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HEALTH AND ENVIRONMENTAL AFFAIRS DEPARTMENT

API PUBLICATION NUMBER 332

AUGUST 1995

# Comparison of Screening Values from Selected Hydrocarbon Screening Instruments





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# Comparison of Screening Values from Selected Hydrocarbon Screening Instruments

Health and Environmental Affairs Department

**API PUBLICATION NUMBER 332** 

PREPARED UNDER CONTRACT BY: RADIAN CORPORATION 10389 OLD PLACERVILLE ROAD SACRAMENTO, CA 95827

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Julian Blomley, UNOCAL

Miriam Lev-On, ARCO Products Company

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## ABSTRACT

Fugitive emissions from leaking equipment are being monitored by refineries, chemical plants, petroleum marketing terminals and oil and gas production operations. Different instruments, each capable of measuring the fugitive hydrocarbon emissions, or screening values, are being utilized by different studies. The measurement distance to hold the screening instrument from the point of maximum leak also differs for different facilities.

This study evaluated the differences in screening values for the following four different screening instruments:

- Foxboro Organic Vapor Analyzer (OVA) 108;
- Bacharach Threshold Limit Value Sniffer (TLV Sniffer<sup>®</sup>);
- HNU<sup>®</sup> PI-101; and
- Foxboro Total Vapor Analyzer (TVA) 1000, both flame ionization detector (FID) and photo ionization detector (PID).

This study showed that there were differences in screening values for a particular component based on using the different screening instruments. Adjustment factors, or correlation equations, were developed to allow screening values from the TLV Sniffer<sup>®</sup>, and the TVA FID to be converted to comparable OVA screening values. Adjustment factors were not developed relating HNU<sup>®</sup> or TVA PID screening values to OVA screening values because inadequate correlations were found between these screening values.

This study also evaluated the differences in screening values for these screening instruments based on screening as close as possible to the surface of a component at the point of maximum leak versus screening 1 cm away from the component at the point of maximum leak. This study showed that there are differences in screening values if the screening instrument is held at 1 cm away compared to holding the instrument as close as possible to the surface. An adjustment factor, or correlation equation, was developed to convert screening values from the OVA screening instrument using a 1 cm spacer basis to an "at the surface" basis.

Please note that other screening instruments, not studied in this report, may be available.

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A 1979 study on screening distance effects and screening instrument effects was compared to the results of this study. Both studies show comparable differences between the OVA and TLV Sniffer<sup>®</sup> screening values; however, the screening distance differences were more pronounced in the 1979 study than in this study. The reason for the differences in screening distance results is unknown. These differences could be due to screening techniques, in ambient conditions, or in differences in instrument sensitivities.

An analysis was performed to determine other factors that may affect the relationship between screening values. Insignificant, or minimally significant effects were observed for windspeed, component type and service type.

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### EXECUTIVE SUMMARY

Fugitive emissions from leaking equipment are being monitored by refineries, chemical companies, and petroleum marketing terminals. Several different instruments, each capable of measuring the fugitive hydrocarbon emissions, or screening values, are being utilized by these facilities. Furthermore, the distance that the screening instrument is held from the surface of the component at the point where the primary leak is measured can vary depending on local practices, the potential for probe-tip contamination, and/or the prescence of rotating parts. To investigate these differences, the Western States Petroleum Association (WSPA) and the American Petroleum Institute (API) commissioned this study.

Specifically, this study's objectives were to:

- Develop a correlation equation for converting screening instrument measurements from other analyzers' to the Foxboro Organic Vapor Analyzer (OVA) 108 measurements by collecting side by side screening measurements from four different screening instruments:
  - Foxboro OVA 108,
  - Bacharach Threshold Limit Value Sniffer (TLV Sniffer<sup>®</sup>),
  - HNU® PI-101, and
  - Foxboro Total Vapor Analyzer (TVA) 1000, both flame ionization detector (FID) and photo ionization detector (PID).
- Develop a correlation equation converting screening measurements made at a distance of 1 cm to screening done as close as possible to the surface.

These correlation equations enable facilities that collect data with different instruments and different screening distances to convert their data to screening values that can be applied to mass emission correlation equations (i.e., that relate the mass in lb/hr to a particular screening value). However, other comparisons between instruments and screening distances may also prove beneficial to facilities monitoring fugitive emissions. Some of these additional comparisons were also evaluated in this study.

Please note that other screening instruments, not studied in this report, may be available.

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For this study, equipment leaks screening data were collected from two refineries, one located in southern California and one in northern California. The testing at one refinery occurred in December, 1993. The testing at the second refinery took place in January, 1994. Of the approximately 400,000 valves and connectors available in both refineries, less than 300 components were selected for this intercomparison. The statistical sampling used was designed to provide information on the sensitivity of various portable instruments throughout the range of potential screening values. Therefore, the hydrocarbon concentrations measured when screening these components are not representative of routine data collected during leak detection and repair programs at petroleum refineries. Although not every component selected for this study was screened with each of the four portable instruments, all components were screened at least with the OVA 108. Fewer measurements were made with the other instruments because of instrument difficulties. Screening took place over a one week period at each of the two refineries.

Of the 271 components tested, 227 were valves and 44 were connectors. The majority of the components to screen were identified by refinery inspection and maintenance (I/M) teams as part of their routine I/M program. The remainder were found by Radian field staff. Because of the deliberate focus on higher leaking components identified by the I/M teams, the screening value distribution of the data is certainly biased toward higher percentages of high screening value components than would be found with a random screening program at either refinery.

### **RESULTS FROM DIFFERENT SCREENING INSTRUMENTS**

The four instruments use three unique methods to detect the hydrocarbon concentration. The OVA 108 and the TVA 1000 (FID) are both flame ionization detectors. The HNU<sup>®</sup> and the TVA 1000 (PID) are both photo ionization detectors. The TLV Sniffer<sup>®</sup> uses a combustion gas detector. The different hydrocarbon detection systems are believed to be the primary reason for the different results between instruments. The two FID instrument results and the two PID instrument results were much more comparable to each other than to instruments using different detection systems (FID vs. PID vs. combustion gas).

Recently completed studies by WSPA and API for refineries, petroleum marketing terminals and the oil and gas production industry have all used the OVA 108 as the screening instrument. For facilities that use other screening instruments that would like to apply results

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of these recent studies to their facilities, an adjustment factor needs to be applied. A set of adjustment factors, or correlation equations, have been developed as part of this study to convert screening values from the TLV Sniffer<sup>®</sup> and TVA FID instruments to screening values measured with an OVA. These correlation equations are shown on Table ES-1. Plots showing the data comparing the different instrument results to each other are found in Section 3 of this report.

Variables Correlated	Screening Distance	Number of Data Pairs	Correlation Equation	Correlation Coefficient
OVA versus	@ Surface	174	$OVA@ = (6.09 \times 10^{-1}) \times (TLV@)^{1.216}$	0.85
TLV Sniffer	1 cm	164	$OVA1 = (4.58 \times 10^{-1}) \times (TLV1)^{1.222}$	0.75
OVA versus	@ Surface	54	$OVA@ = (1.54) \times (TVAF@)^{0.935}$	0.90
TVA FID	1 cm	52	$OVA1 = (1.02) \times (TVAF1)^{1.013}$	0.83

\* For maximum sustainable screening values.

<u>Key</u>

=	OVA screening value at the surface of a component.
=	OVA screening value obtained with a 1 cm spacer.
=	TLV Sniffer <sup>®</sup> screening value at the surface of a component
=	TLV Sniffer <sup>®</sup> screening value obtained with a 1 cm spacer.
=	TVA screening value at the surface of a component.
=	TVA screening value obtained with a 1 cm spacer.

No correlations were developed to relate HNU<sup>®</sup> or TVA PID screening values to OVA screening values because an adequate correlation was not found between these screening values. Therefore, it is <u>not</u> advisable to use mass emission correlation equations that were developed with an OVA when HNU<sup>®</sup> or TVA PID screening measurements are obtained.

Study results indicate that the differences between peak screening values (i.e., the highest observed screening value) and the maximum sustainable screening values (i.e., the maximum screening value observed for two to three seconds or which was repeated multiple times in 30–60 seconds) were not statistically significant.

# **RESULTS FROM DIFFERENT SCREENING DISTANCES**

Most facilities that routinely screen for fugitive emissions from leaking equipment screen as close to the surface as possible but not so closely that it causes hydrocarbon contamination of

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the probe tip, thereby causing erroneous screening measurements. The instrument probe is normally held from the point of the highest leak on the component and the probe distance from the surface can vary from less than 1 mm to as much as 1 cm. If a 1 cm standoff basis is used, a spacer that maintains this distance can be applied to the end of the probe tip. In other cases, the inspector uses his or her experience and judgment to maintain this distance of approximately 1 cm.

For testing purposes in this study, a 1 cm spacer was applied to the probe tip to maintain a standardized distance for the 1 cm measurements. The surface measurements were made as closely as possible to the surface, recognizing that because of the instrument probe dimensions and component geometry, the actual probe distance from the surface could vary from one component type to another. The actual probe distance from the surface of the component could be some immeasurable distance which is less than 1 cm.

The recent refinery and petroleum marketing terminals studies were performed by screening components as close as possible to the surface. For facilities that use a 1 cm spacer that would like to apply results of these recent studies to their facilities, an adjustment factor needs to be applied. The adjustment factor for an OVA at the surface (OVA@) versus an OVA at 1 cm (OVA1) is given in the equation below:

$$OVA@ = (3.60) \times (OVA1)^{0.962}$$
 (Equation ES-1)

The recommended approach for converting screening values from the TLV Sniffer<sup>®</sup> and the TVA FID, when these instruments use a 1 cm spacer, to comparable OVA screening values at the surface is to first convert to comparable OVA values at 1 cm by using the correlations in Table ES-1 and then apply the above equation. Because of the lack of correlation for the HNU<sup>®</sup> and TVA PID to OVA screening values it is not recommended to convert any screening values from these instruments to OVA screening values.

Each of the instruments had screening values compared with that instrument at the surface to those with that same instrument at 1 cm. The effects of screening at the surface versus screening at 1 cm appears to have roughly the same impact for each instrument type. The screening values are two to three times lower, on the average, when obtained at a 1 cm

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screening distance. Plots showing the data comparing results for the different instruments are found in Section 3 of this report.

## **COMPARISON OF STUDY RESULTS TO EARLIER STUDY**

A previous study, entitled Valve Screening Study at Six San Francisco Bay Area Petroleum Refineries, or the "1979 Screening Study," reported on results for similar analysis of the TLV Sniffer<sup>®</sup> and the OVA 108. The current study, or "1994 Screening Study", evaluated more components, included connectors in the analysis, included additional screening instruments, and looked at additional factors that could influence test results such as windspeed, component type and service type.

Both studies show comparable differences between OVA vs. TLV Sniffer<sup>®</sup> screening values; however, the screening distance differences were more pronounced in the 1979 Screening Study than in the 1994 Screening Study. The reason for the differences in screening distance results is unknown. These differences could be due to differences in screening techniques, in ambient conditions, or in instrument sensitivities.

# COMPARISON OF OTHER FACTORS THAT MAY AFFECT THE CORRELATION EQUATIONS

An analysis was performed to determine other factors that may affect the relationship between screening values. Windspeed was found to have a statistically significant effect for some of the inter-instrument comparison correlation equations. However, the impact of windspeed on the correlation equations was minor. Only marginal improvements in the correlation coefficients were found by including windspeed in the equations for which windspeed was significant. For example, the correlation coefficient for the OVA at the surface versus OVA at 1 cm correlation equation improves from 0.929 to only 0.930 by including windspeed.

Component type and service type were shown to have a significant effect for a few of the screening value correlations developed; however, these may either be anomalous occurrences or questionable due to limited data for a specific factor. Investigations to determine any other reasons for the significant effects are beyond the scope of this project. Future research might investigate whether or not different component types with different geometries could effect the

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actual distance the instrument probe is away from the surface and quantify the variation effect on screening values. In addition, future research could investigate whether service type (low vapor pressure, high vapor pressure, low viscosity liquid, high viscosity liquid, etc.) could have a similar effect on measured screening values.

# Section 1 INTRODUCTION

Fugitive emissions from leaking equipment such as valves and connectors are being monitored by refineries, chemical companies, and petroleum marketing terminals. Several different instruments, each capable of measuring the fugitive hydrocarbon emissions, called "screening values," are being utilized by these facilities. Furthermore, the distance that the screening instrument is held from the surface of the component at the point where the primary leak is measured can vary depending on local practices, the potential for probe-tip contamination, and/or the presence of rotating parts. To investigate these differences, the Western States Petroleum Association (WSPA) and the American Petroleum Institute (API) commissioned this study, entitled "Comparison of Screening Values from Selected Hydrocarbon Screening Instruments and Different Screening Distances" and is referred to here as the "1994 Screening Study."

# STUDY OBJECTIVES

This study's objectives were to:

- Develop a correlation equation for converting screening instrument measurements from other analyzers to the Foxboro Organic Vapor Analyzer (OVA) 108 measurements by collecting side by side screening measurements from four different screening instruments\* including:
  - -Foxboro OVA 108,
  - -Bacharach Threshold Limit Value Sniffer (TLV Sniffer®),
  - -HNU® PI-101, and
  - --- Foxboro Total Vapor Analyzer (TVA) 1000, both flame ionization detector (FID) and photo ionization detector (PID).
- Develop a correlation equation converting screening measurements made at a distance of 1 cm to screening done as close as possible to the surface.

Please note that other screening instruments, not studied in this report, may be available.

The correlation equations convert screening values from one instrument to those with an OVA. The reason that the reference point was an OVA was because that was the basis for the recently completed studies from WSPA and API for refineries (API, 1994) and petroleum marketing terminals (API, 1993). Another desired product of the study was an adjustment factor, or correlation equation, that could convert screening values for an OVA at one screening distance to comparable values at a different screening distance, since in the two API studies, components were screened as close to the surface as possible.

A previous study, entitled Valve Screening Study at Six San Francisco Bay Area Petroleum Refineries (Radian, 1979), referred to as the "1979 Screening Study" in this report, reported on results for similar analysis of the TLV Sniffer<sup>®</sup> and the OVA 108. The 1994 Screening Study evaluated more components, included connectors in the analysis, included additional screening instruments, and looked at additional factors that could influence test results (windspeed, component type and service type). The 1994 Screening Study results have been compared to the 1979 Screening Study results in this report.

### **PROJECT DESCRIPTION**

For this study, equipment leaks screening data were collected from two refineries, one located in southern California and one in northern California. The testing at one refinery occurred in December, 1993. The testing at the second refinery took place in January, 1994. A total of 271 components were screened. Although not every component was screened with each of the four screening instruments, all components were screened at least with the OVA 108. Instrument difficulties resulted in fewer measurements with the other instruments. Screening took place over a one week period at each of the two refineries. A total of 227 valves and 44 connectors (9 flanged connectors and 35 non-flange connectors) were screened. The majority of the components to screen were identified by refinery inspection and maintenance (I/M) teams as part of their routine I/M program. The remainder were found by Radian field staff. Because of the deliberate focus on higher leaking components identified by the I/M teams, the screening value distribution of the data is biased toward higher percentages of high screening value components than would be found with a random screening program at either refinery.

### **REPORT ORGANIZATION**

This report is organized as follows:

- Section 2 documents the test procedures including a description of the equipment, QA/QC, and sampling procedures;
- Section 3 discusses the data analysis, including comparison of the screening instrument screening values, comparison of screening values as a function of screening distance, comparison of 1994 Screening Study results to 1979 Screening Study results, and analysis of other factors that may affect the correlation equations;
- Section 4 presents the conclusions and recommendations; and
- Section 5 includes the references.

# Section 2

## **TEST PROCEDURES**

This section describes the test procedures, including a description of the equipment, quality assurance/quality control (QA/QC), and sampling procedures.

### EQUIPMENT

Four different screening instruments were used in this study:

- Foxboro Organic Vapor Analyzer (OVA) 108;
- Bacharach Threshold Limit Value (TLV) Sniffer<sup>®</sup>;
- HNU<sup>®</sup> PI-101; and
- Foxboro Total Vapor Analyzer (TVA) 1000, both flame ionization detector (FID) and photo ionization detector (PID).

The first three instruments have been heavily used in past studies and in I/M programs. The final instrument is new and represents a potentially popular instrument for future studies and I/M. Please note that other screening instruments, not studied in this report, may be available. Each of the four screening instruments is briefly described:

## OVA 108

The Foxboro OVA 108 was used for screening every component in this study. The OVA 108 is a portable FID, powered by a refillable hydrogen tank. The OVA 108 internal vacuum pump is powered by a rechargeable battery. The pump continuously draws sampled hydrocarbons and air from the probe tip to the analyzer at a flow rate of approximately one liter per minute. The hydrocarbons are analyzed by the FID. The detector output is read on a hand-held logarithmic meter scale which is graduated from 1 to 10,000 ppmv. The OVA 108 was calibrated with methane. Hydrocarbon concentrations greater than 10,000 ppmv can be measured by use of a dilution probe. The dilution probe mixes charcoal scrubbed ambient air with the sample. The charcoal was used in an attempt to remove hydrocarbons from the background dilution air. In general, a dilution ratio of 10:1 was used in this study, allowing hydrocarbon concentrations up to 100,000 ppmv to be measured.

### TLV Sniffer®

The Bacharach TLV Sniffer<sup>®</sup> is a portable hydrocarbon detector that uses a catalytic combustion cell to determine hydrocarbon concentrations. A rechargeable battery provides the power for the internal sample pump which draws the sample through the detector chamber at a flow rate of approximately two liters per minute. The detector element catalytically oxidizes the hydrocarbon in the sample in order to determine the heat of combustion. This heat of combustion is expressed as an equivalent concentration. The TLV Sniffer<sup>®</sup> was calibrated with hexane. The TLV Sniffer<sup>®</sup> measures hydrocarbons from 1 to 10,000 ppmv. A dilution probe can extend the range of the TLV Sniffer<sup>®</sup> to 100,000 ppmv. However, a dilution probe was not used in this particular study for the TLV Sniffer<sup>®</sup>.

# HNU<sup>®</sup>

The HNU<sup>®</sup> Systems Inc. PI-101 detector (HNU<sup>®</sup>) used was a 10.2 eV lamp PID. Similar to the previously mentioned instruments, the HNU<sup>®</sup> uses a rechargeable battery to power the internal sample pump to draw the sample through the detector chamber at a flow rate of approximately 0.10–0.18 liters per minute. The PID ionizes the sample by an ultraviolet (UV) light. The detector output is displayed on a scale with three settings: 0-20 ppmv, 0-200 ppmv, and 0-2000 ppmv. The HNU<sup>®</sup> was calibrated with isobutylene. The PID measures halogenated hydrocarbons, aldehydes, ketones, aromatics, and any other compound with an ionization potential of 10.2 eV or less, including several that cannot be measured by an FID. The PID, however, does not respond well to many alkanes, particularly in the lower carbon number ranges. There are dilution probes available for many PID instruments, but none was available for use on this study.

### <u>TVA 1000</u>

Foxboro has recently introduced into the market an instrument that has both FID and PID capabilities, called the TVA 1000. The FID operates in nearly exactly the same manner as the OVA 108 FID. The PID operates with the same basic principles as the HNU<sup>®</sup> PID. The TVA PID uses a 10.6 eV lamp, which is relatively close to the 10.2 eV used in the HNU<sup>®</sup> The flow rate into the PID and FID combined is approximately one liter per minute. The sample stream is split into two paths within the TVA 1000 to allow for simultaneous analysis by the FID and PID. The TVA 1000 FID was calibrated with methane. The PID was calibrated with

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isobutylene. The range of the TVA 1000 without the dilution probe is from 1 to 50,000 ppmv for the FID and from 1 to 2,000 ppmv for the PID. A dilution probe can be attached to the TVA 1000 to extend the range. A dilution probe was used in this study to extend the range by approximately a factor of 10. The hydrocarbon concentrations were displayed in digital readouts on the hand-held sample probe and also on the body of the analyzer. The TVA 1000 also allows data to be logged internally for data collection purposes; however, this feature was not used for this study.

### QUALITY ASSURANCE/QUALITY CONTROL (QA/QC)

Each screening instrument was calibrated at least once each day. If batteries needed to be replaced, the instrument was recalibrated.

The OVA 108 was calibrated using a 100 ppm methane standard (certified at plus or minus 2%). To ensure that the OVA 108 was responding adequately over the entire range of hydrocarbon concentrations, the OVA 108's response was also checked with a certified zero air standard and with 10 ppm, 1000 ppm, and 10,000 ppm methane in zero air standards (each hydrocarbon standard certified at plus or minus 2%). The OVA 108 response to all of the hydrocarbon concentrations was checked by a linear regression. A correlation coefficient (r) of 0.995 or greater was required or the instrument was repaired. The OVA 108 dilution probe was set to a dilution ratio of approximately 10:1 based on using the 10,000 ppm was also checked and recorded.

The TLV Sniffer<sup>®</sup> was calibrated with a 500 ppm hexane standard and a 4000 ppm hexane standard. The HNU<sup>®</sup> was calibrated with a 95 ppm isobutylene standard at the first refinery and with a 102 ppm isobutylene standard at the second refinery. The TVA 1000 FID was calibrated in the same manner as the OVA 108 with the exception that the automatic calibrating mode was generally used for the TVA 1000. The automatic calibrating mode of the TVA 1000 allows for the instrument to calibrate itself when a known concentration of a calibration gas is examined. The TVA 1000 PID was calibrated in the same manner as the HNU<sup>®</sup> with the same exception that the automatic calibrating mode of the TVA 1000.

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Calibration gases were carried into the field in Tedlar<sup>™</sup> bags during all field testing. Each instrument was checked for accuracy after approximately every five samples. If an instrument failed this QA/QC check then the previous readings until the last verified QA/QC check were excluded or retested with a recalibrated instrument. In practice, very few samples needed to be excluded. The excluded samples, along with all of the raw sampling data, are shown in Appendix A.

### SAMPLING PROCEDURES

In general, the screening measurements were made in accordance with the latest version of the United States Environmental Protection Agency's (U.S. EPA) Reference Method 21. U.S. EPA Method 21 instrument specifications are summarized in Table 2-1. The requirements that were followed in this study exceeded the requirements of U.S. EPA Method 21. Table 2-2 outlines the general screening procedures that were followed for all four of the screening instruments.

Table 2-1. Summa	ry of EPA	Method 21	Requirements
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Determination of Volatile Organic Compound Leaks
1. Analyzer response factor <10
2. Analyzer response time ≤30 seconds
<ol> <li>Calibration precision ≤10% of calibration gas</li> </ol>
4. Internal pump capable of pulling 0.1 to 3.0 L/min
5. Intrinsically safe
6. Single hole probe with maximum ¼-inch OD
7. Linear and measuring ranges must include leak definition value (may include dilution probe)
8. Instrument readable to ±2.5% of leak definition
9. No detectable emissions (NDE) value defined as $\pm 2.5\%$ of leak definition (i.e., $\pm 500$ ppm)

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Data collected from screening were recorded on forms like the one shown as Figure 2-1. Five different readings were made with each screening instrument for each component. The first reading was a background reading measured in an area close to the component. Once the point of maximum leakage was found on the component as close as possible to the component's surface, then the maximum sustainable leak rate and the peak leak rate were recorded. The maximum sustainable leak rate was the screening value that stabilized for two

2-4

to three seconds, or was repeated multiple times in 30-60 seconds. The peak leak rate was the highest observed screening value on the instrument, even if the screening value were only a fleeting spike.

Table 2-2. Summary of Screening Procedures

General Screening Procedures
1. Prepare analyzer for sampling.
2. Calibrate analyzer.
3. Check analyzer for leaks.
4. Without fouling the tip, and without restricting flow into the analyzer probe, place probe as close as possible and approximately perpendicular to the component surface or seam where leakage could occur.
<ol><li>Move the probe slowly along the line of potential leakage to obtain the maximum reading.</li></ol>
<ol><li>Leave the probe tip at the maximum reading location for approximately two times the instrument response time.</li></ol>
<ol><li>Record the maximum sustainable screening value and the peak screening value on the data form.</li></ol>
8. If the reading exceeds full scale, use the dilution probe, if the instrument has a dilution probe.
9. Add 1 cm spacer to the probe tip.
10. Repeat steps 5 through 8.
11. Repeat steps 1 through 10 for the remaining screening instruments.

The next two readings (maximum sustainable and peak) were taken at a 1 cm standoff from the surface of the component. The readings at 1 cm were generally, but not always, 1 cm away from the point of highest leak at the surface of the component. The component was always rescreened to determine, independent of the surface readings, where the point of highest leak at 1 cm was found. A 1 cm spacer, supplied by Foxboro, was provided for screening at 1 cm with the OVA 108 and the TVA 1000. A different 1 cm spacer was constructed for use with the TLV Sniffer<sup>®</sup> and the HNU<sup>®</sup>.

Valves screened for this study were usually identified by the refinery inspection and maintenance (I/M) teams. The remaining valves were found by Radian staff when insufficient numbers of valves for Radian to test were located by the I/M teams on the day of Radian's testing, or if there was a need to obtain more diversity in screening values tested. In order to strengthen the statistical significance of the desired correlations, Radian attempted to obtain screening values from the whole leak range from 1 ppmv to 100,000 ppmv for the OVA 108,

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from 1ppmv to 10,000 ppmv for the TLV Sniffer<sup>®</sup>, from 1 to 2000 ppmv for the HNU<sup>®</sup> and from 1 to over 500,000 ppmv for the TVA 1000. Components that tested beyond the range of the analyzers (pegged components) were also screened with the pegged value recorded.

The majority of the connectors that were tested for this study were located by Radian. This was primarily because these connectors were not tagged and locating leaking connectors from the records of the I/M team was significantly more difficult than searching for these leaks independently. Furthermore, fewer leaking connectors than valves, at least on a percentage basis, are found in these refineries.

After the screening values were all recorded for a particular component, then the ambient temperature was recorded from a digital thermometer and the windspeed was recorded from an anemometer. The temperature and the windspeed were measured as close as possible to the highest leaking point on the component. As shown in Figure 2-1, also recorded was the component tag ID, the component subtype (i.e. gate, glove, plug or other type of valve), the component actuation if a valve (either control or manual), the size of the component, and the service category (light liquid, heavy liquid or gas). For this study, light liquids are defined as any liquid with vapor pressure greater than kerosene.

