirements for those organizations who wish to voluntarily obtain an API license to provide API monogrammed products that satisfy the requirements of the applicable API product specification(s) and/or standard(s) and API Monogram Program requirements.

For information on becoming an API Monogram Licensee, please contact API, Certification Programs, 1220 L Street, N. W., Washington, DC 20005 or call 202-682-8145 or by email at [certification@api.org](mailto:certification@api.org).

#### **A.2 References**

In addition to the referenced standards listed earlier in this document, this annex references the following standard:

API Specification Q1, *Specification for Quality Management System Requirements for Manufacturing Organizations for the Petroleum and Natural Gas Industry*

ISO/IEC 17025, *General Requirements for the Competence of Testing and Calibration Laboratories*

For Licensees under the Monogram Program, the latest version of this document shall be used. The requirements identified therein are mandatory.

#### **A.3 API Monogram Marking Requirements**

These marking requirements apply only to those API Licensees wishing to apply the API Monogram.

There are no specific marking requirements for the API Monogram on API 6AV1 test reports.

Application of the API Monogram shall be per the manufacturer's procedures as specified in API Specification Q1, which requires marking of the license number and date of original manufacture.

## **A.4 Test Agency License Criteria**

### **A.4.1 Independence**

The test agency performing validation testing must meet the requirements of API 6AV1. In addition, for compliance with these API Monogram Program requirements, the test agency must be an independent third party and must be licensed by API in order to test SSVs or USVs that are intended to be marked with the API Monogram.

### **A.4.2 Quality Program Requirements**

Laboratories desiring license under this annex shall have a functional quality program in accordance with ISO/IEC 17025 and the requirements of API Q1 except for the requirements related to Design and Development, Control of Production and Service, and Release of Nonconforming Product under Concession. All remaining requirements of API Q1 shall apply. Laboratories desiring licensing under this annex shall make application, pay applicable fees and undergo audits (both scheduled and unscheduled) per program procedures. API shall maintain a list of licensed laboratories, which shall appear in the API Composite List of manufacturers licensed for use of the API Monogram. Removal of the laboratory from the API Composite List shall occur for failure to meet the requirements of the API Monogram Program such as not satisfying audit obligations or for failure to pay applicable program fees.

### **A.4.3 Use of the API Monogram in Advertising**

Licensee shall not use the API Monogram on letterheads or in any advertising (including company-sponsored web sites) without an express statement of fact describing the scope of Licensee's authorization (license number). The Licensee should contact API for guidance on the use of the API Monogram other than on products.

## **A.5 Capability**

The API Monogram Program is designed to identify facilities that have demonstrated the ability to manufacture equipment or provide testing services that conform to API specifications and/or standards. API may refuse initial licensing or suspend current licensing based on a facility's level of manufacturing or testing capability. If API determines that additional review is warranted, API may perform additional audits (at the organization's expense) of any subcontractors to ensure their compliance with the requirements of the applicable API product specification(s) and/or standard(s).

## **A.6 API Monogram Program: Nonconformance Reporting**

API solicits information on nonconformances associated with API specified requirements, as well as field failures (or malfunctions), which are judged to be caused by either specification deficiencies or nonconformities with API specified requirements. Customers are requested to report to API all problems with API monogrammed products. A nonconformance may be reported using the API Nonconformance Reporting System available at <http://compositelist.api.org/ncr.asp>.

## Bibliography

- [1] *API Manual of Petroleum Measurement Standards (MPMS) Chapter 15, Guidelines for Use of the International System of Units (SI) in the Petroleum and Allied Industries*
- [2] *API Specification 14D, Wellhead Surface Safety Valves for Offshore Service*





# THERE'S MORE WHERE THIS CAME FROM

## REQUEST A QUOTATION

[www.api.org/quote](http://www.api.org/quote)

### **API Monogram® Licensing Program**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [certification@api.org](mailto:certification@api.org)  
Web: [www.api.org/monogram](http://www.api.org/monogram)

### **API Quality Registrar (APIQR®)**

- ISO 9001
- ISO/TS 29001
- ISO 14001
- OHSAS 18001
- API Spec Q1®
- API Spec Q2®
- API QualityPlus®
- Dual Registration

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [certification@api.org](mailto:certification@api.org)  
Web: [www.api.org/apiqr](http://www.api.org/apiqr)

### **API Training Provider Certification Program (TPCP®)**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [tpcp@api.org](mailto:tpcp@api.org)  
Web: [www.api.org/tpcp](http://www.api.org/tpcp)

### **API Individual Certification Programs (ICP®)**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [icp@api.org](mailto:icp@api.org)  
Web: [www.api.org/icp](http://www.api.org/icp)

### **API Engine Oil Licensing and Certification System (EOLCS)**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [eolcs@api.org](mailto:eolcs@api.org)  
Web: [www.api.org/eolcs](http://www.api.org/eolcs)

### **Motor Oil Matters**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [motoroilmatters@api.org](mailto:motoroilmatters@api.org)  
Web: [www.motoroilmatters.org](http://www.motoroilmatters.org)

### **API Diesel Exhaust Fluid Certification Program**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [apidef@api.org](mailto:apidef@api.org)  
Web: [www.apidef.org](http://www.apidef.org)

### **API Perforator Design Registration Program**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [perfdesign@api.org](mailto:perfdesign@api.org)  
Web: [www.api.org/perforators](http://www.api.org/perforators)

### **API WorkSafe®**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [apiworksafe@api.org](mailto:apiworksafe@api.org)  
Web: [www.api.org/worksafe](http://www.api.org/worksafe)

### **API-U™**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [training@api.org](mailto:training@api.org)  
Web: [www.api-u.org](http://www.api-u.org)

### **API Data®**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Service: (+1) 202-682-8042  
Email: [data@api.org](mailto:data@api.org)  
Web: [www.APIDataNow.org](http://www.APIDataNow.org)

### **API Publications**

Phone: 1-800-854-7179  
(Toll-free U.S. and Canada)  
(+1) 303-397-7956  
(Local and International)  
Fax: (+1) 303-397-2740  
Web: [www.api.org/pubs](http://www.api.org/pubs)  
[global.ihs.com](http://global.ihs.com)

### **API Standards**

Sales: 877-562-5187  
(Toll-free U.S. and Canada)  
(+1) 202-682-8041  
(Local and International)  
Email: [standards@api.org](mailto:standards@api.org)  
Web: [www.api.org/standards](http://www.api.org/standards)



AMERICAN PETROLEUM INSTITUTE



AMERICAN PETROLEUM INSTITUTE

1220 L Street, NW  
Washington, DC 20005-4070  
USA

202-682-8000

**Additional copies are available online at [www.api.org/pubs](http://www.api.org/pubs)**

Phone Orders: 1-800-854-7179 (Toll-free in the U.S. and Canada)  
303-397-7956 (Local and International)  
Fax Orders: 303-397-2740

Information about API publications, programs and services is available  
on the web at [www.api.org](http://www.api.org).

**Product No. G6AV102**