Duplicate measurements were taken, on the average, for every twentieth component screened. For the duplicate tests, all instrument readings were retaken exactly as on the first measurement, both for the different instruments and the different screening distances.

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Figure 2-1 Screening Value Data Collection Sheet

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### Section 3

# DATA ANALYSIS

Throughout this section the following notation will be used to refer to the screening instrument and distance:

OVA@/OVA1 —	Screening values obtained using the OVA at the surface and at 1 cm, respectively;
TLV@/TLVA1 —	Screening values obtained using the TLV Sniffer <sup>®</sup> at the surface and at 1 cm, respectively;
HNU@/HNU1 —	Screening values obtained using the HNU <sup>®</sup> at the surface and at 1 cm, respectively;
TVAF@/TVAF1 —	Screening values obtained using the TVA FID at the surface and at 1 cm, respectively; and
TVAP@/TVAP1 —	Screening values obtained using the TVA PID at the surface and at 1 cm, respectively.

In general, no appreciable differences were noted between the maximum sustainable screening values versus the peak screening values. Plots of both types of screening value measurements are included in this section. Correlation equations were developed using only the maximum sustainable screening value measurements, however, because it is believed that this is the type of screening value measurement typically collected by refineries.

Pegged values were obtained during the 1994 Screening Study; however, these pegged values were not included in any of the emission correlation equations and were therefore excluded from any of the statistical analysis in this report.

Statistical analyses were performed on the screening data to examine the following:

- Correlation between screening values obtained from different instrument types (OVA, TLV Sniffer<sup>®</sup>, HNU<sup>®</sup>, and TVA);
- Correlation between screening values at different screening distances (screening at the surface versus a 1 cm screening distance) for a given instrument;

- Differences between the 1979 Valve Screening Study (1979 Screening Study) results and the current 1994 Screening Study results; and
- Other variables that may affect screening results (e.g., component type, component service, windspeed).

The analyses performed for each of the aforementioned areas are discussed in detail and briefly summarized in the following sections.

The factor which could potentially cause the largest differences between the measured screening values is the type of screening instrument used. Two sets of the instruments tested during this study employ similar analytical methods in determining a screening value. The OVA and the TVA FID are both flame ionization detectors (FIDs); and the HNU® and the TVA PID are both photo ionization detectors (PID). The TLV Sniffer<sup>®</sup> instrument is neither an FID nor a PID, but uses a combustible gas detector to determine hydrocarbon concentrations. Although screening values from similar instrument types tended to be highly correlated. screening values from non-similar instrument types tended to show very low correlations. In fact, screening measurements from the OVA and TVA FID, and from the HNU® and TVA PID provided virtually a one-to-one correlation; whereas for dissimilar instrument types (i.e., the OVA and HNU®, and the OVA and the TVA PID) the correlation between screening value measurements was virtually zero in some instances (i.e., the correlation coefficient was very small and not statistically different from zero). When comparing OVA screening values to the TLV Sniffer<sup>®</sup> screening values, the differences between screening measurements tended to increase as the screening values increased. Thus, for example, an OVA screening value at 100 ppm may differ from a TLV Sniffer<sup>®</sup> screening value by only a factor of 1.5 to 2.0. whereas an OVA screening value at 10,000 ppm may differ from a TLV Sniffer<sup>®</sup> screening value by a factor of 4 to 7.

For every instrument type, screening distance (at the surface versus 1 cm) was found to have a significant effect on the measured screening value. In general, screening values obtained at a 1 cm screening distance were found to be about 2 to 3 times smaller than screening values obtained at the surface for every instrument type. This factor of 2 to 3 was found to be fairly consistent throughout the range of screening values obtained. For example, on the average,

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an OVA screening value of 3 ppm obtained at the surface would screen at roughly 1 ppm when screened at 1 cm screening distance; and an OVA screening value of 30,000 ppm at the surface would screen at roughly 10,000 ppm when screened at 1 cm screening distance.

Screening measurements obtained using the OVA and TLV Sniffer<sup>®</sup> screening instruments were compared to the same types of screening measurements obtained during the 1979 Screening Study. During the 1979 Screening Study a number of valves were screened using both an OVA and a TLV Sniffer<sup>®</sup> instrument. Measurements were collected at the component surface and at a 1 cm screening distance. When comparing the OVA screening values at the surface versus the TLV Sniffer<sup>®</sup> screening values at the surface, and the OVA screening values at 1 cm versus the TLV Sniffer® screening values at 1 cm, no statistically significant differences were found between the correlation equations obtained using the 1979 Screening Study data and the 1994 Screening Study data. However, when comparing the OVA screening values at the surface versus the OVA screening values at 1 cm, and the TLV Sniffer® screening values at the surface versus the TLV Sniffer® screening values at 1 cm. statistically significant differences were found between the correlation equations obtained using the 1979 Screening Study data and the 1994 Screening Study data. In summary, both studies show comparable results between OVA vs. TLV Sniffer<sup>®</sup> screening values; however, the screening distance differences are more pronounced in the 1979 Screening Study than in the 1994 Screening Study. The cause of these significant effects is unknown. However, they could be due to differences in screening techniques used during the two studies, in ambient conditions, or in instrument sensitivities.

Lastly, an analysis was performed to determine other factors that may affect the relationship between screening values. The results of this analysis showed that windspeed had a statistically significant effect on the OVA@ to OVA1 equation (that is, windspeed accounted for a significant portion of the variability in the OVA@ to OVA1 equation). Windspeed was also found to have a significant effect on the OVA@ versus TVAF@ correlation equation, the TVAP@ versus HNU<sup>®</sup>@ correlation equation, and the TVAP1 versus HNU<sup>®</sup>1 correlation equation. Investigations to determine the degree of variability of measured screening values as a function of windspeed is beyond the scope of this project. Future research might investigate the degree of screening value variability as a function of windspeed, instrument probe

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sampling velocity, and equipment component emission velocity. The impact of windspeed on the correlation equations, however, is minor. For example, the correlation coefficient for the OVA at the surface versus OVA at 1 cm correlation equation improves from 0.929 to only 0.930 by including windspeed. Windspeed was not found to have a significant effect on the other correlation equations developed. Component type and service type were shown to have a significant effect for a few of the screening value correlation equations developed; however, these were thought to be either anomalous occurrences or questionable due to limited data for a specific factor.

# COMPARISON OF SCREENING INSTRUMENT SCREENING VALUES AT MAXIMUM SUSTAINABLE RATE AND PEAK RATE

Comparisons were performed between the OVA instrument screening values and screening values obtained using the other three instrument types. Recently published emission correlation equations (e.g., marketing terminals study and 1993 Refinery Study) were developed using an OVA instrument. Thus, it was of primary interest to compare the OVA screening values to screening values from every other instrument type rather than comparing screening values from every combination of instrument types. However, screening value measurements obtained from the HNU<sup>®</sup> and the TVA PID were also compared, because these are similar instrument types (both are photo ionization detectors). In summary, screening values from the following instruments were compared:

- OVA versus the TLV Sniffer<sup>®</sup>;
- OVA versus the HNU<sup>®</sup>;
- OVA versus the TVA FID;
- · OVA versus the TVA PID; and
- HNU<sup>®</sup> versus the TVA PID.

Screening measurements collected at the component surface as well as screening measurements collected at 1 cm from the component surface were compared for different instrument types. In addition, the maximum sustainable screening values and the peak screening values were compared for different instrument types, resulting in a total of four sets of correlation equations that were evaluated for each inter-instrument comparison. Figures 3-1 through 3-5 show the comparisons that were performed for each of the five inter-instrument categories listed above. The upper left corner of each of these figures (labeled "a")

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shows a plot of the maximum sustainable screening values at the surface. The upper right corner of each of these figures (labeled "b") show plots of the peak screening values at the surface. The lower left corner of each of these figures (labeled "c") show plots of the maximum sustainable screening values at 1 cm and the lower right corner of each of these figures (labeled "d") show plots of the peak screening values at 1 cm. Each of the figures shows the corrected screening data (after subtracting the background screening value).

Correlation equations were developed using measurement error methods in which the errors in x were assumed to be equal to the errors in y, as discussed in Appendix B. Predictive correlation equations are presented only for the following inter-instrument comparisons:

- OVA versus the TLV Sniffer<sup>®</sup>;
- OVA versus the TVA FID; and
- HNU<sup>®</sup> versus the TVA PID.

Although there was a positive correlation between the OVA and the HNU<sup>®</sup>, and the OVA and the TVA PID, there was not a strong correlation. The models evaluated for these two interinstrument relationships were not sufficiently adequate for predictive purposes. Therefore, no predictive correlation equations were developed for these two inter-instrument comparisons.

The primary objective of this study was to develop correlation equations between screening values collected using instruments other than an OVA screening instrument (e.g., a TLV Sniffer<sup>®</sup>, an HNU<sup>®</sup>, etc.) to those with an OVA instrument to use in emission correlation equations that relate lbs/hr emission rates to OVA screening values. OVA screening values were found to be highly correlated to TLV Sniffer<sup>®</sup> screening values and TVA FID screening values. Equations or adjustment factors were developed for these sets of correlation equations. OVA screening values were found to not be highly correlated with HNU<sup>®</sup> screening values or TVA PID screening values. Thus, using HNU<sup>®</sup> or TVA PID screening values to predict mass emissions based on emission correlation equations developed for OVA screening instruments is questionable.

Table 3-1 gives the correlation equations that were developed relating screening values from the different instrument types. As stated previously, correlation equations are only given for the maximum sustainable screening values (instead of the peak screening values).

Variables Correlated	Screening Distance	Number of Data Pairs	Correlation Equation	Correlation Coefficient
OVA versus TLV Sniffer®	@ Surface	174	$OVA@ = (6.09 \times 10^{-1}) \times (TLV@)^{1.216}$	0.85
	1 cm	164	$OVA1 = (4.58 \times 10^{-1}) \times (TLV1)^{1.222}$	0.75
OVA versus TVA FID	@ Surface	54	OVA@ = (1.54) x (TVAF@) <sup>0.935</sup>	0.90
	1 cm	52	$OVA1 = (1.02) \times (TVAF1)^{1.013}$	0.83
TVA PID versus HNU®	@ Surface	21	TVAP@ = (5.88 x 10 <sup>-1</sup> ) x (HNU@) <sup>0.950</sup>	0.88
	1 cm	21	$TVAP1 = (1.69 \times 10^{-1}) \times (HNU1)^{1.186}$	0.59

Table 3-1. Equations Relating Screening Values From Different Instruments<sup>a</sup>

\* For maximum sustainable screening values.

<u>Key</u>

OVA@	=	OVA screening value at the surface of a component.
OVA1	=	OVA screening value obtained with a 1 cm spacer.
TLV@	=	TLV Sniffer® screening value at the surface of a component.
TLV1	=	TLV Sniffer <sup>®</sup> screening value obtained with a 1 cm spacer.
TVAF@	=	TVA FID screening value at the surface of a component.
TVAF1	=	TVA FID screening value obtained with a 1 cm spacer.
HNU@	=	HNU <sup>®</sup> screening value at the surface of a component.
HNU1	=	HNU <sup>®</sup> screening value obtained with a 1 cm spacer.
TVAP@	=	TVA PID screening value at the surface of a component.
TVAP1	=	TVA PID screening value obtained with a 1 cm spacer.

Figure 3-1 shows the correlation equations that were developed between the OVA and the TLV Sniffer<sup>®</sup>. Currently, all published emission correlation equations (i.e., relating mass emissions to screening value measurements) were developed using either an OVA or a TLV Sniffer<sup>®</sup> instrument. As shown by the predictive correlation equation in the figure, for low screening value ranges the OVA and TLV Sniffer<sup>®</sup> show similar screening value measurements, on the average. The difference between screening value measurements increases, however, as the magnitude of the screening values increases, with the OVA resulting in consistently higher screening value measurements. Thus, for example, on the average, an OVA screening value at 100 ppm may differ from a TLV Sniffer<sup>®</sup> screening value by only a factor of 1.5 to 2.0, whereas an OVA screening value at 10,000 ppm may differ from a TLV Sniffer<sup>®</sup> screening value by a factor of 4 to 7.

Figure 3-2 shows plots of the OVA screening value data versus the HNU<sup>®</sup> screening value data. As shown in the plots there is a lot of scatter in the data and the correlation coefficient is less than 0.40 for every type of correlation equation evaluated (i.e., for the maximum sustainable screening value at the surface and at 1 cm; and peak screening value at the surface and at 1 cm). In addition, the OVA screening instrument provides screening values that are typically an order of magnitude higher than the HNU<sup>®</sup> screening values. As discussed, however, the OVA and HNU<sup>®</sup> are different types of analytical instruments (the OVA is a flame ionization detector and the HNU<sup>®</sup> is a photo ionization detector).

Plots of the OVA screening values versus the TVA FID screening values are given in Figure 3-3. Note that the predictive correlation equation shows virtually a one-to-one correspondence between the OVA screening values and the TVA FID screening values for every type of screening measurement collected (i.e., maximum sustainable screening values and peak screening values at the surface and at 1 cm). That is, there appears to be no bias, but there is scatter about the regression line. As shown in the figures, the correlation equations form almost a perfect 45° line from (1,1) to (100000,100000).

Figure 3-4 shows plots of the OVA screening value data versus the TVA PID screening value data which look very similar to the plots obtained for the OVA versus the HNU<sup>®</sup> screening values. The correlation coefficients between screening values from the OVA and the TVA PID are very low (usually less than 0.40), and for figures (a) and (c) the correlation coefficients were not statistically different from zero ( $\alpha = 0.05$ ).

Because the HNU<sup>®</sup> and the TVA PID are similar instrument types (i.e., both are photo ionization detectors) it was of interest to compare the screening measurements from these two instruments. In practice, an equation relating these two instrument types would probably be of little use because none of the published emission correlation equations (i.e., relating mass emissions to screening values) were developed using an HNU<sup>®</sup> or TVA PID instrument. As would be expected, however, screening value measurements from these two instruments are highly correlated. Figure 3-5 shows plots of the data and the predictive correlation that would be obtained based on the limited data available for these two instruments. Although both of these instruments are capable of measuring concentrations greater than 2,000 ppm with the





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OVA vs. TVA FID Screening Instrument

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OVA vs. TVA PID Screening Instrument

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TVA PID vs. HNU<sup>®</sup> Screening Instrument

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use of a dilution probe, a dilution probe was not used for this study for the HNU<sup>®</sup>. Thus, no HNU<sup>®</sup> measurements greater than 2,000 ppm are plotted (because these were recorded as "pegged at >2,000 ppm").

The correlation equations given in Table 3-1 are shown in Figure 3-6 along with the 95% confidence intervals for the mean. The plots labeled "a", "b", and "c" in Figure 3-6 show the correlation equations for the:

- OVA versus the TLV Sniffer<sup>®</sup>;
- · OVA versus the TVA FID; and
- TVA PID versus the HNU®, respectively.

The equations and the confidence intervals are given for screening values obtained at the surface (the solid lines) and screening values obtained at 1 cm from the surface (the dashed lines). In each case, the center line is the correlation equation and the outer lines are the 95% confidence intervals for the mean. As stated previously, the correlation equations were developed using measurement error method (MEM) techniques. The MEM technique is discussed in Appendix B.

# COMPARISON OF SCREENING DISTANCES AT MAXIMUM SUSTAINABLE RATE AND PEAK SUSTAINABLE RATE

Figures 3-7 through 3-11 show plots of the screening values obtained at the surface versus screening values obtained at 1 cm, for the OVA, TLV Sniffer<sup>®</sup>, HNU<sup>®</sup>, TVA FID, and TVA PID screening instruments, respectively. The first plot on each of these figures (labelled "a") shows the data obtained for the maximum sustainable screening values and the second plot (labelled "b") shows the data obtained for the peak screening values. The solid line overlaid on each plot indicates the correlation equations obtained. These correlation equations were developed using measurement error methods in which the relative variability in the y-axis was assumed equal to the relative variability in the x-axis. A discussion of this method and a justification of the assumptions for this method can be found in Appendix B.



Figure 3-6. Equations Relating Screening Values from Different Instruments

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Figure 3-7 OVA at Surface vs. OVA at 1 cm

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Figure 3-8 TLV Sniffer® at Surface vs. TLV Sniffer® at 1 cm

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HNU<sup>®</sup> at Surface vs. HNU<sup>®</sup> at 1 cm

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Figure 3-10 TVA FID at Surface vs. TVA FID at 1 cm

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(a) Max. Sus. TVA PID SV at Surface Versus Max. Sus. TVA PID SV at 1 cm Correlation Coefficient = .7865, N = 28

(b) Peak TVA PID at Surface Versus Peak TVA PID SV at 1 cm Correlation Coefficient = .9127, N = 77



Figure 3-11 TVA PID at Surface vs. TVA PID at 1 cm

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As shown by the correlation equations overlaid on each of the figures, screening measurements obtained at 1 cm are generally 2 to 3 times lower than screening measurements obtained at the component surface. [A perfect one-to-one correlation would produce a 45° line from (1,1) to (100000,100000)]. This trend appears to be fairly consistent throughout the screening value range for all instrument types.

Note that for the TLV Sniffer<sup>®</sup> instrument and the HNU<sup>®</sup> instrument, there are no screening values greater than 10,000 ppm and 2,000 ppm, respectively. Although dilution probes are available for these instruments (to increase the range of measurable screening values), the dilution probes were not used for this study. A dilution probe was used for the TVA PID instrument; however, no measurable screening values were detected at concentrations greater than 2,000 ppm using this instrument. For all of the instruments, correlation equations developed are most applicable for the range of screening values shown on the plots.

Table 3-2 gives correlation equations relating screening values at the surface to screening values at 1 cm for each of the four instrument types. Correlation equations are only given for

Variables Correlated	Number of Data Pairs	Correlation Equation	Correlation Coefficient
OVA @ Surface vs. OVA at 1 cm	250	OVA@ = (3.60) x (OVA1) <sup>0.962</sup>	0.93
TLV Sniffer <sup>®</sup> @ Surface vs. TLV Sniffer <sup>®</sup> at 1 cm	161	TLV@ = (3.07) x (TLV1) <sup>0.927</sup>	0.87
HNU <sup>®</sup> @ Surface vs. HNU <sup>®</sup> at 1 cm	140	HNU@ = (2.34) x (HNU1) <sup>0.981</sup>	0.84
TVA FID @ Surface vs. TVA FID at 1 cm	54	$TVAF@ = (1.77) \times (TVAF1)^{1.139}$	0.84
TVA PID @ Surface vs. TVA PID at 1 cm	23	TVAP@ = (2.39) x (TVAP1) <sup>0.891</sup>	0.79

Table 3-2. Equations Relating Screening Values at the Surface to Screening Values at 1 cm<sup>a</sup>

\* For maximum sustainable screening values.

Key

OVA@	=	OVA screening value at the surface of a component.
OVA1	=	OVA screening value obtained with a 1 cm spacer.
TLV@	=	TLV Sniffer <sup>®</sup> screening value at the surface of a component
TLV1	=	TLV Sniffer <sup>®</sup> screening value obtained with a 1 cm spacer.
TVAF@	=	TVA FID screening value at the surface of a component.
TVAF1	=	TVA FID screening value obtained with a 1 cm spacer.
HNU@	=	HNU <sup>®</sup> screening value at the surface of a component.
HNU1	=	HNU <sup>®</sup> screening value obtained with a 1 cm spacer.
TVAP@	=	TVA PID screening value at the surface of a component.
TVAP1	=	TVA PID screening value obtained with a 1 cm spacer.

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the maximum sustainable screening values (instead of the peak screening values). It is believed that the maximum sustainable screening values are the screening measurements refineries typically collect. As shown in the figures, however, there was very little visible difference between the equations obtained for the maximum sustainable screening value correlation equations and the peak screening value correlation equations. Table 3-2 also shows the number of data pairs used to develop the correlation equations and the correlation coefficient for each of the equations. As shown in the table, the correlation coefficients ranged from 0.79 to 0.93.

Figure 3-12 shows plots of the correlation equations given in Table 3-2. The 95% confidence intervals for the mean are also overlaid on these figures. The solid lines in the figures indicates the regression equations and the dashed lines indicate the 95% confidence intervals for the mean. The plots labeled "a" through "e" show the correlation equations for the:

- OVA screening values at the surface versus OVA screening values at 1 cm;
- TLV screening values at the surface versus TLV screening values at 1 cm;
- HNU<sup>®</sup> screening values at the surface versus HNU<sup>®</sup> screening values at 1 cm;
- TVA FID screening values at the surface versus TVA FID screening values at 1 cm; and
- TVA PID screening values at the surface versus TVA PID screening values at 1 cm.

The equations given in Table 3-2 and shown in Figure 3-12 were developed using a measurement error method (MEM) as discussed in Appendix B of this report.

### COMPARISON OF CURRENT STUDY DATA TO 1979 SCREENING STUDY DATA

A screening value study was conducted for several west coast refineries in 1979. The results of this study are published in a report, entitled *Valve Screening Study of Six San Francisco Bay Area Petroleum Refineries* (Radian, 1979), also referred to as the "1979 Screening Study" for this report. During the 1979 Screening Study, over 100 valves were screened using both an OVA and a TLV Sniffer<sup>®</sup> screening instrument. In addition, screening measurements were

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Figure 3-12 Equations Relating Screening Values at the Surface to Screening Values at 1 cm







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96% confidence intervals for the mean

Regression equation

obtained at the component surface and at 1 cm from the component surface. Data collected for the 1979 Screening Study (as given in Appendix B of the 1979 Screening Study report) were compared to data collected for the 1994 Screening Study. It should be noted, however, that it is not known whether background measurements were taken for the 1979 Screening Study and subtracted from the component screening values, which was the procedure used for the 1994 Screening Study. In addition, the 1979 Screening Study data included pegged screening measurements (i.e., those screened beyond the range) which were removed before comparing them to the 1994 Screening Study data. As mentioned previously, pegged screening values were also obtained during the 1994 Screening Study; however, these values were not included in any of the analysis.

Differences between the following screening value comparisons were examined for the 1979 Screening Study data and the 1994 Screening Study data:

- OVA screening values at the surface versus OVA screening values at 1 cm;
- TLV Sniffer<sup>®</sup> screening values at the surface versus TLV Sniffer<sup>®</sup> screening values at 1 cm;
- OVA screening values at the surface versus TLV Sniffer<sup>®</sup> screening values at the surface; and
- OVA screening values at 1 cm versus TLV Sniffer<sup>®</sup> screening values at 1 cm.

Figure 3-13 shows plots of the 1979 Screening Study data and the 1994 Screening Study data for the four relationships listed above. The 1979 Screening Study data are indicated by an asterisk (\*) in the figures and the 1994 Screening Study data are indicated by a dot. Correlation equations were developed for each of the studies, separately, and are overlaid on these plots. The dashed line indicates the correlation equation obtained using the 1979 Screening Study data and the solid line indicates the correlation equation obtained using the 1994 Screening Study data. Both sets of correlation equations were developed using measurement error methods in which the variability in the x value was assumed equal to the variability in the y value, as discussed in Appendix B of this report.

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Analysis of covariances (ANCOVAs) performed on the 1979 and 1994 data indicated that there were significant differences between the studies when comparing the OVA screening values at the surface to the OVA screening values at 1 cm, and when comparing the TLV Sniffer<sup>®</sup> screening values at the surface to the TLV Sniffer<sup>®</sup> screening values at 1 cm. The equations developed for each of these correlation equations are shown in plots (a) and (b) of Figure 3-13. As shown in the plots, the 1979 Screening Study equation results in screening values that are roughly 2 to 3 times different, on the average, for high screening value ranges. Differences between the studies were not as apparent for the lower screening value ranges. These differences between studies are fairly consistent for both the OVA and the TLV Sniffer<sup>®</sup> correlation equations. The cause for this difference between studies is not known. However, differences between studies could be attributable to different screening techniques, different ambient conditions, or different instrument sensitivities. It is also noted, that although statistically significant differences between the correlation equations for the two studies were found, the data are fairly well interspersed for low screening value ranges (i.e., < 1,000 ppm).

Plots (c) and (d) of Figure 3-13 show the correlation equations obtained for the two studies for the OVA versus the TLV Sniffer<sup>®</sup> screening measurements at the surface, and the OVA versus the TLV Sniffer<sup>®</sup> screening measurements at 1 cm, respectively. The ANCOVA results showed that there were no statistically significant differences between the studies for these two sets of correlation equations. In fact, the correlation equations shown in plot (c) are nearly identical.

### ANALYSIS OF OTHER FACTORS THAT MAY AFFECT THE CORRELATION EQUATIONS

Analysis was performed to evaluate whether or not other factors, such as component type (connector or valve), service (light liquid, heavy liquid, or gas) or windspeed, may affect the correlation results. This analysis was performed only for those cases where a correlation equation was developed.

Analyses of covariance (ANCOVAs) were performed to determine if any other measured factors (i.e., component type, service, or windspeed) had a significant effect on the relationship between the logarithm of the y variable and the logarithm of the x variable. One of the assumptions in performing ANCOVAs is that the errors are normally distributed and that

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the variances are constant for different factors or ranges. These assumptions were met by taking the natural logarithms of the x and y values.

Testing for the significance of main effects (or factors) and the factor multiplied by log(x) (the interaction term) in an ANCOVA is analogous to testing whether separate regression equations developed for those factors will have intercepts and slopes, respectively, that are statistically different.

Table 3-3 shows the results of the ANCOVAs performed for the five sets of correlation equations developed which relate screening values at the surface to screening values obtained at 1 cm, and Table 3-4 shows the results of the ANCOVAs performed for the three sets of correlation equations developed relating screening values from different instrument types. The p-values for the main effect (i.e., the intercept) and the interaction term (i.e., the slope) are given in parenthesis for each of the factors. Those factors that have a statistically significant main effect (i.e., the intercepts of the different equations are significantly different) or have a statistically significant interaction term (i.e., the slopes of the different equations are significantly different) at the 0.10 level are noted with an "S" (significant) in the tables. Those factors for which the main effect and the interaction terms were not statistically significant at the 0.10 level are noted with an "NS" (not significant) in the table.

As shown in Tables 3-3 and 3-4, component type was found to have a significant effect only for the TVAF@ versus the TVAF1 correlation equations. Component type was not found to have a significant effect for the other correlation equations developed. This is consistent with the visual evidence shown in Figures 3-1 through 3-9 and 3-11. In each of these figures, different symbols were used to indicate the different component types (i.e., connector or valve). As shown in the figures, screening value measurements obtained for these two different component types were fairly well interspersed. The data shown in Figure 3-10 (i.e., for the TVAF@ versus the TVAF1) is redrawn in Figure 3-14 and overlaid with correlation equations developed for the different component types. Figure 3-14(a) did not have sufficient data for connectors to develop an adequate correlation equation. Although the differences in correlation equations for connectors and valves is apparent in Figure 3-14(b), the large differences could be attributable to the fact that there were insufficient data to adequately

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			(After accounting	Factor Tested	the X-variable)
Equation Group	Equation (Y vs X)	Screening Type	Component Type (connector, valve)	Component Phase (LL, HL, Gas)	Windspeed
1	OVA@	Maximum Sustainable SV	NS (0.39, 0.88)	S (0.02, 0.65)	S (0.08, 0.91)
	VS OVA1	Peak Screening Value	NS (0.21, 0.50)	S (0.02, 0.54)	S (0.04, 0.86)
2	TLV@ vs	Maximum Sustainable SV	NS (0.72, 0.46)	NS (0.32, 0.12)	NS (0.77, 0.95)
	ILV1	Peak Screening Value	NS (0.89, 0.34)	NS (0.40. 0.17)	NS (0.65, 0.83)
3	HNU@	Maximum Sustainable SV	NS (0.57, 0.77)	NS (0.49, 0.57)	NS (0.44, 0.95)
	vs HNU1	Peak Screening Value	NS (0.65, 0.27)	NS (0.32, 0.74)	NS (0.46, 0.99)
4	TVAF@	Maximum Sustainable	S (0.05, 0.98)	NS (0.36) <sup>a</sup>	NS (0.65, 0.32)
	TVAF1	Peak Screening Value	S (0.07, 0.64)	NS (0.75, 0.18)	NS (0.70, 0.46)
5	TVAP@	Maximum Sustainable SV	NS (0.57, 0.85)	NS (0.83) <sup>a</sup>	NS (0.51, 0.97)
	TVAP1	Peak Screening Value	NS (0.46, 0.89)	NS (0.53, 0.32)	NS (0.40, 0.11)

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Table 3-3. Results of Multivariate Analysis for Correlations Between Screening Distances

Key:

HL HNU@	=	Heavy liquid HNU® screening value at the surface of a component.
HNU1	=	HNU <sup>®</sup> screening value obtained with a 1 cm spacer.
LL	=	Light liquid
NS	=	Not statistically significant at the 0.10 significance level (p-values for intercept and slope, respectively, given in parenthesis).
OVA@	=	OVA screening value at the surface of a component.
OVA1	=	OVA screening value obtained with a 1 cm spacer.
S	=	Statistically significant at the 0.10 significance level (p-values for intercept and slope, respectively, given in parenthesis).
SV	=	Screening value
TLV@	=	TLV Sniffer® screening value at the surface of a component.
TLV1	=	TLV Sniffer <sup>®</sup> screening value obtained with a 1 cm spacer.
TVAF@	=	TVA FID screening value at the surface of a component.
TVAF1	=	TVA FID screening value obtained with a 1 cm spacer.
TVAP@	=	TVA PID screening value at the surface of a component.
TVAP1	=	TVA PID screening value obtained with a 1 cm spacer.

<sup>a</sup> Insufficient data to test both slope and intercept terms.

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			(After accounti	Factor Tested ng for variation in th	e X-variable)
Equation Group	Equation (Y vs X)	Screening Type	Component Type (connector, valve)	Component Phase (LL, HL, Gas)	Windspeed
	OVA@ vs TLV@	Maximum Sustainable SV	NS (0.83, 0.94)	S (0.43, 0.08)	NS (0.63, 0.90)
		Peak Screening Value	NS (0.86, 1.00)	S (0.36. 0.10)	NS (0.52, 0.97)
	OVA1 vs TLV1	Maximum Sustainable SV	NS (0.39, 0.60)	NS (0.28, 0.73)	NS (0.25, 0.51)
		Peak Screening Value	NS (0.33, 0.29)	NS (0.36, 0.74)	NS (0.31, 0.74)
	OVA@ vs TVAF@	Maximum Sustainable SV	NS (0.61, 0.95)	NS (0.66) <sup>a</sup>	NS (0.40, 0.19)
2		Peak Screening Value	NS (0.99, 0.62)	S (0.04, 0.87)	NS (0.24, 0.07)
	OVA1 vs TVAF1	Maximum Sustainable SV	NS (0.29, 0.52)	NS (0.34) <sup>a</sup>	NS (0.69, 0.18)
		Peak Screening Value	NS (0.80, 0.13)	S (0.13, 0.07)	NS (0.19, 0.63)
	TVAP@ vs HNU@	Maximum Sustainable	NS (0.25) <sup>a</sup>	NS (0.51) <sup>a</sup>	S (0.03, 0.36)
3		Peak Screening Value	NS (0.61) <sup>a</sup>	NS (0.50, 0.59)	S (0.05, 0.70)
	TVAP1 vs HNU1	Maximum Sustainable	NS (0.59) <sup>a</sup>	NS (0.37) <sup>a</sup>	NS (0.54, 0.19)
		Peak Screening Value	NS (0.70) <sup>a</sup>	NS (0.64, 0.75)	S (0.27, 0.10)

Table 3-4.	Results of	Multivariate	Analysis	for Correlations	between	Instrument	Types
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Statistically significant at the 0.10 significance level (p-values for intercept and slope, respectively, given in parenthesis). Not statistically significant at the 0.10 significance level (p-values for intercept and slope, respectively, given in parenthesis). S =

NS =

<sup>a</sup> Insufficient data to test both intercept and slope terms.

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Figure 3-14 Plots Illustrating Effects of Component Type

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represent connectors, especially for the larger screening value ranges. Thus, the significant effect found for component type for the TVAF@ versus the TVAF1 correlation equations may be an anomaly.

Component service (i.e., light liquid, heavy liquid, or gas) was found to have a significant effect for six of the correlation equations evaluated. These were for the OVA@ versus OVA1 correlation equations (maximum sustainable and peak screening values), the OVA@ versus TLV@ correlation equations (maximum sustainable and peak screening values), the OVA@ versus TVAF@ correlation equation (peak screening values), and the OVA1 versus TVAF1 correlation equation (peak screening values). Figure 3-15 shows the data for each of these correlation equations overlaid with the service specific correlation equation. Although the ANCOVA results indicated that these equations were statistically different, the differences between the equations in plots (a), (b), and (e) of Figure 3-15 do not seem to be very large and may not be of practical significance. Plots (c), (d), and (f) of Figure 3-15 show larger differences between the correlation equations developed; however, these large differences may be due, in part, to the lack of data available to define some of the service types.

The last factor evaluated was windspeed. It was hypothesized that windspeed could potentially have a significant effect, especially for screening value readings obtained at 1 cm. Windspeed was found to have a significant effect for six of the correlation equations developed - the OVA@ versus OVA1 correlation equations (maximum sustainable and peak screening values), the OVA@ versus TVAF@ correlation equation (peak screening values), the TVAP@ versus HNU<sup>®</sup>@ correlation equations (maximum sustainable and peak screening values), and the TVAP1 versus HNU1 correlation equation (peak screening value). Thus, windspeed was found to account for a significant portion of the variability in the correlation equations developed for these six cases. The degree of variability of measured screening values as a function of windspeed is beyond the scope of this project, although, it could be investigated in future related work. However, the impact of windspeed on the correlation equations was minor. Only marginal improvements in the correlation coefficients were found for the equations for which windspeed was significant. For example, the correlation coefficient for the OVA@ versus OVA1 correlation equation improves from 0.929 to only 0.930 by including windspeed.

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Figure 3-15 Plots Illustrating Service Type Effects



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Figure 3-15 Plots Illustrating Service Type Effects (Continued)

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# Section 4 CONCLUSIONS AND RECOMMENDATIONS

### **RESULTS FROM DIFFERENT SCREENING INSTRUMENTS**

The four instruments use three unique methods to detect hydrocarbon concentrations. The OVA 108 and the TVA 1000 (FID) are both flame ionization detectors. The HNU<sup>®</sup> and the TVA 1000 (PID) are both photo ionization detectors. The TLV Sniffer<sup>®</sup> uses a combustible gas detector. The different hydrocarbon detection systems are believed to be the primary reason for the different results between instruments. The two FID instrument results and the two PID instrument results were much more comparable to each other than to instruments using different detection systems (FID vs. PID vs. combustible gas).

Results from this study indicate that measured screening values from different instruments are different for the same component. A set of adjustment factors, or correlation equations, have been developed as part of this study to convert screening values from the TLV Sniffer® and TVA FID instruments to those measured with an OVA. These correlation equations are shown on Table 4-1.

Variables Correlated	Screening Distance	Number of Data Pairs	Correlation Equation	Correlation Coefficient
OVA versus TLV Sniffer®	@ Surface	174	$OVA@ = (6.09 \times 10^{-1}) \times (TLV@)^{1.216}$	0.85
	1 cm	164	$OVA1 = (4.58 \times 10^{-1}) \times (TLV1)^{1.222}$	0.75
OVA versus TVA FID	@ Surface	54	OVA@ = (1.54) x (TVAF@) <sup>0.935</sup>	0.90
	1 cm	52	$OVA1 = (1.02) \times (TVAF1)^{1.013}$	0.83

Table 4-1. Equations Relating Screening Values From Different Instruments<sup>a</sup>

\* For maximum sustainable screening values.

Key

OVA@ = OVA screening value at the surface of a component.

OVA1 = OVA screening value obtained with a 1 cm spacer.

 TLV Sniffer<sup>®</sup> screening value at the surface of a component.
TLV Sniffer<sup>®</sup> screening value obtained with a 1 cm spacer. TLV@

TLV1

TVAF@ = TVA screening value at the surface of a component.

TVAF1 = TVA screening value obtained with a 1 cm spacer.

No correlations were developed to relate HNU® or TVA PID screening values to OVA screening values because an adequate correlation was not found between these screening

4-1

values. Therefore, it is <u>not</u> advisable to use mass emission correlation equations that were developed with an OVA when HNU<sup>®</sup> or TVA PID screening measurements are obtained.

Study results indicate that the differences between peak screening values and the maximum sustainable screening values were not significant.

### **RESULTS FROM DIFFERENT SCREENING DISTANCES**

The recent refinery and petroleum marketing terminals studies were performed by screening components as close as possible to the surface. For facilities having data obtained using a 1 cm spacer, that would like to apply results of these recent studies to their facilities, an adjustment factor needs to be applied. The adjustment factor for an OVA at the surface (OVA@) versus an OVA at 1 cm (OVA1) is given in the equation below:

 $OVA@ = (3.60) \times (OVA1)^{0.962}$  (Equation 4-1)

The recommended approach for converting TLV Sniffer<sup>®</sup> and the TVA FID screening values to comparable OVA screening values at the surface, when a 1 cm spacer is used with these instruments, is to first convert to comparable OVA values at 1 cm by using the correlations in Table 4-1 and then apply the above equation. Because of the lack of correlation for the HNU<sup>®</sup> and TVA PID to OVA screening values it is not recommended to convert any screening values from these instruments to OVA screening values. It should be noted that if a mass emission rate-screening value correlation line is plotted on log-log scale graph paper, based upon OVA screening measurements 1 cm away from the surface, and then Equation 4-1 is used to convert the 1 cm screening values (OVA1) to at the surface values (OVA@) and the straight line is replotted with the converted values on the same graph, the new line will be shifted to the right and will be lower than the original 1 cm mass emission rate-screening value correlation line.

Each of the instruments had screening values compared with that instrument at the surface to those with that same instrument at 1 cm. The effects of screening at the surface versus screening at 1 cm appears to have roughly the same impact for each instrument type. The screening values are two to three times lower, on the average, when obtained at a 1 cm screening distance.

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### COMPARISON OF STUDY RESULTS TO EARLIER STUDY

A previous study, entitled Valve Screening Study at Six San Francisco Bay Area Petroleum Refineries, or the "1979 Screening Study," reported on results for similar analysis of the TLV Sniffer<sup>®</sup> and the OVA 108. The current study, or "1994 Screening Study", evaluated more components, included connectors in the analysis, included additional screening instruments, and looked at additional factors that could influence test results such as windspeed, component type and service type.

Both studies show comparable differences between OVA and TLV Sniffer<sup>®</sup> screening values; however, the screening distance differences were more pronounced in the 1979 Screening Study than in the 1994 Screening Study. The reason for the differences in screening distance results is unknown. These differences could be due to differences in screening techniques, in ambient conditions, or in instrument sensitivities.

# COMPARISON OF OTHER FACTORS THAT MAY AFFECT THE CORRELATION EQUATIONS

An analysis was performed to determine other factors that may affect the relationship between screening values. Windspeed was found to have a statistically significant effect for some of the inter-instrument comparison correlation equations. However, the impact of windspeed on the correlation equations was minor. Only marginal improvements in the correlation coefficients were found for the equations for which windspeed was significant. For example, the correlation coefficient for the OVA at the surface versus OVA at 1 cm correlation equation improves from 0.929 to only 0.930 by including windspeed.

Component type and service type were shown to have a significant effect for a few of the screening value correlations developed; however, these are thought to either be anomalous occurrences or questionable due to limited data for a specific factor.

### Section 5

### REFERENCES

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- 2. American Petroleum Institute, 1994. *1993 Study of Refinery Fugitive Emission from Equipment Leaks*. API Publication Numbers 4612 and 4613. Prepared by Radian Corporation. Glendale, CA. February 1994.
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# APPENDIX A Screening Value Data

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Refinery	Compor	herd Informed	5			Amblent Co	nditions			Screening	ł			
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API / WSPA Screening Study Data

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12	a la	Gete	X	•	1	8	241	HN	02	02	5	0.2	02	
2	aviav	Gate	¥		Ľ	55	241	TVA 1000 (FID)						
12	N.S.	Gate	Ξ		11	55	241	TVA 1000 [PID]						
5	Mes	Gete	Z	:	LL LL	53	120	OVA 108	•	120	8	8	8	H2 ren eut.
5	aview	Gate	¥	:	LL L	53	120	TLV Sniffer						
5	wier	Gete	X	:	Ľ	8	120	MM	02	8	R	┛	2	Invald surface readings.
5	wiew	Gate	X	:	ц	8	120	TVA 1000 (FID)						
5	with	Gate	Z	:	Ľ	8	120	TVA 1000 (PID)						
-	war	Gete	¥	2	II	4	8	OVA 106	~	8	8	R	8	
	avier.	Gete	ž	2	1	4	480	TLV Shifter	2	8	8	8	8	
7	valve	Gate	I	2	1	3	400	HMu	10	10	8	5	13	
2	a Mar	Gete	Ξ	2	1	4	400	TVA 1000 (FID)	~	S	٤	5	8	
=	valve	Gete	Z	~	11	\$	8	TVA 1000 (PID)	5	15	8	7	•	
15	valve	Piug	Z	•	3	\$	ŝ	OVA 106		2200	220	1,100	1 600	
15	a her	P.	¥	•	3	8	9	TLV Sniffer	18	850	8	8	8	
15	with	Plue	¥	•	=	8	•	PAR F	<b>7</b> 0	99	8	8	R	
15	stist	Phus	¥	•	3	8	10	TVA 1000 [FID]	\$	1000	100	8	2700	Variable reading
15	W	Plug	Z	•	=	Ş	9	TVA 1000 (PID)	•	90	8	128	8	Variable reading
16	war	Gete	Z	•	=	8	5	OVA 108	~	2	8	8	8	
10	with	Gate	Z	•	=	8	5	TLV Sniffer	₽	8	Ş	8	8	
9	e yeke	Gate	Z	•	3	8	5	NH	10	9	ę	8	8	
9	valve	Gete	Z	•	н	8	51	TVA 1000 (FID)	2	<del>,</del>	8	8	8	
9	wiew	Gete	Ξ	•	3	8	51	TVA 1000 (PID)	•	8	8	ę	5	
17	when	Gate	U	•	H	\$	670	OVA 106	₽	2400	2400	8	88	
11	vehe	Gete	U	10	H	8	020	TLV Smiller	•	1.400	8	88	8	
17	vahe	Gete	ů	9	=	8	670	MH	F'0	8	8	\$	<b>\$</b> \$	
17	vehe	Gete	ů	<b>9</b>	=	\$	670	TVA 1000 (FID)						
17	MIN	Geta	J	9	=	ę	670	TVA 1000 (PID)						
18	May	Gete	Z	•	3	4	22	OVA 106	8	9,000	0.00	1 000	2,500	

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Refinery	Compon	ent Informeti	5			Ambient Co	nditiona			Screening	3			
	Component Type	Subcategory	Actuellon	818 ()	Service	Amblent Temp. Prevensel	Amblent Windspeed (fomin)	hredrument Type	Background Screening Value (ppm)	Maxtmum Sustainable Screening et Surtece (ppm)	Peek Berrenning et Surrince (ppm)	Maximum Bustainable Screening at 1 cm (ppm)	Peak Screening et 1 cm (Ppm)	Comments
18	when	Gate	¥	•	ц	47	<b>2</b> 20	TLV Sniffer	8	1,400	1.400	650	950	
18	vehre	Gate	X	9	ц	47	250	HNU	8	350	\$0 <b>4</b>	250	320	
91	win	Gate	X	8	n	47	220	TVA 1000 (FID)						
16	with	Gete	X	9	11	47	220	TVA 1000 (PID)						
10	when	Gate	¥	9	11	2	130	OVA 108	8	1,600	1,600	450	<b>8</b> 8	
10	with	Gete	¥	•	1	3	130	TLV Sniffer	15	650	660	420	420	
10	ş	Gete	¥	0	۲ ۲	2	130	N#I	•	300	8	150	9	
10	whe	Gate	x		11	2	130	TVA 1000 (FID)						Flame out PID too tour
\$	where	Gete	Z	9	3	2	130	TVA 1000 (PID)						Flarms out PHD too tow.
8	with	Gate	¥	12	r r	8	210	OVA 106	10	900	000	300	350	
8	wave	Gate	X	12	ц	62	210	TLV Souther	8	780	780	520	\$20	
8	wahe	Gate	¥	12	u l	62	210	HNU	3	300	8	220	82	
8	eview	Gate	X	12	n	62	210	TVA 1000 (FID)						Flame auf PID too tow.
8	ware	Gete	¥	12	Ч	62	210	TVA 1000 (PID)						Flame out. PID too tow
21	evies.	Plug	X	õ	11	8	130	OVA 105	10	550	650	8	8	
31	aviar	Plug	¥	10	n	8	130	TLV Sniffer	12	200	380	170	170	
21	valve	Phug	X	10	11	8	130	HNU	0	ę	8	250	320	Variable
21	wher	Phot	æ	0	1	86	130	TVA 1000 (FID)						
24	value	BNd	X	9	n	58	130	TVA 1000 (PID)						
R	vahe	Gate	I	٠	ц	8	110	OVA 106	10	1,000	1,500	140	140	
22	waite	Gete	Ŧ	-	3	8	110	TLV Shifler	5	8	8	8	20	
и	M	Gate	Ξ	-	н	8	10	INU	04	350	200	<del>1</del> 0	140	
8	with	Gata	X	-	3	8	10	TVA 1000 (FID)						
z	eview	Gate	ž	-	3	8	10	TVA 1000 (PID)						
£	aves	Gate	Σ	•	=	ş	88	OVA 108		180	8	110	140	
R	wher	Gete	Σ	•	=	8	8	TLV Shifter	\$	270	ß	I	z	
R	a la	Gete	2	•	3	8	995	Ψ	•	220	8	8	45	
R	A SA	Gete	Σ	•	3	8	550	TVA 1000 (FID)						
8	with	Gete	Σ	•	=	8	550	TVA 1000 (PID)						
74	valve	Gate	¥	•	E	\$	750	OVA 106	•	1,400	1,40	82	8	
7	Alla	5	Σ	•	=	\$	750	TLV Solfier		679	g	410	410	
24	N.S.	Gate	z	•	=	\$	750	IAN	•	140	8	ę	8	
24	e ves	Gete	Σ	•	=	ę	<b>9</b> 52	TVA 1000 (FIC)						
24	when	Gete	Z	•	Э	ş	750	TVA 1000 (PID)						
22	wave	Gente	X	-	GAS	22	210	OVA 108	11	8	₿	¥	8	
8	ever	Garte	¥	-	GAS	22	210	TLV Sniffer	8	8	8	8	8	
22	vahe	Gate	Z	٠	GAS	52	210	HAL	0	0	•			
22	a la	Gete	¥	-	GAS	22	210	TVA 1000 (FIC)						
8	way	afe O	¥	٠	GAS	ß	30	TVA 1000 (PID)						
8	wher	Gete	Σ	-	GAS	8	2	OVA 106	8	8	8	9	8	
R	wher	Gete	X	-	GAS	8	2	TLV Sniffer	5	R	a	8	Ş	
8	war	Gate	¥	-	GAS	ន	2	HNU	0	0	•	0	0	
8	vahe	Gate	W	•	GAS	8	~	TVA 1000 (FID)						TVA 1000 (FID) het IN BA140F

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API / WSPA Screening Study Data

Line component automatication and anti- sequence component automatication and anti- 27 velve carlos		ii E Se	87	Amblen Vice Tomp.	Amblert Windspeed	Instrument	Beckground	Meximum	Ĩ	Maxhmum	Ĩ	
20 value Call   27 value Call   28 value Call   29 value Call   20 value Call   21 value Call   21 value Call   21 value Call			_	le rest	e) (numin)		Screening Vatue (ppm)	Burtahable Boreaning at Burtace (ppm)	et Surface (ppm)	Sustainable Screening at 1 cm (ppm)	et 1 cm (ppm)	Comments
27 velve Gen   28 velve Gen   29 velve Gen   20 velve Gen   29 velve Gen   20 velve Gen   21 velve Gen   31 velve Gen			9	AS 50	2	TVA 1000 (PID)						
27     value     Qan       27     value     Qan       27     value     Qan       27     value     Qan       28     value     Qan       29     value     Qan       20     value     Qan       28     value     Qan       29     value     Qan       20     value     Qan       20     value     Qan       29     value     Qan       20     value			9	AS 51	8	OVA 108	•	8	٩	8	8	
27     value     Oat       27     value     Oat       28     value     Oat       29     value     Oat       20     value     Oat       29     value     Oat       20     value		-	Ö	AS 51	ą	TLV Sniffer	5	£	8	ę	ę	
27 valve Cat   28 valve Cat   26 valve Cat   27 valve Cat   28 valve Cat   29 valve Cat   20 valve Cat   28 valve Cat   29 valve Cat   20 valve Cat   21 valve Cat   21 valve Cat			ğ	AS 51	¥	<b>NN</b>	•	•	•	0	•	
21 rative Ore   28 rative Ore   29 rative Ore   29 rative Ore   29 rative Ore   29 rative Ore   20 rative Ore   21 rative Ore   22 rative Ore	2 2 2 2		ð	AS 51	¥	TVA 1000 (FID)						
78 value   28 value   29 value   28 value   29 value   20 value	222		G	AS 51	¥	TVA 1000 (PID)						
28     velve     Gen     Gen       28     velve     velve     Gen     Gen       29     velve     velve     Gen     Gen       20     velve     velve     Gen     Gen       21     velve     gen     Gen     Gen       21     velve     gen     gen     Gen	22			8	•	OVA 108	•	<b>36,000</b>	<b>20,000</b>	88	2,500	
28 value   29 value   29 value   29 value   29 value   29 value   29 value   20 value   20 value   20 value   20 value   20 value   21 value   22 value   23 value   24 Qar   25 Qar   26 Qar   27 value   28 Qar   29 Qar   21 value   22 Qar	2			95 1	•	TLV Sniffer	₽	400	4,000	2,000	2,000	
28 velve Cath   28 velve Qar   29 velve Qar   21 velve Qar   21 velve Qar   21 velve Qar				T 50	•	NNH	0	ŝ	ž	8	80	
28 value   29 value   20 value   28 value   29 value   20 value   21 value   22 value   23 value   24 Qar   25 value   26 Qar   27 value   28 value   29 Qar   21 value   22 Qar	ž 			96 T	0	TVA 1000 (FID)						
28 valve Carl   29 valve Carl   21 valve Carl   23 valve Carl   24 valve Carl   25 valve Carl   26 Carl Carl	2		Ļ	8	0	TVA 1000 [PID]						
28 value   29 value   21 value   21 value   22 value   23 value   24 value   26 value   27 value   28 value   29 value	2		Ļ	10	10	OVA 108	11	+112,000	+112,000	89,600	80,600	
28 valve Get   29 valve Get   21 valve Get   23 valve Get   24 valve Get   29 valve Get   21 valve Get	2	Ľ		6 1	16	TLV Sniffer	10	>10,000	>10,000	>10,000	+10,000	
28 valva Gat   28 valva Gat   28 valva Gat   20 valva Gat   20 valva Gat   20 valva Gat   21 valva Gat   23 valva Gat	2			L 61	16	NN	0	4.000	5,000	3,000	4,000	Erroneous readings (beyond range)
28 velve Get   90 velve Get   90 velve Get   90 velve Get   90 velve Get   91 velve Get   92 velve Get   93 velve Get	2			1 01	16	TVA 1000 (FID)						TVA 1000 (FID) Instr. M. AA1585
XX velve Qet	2			1 01	16	TVA 1000 (PID)						
30     value     Qat       30     value     Qat       30     value     Qat       31     value     Qat	4 2			8	110	OVA 108	10	1,100	120	88	8	
30     valve     Qar       30     valve     Qar       31     valve     Qar	4 N	-		8	110	TLV Shifter	8	054	8	22	420	
30 velve Ger 30 velve Ger 31 velve Ger	4			8	110	NN	-	ē	150	8	8	
30 velve Gel	4	-		8	10	TVA 1000 (FID)						
31 velve Ger	4	1		8	10	TVA 1000 [PIO]						
	2			5 1	8	OVA 106	12	0007	5,000	3000	3,500	
31 valve Ge	2			11	8	TLV Sniffer	8	1.800	80	1,600	1800	
31 valva Gei	2		]	5	8	NH	-	8	ŝ	8	8	
31 valve Ger	2			5	8	TVA 1000 (FID)						
31 valve Gar	2			5	2	TVA 1000 (PIO)						
32 valve Ga	4 9		]	8	Z	OVA 106	9	2800	3,300	1000	178	
32 valve Ga	4		]	8	2	TLV Shiffer	0	80	8	88	80	
32 value Ga	۲ ۲	]		8	Z	Ŧ₩	•	R	Ŕ	8	82	
32 valve Gal	4 9	1	$\frac{1}{2}$	8	2	TVA 1000 FID)						
32 value Gal	4 8	]		8	3	TVA 1000 [PID]						
33 con non 11			$\frac{1}{2}$	8	Z	OVA 106	•	8	8	8	8	
33 con-non Th		-		11 50	3	TLV Shifter	•	•	•	•	•	
33 con-non T	: 			11 <b>8</b>	2	PMH	•	8	ę	82	80	
33 con-non Th	-	-		8	z	TVA 1000 (FID)						
33 con-non Th	-	-		8	3	TVA 1000 (PID)						
34 valve Ger	te R			8	3	OVA 108	6	110	110	8	Ş	
34 valve Ger	4	-		8	Z	TLV Shifter	0	2	2	5	12	
34 valve Ger	đ Đ			8	3	Ŗ	0	120	Ĕ	۶	130	
34 valve Gai	2			11 8	8	TVA 1000 (FIC)						
34 valve Gei				8 7	J	TVA 1000 (PID)						
35 willia Ga	4			8 7	8	OVA 106	•	+112,000	+112,000	+112.000	+112,000	
35 valve Ge	- 			11 28	8	TLV Sniffer	0	>10,000	>10,000	>10,000	+10,000	

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Refinery	Compon	ent Informetic	ş			Amblent Co	nditions			Screening L	ł			
Laduena	Component Type	Subcringory	Actuation	N TE	Service	Amblant Tomp.	Amblert Windepeed (Minin)	Irype Type	Beckground Screening Value	Maximum Surtainable Screening at	Peak Bornenky at Surface	Maximum Sustainable Screening at 1 cm (pom)	Berwenting M 1 cm	Comments
	I		Ī	ŀ		ŀ	ļ			1	2	000	and the second sec	
8	Men	Gate	Z											
8	ala	Gate				8	2,5					T		
35	Ma	e D	<b>2</b>			8 8			•	5	1	5	Ş	
8	avax	e Gefe	=	-			\$			\$	\$		5	
8	· WEX	e o	Σ	-						2 5	2	28	2	
8	Mex	Gate	Σ	-		6	8	Ĩ		M	<u>A</u>	8	2	
8	Max	Gate	Σ	-		6	8	TVA 1000 (FID)						
8	vahe	Gate	¥	-	3	67	8	TVA 1000 (PID)						
37	Nex	Gate	X	9	11	57	8	OVA 106	5	2000	36.040	10,000	11,000	
8	Ň	Gete	X	•	11	57	103	TLV Sniffer	0	5.400	5.400			
5	1	Gete	z	•	=	57	18	HNU	0	1.000	1200			Variation
		ę	Σ	-	E	5	18	TVA 1000 (FID)						
, ,		e e e	₹	•	<u>و</u> .	57	103	TVA 1000 (PID)						
; ;	2	Gete	U	8	3	8	8	OVA 108	8	120	8	۶	75	
3 5	1	ate S	U	8	E	8	8	TLV Souther	ŝ	82	82			
			6	8	=	8	8	nut.	0	671	80			
8				8	=	8	8	TVA 1000 FED						
8		1		8 8		8	8	TVA 1000 (PIC)						
8 8				8	=	8	•	OVA 108	6	450	450	200	ŝ	
8				8	=	8	•	TLV Shifter	8	450	400	460	89	
				5	=	8		A.	8	300	340	٤	100	
8 8		Gata	0	8	=	8	•	TVA 1000 (FID)						
8 9	, in the second s	Gate	U	8	E	8	•	TVA 1000 (PIC)						
5	guu	u	:	•	3	8	270	OVA 108	•	8	8	12	2	
	<b>U</b> uuu		:	5	Ξ	8	270	TLV Souther	4	z	2	2	Ş	· Steam too by an 00 per mean
	y we		:		2	8	270	NH	0	8	8	6	ē	- Special has big an 10 ppm reading
	Con-f		:	5	E I	8	270	TVA 1000 (FID)						
	<b>Fron</b>		:	5	11	8	270	TVA 1000 (PID)						
5	aviar	Gete	X	•	II.	8	2	OVA 108	\$	112,000	112.000	80,000	100.000	
1	Max	Gate	2	•	IL I	8	2	TLV Sottler	-	+10,000	×10.000	×10,000	+10.000	
	MEX	Gate	Z	9	11	8	z	Ĩ	•	80	88	8	8	
1	eviev	Gete	X	•	Γ	8	12	TVA 1000 (FID)						
1	M	Gete	Σ	•	11	88	11	TVA 1000 [PD].						
:	N S	Brid	¥	•	11	8	8	OVA 106	12	8	8	8	Ş	
2	5	Ple	z	•	F	8	8	TLV Solfler	200					Bedground too Mgh.
	3	6	×	•	=	8	90	INN	0	Ŧ	-	4	ę	
2	a de la	9	×	•	1	8	8	TVA 1000 FTDI					·	
2	a May	S G	Z	•	LL	8	8	TVA 1000 (PID)						
2	Mex	Gate	¥	2	GAS	ន	250	OVA 108	•	8	8	8	8	
2	ever	Gete	¥	2	GAS	8	280	TLV Somer						Beckgrund tee Ngh.
8	Mer	Gate	¥	~	GAS	8	82	NH	•	0	•	0	•	
9	-	Gete	W	2	GAS	8	82	TVA 1000 (FIO)			Ī			
2	a Nev	Gete	X	~	GAS	8	250	TVA 1000 (PIC)						

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	Commenta								Rory thed									rafil. Fathel OC check.																										
	Peek Borwening M 1 cm (ppm)	16,000		8			5000	ĝ	2			7000	120				88	# 82	-			8	8	_			2000	<b>\$</b>				BBR	1,200				₿	8				000	82	
	Maximum Bustainable Screening at 1 cm (ppm)	10,000		8			4 500	8				0000	120				8	220				ę	8				2,000	<b>5</b> 8				3,000	1,200				<u>8</u>	8				200	82	
<b>Nets</b>	Peek Screening et Surface (ppm)	>112,000		<b>&gt;2,000</b>			18,000	00				61,600	<b>9</b> 2				90 1	8				٤	8				10,000	2,400					200				B	Ŗ				8	8	
Screening L	Maximum Sertening at Burtace (ppm)	+112,000		+2,000			16,000	Ş				61,600	88				1,000	8				8	80				14,000	2.400				DDD'E	1,200				8	021				1,000	940	
	Beckground Screening Value (ppm)	10		•			R	8				8	8				8	<b>8</b>				5	۶				2	8				R	8			!	₽	8				₽	8	
	hetrument Type	OVA 106	TLV Shiffer	ł	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Shifler	HNU	TVA 1000 (FIC)	TVA 1000 (PIO)	OVA 106	TLV Sniffer	HNN	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Sniffer	HNU	TVA 1000 (FIO)	TVA 1000 (PID)	OVA 108	TLV Shiffer	HNN	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Solfier	Ŵ	TVA 1000 (FID)	TVA 1000 (PIO)		TLV Solfler	RAL	TVA 1000 F1U1		OVA 108	TLV Shifler	<b>7</b>	TVA 1000 [FID]	TVA 1000 (PID)	OVA 108	TLV Shifter	INN
nditione	Ambient Windapeed (Twhin)	8	8	8	8	8	115	115	115	115	115	\$	<u>8</u>	190	8	<b>1</b> 80	155	155	155	155	155	8	300	90	30	8	ş	88	987	Ş	<b>Ş</b> :	2	2;	21	2;		8		2	<u>s</u>	8	8	ē	ŝ
Amblent Ct	Ambient Temp. (Parenter)	8	8	8	8	8	8	8	90	8	8	3	2	2	3	2	8	8	8	ş	8	\$	88	84	8	84	4	47		-		8	*	8	8 3	8	22		3	22	52	3	52	52
	Bentce	r	11	11	LL LL	n	n	Π	n	'n	=	3	=	3	3	=	H	╡	=	3	=	=	E	Ε	3	3	₹	╡	╡	=			╡╴						╡	╡	╡	╡	=	LL LL
	8126 (.m)	4	4	4	4	4	0	•	9	•	•	۰	•	•	•	٩	•	•	•	•	•	•	•	•	•	•	-	-	-	-	- -	•	•	•		•		₽ 	╸	┛	•	•	•	•
ton	Actuation	×	Z	¥	X	X	X	X	X	X	X	Z	Ξ	Ξ	Ξ	Ξ	Z	z	Σ	2	Ξ	Ξ	Z	Z	Z	E	<b>0</b>	0	0	0	•		<b>3</b>			E			<b>u</b>	<b>u</b>	<b>u</b>	×	×	¥
vent Informet	Bubcategory	Gete C	Gate	Gate	Gate	Gete	Gate	Gate	Gete	Gate	Geta	S S	Gate	ŝ	Gate	Gate	<b>4</b> 0	Gate	Gee G	Geb	Gate	Gate	Gate	Gate	Gate	Gate	A B B	ŝ	Ś	λ.	ž						e de		Gate	e G	Gete	Qafe	Gate	Gete
Compor	Component Type	Nev	valve	wine	water	v eviev	eviev	withe	vahe	vahe	Alive	evite	e viev	a la	Ala	Ala	ave.	wiev	ever Nev	M	wher	M	eviev	M	a Mer	e Mer	with	May	Alle	MIN	ala Mar		84 F				N.S.	M.	M	May	e Mer	e ye	Mex	a Mar
Refinery	L Selection	\$	44	4	4	44	45	45	\$	45	45	\$	\$	\$	8	94	47	47	47	47	47	8	8	8	8	48	9	\$	9	ę	\$	8	8	8	8	8	5	51	51	51	51	52	52	52

Definition	Common Common	and Information	8		ſ	Amblent Co	ndttone			Screening L	ş			
	Component	Subcritegory	Actuation	Sire	Bervice	Amblent Temp.	Ambient Windspeed	Instrument Type	Beckground Screening	Mextmum Suetainable	Peak Borreening	Maximum Sustainable Acreening at	Peak Screening at 1 cm	Comments
NUMber	Type			Ē		(Laborated)	(Tumin)		(mdd)	Surface (ppm)	(udd)	1 cm (ppm)	(udd)	
	1	a de la constante de la consta	3	•	3	52	8	TVA 1000 FIDI						
	Way	Gate	Z	•	Ц	52	180	TVA 1000 (PID)				1		
2	way	d ete	¥	-	3	51	120	DVA 106	8	3,500	mere	3		
	a New	Gete	Σ	-	1	5	120	TLV Soffler	8	8801	1.000	256	2 2 2	
		e Be	I	-	11	51	120	MH						
2	a day	e te c	Z	-	1	51	120	TVA 1000 (FID)						
3		a c	¥	-	5	51	120	TVA 1000 (PID)						
				5	=	s	140	OVA 106	10	>112,000	112000	>112,000	>112,000	High vertebbe with Tom.
8	A N		,	5	=	8	140	TLV Sniffer	8	> 10.000	+10,000	×10,000	+10,000	
8	MA		, ,	5	=	8	140	HNU						
85	M			5	=	8	94	TVA 1000 (FID)						
8	ME		, <b>,</b>	5	=	2	140	TVA 1000 (PIO)						
2	MEN	CINCK	> >	•	=	3	230	OVA 106	10	10,000	10,000	8	10,000	
530	A A		E 3		=	3	230	TLV Solffer	£	2,600	2,600	1,100	1,100	
28	M		E	•	=	2	230	NNH						
25	MRA		E 3	•	=	8	230	TVA 1000 (FIC)						
550	MEA	Gate	Ξ	•		5	86	TVA 1000 (PID)						
25	May		¥ :	•	100	2 5	8	OVA 108	7	750	750	360	805	
2	WEA		Ξ.	•	240	3 5	8	TLV Sniffer	и	370	37	8	8	
3	Way		E	•	200	5	8	HNM	-	300	<b>3</b> 60	902	R	
2	with	Gate	2			2 5	8	TVA 1000 ED		1,400	1,700	1,800	2,200	Highly variable
2	AN AN	Oate	Σ		899	8 5	2		5	170	172	170	8	
54	ever	Gate	Σ	•	283	8				900	1,100	20	250	
8	vahe	Plug	Z	-	з	1	210		- 5	ş	8	82	83	
8	vahe	Phys	Σ	-	=	47	210	ILV Shime	2.		, in the second s	R.	992	
2	May	Plue	¥	4	=	47	210	INU		8			Ē	Hardte verhalten
3	vaha	Pue	¥	4	II II	47	210	TVA 1000 FID	•	<b>0</b> 6		8 8		
3	aviav	đ	¥	4	L L	47	210	TVA 1000 (PID)	67	011			ş	
3		anta	Z	•	1	8	230	OVA 108	ę	Ø	me	3	2	
3	-	Ptus	ž	4	3	\$	230	TLV Shifler	20	08/	2	2		
8	1	and Alto	Z	•	Ħ	48	20	NH	-	92X	B			
R		9	Σ	•	=	919	230	TVA 1000 [FID]	-	1,100	0051	006.1	7.000	and the second se
B		5	Z	-	2	84	230	TVA 1000 [PIO]	\$	5	82	Bez	me	
8			U	-	3	45	250	OVA 108	•	>110,000	>110,000	110,000	000/0114	Lucord Put IAA
57	5			-	=	45	8	TLV Shiffer	8	×10,000	+10,000	×10,000	×10,000	
57	WR		    -		=	\$	220	NNH	8	<b>*2,000</b>	v2000	8	8	
57	-		,  -	1	=	¥	92	TVA 1000 (FID)	•	302,400	372,960	163,800	277,200	
57	AMEN	Cate		•		2	ş	TVA 1000 (PIO)	5	740	961	700	800	
57	ever.	Gate	3	•		;;;			ę	2	8	15	15	
8	with	Gete	5	:				110	-	•	0	0	0	
8	Way	Gate	0	:			8	ILV SAMTO	,	•	~	2	7	
8	war	Gate	0	:	=		<u>8</u>	DATE:	.		¥	ţ	:	
8	waw	Gate	0	:	=	9	100	TVA 1000 (FILO)	•	•	2	2 =	=	
8	eviev	Gate	v	:	=	47	8					902	2002	
9	ANEX	Gate	¥	-	3	ę	100	OVA TUB	<u> </u>	~				

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	Comments																				Spacer tee Mg.													No lead the to FID theme aut									
	Peek Boreening at 1 cm (ppm)	300	2	1,200	0.5	700	800	16	2,100	8	550	5	¥	8	3	8	100	8		40	0,000	1,200	9	400	2	3,000	80	<u>1</u> 8	999	2	×110,000		>176.400		220	82	ę	2000	17	₿	0	82	
	Maxtmun Buoteinable Berreening at 1 cm (ppm)	300	15	000	•	500	044	16	8	17	550	8	8	200	8	8	8	8		10	3,000	1,200	9	300	8	2,500	8	8	647	5	×110,000	2007L	>176.400		8	8	₽	1,500	17	8	0	5	
ł	Peek Bertaching A Berthera (prim)	440	\$	1,300	10.5	0.500	1,000	t)	11,000	27	8	220	ê.	1.610	\$	100	8	75	1,005	11	10,000	2,300	2	16,000	ĸ	3,000	100	2	5,000	2	>110.000		>178,400		2300	1.00	4	3,100	10	<u>8</u>	0	180 1	
Screening D	Maximum Businable Accessing at Burlince (ppm)	044	5	006	10	6,500	1,000	13	6,000	~	1,000	82	5	8	8	1000	₽ <b>₽</b>	75	1,800	٥	6,000	2.300	7	1,100	۶	3,000	1 000	ŝ	5,300	8	>110,000		>176.400		2,300	8	7	3,100	17	8	•	5 25	
	Beckgreund Screening Vatue (ppm)	0	1 1	3.	6.6	•	0	0	+	6.3	•	•	0	5	0	~	0	0	0	0	8	0	0	10	₽	~	•	•	•	•	₽		,	12	₽	•	•	•		1	•	•	
	hotemont Type	TLV Sniffer	HAN	TVA 1000 (FIC)	TVA 1000 (PID)	OVA 108	TLV Shiffer	HNU	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Smither	NA	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Shiffer	<b>NM</b>	TVA 1000 (FIO)	TVA 1000 (PID)	OVA 108	TLV Sniffer	HNN	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Soffier	M	TVA 1000 (FID)	TVA 1000 (PIO)	DVA 108	International Station	TVA 1000 (FID)	TVA 1000 (PID)	OVA 100	TLV Smiller	NNH	TVA 1000 (F10)	TVA 1000 [PIC)	OVA 106	TLV Shiffer	N.	
nditione	Amblent Windepeed (19min)	180	100	160	100	230	230	230	200	20	R	R	8	8	8	\$	04	8	Q.	8	156	156	156	156	156	٤	٤	٤	٤	2	8 8	3 8	8	8	R	SZ.	\$	8	R	24	24	24	
Ambient Co	Amblent Temp. Preserves	48	\$	8	84	¥	8	<b>8</b>	8	¥	\$	\$	Ş	\$	Ş	S	8	53	53	8	2	2	2	2	3	51	2	5	2	51	5	, <b>;</b>	57	57	57	57	57	57	57	2	2	2	
	Bervice	n	'n	11	n	١٢	11	11	ц	n	1	11	11	rr I	H	η	II.	LL L	L.	Ц	L L	Н	ц	Ц	=	4	3		3	=	=	-	3	۲	11		LL	1	L.	3	=	11	
	8120 (ini)	•	-	-	-	•	•	•	•	9	-	-	-	-	-	•	6	C	3	\$	0	0	8	0	•	-	-	┨	-	-	4.		2	•	2	2	2	2	2	•		9	
5	Actuellon	×	X	¥	æ	¥	¥	X	Z	X	Σ	X	Z	X	Z	v	o	υ	J	S	v	v	ပ	v	J	¥	¥	¥	¥	×	<b>x</b> :	E 3	z	×	¥	X	¥	×	¥	¥	Σ	X	
Hent Informed	Subcempory	Gate	Gete	Gete	Gete	Gate	Gete	Gete	Gete	Gete	Gate	Gate	Gate	Gate	Gate	Gate	Gete	Gate	Gate	Gette		L	u	L	•	Gete	et o	e e e e e e e e e e e e e e e e e e e	C at	Gate	e d		o te O	Gete	Gene	Gete	Gete	Gete	Gete	Set C	Gete	Gette	
Compon	Component Type	avier.	eview	vahe	eview	when .	eviev	a the	velve	vehe	even	a la	with	evier	vaive	valve	valve	vahe	vahe	valve	con-fl	con-fl	con-fl	con-fl	con-A	a Mari	Mar	e ve ve	ANA	even	N I		N.	N.S.	¥.	vahe	vahe	valve	eviev	eyex	ş	eves	
Refinery	-H	3	8	8	8	80	8	8	8	80	5	61	91	61	61	62	62	62	8	82	8	8	8	8	8	2	8	8	2	2	81	B	3 18	8	8	8	8	8	8	67	67	67	

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Refinery	Compon	ent Informeti	5			Amblent Co.	nditione			Screening L	ate			
	Component Type	Subcategory	Actuation	Ê	Bervics	Ambient Temp. Persenal	Amblent Windspeed (17min)	hattument Type	Beckground Bcreening Value (ppm)	Maximum Bustainable Bustaening at Surface (ppm)	Presk Borrening at Burbors (ppm)	Maxtmum Buetalmable Screening at 1 cm (ppm)	Peak Bereaning M 1 cm (ppm)	Comments
67	May	ę	Z	•		2	24	TVA 1000 (PID)		8	120	11	8	
8	Max	Gate	Z	٠	u	3	24	OVA 106	•	10	\$	13	6	
8	avier	ete O	Ξ	•	=	м	24	TLV Sniffer	0	0	•	0	•	
8	Max	đ	Z	-	2	35	24	HNU	0	9	5	•	6	
8	avlay	đ U	Z	-	۲ ۲	2	24	TVA 1000 (FID)	2	15	1	\$	Ŧ	
5	Max	đ	Z	-	E	3	24	TVA 1000 (PIO)	7	\$	<b>9</b>	10	1	
and a	a ha	9 9 9	Z	•	F	\$		OVA 108	7	009	ĝ	8	900	
88	a hav	Gete	Ŧ	•	3	8		TLV Shiffer	0	8	Ŗ	0	0	
5	with	Gate	Ŧ	•	T T	8	•	HNU	0	•	•	-	•	
888	May	0	X	9	n	8		TVA 1000 (FID)	-	202	2	83	8	Invekt readings at 1 cm.
BAA	a Nex	Q ata	¥	0	u. I	55	•	TVA 1000 (PID)	7	•	<b>6</b>	•	•	
8	N.	Gete	Z	÷	n I	8	<b>1</b> 80	OVA 106	7	5.000	88.2	5,000	2,000	
8	a de la	đ	3	-	E	8	180	TLV Sniffer	2	1,800	1,800	3,600	3,600	
8	a ver	e e e	Z	-	n,	3	<u>1</u> 80	Ņ	0	8	•	•	9	
8	Mes	Gate	2	-	H	53	160	TVA 1000 (FID)	-	16,000	21,000	18,000	21,000	
8	a la	Gete	2	-	2	8	160	TVA 1000 (PIC)	7	R	8	8	8	
8	N.	Gett	Ŧ	~	ц	\$	42	OVA 108	80	650	000	82	82	
2 8	N.	5	Z	~	H	8	42	TLV Sniffer	52	240	340	350	88	
2 8	-	Gate	2	~	3	8	42	HNM	-	•	•	8	•	
2 8	a Mary	Gete	Z	~	L I	8	42	TVA 1000 (FTD)						Service the connect broke
2 2	when	e e co	X	~	3	8	4	TVA 1000 (PID)						
14	avia	Gate	ž	2	ц	57	8	OVA 106	•	ę	8	8	250	
~	eviev	0 afe	ž	2	ц	57	Ř	TLV Shiffer	0	9 <b>2</b> 4	\$	ę	140	
5	e yes	Gete	Z	2	ц	57	8	HNN	٥	\$	8	12	8	
2	eview	Gete	X	2	н	57	82	TVA 1000 (FID)						
-	avier	0 ete 0	X	2	ц	57	Ř	TVA 1000 [PID]						
A27	Mar	Plug	X	e	Ц	8	200	OVA 108		1000	80	8	80	
A27	Mar	evid	¥	8	'n	8	8	TLV Sniffer	8	000	8	80	992	
Va	Mar	5 M	I	¢	u	8	ŝ	7¥I	0	8	8	ଛ	ę	
¥27	W	Bind	X	•	ц	8	8	TVA 1000 (FID)						
724	vahe	Plug	Ŧ	•	3	8	8	TVA 1000 [PIC]	Ī					
728	ww	Gate	Z	È	=	8	8	OVA 108	~	9 <u>5</u>	8	8	0001	Dear of Star teatra
821	NBA	Gate	Σ	Ë	3	8	8	TLV Snifler	•	480	400	220	ŝ	
822	a a a a a a a a a a a a a a a a a a a	Gate	¥	ġ	Η	8	8	NNH	•	ĝ	8	8	8	
87.1	wer	Gate	Z	2	ц	8	8	TVA 1000 (FID)						
877	a May	Gete	X	12	ц	8	8	TVA 1000 (PID)						
2	44	e e e	X	12	L I	8	132	OVA 108	~	320	8	<del>1</del> 50	ŝ	
2	Ņ	e e e	X	12	Ч	28	132	TLV Shifter	2	150	150	₿	₿	
2	a de la	Gate	¥	ġ	П	\$	132	NAH	0	80	8	₿	Ş	
R	e vier	Gafe	X	2	н	\$	132	TVA 1000 [FID]						
2	a de la	Gate	¥	21	н	8	132	TVA 1000 (PID)						
2	MAN	Ptue	X	2	'n	8	2	OVA 108	~	1.600	2500	88	8	
	a de la compañía	Pide	Σ	~	H	8	8	TLV Shiffer	0	8	8	200	300	

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Refinerv	Compo	and Informed	8			Amblent Co	viditions			Screening				
	Component	Subcriegory	Actuation	ž ž	Bervice	Amblert Tomp.	Amblert Mindspeed	hadrument Type	Beckground Beckground Bereentry Value	Restanting to		Mextmum Bueternebie	A Service 1	Commenta
				Ì					(mqq)	Surface (ppm)	(undd)	1 cm (ppm)	(mqq)	
24	valve -	Phug	W	2		8	20	HIM	0	200	1,000	10	200	
24	evier	Brid	X	2	F	8	8	TVA 1000 (FID)						
2	Max	5	¥	~	E	8	2	TVA 1000 [PID]						
2	when	Gete	0	~	E	3	13	OVA 108	~	1,600	2,200	1,100	1,100	
2	Max	Gete	0	~	3	2	13	TLV Shiffer	3	80	8	8	8	
8	eview	Gete	0	~	3	3	13	NH	•	8	1.00	8	8	
ĸ	avlav	Gute	0	~	=	8	5	TVA 1000 (FID)						
8	vahe	Gate	0	~		3	13	TVA 1000 (PID)						
2	Mex	Gate	3	-	=	8	8	OVA 106	•	98	8	8	8	
٩	Max	Gete	E		=	8	8	TLV Sniffer	3	240	240	175	175	
2	A S	Gete	3	•	3	8	8	NNH	0	90	88	90	170	
R	ever	Gete	3	•	1	8	8	TVA 1000 (FID)						
92	aver	Gate	Z	•	=	8	96	TVA 1000 (PID)						
2	Mex	Phys	Z	~	E	57	140	OVA 106	2	>110,000	>110,000	10,000	11,000	
"	ever.	Phua	Z	2	3	57	140	TLV Sniffer	2	5,500	5,500	4,300	4,300	
4	evier	Big	Z	~	3	5	140	NNH	•	900	8	200	000	
2	aviav	Buid	Z	~	Ξ	57	140	TVA 1000 [FID]						
4	e viev	Pice	×	~	E	5	945	TVA 1000 (PID)						
82	WEA	Gete	с о	2	1	8	8	OVA 108	7	902	1,100	375	325	
70	vehe	Gete	c	2	1	3	8	TLV Shiffer	4	230	230	8	8	
82	vahe	Gete	C	2	u l	\$	8	HNN	4	004	909	200	200	
84	Aline	Gate	ပ	2	r	8	8	TVA 1000 (FID)						
78	vahe	Gate	υ	2	ι	8	8	TVA 1000 [PID]						
٩	vahe	Plug	X	2	H	8	8	OVA 108	4	140	180	160	160	
٩	Max	Plug	X	~	1	8	8	TLV Shiffer	0	8	8	42	4	
8	when	Plug	X	2	1	8	20	HNU	•	290	300	\$	45	
٩	water	Plug	Z	2	3	56	8	TVA 1000 (FID)						
٩	vahe	Plue	X	~	11	8	R	TVA 1000 [PID]					_	
8	valve	Plue	Z	-	1	57	125	OVA 108	7	86	8	45	45	
8	valve	Plue	¥	-	=	57	125	TLV Solller	0	10	\$	0	0	
8	aviev	P	¥	-	=	57	125	HNU	0	-	\$	2	2	
8	Alite	Big	¥	-	=	57	125	TVA 1000 (FID)						
8	with	Plug	¥	-	3	57	125	TVA 1000 (PID)						
81	valve	Gate	X	~	н	8	165	OVA 108	7	806	8	250	250	
81	valve	Gete	Σ	~	н	8	185	TLV Shiffer	0	8	100	8	8	
81	vahe	Gate	Σ	~	3	8	185	HNU	0	250	300	100	130	
61	valve	Gete	Ŧ	~	Ξ	8	185	TVA 1000 (FID)						
81	eviev	Gate	Σ	~	Ξ	8	185	TVA 1000 (PID)						
29	aviav V	Gate	Ξ	م	3	8	400	OVA 108	10	8	8	16	10	
8	ŅS	Gate	Ξ	~	3	8	994	TLV Sniffer	0	10	10	0	0	
82	vahe	0.ete	3	~	=	8	400	HNU	0	R	8	•	¢	
8	wer	Oate	Z	٩	=	8	400	TVA 1000 (FID)						
2	ANN	Gate	Σ	2	3	8	8	TVA 1000 (PID)						

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Kellnery	Compor			ſ			AND DO DO			OCLAMINA DO				
	Component	Subcategory	Actuation	8128 ('u')	Service	Amblent Temp. (Fernind)	Amblent Windspeed (Tomin)	histrument Type	Beckground Screening Value (ppm)	Maximum Bertainable Screening at Surface (ppm)	Peek Bertening (ppm)	Maximum Suetainable Screening at 1 cm (ppm)	Peak Screening at 1 cm (ppm)	Comments
2	ad an	Gete	2	٩	ŀ	8	R	OVA 106	~	8	8	\$	22	
2			2	~	=	8	ŝ	TLV Sniffer	0	0	•	0	0	
2		Gebe	2	~		8	8	NH	0	10	\$2	10	10	
	a la	ł	3	~	=	8	290	TVA 1000 (FID)						
8	when .	de C	I	~	=	8	280	TVA 1000 (PIC)						
2	MEX	o de fo	¥	~	E	8	75	OVA 108	11	8	8	R	8	No component ID number found
2		C etc	2	~	=	8	75	TLV Sniffer	16	29	\$2	8	10	
		ete C	3	-	=	8	22	Ĩ	•	136	8	8	20	
	3	Gate	3	~	=	8	2	TVA 1000 (FID)						
2	win	Gate	×	~	1	8	75	TVA 1000 [PID]						
8	when	Gete	υ	~	2	8	46	OVA 106	11	×110,000	>110,000	+110,000	>110,000	
2	Max	Gate	U	2	3	8	48	TLV Sniffer	2	6,000	<b>6</b> ,000	8	R	
2	win	Gate	U	~	2	8	8 <b>8</b>	HNN						
2	avlay	Gete	· u	~	2	8	46	TVA 1000 (FID)						
3 8		Safe		~	=	8	84	TVA 1000 (PIO)						
3		ate C	3	-	=	8	8	OVA 108	7	360	36	250	82	
3		ę	3	•	3	8	8	TLV Sniffer	0	220	220	160	180	
8		Gate	2	-	1	8	8	ny H	•	300	300	80	٤	
3			-	-		8	8	TVA 1000 (FID)						
8		Cate	2	-	=	8	R	TVA 1000 [PID]						
8			2	•		10	9	OVA 106	7	4,000	4,000	5,000	5,000	
20		ate C	3	-	3	ē	10	TLV Sniffer	0	1,200	1,200	044	440	
	a la	Gete	Ξ	-	F	5	18	NH	0	660	920	8	8	
6	a view		×	-	E	5	18	TVA 1000 (FID)						
			3	-	=	5	18	TVA 1000 (PID)						
2		te c	2		=	8	8	OVA 106	10	5,000	6,000	2,000	2,000	
5	winv	e e e	Ξ	~	=	2	8	TLV Solfler	0	1,000	1,000	70	ŝ	
8	a de la compañía	Gete	¥	2	1	2	<b>6</b> 5	HNU	14	8	8	880	959	
8	eview	Gate	X	2	'n	2	8	TVA 1000 (FIO)						
8	vahe	Gate	¥	2	1	z	5	TVA 1000 [PID]						
8	a May	Gate	¥	2	1	5	5	OVA 106	8	8	8	80	8	
8	vahe	Gate	Σ	~	=	9	\$	TLV Soffer	2	96	8	8	8	
8	wahe	Gete	X	2	1	9	57	NH	ē	8	8	88	200	
9	valve	Gate	Σ	2	н	5	43	TVA 1000 (FID)						
8	value	Gete	Σ	2	3	9	57	TVA 1000 (PID)						
8	2	Gete	X	2	1	8	2	OVA 108	8	<b>\$</b>	\$	250	82	
8	aver	Gate	W	2	ц	8	2	TLV Shifter	14	230	8	120	120	
8	even	Gate	M	2	11	8	72	NH	ţ	660	88	45	8	
8	avia	Gate	M	2	n	8	2	TVA 1000 (FID)						
8	a Mar	Gate	X	2	ц	8	2	TVA 1000 (PID)						
5	avier	Gate	X	-	3	8	8	OVA 108	10	2400	2,500	1,200	900	
2	a la	Gene	¥	-	ľ	8	8	TLV Shifter	0	1000	900 F	200	8	
6	-	et c	z	-	3	8	8	Ĩ		600	800	350	004	

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Refinery	Compon	went informatio	8			Amblent Co	nditione			Screening	3			
	Cemponent Type	Subcategory	Actuation	erre (m.)	Bervice	Ambient Temp. Prevenses	Amblent Windspeed (Tbinin)	hreirument Type	Beckground Screening Value (ppm)	Maximum Burtanatia Burtace (ppm)	Peak Bicreening At Surface (ppm)	Maximum Sustainable Screening at 1 cm (ppm)	Peak Berwaning at 1 cm (ppm)	Comments
5	Mar	Cete C	X	·	11	8	8	TVA 1000 (FIO)						
5	a yes	Gete	Σ	-	-	00	00	TVA 1000 (PID)						
8	ever	Gate	¥	9	11	8	8	OVA 108	0	10,000	10,000	000,0	0,000	
8	May	Gette	3	9	L I	8	8	TLV Shiffer	0	8	8	120	8	
8	Mex	Gate	×	•	11	8	8	PNF1	7	8	8	8	8	
8	ave.	Qate O	¥	•	11	8	8	TVA 1000 (FID)						
8	e viev	Gate	×	•	11	8	8	TVA 1000 (PID)						
8	Mer	Gete	¥	2	n l	88	230	OVA 106	¢	8	240	110	110	
8	Max	Gate	X	2	ц	55	230	TLV Shiffer	0	8	₿	8	8	
8	Ne.	Gette	¥	2	n	55	230	NH	7	160	ŝ	8	110	
8	M	Gatte	X	2	L L	8	230	TVA 1000 (FID)						
8	Mer	Gete	X	2	n	55	220	TVA 1000 (PID)						
2	a Mar	Gate	X	2	u l	2	220	OVA 108	10	054	Ş	220	8	
2	vahe	Gate	X	2	L L	2	22	TLV Sniffer	0	280	8	120	120	
3	evier	Gate	X	2	11	3	20	NN	0	<b>200</b>	8	<b>1</b> 00	200	
2	velve	Gate	X	2	11	3	82	TVA 1000 (FID)						
2	valve	Gate	X	2	н	2	82	TVA 1000 [PID]						
8	avier,	Gate	¥	~	3	8	ē	OVA 108	6	1000	2000	8	ŝ	Supe.
8	eview	Gete	I	٩	3	3	ē	TLV Shifter	0	88	8	320	320	
8	with	Gete	3	2	H	3	8	R	~	8	8	8	<b>\$</b> 3	
8	with	Gate	Z	٩	3	8	8	TVA 1000 (FID)						
8	ayay	Gete	Z	~	Ξ	8	8	TVA 1000 (PID)						
8	ww	Gate	Z	~	H	3	₹	OVA 106	-	1,400	8	1,000	1200	Sum.
8	MM	Gete	æ	~	3	8	ž	TLV Shiffler	0	8	8	240	540	
8	e ve	Gete	×	~	=	3	8	PNR	•	8	8	ĝ	ĝ	
8	ever Nev	ee o	Σ	~	3	8	ŝ	TVA 1000 (FID)						
8	e ve ve	Gate	¥	~	3	3	5	TVA 1000 (PIC)						
6	with	36	Σ	•	3	\$	8	OVA 108	~	25,000	<b>15 000</b>	10,000	80	3 <u>5</u> m.
ه/	A A		₹ I	•		5	8		8			N,		
6 6		5 5	Σ	•	=	\$ 9	8 9	TVA 1000 FEITA		•	2150			TVA 1000 (FD) trate 14 6A1508 Began VOC by mode
. 6		Dig	3	•	E	9	8	TVA 1000 (PID)	9		\$		ę	TVA 1000 (PID) Indf 14 6A1506
: 8	Way	54	Z	•	E	8	175	OVA 106	12	000'06	<b>95</b> ,000	000'8	10,000	
8	aver	Plug	¥	9	11	55	175	TLV Sniffer	9	7,600	7,500	1,800	1,600	
8	ever	Plug	X	8	11	58	175	HNV	0	00#	400	380	360	
8	vahe	Plug	¥	•	Ц	8	175	TVA 1000 (FIO)	2		23,467		13,140	
8	e viev	Pig	¥	•	3	R	175	TVA 1000 [PID]	40		526		82	
8	e viev	P <sub>2</sub>	Σ	•	=	52	8	OVA 108	12	2000	2,000	8	ĝ	
8	with	Pige	Σ	•	=	52	8	TLV Sniffer	-	1,000	1 000	320	8	
8	MEN	Pho	X	•	=	25	8	HNU	•	150	ŝ	130	5	
8	Alle	B	¥	•	=	8	20	TVA 1000 (FID)	6		4.740		1.520	
8	W	<b>M</b> A	×	•	=	52	8	TVA 1000 (PID)	12		8		11	
<b>6</b>	aya	Pwa	Σ	•	=	8	55	OVA 108	\$	2,000	2200	- 40	1,000	

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	1	Π	7		Т	Т	Τ	7	Τ	1	Т	Т	Τ	Т	Т	Т	1	T	Т	T	Т	Т	Т	Т	Т	Т	Т	Т	T	Τ	Γ			Т	1	Т	Т		T	Т	Т	-
	Comments							Erroneous readings (beyond range)																														1 cm - No CM.				
	Peak Borsening at 1 cm (ppm)	340	130	2,430	ž	750	760	2,000	1.476	178	3,500	1,000	185	7,631	270	30,000	1,000	•	8	Z	8	9	0	414	13	2,000	8	Re	<u>817</u>		5	-	9,214	31	000 (Q4	8	8	12,400	8	1,000	1000	Ę
	Maxtmen Burtaineble Bcreening at 1 cm (ppm)	340	130			250	700	2000			300	1,000	ŝ			20,000	900-	•			8	<b>9</b>	0			1400	80	R			2	F			40,000	200	•			000	<b>00</b>	ş
	Peek Bersening at Burbers (ppm)	906	250	7,785	164	2,000	g	2,400	5.075	16	20,000	2.000	8	0.00	376	+100,000	2300	2	0.002	ħ	88	2	•	5	2	350	8	8	5.46		a ta	=	45,236	8	×100,000	130	•	010.00	8	800	100	-
Screening L	Maximum Burtainable Screening at Burface (ppm)	300	250			2.600	96	2.400			50,000	2,000	185			100,000	2300	\$			300	270	٥			3,500	1,000	0 <u>6</u> 2			2 100	1			+100,000	4,500	•			0,000	1,600	
	Beckground Bereening Value (Ppm)	21	•	6	12	10	0	2.5	•	5	5	•	•	~	12	\$	•	•	•	5	~	•	•	•	12	-	•	0	,					õ	4	\$	0	2	12	7	-	
	histumoni Type	TLV Sniffer	2¥	TVA 1000 (FID)	TVA 1000 (PIO)	OVA 106	TLV Suffer	N.	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Sollier	RN	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Sniffer	ANH	TVA 1000 (FTD)	TVA 1000 [PID]	OVA 106	TLV Sniffer	Ĩ	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Shifter	7¥	TVA 1000 (FIO)	TVA 1000 (PIC)		HAL	TVA 1000 (FIO)	TVA 1000 (PID)	OVA 106	TLY Shifter	HNN	TVA 1000 (FTU)	TVA 1000 (PIC)	OVA 108	TLV Shifter	
nditione	Amblant Windspeed (formin)	8	S	s	\$	ž	84	2	2	5	R	8	R	8	R	8	ē	100	ě	100	88	8	88	86	8	٤	٤	2	2	2		ŝ	8	8	240	240	240	240	240	140	94	
Amblent Co		8	25	52	2	ŝ	\$	8	8	<b>\$</b> \$	51	51	51	51	51	8	8	80	8	50	40	8	07	84	Ş	52	52	52	52	22	8	8 5	2	8	\$	\$	ş	\$	ą	4	Ş	
	Bervice	Ę	1	=	1	3	E	II.	1	וו	1	11	L L	11	11	<b>GAS</b>	GAS	GAS	GAS	GAS	11	1	n	E	IL I	IJ	H	=	=	3	3		=	=	1	מ	F	Ŀ	E	11	=	
	Ĩ	•	•	•	•	•				•	•	0	•	0	•	2	2	2	2	2	-	-	+	-	-	•	•	•	•	•	•	•		•	6	•	-	•	-		•	
5	Actuellon	],	2		×	×	¥	Z	z	Ŧ	Σ	¥	¥	N	¥	Ξ	Σ	Ξ	Z	¥	Σ	Ξ	Z	×	¥	X	X	Σ	I	Σ	Z			E	2	Z	I	Z	×	×	Σ	
ant Informed	Subcringory	5	5		5 Mg	a d	5	8	5	ond.	Gate	Gute	Gatte	Gente	Gate	Gate	Qate	Gate	Gete	Gerte	det o	Gete	Gate	Gete	Gete	Gate	đ	Gefe	Gate	S.	9 B				e C	5	ę	ge	82	a de la compañía de la Compañía de la compañía	e co	
Compo	Component						3	1	va ha	aviev A	wiew	MEX	e Mar	even	eviev	wiew	N.S.	waha	Mer	a de la compañía	eview N	avie,	e viev	a May	ever	wave	valve	with	A P	e yes	WEX	MR				2	5	2	1	M S	N.	
Refinery			3 5	3	8	Ę	5	2	E E	Ę	102	ţ	ŝ	102	8	8	8	Ę	8	æ	Į	2	Ş	Ş	Į	<b>1</b> 8	105	105	105	105	9	8	8	B	<u>8</u>	104	- LO	101	200	5	s t	2

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Refinery	Compon	and informedic	ş		1	<b>Umblent</b> Co	ndfilone			Screening L	ł			
-11	Component	Bubcategory	Actuation	₽ÎÊ BÊ	Bervice	Amblerk Temp. Personal	Amblent Windepeed (Wimin)	freetrument Type	Bechground Screening Value (ppm)	Meximum Bustamatria Borraning at Burtace (ppm)	Peak Screening st Burtace (ppm)	Maximum Sustainable Screening at 1 cm (ppm)	Peak Acreaning at 1 cm (ppm)	Comments
106	arter v	Gete	z	•	=	40	140	TVA 1000 (PID)	¥		307		2	
8 <b>9</b>	e i e	Gete	Ξ	12	3	8	200	OVA 106	7	+100,000	×100,000	7,000	10,000	1 cm - No DR.
8	245	Gate	æ	12	11	8	82	TLV Sniffer	•	×10,000	×10,000	×10.000	+10.000	
8	eviev	Gete	Z	12	ų	50	8	Ž	•	•	-		•	
8	. Way	0 ete 0	Z	12	n	8	280	TVA 1000 (FID)	2		403,250		10,304	
8	with	ete O	×	12	u I	8	80	TVA 1000 (PIO)	12		2		7	
Ģ	Alve	e e e	ပ	-	3	8	110	OVA 108	~	450	8	ŝ	8	
0.1	a day	e Personal P	0	-	E	8	110	TLV Shifter	•	8	8	240	240	
110	a line	Gete	U	•	3	50	110	Ĩ	0	2	~	•	•	
110	MA	e co	0	•	ц	8	110	TVA 1000 (FID)	~	80		70		
19	ş	Gete	U	•	ц	8	110	TVA 1000 [PID]	12	2		5		
11	N.S	Safe	z	•	r I	51	270	OVA 108	~	10,000	16.000	10,000	10,000	1 cm - No DR
11	N.S.	Gete	¥	•	11	51	270	TLV Sniffer	•	0,700	0.700	3,400	3.400	
:	Men	Gete	2	•	n	51	270	PNH	0	88	320	8	ß	
1	A	Gate G	z	•	11	51	270	TVA 1000 FTD1	2		62,346		5.073	1 em - Na DR.
11	ave.	e e	Ξ	•	11	51	20	TVA 1000 (PIC)	12		60		Ŕ	
112	Mey	e e	¥	10	11	48	220	OVA 106	7	+100.000	×100,000	12,000	18,000	
:	vahe	Gete	æ	ç	n l	48	220	TLV Sollier	5	8,500	0.500	3,600	3,000	
11	A	Gate	I	₽	н	8	220	MM	0	8	R	170	10	
112	vahe	Gate	¥	9	H	88	220	TVA 1000 FIDI	:		30,310		74,202	
112	Mer	Gate	¥	10	3	8	220	TVA 1000 [PIC)	12		5		ş	
113	eview	Gate	ပ	14	GAS	80	185	OVA 106	•	8	ē	8	8	
113	ever Nev	Gete	v	14	GAS	8	185	TLV Shifler	\$	R	Ş	R	R	
113	e vier	Gete	U	14	GAS	8	185	₹¥	0	8	8	<b>6</b>	9	
113	Mer	Gate	v	14	GAS	8	185	TVA 1000 (FID)	4		4		5	
611	with	Gate	ပ	14	GAS	8	185	TVA 1000 (PIO)	13		2		2	
114	MEX	Gate	¥	14	GAS	S	8	OVA 108	•	000	100	ĝ	8	
114	N.S.	Gate	X	14	GAS	3	z	TLV Shifter	•	2,600	2 <b>60</b>	1 800	1 800	
114	a Mex	Gate	Z	14	GAS	8	8	AM H	•	8	8	5	13	
114	way	Gate	X	14	GAS	8	z	TVA 1000 (FIO)	•		1.58		۶	
114	wave	Gate	Σ	4	GAS	8	z	TVA 1000 [PID]	13		ę		15	
115	war	Gate	¥	•	GAS	52	ş	OVA 106	6	8	8	8	8	
115	avier	Gate	æ	•	GAS	52	ţ	TLV Sniffer	0	8	8	8	8	
115	eviev	Gate	W	9	GAS	52	<b>8</b>	HUM	0	•	•	6	•	
115	Mex	Gate	H	8	GAS	52	ţ	TVA 1000 (FID)	2		133		8	
115	May	0 ete	¥	0	GAS	52	105	TVA 1000 (PID)	14		2		\$	
116	Mex	Q ete	M	9	GAS	8	110	OVA 108	•	8	100	8	82	
116	wiav	afe O	æ	0	GAS	95	110	TLV Solfler	0	30	8	R	992	
118	eviev	Gete	¥	0	GAS	8	110	HNN	0	8	8	10	9	
116	evers S	Gete	Z	•	GAS	8	110	TVA 1000 (FID)	2		8		362	
116	275	Gate	¥	•	GAS	8	110	TVA 1000 (PID)	14		۶		5	
11	e de la compañía	O afte	X	9	GAS	3	8	OVA 108	8	3,500	0000	1.00	1,800	
117	May	e S	Σ	-	GAS	3	ន	TLV Sniffer	0	88	82	8	8	

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Refinerv	Combon	ent Antormedi	5			Amblent Co	nditione			Screening (	25			
	Component	Subcriegory	Actuation	818 (	Bervice	Ambient Temp.	Amblert Windspeed (Trimin)	Institument Type	Beckgrowne Screening (ppm)	Maximum Bustahrabie Screening at Surface (ppm)	Peek Bernenning at Burthece (ppm)	Maximum Bustainable Screening at 1 cm (ppm)	Peak Berwening at 1 cm (ppm)	Comments
		ł	],	ŀ	GAS	3	8	NH	•	13	120	13	14	
		e c	2		GAS	2	8	TVA 1000 [FID]	2		4.670		2.436	
		e B	3	•	GAS	2	50	TVA 1000 (PID)	17		5		128	
411	a la	Gate	3	~	GAS	88	22	OVA 106		2,300	2300	1,600	1,800	
815	win	0 Be	I	2	GAS	8	z	TLV Sniffer	0	+10.000	×10,000	000 6	0000	
11	eview	Gate	Z	~	GAS	\$	8	PNE	0	~	~	-	•	
	eview	Gehe	Z	~	GAS	8	8	TVA 1000 (FID)	2		2.012		1.480	
	when	Gete	z	~	GAS	8	z	TVA 1000 (PID)	10		R		R	
10	waite	Gete	z	~	GAS	8	8	OVA 108	•	45,000	000 SF	5,000	5,000	1 em vithout DP.
10	eview	Gete	¥	~	GAS	8	ę	TLV Soffier	•	>10,000	>10.000	+10.000	>10,000	
110	eyes	Gete	¥	2	GAS	8	ę	Ĩ	•	-	-	~	2	
110	eview	Gete	¥	2	GAS	8	Ş	TVA 1000 (FID)	7		1715		10,500	
110	vaha	Gate	¥	2	GAS	8	Ş	TVA 1000 (PID)	10		2		8	
8	Mex	Gate	Z	2	GAS	57	65	OVA 108	•	0001	8	82	88	1 cm specer too fet
120	aver	Gete	¥	2	GAS	57	8	TLV Sniffer	2	1000	1000	000	000	
121	avjav	Gete	¥	2	GAS	57	8	NH	•	27	2	8	8	
8	aviav	Gete	¥	2	GAS	57	8	TVA 1000 (FID)	2		1,155		756	1 cm specar los M.
<u>8</u>	when	Gete	2	~	GAS	57	8	TVA 1000 (PIC)	10		5		8	
121	a de la	Gete	Z	:	GAS	8	8	OVA 106		000'0	000	5,000	5,000	
121	way	Gate	Σ	:	GAS	00	8	TLV Souther	12	2,000	7,800	1000	7.200	
121	vaha	Gate	×	:	GAS	8	8	HNU	-	8	\$	15	15	
121	waw	Gete	Σ	:	GAS	8	8	TVA 1000 (FID)	2		0.100		1.401	
121	Mev	Gete	Σ	;	GAS	8	8	TVA 1000 (PID)	9		ē		57	
12	eviev	Gate	W	-	GAS	51	10	OVA 106	8	12,000	20,000	1400	2,500	ton without distor.
12	war	Gete	X	4	GAS	51	2	TLV Shirler	12	4 000	8	3,600	3,600	
5	vaha	Gerte	¥		GAS	51	5	INN	•	8	2	8	8	
122	eview	Gate	M	-	GAS	51	15	TVA 1000 (FIC)	2		5.676		200	
13	vahe	Gate	¥	4	GAS	51	5	TVA 1000 [PID]	•		8		48	
123	vehe	Gete	X	4	GAS	\$	315	OVA 108	•	1,200	120	000	000	Sea
123	valve	Gafe	¥	-	<b>GAS</b>	¥	315	TLV Sniffer	•	220	8	Ŗ	320	
123	valve	Gete	Σ	•	GAS	\$	315	Ĩ	•	9	2	-		
123	valve	Gate	X	•	GAS	*	315	TVA 1000 (FID)	~		11		1/1	
123	valve	Gete	X	-	OAS	*	315	TVA 1000 [PID]	¢		2		8	
124	wier	Gate	W	4	GAS	ş	315	OVA 108		+100,000	>100,000	>100,000	*100,000	(toutha
121	war	Gete	X	4	GAS	¥	315	TLV Soffer	0	×10.000	×10.000	×10,000	×10,000	
101	valva	Get	X	•	GAS	94	315	INU	•	8	8	8	ę	
100	selve v	Gate	Z	•	GAS		315	TVA 1000 (FID)	~		10,494		35,207	
101	with	Gete	z	-	GAS	94	315	TVA 1000 [PID]	10		11		8	
¥.1	a la	Gete	3	•	GAS	4	370	OVA 108	R	+100,000	×100,000	80 00	20,000	
×.	a han	Ser	×	•	GAS	4	370	TLV Solfler	0	×10,000	×10,000	+10,000	×10,000	
X	5	Gets	×	•	GAS	Ħ	370	THE	•	45	\$			
X	with	Gate	Z	•	GAS	4	370	TVA 1000 (FID)	~		179,850		60 000	
X	May	a teo	Z	-	GAS	¥	370	TVA 1000 (PID)	5		11		961	

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	Comments							Falled OC sheck					brated at 1513, thread 7 area OC dress																															
	Peek Screenling et 1 cm (ppm)	90,000 Digite	×10,000	ą	130,250	124	88	2,100 mm		626	-	81			01	, ș	00001			80.5	2	2500	1000		1013	2	110	8		\$	2	000	8		2,088	107	50,000	6.200		10,700	1,324	180	120	
	Maximum Buetainable Screening at 1 cm (ppm)	000'00	×10.000	ą			80	2,100				81	R			e c		200721				2500	1,000				ŝ	8				8	8				50,000	<b>6,200</b>				9	130	
le te	Peek Borrenting at Burring	+100,000	>10,000	91	132,000	121	1 400	4 200		1000	₽	8	B	1	8 8					19.308	8	2,20	8		92. -	ē	ŝ	8		Ş	Ş	8	ş		750	2	+100,000	0,100		113,300	1.087	ĝ	120	
Screening D	Maximum Sustainable Screening et Surtece (ppm)	+100,000	>10.000	48			1,400	3,600				8	4,600				9,000					2200	1000				ĝ	82				ğ	550				+100,000	9,100				8	120	
	Background Beckground Bernoning Value (ppm)	8	0	0	2	6	•	ę		-	•	•	Ş		- :			Ŷ	ľ	~	9	9	R		٠	8	9	35		-	8	•	8	•	2	21	•	₿	Mar and a	-	21	0	5	
	hadrumant Type	OVA 106	TLV Sniffer	HNW	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Shiffer	NH	TVA 1000 [FID]	TVA 1000 [PID]	OVA 108	TLV Sollier	NNN			OVA 105		Ž	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Shiffer	Ŋ	TVA 1000 (FID)	TVA 1000 (PIC)	OVA 108	TLV Shifter	<b>N</b> H	TVA 1000 (FID)	TVA 1000 (PID)	OVA 106	TLV Solite	Ĩ	TVA 1000 [FID]	TVA 1000 (PID)	OVA 106	TLV Shifter	HNU	TVA 1000 (FID)	TVA 1000 (PID)	OVA 106	TLV Shiffer	NH
notrione	Amblent Windspeed (remin)	616	370	370	370	370	210	210	210	20	30	8	8	8	R	8		2	320	32	88	175	175	175	175	£	310	310	310	310	310	8	88	30	ŝ	8	55	<u>8</u>	ŝ	8	5	8	8	180
Ambient Co	Amblent Temp. Personal	1	3	3	3	3	8	8	8	8	8	2	5	5		5	8	8	ę	Ş	ę	Ş	Ş	ę	8	Ş	Ş	ę	Ş	\$	\$	\$	\$	8	84	8	8	8	8	8	8	8	\$	48
	Bervice	a de la del	20	GAS	SAG	GA9	GAS	GAS	GAS	GAS	GAS	GAS	GAS	GAS	GAS	243	GAS	GAS	GAS	0AS	GAS	н	3	Ξ	=	1	3	3	=	=	╡	3	Ш	3	EL	1	3	1	3	1	11	1	1	11
	₿Ē	ŀ	•	•		-	•	•	0	•	•	┥	┥	┥	•	•	•		•	•	•	•	•	•	•	•	~	~	~	~	-	~	~	~	~	~	•	•	•	•	•	~	~	2
8	Actuation		5	2	2	3	U	0	J	v	U	U	ů	0	<b>.</b>		<b>.</b>	0	5	J	v	v	U	v	S	v	X	Σ	X	z	Ξ	0	U	ပ	U	U	X	Σ	X	Σ	Z	C	J	U
ant Information	Subcategory	ł		te C	400	et et	ete O	Gate	Gete	Gete	Gete	Gete	Gete	e e e e e e e e e e e e e e e e e e e	Oate	Gete	Qute	Oate	e o	Gate	Gete	Gete	Gate	ete O	Gate	Gate	Gate	Gate	Gete	Gate	Gate	Gate	Gete	Gete	Gate	Gate		:	:	:	:	Qute	Gate	Gete
Combon	Component					1	-	Wex	Mar	eviev	¥,	e les	N N	W	e ve	A A	M	Mer	MR	e Mar	walve	walve	eviev	with	NS.	vahe	vahe	wahe	ever	ever	a ya	A PA	Max	eviev	e ver	ww	e Nev	e ve	May	A A	e e e e e e e e e e e e e e e e e e e	vahe	wher	Mer
Refinerv			2	e c			127	127	127	127	127	128	128	126	128	128	120	120	120	120	120	130	130	130	130	130	131	131	131	131	131	132	132	132	132	132	133	ŝ	133	133	13	134	NC1	131

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NI'V' - Com	berneti Informed	5			Amblent Co	nditions			Screening C	atte				
-Abo	ent Bubcitegory	Achuellon		Bervice	Amblent Temp.	Amblent Windspeed (Temin)	Instrument Type	Bechground Acreening Value faom)	Maximena Bustening at Bustening at Bustening at	Peek Acresting at Surface	Martimen Busteinebbe Bersening et Cen (port)	Peek Screening H 1 cm (pem)	Comments	
	10		ſ		ļ	ŝ	TVA 1000 (FID)	-		627		51		
		, c	•	=	\$	8	TVA 1000 (PID)	8		R		24		
	O de	3	~	3	40	250	OVA 108	7	73	2	n	a		
avlay	Gate	3	~	n	<b>8</b> 8	220	TLV Shifter	ĝ	8	8	8	8		
a de la companya de	Gate	Σ	2	1	8	<b>9</b> 2	RAN							
a de la comparación de	Gate	Σ	2	11	<b>8</b> 8	9 <u>2</u>	TVA 1000 (FID)	•		ž		8		
	Gate	X	~	3	8	250	TVA 1000 [PID]	8		R		R		
	e e	X	~	3	ę	8	OVA 108	٢	1.500	1 500	1200	120		
	5	2	~	3	40	R	TLV Shifler	8	8	8	1000	1000		
	Grie	¥	2	n	9	8	NW.							
	Gehe	¥	2	1	8	8	TVA 1000 (FID)	3		3.292		176		
	Gate	Z	~	1	8	8	TVA 1000 (PIC)	8		R		8		
Nev I	Gate	Z	-	3	80	8	OVA 106	~	4,500	<b>2</b> 2	1500	2000		
Maw 71	Gete	Ξ	-	n	8	8	TLV Sniffer						Falled OC,	
Max -	Gete	ž	•	n	ŝ	8	INN							
	0 ete 0	Z	-	2	8	8	TVA 1000 (FID)	\$		0.18		8,337		
vilv.	Gete	Ξ	ł	'n	50	8	TVA 1000 [PID]	2		8		4		
M	efe O	Z	Ŧ	11	84	8	OVA 108	•	20,000	2000	5,000	5000	1 on whold Adv.	
May	Gete	×	ł	11	8	8	TLV Shifter						Falled OC.	
Max	e Gate	X	-	н	8	200	Ŧ							
May	e (Jete	æ	-	3	\$	8	TVA 1000 FIDI	\$		101.632		12,000		
Max 8	e Gete	X	-	ц	\$	20	TVA 1000 (PIC)	2		21		2		
May 0	Gete	Σ	-	Ц	5	8	OVA 108	•	1,800	2 <u>30</u>	1800	R	trudd readings at 1 cm.	
Mav 0	Gate	X	-	3	4	ě	TLV Shifter						Beckground too Mgh. Falled OC	
May 0	Gete	Z	-	=		<u>8</u>	N					•		
Max	e Gate	×	-	3	=	ŝ	TVA 1000 [FID]	-				8		
May 0	Gate	X	-	3	-	<b>1</b> 8	TVA 1000 (PID)	R				3		
Valv	Gate	Σ	2	Ŧ	\$	2	0VA 109		021					
May 0	e Gate	X	2	z	¥	e	ILV Some					3		
MPA 0	Gate	S I	5	Ŧ	8	R 1	NNH	•	61			1 7.61		
Ver D	Gete	3	2	Ŧ	8	2 2						~		
Aev 0	Gete	2	2	¥	8	2	TVA 1000 (PR)	-			8.			
1 Valv	Gate	×	2	Ŧ	<b>F</b>	8	BUL VIO		M/1		2	2		
Mer 1	Gate	₹	2	Ŧ	=	8	TLV Sollier	5	1,000		8.	B		
11 Velv	Gate	Σ	2	Ŧ	4	8	R.	0	P	2				
May 1	e Gete	Z	12	Ŧ	41	8	TVA 1000 FTD1	2		2.070		2025		
May 1	e Gere	Σ	2	¥	1	8	TVA 1000 (PID)	18		8		=		
Aev.	e Gete	U	8	Ŧ	47	82	OVA 109	8	3,000	3000	8	8		
Alla	e Gate	<b>ს</b>		Ŧ	4	8	TLV Snifler	•	1.000	8	1000	8		
2 vah	<ul> <li>Gete</li> </ul>	с П	8	¥	47	82	NH	0	=	=	12	2		
All All	e Gate	U	•	Ŧ	4	2	TVA 1000 (FIC)	-		8				
Vev 21	e Gate	с С	•	Ŧ	47	82	TVA 1000 [PIO]	9		ę		2		
Mev ()	e Gele	v	•	Ŧ	Ş	8	OVA 108	0	82	8	R	Ş		

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elinery	Compon	ant Informatic	s	Ì		Amblent Co.	notitione			Screening	ţ			
T and the second	Component	Bubcategory	Actuation	i i	Service	Amblent Temp.	Amblent Mindepeed (Mimbi)	hetrumont Type	Beckground Screening Value	Mertimento Burstainable Bernanting at	Pres Borreening at Surface	Maximum Burtainable Screening at	Pack Bernening Rf 1 cm	Commants
			Ī	Ţ					Innet		(model)	ו כש (ואשעון	(mqq)	
E E	e e e e e e e e e e e e e e e e e e e	Seb	0	7	¥	\$	2	TLV Snifler		88	8	320	320	
19	MM	Sete	0	-	Ŧ	ę	2	Ĩ	•	5	ę	6	9	
<del>1</del> 8	M	et o	U	-	Ŧ	\$	Ř	TVA 1000 (FID)	~		1,104		1,502	
143	a la	v	v	ĉ	Ŧ	\$	200	TVA 1000 (PID)	40		32		32	
144	value -	Gete	N	2	Ŧ	8	220	OVA 108	9	1,000	1,000	1.80 001	000	
144	valve	Gette	æ	2	H.	50	220	TLV Sniffer	9	650	050	88	300	
144	s ter	Gute	¥	~	H	50	220	HNU	0	16	16	•		
144	ş	Gate	X	2	Ŧ	80	220	TVA 1000 (FID)	2		2.397		ž	
14	evier	Gate	2	~	Ŧ	8	220	TVA 1000 (PID)	8		8		8	
145	¥,	Gate	I	~	Ŧ	3	8	OVA 108		1.050	1 060	ŝ	5	Dateie
145	a view	Gate	z	~	¥	8	88	TLV Sniffer	8	000	8	88	007	
145	R S	e e e	z	~	Ŧ	8	88	Ĩ	•	=	:			
15	a la	ę	3	<b>.</b>	-	8	, Se	TVA 1000 FICH			53		5111	The second the state let - Marilla for some second
145		400		•	1	2 2	×	TVA 1000 PU	Ę				1.00	
		4		ļ	-		;					5	-	
				2		*			•			3	<b>***</b>	
	away .			Ţ		8	2	ILV Shifter	F	1,000	am'	002	200	
8	ave.	ete C	J	₽	Ŧ	8	8	쿨	-	-	•	5	s	
¥	a a a a a a a a a a a a a a a a a a a	e G e F	0	우	Ŧ	8	₽	TVA 1000 FTD1	2		5.324		4.640	
<b>8</b>	ş	Gate	0	9	Ŧ	8	:	TVA 1000 (PIC)	18		2		8	
5	Aller	Gate		٩	Ŧ	8	8	OVA 108	8	3,500	5,000	2,400	3,000	
Ę	A	Gate		2	¥	8	2	TLV Soffer	8	540	540	83	83	
Ē	ş	Gate	0	₽	¥	8	R	IN	2	~	2	2	2	
Į.	eves	Gate	0	٤	¥	S	٤	TVA 1000 FIDI	~		5,963		14	
147	a de la compañía	Gate	0	2	¥	S	٩	TVA 1000 (PIC)	18		43		18	
Ę	Mex	Gate	ů	2	Ŧ	8	46	OVA 108	1	2,200	2200	300	8	Deterto.
148	with	Gate	ů	5	¥	8	140	7LV Shiffer	8	82	29	8	8	
140	MAN	Gate	0	<u></u>	Ŧ	8	140	HNN	•	1	•	•	-	
8	a la la	Qute	ů	2	£	ន	140	TVA 1000 (FIC)	2		3,636		3	
18	a de la dela	Gate	3	2	Ŧ	8	8	TVA 1000 (PID)	17		37		10	
140	a la	Gate	Ξ	~	Ŧ	Ş	360	OVA 106	1	2	22	2	1	
ŝ	-	Cate	Z	~	Ŧ	\$	340	TLV Shiffer	88	8	8	8	8	
\$	a la	Gete	3	~	Ŧ	\$	340	INN	F	-	-	-	F	
<del>1</del> 8	A	Gate	Ξ	-	Ŧ	\$	340	TVA 1000 (FID)	2		8		•	
140	sta	Gate	Ŧ	~	Ŧ	40	340	TVA 1000 [PID]	17		17		17	
130	A	Gate	Σ	•	Ŧ	8	44	OVA 108	•	8	8	8	88	
150	w	afe O	X	•	¥	50	**	TLV Sniffer	8	880	88	96	340	
150	Alex	Gate	I	4	Ŧ	8	4	Ĩ	~	~	2	~	~	
150	Max	ę	Ŧ	•	Ŧ	8	44	TVA 1000 (FIO)	~		1.744		2,200	
ŝ	A N	Gate	Ŧ	4	Ŧ	ន	44	TVA 1000 (PID)	17		7		8	
151	e verte a constante constante constante a constante a constante a	Gete	Ξ	•	Ŧ	9	205	OVA 106	•	45,000	45,000	20,000	20,000	
151	N.	Gete	Σ	•	Ŧ	\$	205	TLV Shifter	8	7,600	7,600	1.00 1.00	1,000	
151	wher	Gete	¥	•	Ŧ	40	205	144u	~	8	8	ଛ	8	
151	way	afe O	×	┛	Ŧ	ę	33	TVA 1000 (FID)	4		302,470		60,092	

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Τ		Π	Т	T	Τ	Τ	T	٦		Π	Т	T	Т	Т	T	T	Ţ	Г	Τ	Т	Ţ	Τ	Γ	T	Γ			Ι	Τ	Τ	Τ	Τ	Т	Τ	Τ		Γ	Γ		Γ	Γ	Γ
	Comments												Digitate.																													Dupticare,
	Peak Bereening at 1 cm (ppm)	8	2.400	1,000	0	2,710	8	10,000	3,200	8	13,000	52	45,000	3,200		18,300	8 3	8	801		8	F.	Z	<b>Ş</b> .		and a	12 000	2,000	-	12,300	2	00000	+10.000		00.00			MIT			2 4	20 min
	Maxhmen Burtainabio Bcreening at 1 cm (ppm)		2,400	1,000	0			10,000	00000	8			45,000	3,200				R	8	2			2,500	99	-		10 CT	2,600	1			80,000	×10,000	•				BIT	•			10,000
ą	Peek Bereening A Swrtece (ppm)	62	4,000	1,000	0	2,761	8	10,000		8	20,100	57	40,000	4,100		16,300	57	P	8	-	142	8	2,500	8	-	3,100		2 000	٠	31,200	8	+100,000	×10.000	•	000,200	•	8	2000	•	B1.1		
Screening D	Meximum Burtace (ppm)		3,000	1,000	•					8			40,000	4,100				R	18	2			2,500	8	-			0000				+100,000	×10,000	•			1,000	2000	٩			
	Beckgrowne Screening Value (ppm)	7	•	1	0		• •		•	2.		₽	-	8	-	•	=	-	R	~	~	2	-	•	-	1	2		-	\$	9	7	0	0	13	•	2	•	•	~	•	;
	histrument Type	TVA 1000 PUDA	OVA 10A	1 V Soffer					BAL VA	TUV Some			OVA 106	TLV Sniffer	HHA	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Sniffer	NAT	TVA 1000 (FID)	TVA 1000 (PID)	OVA 106	TLV Souther	HN	TVA 1000 (FID)	TVA 1000 [PIC]	0VA 105	LENIL	TVA 1000 (FIC)	TVA 1000 [PIO]	OVA 108	TLV Sniffer	HNU	TVA 1000 (FID)	TVA 1000 [PID]	OVA TOB	TLV Shifler	HNN	TVA 1000 (FID)	TVA 1000 [PID]	
nditions	Ambient Mindapeed (fitmin)	¥	*	2	3 8	+ 8 1	+ 8 8	8	2	<u>د</u> :	2 2	2 #	2 8	8	8	8	8	14	14	14	14	14	145	145	145	145	145	8	3	<u>8</u>	<u>8</u>	12	12	12	12	12	8	8	8	8	8	
Amblent Col	Amblenk Tomp. Parvelan	ę			;;;				•			;;			5	5	51	51	- 19	51	51	51	3	3	2	2	z	8	8 :	8 5	2 2	3	z	a	2	5	9	61	61	6	5	
	Bervice .	Ţ		240	2	GAS	GAS	GAS	GAS	GAS	GAS	SAS 245	245	SAS	GAS	GAS	GAS	GAS	GAS	GAS	GAS	8V8	Ŧ	Ŧ	¥	¥	Ŧ	GAS	GAS			GAS	0AS	GAS	GAS	GAS	GAS	GAS	GAS	GAS	GAS	
	a î	Ţ	•	•	•	•	•	•	•	•	-	-	-	ŀ		•	•	-	-	ŀ	ŀ	-		-	-	•	•	•	•	•	•	<u>e</u>	\$	₽	9	<b>9</b>	9	2	₽	ę	9	ļ
5	Actualtion		Z I		J	ů	ູ	J	2	¥	X	Z Z	<b>x</b>	E 3	E 3	1	5		:				3	3	×	X	ž	0	0	<b>.</b>		, =	2	3	Z	Z	3	3	Ξ	E	Z	
and information	Subcelegory		Gate	Gete	Gate	Gate	ete O	Gete	Gete	Gete	Gette	Gate	<b>1</b> 0	Care C			ete C	é	4	f	f	f	1		ł	0 ete	Gete	Gate	Gate	Gate	e e e			4	a te	a de la	Oate	e e	Gen	G	0	
Second	Comparent		with	Mar	-	with	. ever	when	value	velve	Mex	9 1 8	ANA	May	MEA				CON-TOOL	100-100		1001-000	Inort-Inor			N N	Mar	eyes	M	MW	e Men	ewen									N S	Prink .
Distriction (1)			151	152	152	152	152	152	153	153	150	153	153	2	151	N	154	5	8	8	81	661	8	8	8	8 5	8	157	157	157	157	157	22	8	8	8	R				5 9	B

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	Componen		Type	avia v	eview	enter	valve	· evier
	Refinery	1	Number	9 <u>1</u>	1 B	100	161	161
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finery :::	Compone	nt informatio	ş			Amblent Co	nditions			Screening L	at a				_
8	New State	Subcringory	Actuation		Service	Amblent Tomp.	Amblent Windspeed (fumin)	Instrument Type	Beckground Screening Value (ppm)	Mextmum Sustainable Sustaina at Surface (ppm)	Peek Borrening at Surface (ppm)	Maximum Sustainable Screening et 1 cm (ppm)	Peak Screening at 1 cm (ppm)	Comments	
	ļ	ete S	]_	₽	GAS	5	25	R N	0	0	0	0	0		_
8		5	3	₽	SVD	5	\$2	TVA 1000 (FID)	•		56,064		20,353		_
8	ş	Gate	3	₽	SAS	5	52	TVA 1000 (PID)	8		2		14		_
2 2	ł	a de la de l	z	₽	GAS	8	58	OVA 108	12	000'00	00000	2,500	25,000		_
	ł	4 O	z	₽	6 G	8	\$	TLV Shifter	0	+10,000	×10.000	×10,000	+10,000		-
101		et c	2	₽	GAS	8	8	HNU	0	0	0	0	0		-
101	1	đ	Σ	₽	SVO	8	8	TVA 1000 (FID)	1		118,202		17,800		-
101	2	e e e	E	9	GAS	8	8	TVA 1000 (PIO)	8		•		0		
5	1	e te c	×	~	<b>GAS</b>	8	8	OVA 108	10	2,000	10,000	9,000 1	10,000		
5	ş	et e	×	~	GAS	8	8	TLV Soffer	0	2,600	2000	320	2,200		
Ē	1	et C	3	~	SAS	8	8	HNU	0	0	•	0	0		
Ē	1	et e C	z	~	GAS	8	8	TVA 1000 (FID)	2		14,200		10,200		_
Ē	N S	e C	3	~	GAS	8	8	TVA 1000 (PID)	9		•		•		-
1		f	:	-	GAS	5	170	OVA 108	7	4,500	4,500	4,500	4,500		-
		Ē	:	-	GAS	6	021	TLV Solfler	0	1,100	1,100	120	120		-
		Ę	:	-	GAS	ų	0/1	HNU	0	0	•	0	0		_
	UQU-UQU	£	:	-	GAS	6	170	TVA 1000 (FID)	2		5.276		507		
1	Non-non	E	:	-	GAS	9	170	TVA 1000 (PID)	9		-		0		
10	NON-NON	f	:	-	GAS	81	130	OVA 106	8	1,200	1,200	ŝ	802		_
2	LON-LOO	ŧ		-	GAS	81	130	TLV Shifter	0	8	8	0	0		-
101	- Lon - Loo	£	:	•	GAS	81	130	HNU	2	Ŧ	-	٠	-		
2	NOT-NO	£	:	•	GAS	81	130	TVA 1000 (FID)	7		8		174		
104	NOT-NOT	£	::	-	GAS	81	130	TVA 1000 [PID]	•		~		2		
ŝ	NON-NON	£	:	•	GAS	8	8	OVA 108	۲	1,100	9 <u>1</u>	802	902		
1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	CON-NON	£	•••	•	GAS	8	R	TLV Sniffer	0	5	₿	8	8	Digitate.	-
8	CON-RON	£	:	-	GAS	8	8	<b>TR</b>	0	٥	•	0	•		_
105	con-non	£	:	-	GAS	8	8	TVA 1000 (FID)	٥		718		ž		
8	con-non	ŧ	:	-	GAS	8	8	TVA 1000 (PID)	Ð		-		۲		-
80	valve	Gate	¥	-	GAS	5	35	OVA 106	•	180	8	160 1	8		_
106	a ter	Gafe	¥	-	GAS	6	R	TLV Sniffer	•	•	0	•	•		
8	ş	Gate	×	-	GAS	61	8	TAN	•	0	•	0	•		_
100	Į	Gate	Z	-	ß	5	8	TVA 1000 F101	7		174		8		_
106	ş	Gate	¥	-	GAS	6	8	TVA 1000 (PIO)	•		~		7		_
167	May	Plug	Z	٩	GAS	8	8	OVA 108	•	40,000	00004	15,000	15,000		-
107	vahe	Plug	Σ	ç	GAS	8	8	TLV Solfler	0	1.000	100	760	760		-
167	Alte Value	Phug	N	5	GAS	8	8	HNU	0	•	•	0	0		
107	value	Plug	Z	ē	GAS	8	8	TVA 1000 (FID)	•		43,180		0.563		-
107	www	Phog	X	õ	GAS	8	8	TVA 1000 (PIO)	6		•		٩		
5	vahe	Gate	Z	~	GAS	82	190	OVA 106	15	8	88	8	920		
100	A No	Gate	Ξ	~	GAS	8	<b>1</b> 8	TLV Shifter	۰	2	z	8	8		-
<b>1</b>	e yek	Gate	3	~	GAS	8	180	HNM	0	0	•	٥	•		_
108	vahe	Gate	Ξ	~	GAS	8	100	TVA 1000 (FID)	e		647		617		-
	a Nes	Gete	2	~	GAS	8	8	TVA 1000 PUD	¢		•		~		

						C maid and				Screening D	ł			
Relinery	Compon	ent informetic	8		Ţ						1	Mandan	Peek	
	Component	Subcitagoly	Actuetion		Service	Amblert Terre.	Amblent Windepeed (Mimin)	Instrument Type	Beckground Screening Value Interio	Maximum Sustainable Boreanling at Burihoca (comi)		Bestaineble Bersening at 1 cm (ppm)	Screening eff 1 cm (ppm)	Comments
LINGHUGN .												ş	8	
and the second se		ľ	1		SVO	8	8	OVA 108	•	900	R			
90	AN S	<b>D</b> ind	¥				1	T V Colline	0	8	100	0	5	
4		200	Z	-	GAS	B	B		•	¢	c	0	•	
6		5	X	-	GAS	8	8	¥	•				2	
B			1	-	GAS	8	8	TVA 1000 FID	-		AN C			
8	M			•	245	8	8	TVA 1000 (PID)	•		-			
8	vahe	Pug	S I		200		1		•	8	8	9	2	
Ę	aviav	Pho	W	-	GAS	8	Ş			6	9	0	0	
2		Dt.	3	•	GAS	8	84	TLV Somer	2	<b>)</b>		•	c	
2	2 S	5 I I		ŀ	a ve	5	84	PN41	0	9	2			
21	ş	<b>N</b>	E	•	2		ş	TVA 1000 FIDI	-		8		2	
170		By d	X	•	GAS	8	Ş				•	:	9	
		5	N	-	QAS	\$	420	TVA 1000 AV1		,	8	¥	8	
DV-			2	110	GAS	8	550	OVA 108	0	»	•	2	c	
171	MIN		2	110	GAS	8	550	TLV Shifter	•			<b>,</b>		
11	AMA					5	550	NH	0	•	•	•		
121	Ĩ	Gate	ĭ		220				-		Ş		8	
	a ka	Gete	¥	112	SS	8	000		,		•		•	
		Sete	W	112	QAS	8	550	TVA 1000 PHU						
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Kennery Kunter Kunter	Component Type	Compon Buth category	Actuation		Berge	Amblent Temp. (Fahrenheit)	Amblent Windspeed (fit / min)	Instrument Type	Background Screening Value (ppm)	Maximum Bustainable Bustainable Bustace (ppm)	Peak Bcreening at Surface (ppm)	Meximum Bustainable Bcreening at 1 cm (ppm)	Peak Screening at 1 cm (ppm)	Comments
		•			-	8	8	OVA 100	1	00\$¥	805	3500	3600	OVA 108 Instrument Id #20143
┛	00-100	=		8	=	3	9	TLV Soffer	-	1100	1100	500	500	TLV Shiffer Instrument Id #WD00546
-		=		5	#=		9	Ĩ	2	950	000	400	88	HNu Instrument (d. #970125
-		= /		8	3 =	8	9	TVA 1000 FIDA					ļ -	TVA 1000 (FID) Instrument Id #A140F
-	101-00	=	:			B								TVA 1000 (PID) Instrument Id #A140F
-	con-non	₽,	•		3 =		6	CVA 100	a	280	280	140	140	
2		₽,			=		8	n V Soller	0	8	80	110	110	
~	60-60	2	:				8	HMU	0	996	360	200	250	
~	00-00	₽,	:	11/10			5	TVA 1000 (FID)						
2	CON-HON	2		11/10	=	603	8	TVA 1000 (PID)						
7	CON-NON		•	8148	3 =	1 02 2 02	8	OVA 108	•	2500	2500	300	8	
6	604-000	,∎	:	31/11	;=		8	TLV Soutier	6	260	995 200	180	180	
		2		1110	;=	- C 69	8	HNU	0	200	85	140	180	
6				2010	3 =		8	TVA 1000 (FID)						
6	0000	₽,	:	01/11 01/11	=	7 G	6	TVA 1000 [PID]						
E	con-non		:		=		0.2	OVA 108	•	8	300	110	190	
◀	00-00	= 1					0.4	TLV Shiffer	4	320	320	160	160	
•	001-000	=	:		=			IN		8	90S	100	140	
•	00-100	⋸╡╡					10	TVA 1000 (FID)						
•	CON-DON	₽₽		5	=		20	(OII-0000 VAL						
•			-	5	=	0.00	57	OVA 106	\$	120	120	20	8	
n	Alina			5	:=	0.09	57	<b>TLV Sniffer</b>	5	11	2	2	02	
	ANIEN		2	5		000	57	HNU	5	160	<del>6</del>	110	0 <u>5</u>	
		2	2	8	E	60.09	57	TVA 1000 (FID)						
<b>"</b>		3		5	Ξ	000	57	TVA 1000 (PID)						
0		=		-	E	60.0	57	OVA 108	5	992	R	190	220	
<b>.</b>		=	:	-	n	60.09	57	TLV Shifter	s					Dead battery on ILV Sniffer instrument
		-		-	H	60.0	57	HNU	\$	240	540	150	80	
		>		-	r	<b>60</b> .0	57	TVA 1000 (FID)						
		-	:	-	IT	<b>60.0</b>	57	TVA 1000 (PID)						
<b>^</b>		E	:	8	r I	660	49	OVA 108	~	8	ē	<b>3</b> 0	805	
,		Ē	:	8	E	680	49	TLV Soffer	2					
.		E		5	E	098	67	HNN	7	450	8	Ŗ	<b>3</b> 8	
		E		8	E	8	4	TVA 1000 (FID.						
		F	:	s	E	88	49	TVA 1000 (PID.						
-	5		:	8	ц	11	125	OVA 106	ç	×10000	*100000	×10000	×10000	
	1.000	L		8	E	11	125	TLV Sniffer						
•	8			8	11	5	125	HNU						
	-uoo	u		8	۲۲	11	125	TVA 1000 (FID						
,				8	=		<u>5</u>	DIA 1000 (PID				_		

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Markets         Tention         Eventsee         Tention         Eventsee         Tention	-finery:		Campon	nt inform	nofe	<u> </u>	Amblent C	anditions			Scr	wing Dete			
9         901         1         10 </th <th><b>x</b> 11</th> <th>Component Type</th> <th>Bub- criegory</th> <th>Actuation</th> <th>a î</th> <th>Service</th> <th>Amblent Temp. Fahrentett</th> <th>Amblent Windspeed (R / min)</th> <th>histrement Type</th> <th>Background Screening Value (ppm)</th> <th>Maximum Sustainable Screening st Surface (ppm)</th> <th>Peak Bcreening at Burtece (ppm)</th> <th>Maximum Bustainable Screening at 1 cm (ppm)</th> <th>Peek Bcreening et 1 cm (ppm)</th> <th>Comments</th>	<b>x</b> 11	Component Type	Bub- criegory	Actuation	a î	Service	Amblent Temp. Fahrentett	Amblent Windspeed (R / min)	histrement Type	Background Screening Value (ppm)	Maximum Sustainable Screening st Surface (ppm)	Peak Bcreening at Burtece (ppm)	Maximum Bustainable Screening at 1 cm (ppm)	Peek Bcreening et 1 cm (ppm)	Comments
*         *					ŧ	=	8	67	OVA 108	5	1300	1500	202	30	
0         1	~ (				\$	3 3	8	67	TLV Sniffer						
0         00000         1         00000         1         000000         1         0000000         1         0000000         1         0000000         1         0000000         1         0000000         1         00000000         1         00000000         1         00000000         1         00000000         1         00000000         1         00000000         1         00000000         1         000000000         1         000000000         1         000000000         1         000000000         1         000000000         1         000000000         1         000000000         1         0000000000         1         0000000000         1         0000000000         1         00000000000         1         00000000000000         1         000000000000000000000000000000000000					\$	Ξ	8	67	HNU	5	999	650	8	88	
0         000000000000000000000000000000000000	<b>,</b>				:  2	=	8	67	TVA 1000 (FID)						
0         were         Cate         H         F         L         70         6         100         700					2	Ξ	8	67	TVA 1000 (PID)						
0         with with with with bound         0         with with with bound         1 <td>~ •</td> <td></td> <td>-</td> <td>2</td> <td>•</td> <td>=</td> <td>2</td> <td>8</td> <td>OVA 108</td> <td>-</td> <td>250</td> <td>9<u>5</u></td> <td>ន</td> <td>8</td> <td></td>	~ •		-	2	•	=	2	8	OVA 108	-	250	9 <u>5</u>	ន	8	
0         www         0         w         0         w         0         w         0         1         7         6         1000000         1         1000000         1000000         10000000         10000000         10000000         10000000         10000000         10000000         100000000         10000000         10000000         100000000         100000000         100000000         100000000         100000000         1000000000         1000000000         10000000000         10000000000000         1000000000000000000000000000000000000	2 9			2	•	3	02	88	TLV Sniffer						
00         www         68e         M         0         M         06         M         0         M         06         M         0         M         06         12         73         56         M         M         0         12         73         56         M         M         0         12         73         50         M         13         75         13         75         13         75         13         75         13         75         13         75         13         75         13         75         13         75         13         75         <	2 9			2		E	20	69	HNU	¥	ន	2	22	2	
0         wate         Calle         H         1         7         56         11         70         56         11         60         12         75         11         10         12          11         wate         Calle         H         6         11         523         750         11/Suffic         7         7         1         10         12           11         wate         Calle         H         6         11         623         750         11/Suffic         4         75         1         10         12           11         wate         Calle         H         6         11         623         750         11/Suffic         4         75         11         10         12         11 </td <td>2 9</td> <td>and and and</td> <td>Gate</td> <td>Ξ</td> <td>•</td> <td>н</td> <td>20</td> <td>8</td> <td>TVA 1000 (FID)</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td>	2 9	and and and	Gate	Ξ	•	н	20	8	TVA 1000 (FID)						
11         wee         Cale         M         6         LL         673         LV         7         1 <th< td=""><td>2 5</td><td>a ha</td><td>Gete</td><td>×</td><td>•</td><td>н</td><td>20</td><td>68</td><td>TVA 1000 (PID)</td><td></td><td></td><td></td><td></td><td>1</td><td></td></th<>	2 5	a ha	Gete	×	•	н	20	68	TVA 1000 (PID)					1	
11         were         Gate         M         6         L         G23         1X         Microscol         1         10         10           11         were         Gate         M         6         LL         623         75         1N         10         1         11         10         11           11         were         Gate         M         6         LL         623         75         1N         17         1         11         11           12         were         Dr          36         LL         623         75         N1         11	2 =	Alle	Gate	Ξ	•	п	62.2	82	OVA 108	•	8	8	₽	2	
11         wise         Gate         M         E         L         G23         255         NN 100 (FD)         T         T         N	=	ANEX	9 Be	Z	•	ц	62.2	295	<b>TLV Shiffer</b>					4	
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$		a yes	ð	Z	•	н	62.2	8	HNU	-	R	75	-	0	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$		avav	Sate S	₹	•	ι	62.2	292	TVA 1000 (FID)						
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	╞	a Nev	e e	Ξ	•	Е	62.2	295	TVA 1000 (PID)						
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	: ;	00-002	2	:	5	н	68.2	0	OVA 108	4	5	4	=	=	
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	2			:	5	Ŀ	68.2	0	TLV Shifter						
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	2		2	:	ន	н	68.2	0	HNU	•	•	•	•	•	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	¥  5			:	ສ	E	68.2	0	TVA 1000 (FID)						
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	# <del>5</del>	CON-NON	2	:	8	ц	68.2	0	TVA 1000 (PID)					•	
$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	:		2	:	8	ц	682	٥	OVA 108	•	9	₽	•	•	
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	5	con-non	1		R	Ч	68.2	٥	TLV Shifler				•	•	
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	5	con-non	1u		ŝ	ц	68.2	0	INI	•	•	•	~	•	
$ \begin{array}{c c c c c c c c c c c c c c c c c c c $	6	con-non	Tu	:	ន	n	68 2	-	TVA 1000 (FID)						
	13		10	:	g	ш	68 2	•	TVA 1000 (PID)			1	- -	,	
	Ŧ	101-100	£	:	-	=	8	-	OVA 108	•	R	8	*	ę	
	7	con-non	£	:	-	╛	8	•	TLV Shifter		,	8	•	ç	
	1	00-000	£	:	-	E	8	•	HNU	•	8	B	,	2	
if         contron         Th          I         LL         690         4         TVA T000 (FU)         5         1100         1200         200 <th< td=""><td>14</td><td>001-000</td><td>£</td><td>:</td><td>-</td><td>E</td><td>8</td><td>•</td><td></td><td></td><td></td><td></td><td></td><td></td><td></td></th<>	14	001-000	£	:	-	E	8	•							
15         contron         1u          3e         LL         69         114         O/A 108         3         1u0         L/A         90         L/A           15         contron         Tu          36         LL         69         114         T/V Sniffer         5         600         600         200         600         600         500         60         70<	14	00-000	£	:	-	E	8	•		•			ß	9	
15         contron         Tu         ····         38         LL         60         114         ITUV Similer         5         600         600         200         400           15         contron         Tu         ···         38         LL         69         114         INV Similer         5         600         600         200         400           15         contron         Tu         ···         38         LL         69         114         INV 1000 (FID)         400         600         600         200         400           15         contron         Tu         ···         38         LL         68         114         INV 1000 (PID)         9         20         20         40           16         contron         Tu         ···         38         LL         68         114         ILV Similer         5         50         50         50         50         60	15		2	:	8	╡	8	114	BOL MA	•	M	<b>M</b> 7			
15       control       Tu        36       LL       66       114       HMu       5       600       000       700<	15	001-000	2	:	ន	Е	8	114	TLV Shifter				ş	Ę	
15       controm       Tu        3/6       LL       69       114       TVA 1000 (FU)       5       50 <th< td=""><td>5</td><td>001-000</td><td>5</td><td>:</td><td>8</td><td>╡</td><td>8</td><td>114</td><td>HNN</td><td>\$</td><td>900</td><td></td><td>ş</td><td>3</td><td></td></th<>	5	001-000	5	:	8	╡	8	114	HNN	\$	900		ş	3	
15       controm       Tu        3/6       LL       650       114       [TVA 1000 (PlD)]       5       50       50       50       60         16       controm       Tu        3/6       LL       666       114       [TVA 1000 (PlD)]       5       50       50       20       40         16       controm       Tu        3/6       LL       666       114       [LV Smillet       5       110       120       10       50 <td>5</td> <td>CON-IION</td> <td>2</td> <td>:</td> <td>8</td> <td>E</td> <td>8</td> <td>114</td> <td>TVA 1000 [FID</td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td>	5	CON-IION	2	:	8	E	8	114	TVA 1000 [FID						
16         contron         Tu          36         LL         66         114         O/A 106         5         30         30         40         40           16         contron         Tu          36         LL         66         114         TLV Smillet         5         110         120         10         50         10         50         10	15	CON-NON	2	:	8	E	8	114	TVA 1000 (PID			1	8	\$	
16         contron         Tu         36         LL         66         114         TLV Shifter         5         110         120         50         9           16         contron         Tu          36         LL         66         114         HNu         5         110         120         10         50           16         contron         Tu          36         LL         66         114         HNu         5         110         120         10         50           16         contron         Tu          36         LL         66         114         TvA 1000 (FID)         5         10         50         50           16         contron         Tu          36         LL         66         114         TvA 1000 (PID)         50         10         50         50	ę	CON-NON	Ţ	:	8	E	8	114	OVA 108	2	8	8	2		
16 contron Tu 36 LL 66 114 HNu 5 110 130 TU 30 L 16 contron Tu 376 LL 66 114 TVA 1000 (FID) 130 TU 30 10 30 11 16 contron Tu 376 LL 66 114 TVA 1000 (PID) 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5 5	9		τ¢	:	8	н н	8	114	TLV Sniffer						
16 con-non Tu 378 LL 66 114 TvA 1000 (FLD) 16 con-non Tu 378 LL 66 114 TvA 1000 (PLD)	9	00-100	Tu Tu	:	36	ц	8	114	HN	8	₽ -	R	2	8	
16 con-non Tu 376 LL 66 114 TVA 1000 (PID)	9	001-100	Tu	:	R	н	8	11	TVA 1000 (FID						
	16	00-000	Τu	:	8	E	8	114	TVA 1000 (PID					8	

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Refinerie		Comoon	haf Informe	uop		Ambient C	onditions			Scr	ening Deta			معتار المراجع ا
R andra	Component Type	Sub- category	Acturition	i î	s trans	Amblent Temp. (Fehrenholt)	Amblent Windspeed (ft / min)	Instrument Type	Background Bcreening Value (ppm)	Maximum Bustainable Bustaing of Bustace (ppm)	Peak Bereening M Burface (ppm)	Mextmum Bustainable Bcreening et 1 cm (ppm)	Peak Screening at 1 cm (ppm)	Comments
		=		ŝ	ŀ	8	¥	TLV Sniffer						
= :		>=		5		8	Ŧ	HNU	4	¢	8	8	<u>5</u>	
:			:	Ē	E	8	4	TVA 1000 (FID)						
		5	:	ä	E	8	4	TVA 1000 (PID)						
:		1	:	s	E	67.2	8	OVA 108	*	8	R	~	~	
2		2	:	8	E	67.2	45	TLV Sniffer						
2		1	:	\$	E	67.2	\$	HNU	4	ę	ę	2	5	
÷		2	:	5	3	67.2	ę	TVA 1000 (FID)						
8	CON-TION	Tu	:	S	۲ ۲	67.2	Ş	TVA 1000 (PID)						
19	Alev	Gate	v	-	וו	22	106	OVA 108	•	8	8	50	8	Fluctuating
Ş	AgNe	Gete	υ	-	н	2	106	TLV Shifler						
Ę	a yes	Gate	0	-	E	22	106	HNU	*	8	8	ន	8	
¢	ave.	Gate	0	-	E	22	<b>6</b>	TVA 1000 (FID)						
¢	aver	O Sete	0	-	н	z	108	TVA 1000 (PID)						
2	wer	Gate	U	-	F	8	30	OVA 108	4	8	20	7	8	
2	wine	Gate	U	-	F	8	8	TLV Shiffer						
		e C	0	-	Е	8	8	HNU	•	ţ	8	s	e	
2 8				-	=	8	8	TVA 1000 (FID)						
2		e e		-	3	8	8	TVA 1000 (PID)						
R R				-	=	8	8	OVA 108	Ŧ	R	8	0	16	Dupitcate
e e	2	e e c	0	-	F	8	8	TLV Shiffer						
S Z	-	5		-	E	8	8	HNU	•	8	8	•	e	
R F			0	-	=	8	8	TVA 1000 (FID)						
R R	a ver	e e	0	-	E	8	8	TVA 1000 (PID)						
21	aver	Gate	2	~	3	6.99	89	OVA 108	•	2	R	•	Ŧ	
	And	Gate	×	~	н	68.3	89	TLV Shifler						
	vaNe	e e e	×	2	LL L	683	8	INU	•	8	ନ୍ଦ	<b>s</b>	₽	
21	valve	Gate	X	2	IL	<b>68</b> 3	88	TVA 1000 (FID)						
21	ANev	Gate	X	2	II	86.3	8	TVA 1000 (PID)						
22	vahe	Gate	v	-	Ξ	645	181	OVA 108	4	60		ŝ	0	
22	vahe	Gate	0	•	=	<b>8</b> .5	181	TLV Somer			•	•		
22	ANBA	Gate	v	-	=	64.5	181	HNU	◀	\$	6			
22	vahe	Gate	ပ	•	Н	645	181	TVA 1000 (FID)						
22	valve	Gete	U	-	Ц	64.5	161	TVA 1000 [PID)						
23	Alle	Gete	c	2	GAS	8	62	OVA 108	-	170	220	580	280	Visible Inquid
23	valve	Gate	υ	~	GAS	8	62	TLV Sniffer	~	86	8	₿	B	
23	vahe	Cate Cate	c	2	GAS	8	29	INU	7	140	-160	8	R	
33	valve	Gate Gate	v	2	GAS	8	8	TVA 1000 (FID)						
23	valve	Gete	ပ	2	GAS	8	82	TVA 1000 (PID)						
24	Alle	Gate	X	•	GAS	88.5	162	OVA 108	~	200	8	8	B	
24	avev Alev	Gate	X	•	GAS	66.5	<u>1</u> 8	TLV Shifter	~			740	740	

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Refinery		Compon	unt informed	5	-1	Imblent Co	onditions			Sor	ming Deta			
Renter Munder	Component Type	Buth- category	Actuetton	e î	Lervice 5	Amblent Temp. Fehrenheit)	Amblent Windspeed (R / min)	Instrument Type	Background Screening Value (ppm)	Maximum Busteinable Bustace (ppm)	Peek Screening at Surface (ppm)	Maximum Bustainable Screening at 1 cm (ppm)	Peek Acreening At 1 cm (ppm)	Comments
2	Mov	Gate	¥		GAS	665	162	HNN	0	300	300	200	300	
24	Alev	Cate	I		SS	665	162	TVA 1000 (FID)						
24	valve	Gate	I	•	GAS	66.5	162	TVA 1000 (PID)						
2	velve	Gate	¥	-	п	66.4	202	OVA 108	7	ę	8	C	8	
\$2	Mev	Gate	Z	-	н	66.4	202	TLV Shifter						
8	WEA	Gate	×	-	3	<b>4</b> 88	202	HNU	0	0	8	0	0	
\$	Mex	Oate O	×		E	68.4	202	TVA 1000 (FID)						
2	Mev	Gate	Z	-	E	<b>96.4</b>	202	TVA 1000 (PID)						
8	CON-FION	£			Ħ	73.1	116	OVA 106	5	140	160	8	22	
2	CONTROL	E		F	1	191	116	TLV Shifter						
2	con-non	E	:	F	н	73.1	116	HNU	0	¥	8	ŝ	ę	
2	Non-non	£	::	-	11	73.1 +	116	TVA 1000 (FID)						
۶	CON-LON	£	:.		n	73.1	116	TVA 1000 (PID)						
27	con-non	£			ц	66.4	111	OVA 108	•	12	12	Ð	•	
27	CON-TION	Æ		H	r T	66.4	111	TLV Shifter						
27	con-non	£	:	H	n L	66.4	111	HNU	0	0	0	0	0	
27	LOT-TOO	ŧ		-	=	8	111	TVA 1000 (FID)						
27	CON-NON	£		-	н	66.4	111	TVA 1000 (PID)						
8	CON-NON	£		4	η	88	28	OVA 108	•	89	909	8	8 <u>8</u>	
28	con-non	£	•	12	۲ ۲	8	28	TLV Shifter						
28	CON-NON	£		12	L L	8	28	HNU	0	ĝ	250	180 1	8	
26	CON-NON	ŧ		ä	Н	8	26	TVA 1000 (FID)						
26	CON-FICH	£	::	Ë	Ц	8	28	TVA 1000 (PID)						
29		£	:	-	1	67.4	239	OVA 108	2	R	8	23	8	
29	CON-NON	£		-	H	67.4	239	TLV Somer						
29	CON-NON	£	•	-	н	67.4	239	HNU	0	8	8	S	•	
29	LON-NOD	£		-	E	67.4	239	TVA 1000 (FID)						
29	con-non	£	:	_[	=	67.4	239	TVA 1000 (PID)						
8	A	Gete	v	~	╡	88.6	8	OVA 106	s	¥	Ş	2	2	
8	vaNe	Gete	0	~	=	8	8	TLV Shifler						
8	even	Cate	o	~	З	886	8	HNU	0	8	ନ୍ଦ	4	•	
8	avev	Gate	v	~	=	89.6	20	TVA 1000 (FID)						
8	Alex	Cate Oate	v	7	=	8	20	TVA 1000 (PID)						
31	vahe	Gate	v	2	=	8	157	OVA 108	S	18	18	Ð	•	
31	vahe	Gate	υ	~	1	8	157	TLV Sniffer						
31	vaNe	Gate	υ	~	=	8	157	INU	0	8	ę	a	0	
31	vahe	Gate	U U	~	ц	8	157	TVA 1000 (FID)						
31	vahe	Gate	υ	~	ц	8	157	TVA 1000 (PID)						
32	A	Gete	ა	2	Ŧ	8	258	OVA 108	ŝ	8	ĝ	1 <u>5</u> 0	ŝ	Visible liquid
32	Mex	Gate	v	2	Ŧ	8	258	<b>TLV Shifter</b>	0	8	Ŕ	200	8	
32	ANA	Gate	- -	5	L L	8	250	INU	0	88	88	175	<u>8</u>	

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Inery	Con	nponen	t Informat	lon	1	Amblent C	onditions			Scre	ening Deta			
	pe cris	4	ctuation 1	in .	bervice	Amblent Temp. Fehrenheit)	Amblent Windspeed (ft / min)	Instrument Type	Background Screening Value (ppm)	Maxtmum Besteinebie Besteening et Bestrece (ppm)	Peak Bicreening at Surface (ppm)	Maximum Bustaineble Screening at 1 cm (ppm)	Peak Bcreening at 1 cm (ppm)	Comments
\$	0 2	ł	0	5	Ŧ	8	<b>3</b> 58	TVA 1000 (FID)						
5	ı S	ate ate	U	2	Ŧ	89	258	TVA 1000 (PID)						
8	3 2	ate	0	₽	E	683	72	OVA 108	15	240	240	70	100 1	
8	g R	ete	0	₽	н	683	72	TLV Sniffer	0	50	8	0	0	
\$	3	ŧ	0	₽	н	68.3	72	HNI	0	200	240	100	8	
6×	0 2	ete B	с о	₽	3	68.3	72	TVA 1000 (FID)						
5	0 2	e e	0	₽	3	68.3	72	TVA 1000 (PID)						
5	3	ę	z	₽	Ŧ	2	262	OVA 106	10	650	650	650	650	Visible liquid.
2	3	e e	Ξ	₽	Ŧ	20	262	TLV Sniffer	0	300	30	300	8	
X	j S	ete	3	þ	Ŧ	2	262	HNU NH	0	750	750	680	680	
2	0 2	ete	¥	þ	Ŧ	2	262	TVA 1000 (FID)						
2	2	ete	E	þ	Ŧ	2	262	TVA 1000 (PID)						
2	Ŭ V	ete	0		E	72.3	5	OVA 108	15	200	350	100	200	Bonnet.
8	0 P	ate	0	-	E	72.3	135	TLV Sniffer	0	200	202	9	¥	
5	Ŭ V	ete	0	-	E	2.5	135	INU	0	300	<b>2</b> 00	8	180	
2	ı Z	9	0		E	72.3	135	TVA 1000 (FID)						
5	0 2	ete te	0	-	E	72.3	135	TVA 1000 (PID)						
2	0	ete	0		SYS	72.0	110	OVA 108	10	20	8	8	R	
2	0 2	ate	U		GAS	72.0	110	TLV Shifter	0	0	0	0	0	Debutanizer overhead
5	S S	et e	v	•	GAS	72.8	110	HNU	•	120	170	8	8	
8	Ne G	ate	с U	•	GAS	72.8	110	TVA 1000 (FID)						
8	Ne G	ate	υ	•	GAS	72.0	110	TVA 1000 (PID)						
7 001	non	£	:	-	н	68.2	318	OVA 108	•	3000	2005	1200	1200	Plug
7 000	-non-	£	:	-	Ц	68 2	318	TLV Smiller	•	2300	2300	1000	ē	
100	-uou-	Ē	:	-	1	68.2	318	HNU	0	360	8	8	Ş	
	non	£	:	-	H	68.2	318	TVA 1000 (FID)						
7 001	-non-	£	:	-	=	68.2	318	TVA 1000 (PID)						
R R	0 N	ate	¥	Z	GAS	76.3	584	OVA 108	•	220	82	R	8	Ges = Methane
8 VB	ğ	ete	Z	ž	GAS	76.3	584	<b>TLV Sniffer</b>	•	•	•	•	•	
8	Ne O	ate	Σ	ž	GAS	76.3	284	HNU	0	180	8	ຂ	22	
6	Me G	ate	¥	ž	GAS	76.3	ğ	TVA 1000 (FID)						
ev 0	Me	ate	¥	ž	GAS	763	564	TVA 1000 (PID)						
84	G.	ate	X	14	GAS	74	266	OVA 108	•	9	18	¢	<b>ç</b>	Gas = Methane.
5	ğ	ate	X	14	GAS	74	268	TLV Sniffer	0	0	0	0	•	
5	Ňe G	ate	Z	ž	SSS	74	266	Ĩ	0	5	5	2	~	
6 A	Ne S	ate	Z	ž	GAS	2	268	TVA 1000 (FID)						
9 V8	Ö	ą	X	¥	GAS	z	266	TVA 1000 (PID)						
0 14	ق ٩	ate	Ξ	-	GAS	2	239	OVA 106	•	8	220	¥	2	Gas = Methane
0	ی و	ete B	Z	-	GAS	"	239	<b>TLV Shifter</b>	0	0	0	•	•	
6 N	Ö	ate	¥	-	GAS	2	239	HNu	0	<u>6</u>	180	R	ę	
EN O	ũ V	ate	Z	-	GAS	2	239	TVA 1000 (FID)						

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inery	_	Compon	int Informa	non		Amblent C	onditions			Scr	ening Dete				
M and a second	Component Type	Bulb- category	Actuation	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	her vice	Amblent Temp. Fahrenheit)	Amblent Windspeed (ft / min)	Instrument Type	Beckground Screening Value (ppm)	Maximum Bustaimebia Bustace (ppm)	Peek Screening at Burhice (ppm)	Maximum Bustainable Bornening ef 1 cm (ppm)	Peak Screening at 1 cm (ppm)	Comments	
Ş	Mey	Gate	Ξ	ŀ	GAS	11	239	TVA 1000 (PID)							
8	a Yes	Gete	Z	-	SS	"	239	OVA 108	9	120	120	12	2	Dupitcate Gas « Methane	
Ş	vahe	Gate	Ŧ	-	GAS	2	239	TLV Shiffer	0	0	0	0	0		-
Ş	valve	Gate	×	-	SSS	11	239	HAN	0	<b>3</b> 0	20	01	10		_
Ę	VBNe	Gate	¥	-	GAS	"	239	TVA 1000 (FID)							
Ş	valve	Gøte	Σ	-	GAS	<i>n</i>	239	TVA 1000 (PID)							_
ŧ	vahe	Gate	z	-	SSS	70.5	199	OVA 108	8	8	70	10	12	Gas = Methane	_
Ŧ	vahe	Gate	Ξ	-	GAS	70.5	199	TLV Sniffer	0	0	0	0	0		_
ŧ	Nex S	Gete	Ξ	-	GAS	70.5	199	HNU	0	8	90	0	0		
ŧ	Alle	Gete	Z	-	GAS	705	199	TVA 1000 (FID)							
ŧ	ever A	Gate	æ	-	GAS	70.5	199	TVA 1000 (PID)							
-	ANev	Gate	U	•	GAS	68.4	167	OVA 108	1	8	8	12	12		
418	A	Gate	v	•	GAS	68.4	167	TLV Shifter	0	0	0	0	0		
ŧ	vahe	Gate	v		GAS	68.4	167	HNU	0	140	140	0#	20		
4	waiter	Gate	v		GAS	68.4	167	TVA 1000 (FID)							
40	vahe	Gete	v	•	GAS	68.4	167	TVA 1000 (PID)							
\$	non-noo	41	••••	2	GAS	6.69	10	OVA 108	8	3	25	8	8	Phone	
42	con-non	£	•	2	GAS	69.8	10	TLV Shifter	0	0	0	0	0		
42	con-non	£	:	~	GAS	8 69	₽	INU	0	3	5	-	-		
42		£	:	~	GAS	889	¢	TVA 1000 (FID)							
42	001-000	E	:	~	GAS	88	ę	TVA 1000 [PID)							
43	vahe	Gate	¥	•	GAS	889	244	OVA 108	5	₿	140	6	2		
5	vahe	Gate	Ŧ	•	GAS	8.0	244	TLV Shifter	0	0	0	0	0		
43	vatve	Gete	æ	•	GAS	80	244	HNU	0	<b>1</b> 00	180	90	ę		
43	vahe	Gate	æ	8	GAS	65.9	244	TVA 1000 (FID)							
63	vahe	Gate	¥	•	GAS	62.9	244	TVA 1000 (PID)							
4	Alle	Gate	U	-	GAS	z	<del>1</del> 5	OVA 108	5	180	160	\$	ę		
Ŧ	ever Nev	Gate	v	-	GAS	S	159	TLV Sniffer	0	0	•	0	-		
\$	Alle	Gate	0	┥	SAS	3	159	HNN	0	8	8	8	₿		
¥	Alle	Gate	0	-	SAS	3	159	TVA 1000 [FID)							
4	Alve	Gete	v	•	SS	3	150	TVA 1000 (PID)							_
Ş	con-ron	£	:	~	3	8	236	OVA 106	~	<b>8</b>	100	8	ន		
45	CON-NON	£	:	7	3	8	236	TLV Shiffer	0	0	0	0	0		_
\$	con-non	£	:	~	3	8	236	HNU	٥	185	185	8	ន		
45		€	:	7	=	8	236	TVA 1000 (FID)							_
ę	WHON NO	£	-	~	=	8	236	TVA 1000 (PID)							_
¥	valve	Cate	3	-	3	51.2	ē	OVA 108	10	200	240	8	58		
8	vahe	Gate	Z	•	=	57.2	16	TLV Shifter	10	23	23	40	ę		
ş	Ale	Gate	3	-	=	57.2	16	HNU							
¥	valve	Gate	₹	-	=	57.2	16	TVA 1000 (FID)							
¥	Alle	Cate	¥	-	н	57.2	48	TVA 1000 (PID)							

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Hennery		Compon	ent informer	5 5	Ì		suonipuo			NON	men buine			
Mumber Mumber	Component Type	Sub- category	Actuation	lin.)	Pervice	Amblent Temp. Fehrenheit	Amblent Windspeed (Ti / min)	Instrument Type	Background Screening Value (ppm)	Maximum Surtamable Screening at Surface (ppm)	Peek Screening at Surface (ppm)	Maxtmum Sustainable Screening at 1 cm (ppm)	Peak Screening at 1 cm (ppm)	Comments
14	-uoo			Ļ		8	~	OVA 108	₽	Ş	700	₿	<u>8</u>	
14	5-000	u	:	I-	E	8	~	TLV Sniffer	ŝ	ð	<b>00</b>	80	5	
14	<b>Froo</b>	L	:	-	E	8	7	HNU						
14	e-u-u-u-u-u-u-u-u-u-u-u-u-u-u-u-u-u-u-u	L	:	-	н	8	7	TVA 1000 (FID)						
14	con-li	u	:	┫	E	8	7	TVA 1000 (PID)						
ş	avex	Gate	2	•	=	57.2	120	OVA 108	₽	140	140	8	8	
\$	aver	Gate	Z	-	3	57.2	120	TLV Shiffer	<b>t</b>	8	60	15	15	
\$	avev	Gate	Z	-	E	57.2	5	HIN						
ŧ	Aller	Gate	×	-	E	57.2	120	TVA 1000 (FID)						
Ş	Aller	Gete	I	-	E	572	120	TVA 1000 (PID)						
2	Aller	Gate	2	-	E	888	5	OVA 108	10	250	250	8	8	
S.	vahe	Gate	3	-	3	20.0	8	TLV Shifter	5	100	100	80	8	
ę	vaNe	Gate	2	-	E	20.0	\$	HNU						
Ş	vahe	Gate	3	-	Ŀ	88	\$	TVA 1000 (FID)						
Ş	even	Gete	Z	-	E	50.8	5	TVA 1000 (PID)						
5	avev	Gate	Ξ	-		57	8	OVA 108	₽	8	8	20	8	
5	aves	Sete	2	-		5	8	TLV Sniffer	s	8	8	32	32	
8	aven	Gate	3	-	н	57	8	HNN						
8	valve	Gate	z	-	E	57	8	TVA 1000 (FID)						
8	vahe	Gete	I	-	З	57	65	TVA 1000 (PID)						
51	ABVe	Gate	Z	:	ц	57.2	174	OVA 108	₽	2000	2000	1800	2000	Bonnet leaking
51	vaNe	Gete	¥	:	ц	57.2	174	TLV Smiller	ę	1600	1800	1400	1400	
51	vahe	Gate	W	:	ц	57.2	174	HNU						
51	vahe	Gate	×	:	н	57.2	174	TVA 1000 (FID)						
51	valve	Gate	Þ	:	r r	57.2	174	TVA 1000 (PID)						
52	valve	Pug	Z	6	ц	565	107	OVA 106	12	8	8	8	2	Pump inter
22	aves	Pho	×	3	Ц	565	107	TLV Sniffer	0	0	0	0	0	
52	valve	Plug	z		Ц	565	107	HNU						
52	vaive	Plug	Z	•	З	565	107	TVA 1000 (FID)						
52	valve	Plug	Ξ	•	3	56.5	107	TVA 1000 (PID)						
8	valve	Gate	X	-	ц	57.4	37	OVA 108	9	8	8	28	28	
ន	vahe	Gate	Z	-	н	57.4	37	<b>TLV Shiffer</b>	0	0	•	•	•	
8	valve	Gate	W	-	μ	57.4	37	HNU						
8	valve	Gate	¥	Ŧ	ц	57.4	37	TVA 1000 (FID)						
8	vave	Gate	Z	Ŧ	н	57.4	37	TVA 1000 (PID)						
2	AMen	Gete	υ	2	Γ	57.2	274	OVA 108	10	25000	30000	2000	3000	Max at end of test was 6000 @ 0cm
2	Alive	Gate	v	2	μ	57.2	274	TLV Sniffer	0	2400	2400	1600	1600	
3	Alve	Gate	v	2	ц	57.2	274	HNU						
2	vahe	Gate	v	~	ц	57.2	274	TVA 1000 (FID)						
2	Alle	Gate	υ	~	ц	57.2	274	TVA 1000 (PID)						
ş	CON-DON	Ē	:	-	E	500	5	OVA 106	ŧ	2	170	8	8	

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Refinery		Compon	int inform	ngou		Amblent C	puditions			Scri	ening Dete			
	component Type	Sub- cetegory	Actuation	8ize (in:)	Bervice	Amblent Temp. (Fehrenhell)	Amblent Windspeed (ft / min)	Instrument Type	Beckground Bcreening Value (ppm)	Maximum Bustainable Boraaning af Burface (ppm)	Peek Bcreening at Surfece (ppm)	Maximum Bustainable Boneening at 1 cm (ppm)	Peak Screening at 1 cm (ppm)	Commants
8	001-002	Ę	:	-	3	60.2	81	TLV Suffer	\$	<b>1</b> 00	8	0	0	
8	CON-NON	£	:	-	E	60.2	81	HNU						
8	CON-NON	E	:	-	E	60 2	81	TVA 1000 (FID)						
8	CON-NON	£	:	-	н	60.2	81	TVA 1000 (PID)						
8	vahe	Gele	Ξ	-	3	8	169	OVA 108	1	R	R	10	9	
8	vahe	Gete	Z		Ľ	8	189	TLV Sniffer	0	0	0	0	0	
8	valve	Gate	¥	•	н	80	189	INN						
8	vahe	Gate	¥	•	н	8	189	TVA 1000 (FID)						
8	valve	Gate	Z		н	8	189	TVA 1000 (PID)						
57	valve	Gete	¥	-	E	8	61	OVA 108	₽	800	3000	88	809	
57	www	Gate	ž	-	Ц	60	81	TLV Sniffer	0	750	750	650	650	
57	Alke	Gete	Z	-	3	8	61	HNM						
57	vahe	Gate	Z	-	Ľ	8	61	TVA 1000 (FID)						
57	vahe	Gate	¥	-	Ľ	8	81	TVA 1000 (PID)						
8	wayes	Gate	Z	-	H	597	13	OVA 108	¢	220	ŝ	220	220	
8	vahe	Gate	Ŧ	•	E	597	13	TLV Sniffer	0	8	8	45	45	
5	wave	Gate	¥	-	ц	59.7	13	HNN						
5	valve	Gate	Ŧ	•	н	59.7	13	TVA 1000 (FID)						
5	vahe	Gate	Ŧ	-	н	59.7	13	TVA 1000 (PID)						
2	U-UO2	u.	:.	2	Ľ	595	205	OVA 108	₽	88	660	140	140	
\$	Fuo	u	:	2	rr L	585	205	TLV Shiffer	0	8	300	120	120	
8	I-los	u.	•••	2	ц	59.5	202	HNU						
8	<b>U-100</b>	ш	•••	2	۲I	505	205	TVA 1000 (FID)						
8	Con-fl	Ľ		2	Ľ	50.5	202	TVA 1000 (PID)						
8	vahe	Gate	X	9	ц	62.4	17	OVA 108	₽	99 <del>9</del>	8	200	8	
8	valve	Gate	M	9	Ц	62.4	17	TLV Shiffer	0	100	ā	8	8	
8	vahe	Gete	M	6	ц	62.4	17	HN						
8	valve	Gete	¥	9	Ľ	62.4	17	TVA 1000 (FID)						
8	vahe	Gate	¥	9	Ŀ	62.4	1	TVA 1000 (PID)						
8	vahe	Gate	X	3	Ц	62.2	197	OVA 108	₽ P	90 <b>4</b>	9 <b>2</b> 4	120	<del>1</del> 60	Dupticate
8	valve	Gate	Z	9	۲L	62.2	197	TLV Shiffer	0	<b>8</b>	ē	16	<b>1</b> 6	
8	vahe	Gete	Z	0	Ľ	62.2	197	HNU						
<b>P</b> 09	valve	Gete	¥	e	Ч	62.2	197	TVA 1000 (FID)						
<b>P</b> 09	wahe	Gate	æ	9	Ц	62.2	197	TVA 1000 (PID)						
61	vaive	Gate	ပ	3	Ц	61	203	OVA 108	10	8	8	12	8	
61	valve	Gate	ပ	9	٦	61	202	TLV Shifter	0	0	0	0	0	
61	valve	Gate	U	9	H	61	200	HNU						
61	vahe	Gate	v	9	Η	61	203	TVA 1000 (FID)						
6	vahe	Gate	υ	e	E	61	203	TVA 1000 (PID)						
22	con-fl	Ľ	:	4	IL	61	232	OVA 106	9	240	240	8	8	Visible liquid
2	5.00	Ľ	:	4	н	61	232	TLV Shifter	0	8	8	5	•	

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Refinery		Compon	ent Inform	non		Amblent C	onditions			Sc2	aning Deta			
H H H	Component Type	Bub- category	Actuation	8/26 (j.i.)	Bervice	Amblent Temp. (fahrenheit)	Amblent Windspeed (It / min)	Instrument Type	Beckground Screening Value (ppm)	Maxtmum Bustninable Berteening at Bertece (ppm)	Peek Bcreening st Surface (ppm)	Maxhmum Bustainable Bcreening at 1 cm (ppm)	Peak Screening at 1 cm (ppm)	Comments
5	1	"	:	-		5	232	INU						
5	-ue		:	•	=	5	232	TVA 1000 (FID)						
8	-us	Ľ	:	-	E	5	232	TVA 1000 (PID)						
8	A B Me	Gete	×	•	E	8	425	OVA 108	8	25	22	15	15	
8	vahe	Gate	z	•	E	8	425	TLV Sniffer	0	0	0	0	٥	
8	weve	Gate	×	•	F	8	425	NAH						
8	Alle	Gete	2	•	н	90	425	TVA 1000 (FID)						
8	Alle	Gate	¥	•	E	8	425	TVA 1000 (PID)						
20	A8Me	Gate	¥	-	Ľ	61.6	22	OVA 108	10	ę	ę	18	18	
2	Alle	Gate	I	-	Е	61.8	22	TLV Sniffer	0	0	0	0	٥	
2	valve	Gate	E	-	E	618	22	HNU						
2	vave	Gate	×	-	F	618	22	TVA 1000 (FID)						
Z	Ashe	Gate	×	-	F	618	22	TVA 1000 (PID)						
8		Ē	:	-	3	80	315	OVA 108	•	2	۶	8	32	
8	CON-TION	£	:	ŀ	E	8	315	TLV Sniffer	0	0	0	0	0	
8	COL-DO	ŧ	:	-	н	8	315	HNV						
8	CON-NON	€	:	•	Ц	8	315	TVA 1000 (FID)						
55	COLHON	€	:	-	ц	8	315	TVA 1000 (PID)						
8	vahe	Gate	X	12	ц	61.6	80	OVA 108	7	8	22	₽	12	
8	vahe	Gate	X	ğ	Ц	61.6	30	TLV Sniffer	0	0	-	0	•	
8	valve	Gate	M	12	Ч	61.6	88	HNU						
8	valve	Gate	M	12	Ц	61.6	ĝ	TVA 1000 (FID)						
8	vahe	Gate	X	21	Ľ	61.6	30	TVA 1000 (PID)						
67	vathe	5 0	X	30	ц	51.2	8	OVA 108	7	8	009	9 <u>5</u> 2	250	Retested with OVA at surface at 1100 at end o
67	vahe	Plug	X	ЭМ Э	Ч	51.2	8	TLV Shifter	0	026	820	240	240	
67	valve	Plug	X	ЗМ В	н	51.2	8	HNN						
67	valve	Plug	M	8	Ц	51.2	53	TVA 1000 (FID)						
67	valve	Plug	X	8	E	512	8	TVA 1000 (PID)						
89	eviev	Gate	X	•	E	5	10	OVA 108	ç	8	8	8	8	
8	valve	Gate	X	•	н	8	10	TLV Shifter	0	•	•	0	•	
8	vehe	Gate -	X	4	۲ ۲	5.1	9	INU						
8	valve	Gate	X	¥	ц	53.1	9	TVA 1000 (FID)						
83	valve	Gate	¥	4	Ц	8	₽	TVA 1000 (PID)						
8	valve	Gate	¥	2	Ц	623	102	OVA 108	~	R	ខ	15	5	
8	valve	Gate	X	2	н	623	102	TLV Shifter	0	0	0	0	0	
8	valve	Gate	X	2	E	6.29	102	INN						
69	valve	Gate	¥	2	3	62.3	102	TVA 1000 (FID)						
60	valve	Gate	¥	7	Ы	62.3	102	TVA 1000 (PID)						
02	valve	Gate	¥	-	3	88.1	161	OVA 108	•	8	8	8	ଛ	
70	valve	Gate	Σ	-	Е	<b>8</b>	161	TLV Shifter	•	0	•	•	•	
02	valve	Gate	Z	-	Ч	69.1	161	HNU						

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Refinery		Compon	ant Informe	don	-	Amblent Co	onditions			Ser	ening Dete			
	Component Type	sub- cringory	Actuation	6126 (1n.)		Amblent Temp. Fehrenhett	Amblent Windspeed (ft / min)	Instrument Type	Background Screening Value (ppm)	Maximum Burtainabia Burface (ppm)	Peek Screening at Surface (ppm)	Maximum Sustainable Screening at 1 cm (ppm)	Peek Screening at 1 cm (ppm)	Comments
02	avev	Gate	¥	-	E	<b>1</b> 89	161	TVA 1000 [FID)	•	04	04	11	11	
70	WEA	Gate	Ξ	-	E	68.1	161	TVA 1000 (PID)	•	24	24	7	7	
12		Ę	:	₹	E	68.3	0	OVA 108	7	110	110	8	8	
11	CON-NON	£	:	ž	3	68.3	8	TLV Shifter	0	8	23	10	8	
2	con-hon	£	:	Z	=	60.3	6	HNU						
14	CON-HON	F	:	Z	E	683	6	TVA 1000 (FID)	3	20	70	11	11	
11	con-hon	Ę	:	Z	E	683	6	TVA 1000 (PID)	3	10	<b>0</b>	1	1	
2	AMe	Gate	×	-	3	82	67	OVA 108	4.5	300	300	8	8	
22	avev	Gate	z	•	H	8	67	TLV Sniffer	0	8	90	0	0	
72	valve	Gate	z	-	E	62	67	HNU						
72	A	Gete	X	•	ц	62	67	TVA 1000 (FID)	2	8	110	8	30	
22	valve	Gate	Ξ	-	н	62	67	TVA 1000 [PID]	0	8	\$2	0	0	
73	A	Gate	ပ	2	n	647	275	OVA 108	2	2000	2800	100	1000	Done earlier and fixed
13	valve	Gate	v	2	μ	647	275	TLV Sniffer	0	1100	1100	450	450	
13	vaNe	Oate Oate	ပ	~	E	64.7	275	HINU						
62	vahe	Gate	v	2	r r	64.7	275	TVA 1000 (FID)	2	3000	2000	300	700	
52	valve	Gate	v	2	π	64.7	275	TVA 1000 (PID)						
2		£	::	-	E I	64.3	178	OVA 108	8	300	80	8	ଛ	
74		£	•••	÷	n	64.3	178	TLV Sniffer	0	8	ଛ	0	0	
74	CON-NON	Ē		-	Ч	64.3	178	HNU						
74	con-noo	£	:	•	ц	64.3	178	TVA 1000 (FID)	c	110	<b>1</b> 50	4	4	
74	CON-DOD	£	:	-	П	64.3	178	TVA 1000 (PID)						
75	con-N	Ľ	••••	3	ц	64.6	39	OVA 108	7	8	R	18	18	From Tetramur overhead pump and Accu
75	con-fl	L	:	•	ц	64.6	39	<b>TLV Shifter</b>	0	8	8	ŝ	\$	
75	con-ll	L	•	3	μ	64 6	39	HNU						
75	COT-A	Ľ		6	п	64.6	39	TVA 1000 (FID)	2	79	79	07	¥	
75	con-ll	Ľ	:	~	Ч	64.6	8	TVA 1000 (PID)						
76	ARMe	Gate	¥	-	3	8	452	OVA 108	6	80	ŝ	ê	8	
76	vahe	Gete	Σ	•	=	8	452	TLV Sniffer	0	ę	<del>1</del> 00	ន	8	
76	valve	Gate	2	-	E	8	452	HNU						
76	valve	Gate	Σ	-	=	8	452	TVA 1000 (FID)	6	1001 1	1200	280	320	
76	valve	Sete	z	-	3	8	452	TVA 1000 (PID)						
11	00-000	£	:	-	З	83	:	OVA 108	•	ឧ	R	~	~	Pug.
11	001-000	Ē	:	-	ä	80.5	11	TLV Sniffer	0	10	10	0	0	
11	00-100	E	:	-	3	835	11	HNU						
11	CON-NON	Ē	:	-	3	835	11	TVA 1000 (FID)	8	ę	ŧ	8	70	
11	001-000	£	:	-	=	835	11	TVA 1000 (PID)						
78	vahe	ĝ	¥	-	E	62.7	<del>1</del> 3	OVA 108	8	8	8	25	¥	Trimmer Bims
78	vahe	Gate	2	-	3	62.7	133	TLV Sniffer	0	8	ę	8	8	
70	Alle	Gate	3	-	╡	62.7	133	NH						
18	avev	Oete	Z	4	=	62.7	133	TVA 1000 (FID)	=	8	130	8	85	

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tefinërý		Compon	mt Inform	ndon		Amblent C	onditions			Scr	ening Dete			
E	Component Type	Buib- celegory	Actuation		Service	Ambient Temp. (Fahrenheit)	Amblent Windspeed (ft / min)	Instrument Type	Beckground Bcreening Value (ppm)	Meximum Bustainable Bertece (ppm)	Peek Screening at Surface (ppm)	Maxtmum Bustainable Bcraening at 1 cm (ppm)	Peet Screening at 1 cm (ppm)	Comments
A7	evies	Gate	Z	-	Ц	62.7	133	(CIIA) 0001 AVT						
2 2	avev	Gate	×	~	E	8	8	OVA 108	6	12	12	8	10	
2	wahe	Gate C	E	~	F	20	8	TLV Shifter	0	0	Ð	0	0	
62	wave	Gate	Ŧ	~	н	82	<b>%</b>	HNU						
62	wahe	Gate	¥	~	3	62	96	TVA 1000 (FID)	10	30	8	8	8	
62	avev	Gate	Z	~	F	62	8	TVA 1000 (PID)						
8		E	:	ŝ	ц	62	70	OVA 108		190 1	<b>9</b> 6	ន	70	
8	CON-NON	F	:	12	ц	62	70	TLV Soffer	0	92	82	ę	45	
8	CON-NON	£	:	12	r	62	20	Ĩ						
8	CON-NON	£	:	12	IL	62	70	TVA 1000 (FID)	ç	700	710	8	110	
8		£	:	12	π	62	70	TVA 1000 (PID)						
ğ	CON-FICH	ŧ	:	ä	Π	62	80	OVA 108	8	150	150	Я	Q	Duplicate Trimmer tower BW 2036 271 02
ş	con-non	E	:	ş	IL IL	62	80	TLV Shiffer	12	120	120	45	45	
8	CON-ROM	Ę	:	ä	Ц	29	80	HNN						
28	CON-NON	Ę	:	Ë	H	62	8	TVA 1000 (FID)	S	8	800	125	130	
Ş	con-non	E	:	ş	н	62	8	TVA 1000 (PID)						
ē	Aller	Gete	3	-	н	61	8	OVA 108	8	3	8	12	12	
ā	evex	Gete	Z	•	н	61	65	TLV Shifter	0	8	8	8	8	
91	valve	Gate	¥	•	ц	61	8	HNU						
81	Alve	Gate	X	-	ц	61	8	TVA 1000 (FID)	ŝ	24	¥	15	21	
5	valve	Gate	J	-	Н	61	8	TVA 1000 (PID)						
82	Aller	Gate	X	2	Ч	61	239	OVA 108	S	320	320	8	2	
8	valve	Gate	X	2	Ц	6	239	TLV Sniffer	0	<b>6</b>	₿	ę	ŧ	
82	ever	Gate	Z	2	IL I	61	239	HNU						
82	valve	Gate	¥	2	Ľ	61	239	TVA 1000 (FID)	s	630	1000	200	805	
82	Alba	Gate	¥	2	Ц	61	239	TVA 1000 (PID)						
8	<del>a</del> vie v	Gate	M	12	Ц			OVA 108	s	18	9	2	16	
ន	Albe	Gate	æ	Ş	н			TLV Sniffer	8	8	8	8	22	
8	Aller	Gate	z	Ċ,	IL			HNu						
8	valve	Gate	X	21	ц			TVA 1000 (FID)	9	8	ន	8	8	
8	valve	Gate	X	12	Ľ			TVA 1000 (PID)						
2	Alle	Gate	ပ	2	Ľ	61.2	46	OVA 108	7	7500	10000	600	700	
Z	wer	Gate	ပ	2	۳	61.2	<b>8</b> 6	TLV Shifter	0	3000	3000	3200	3200	
2	MEA	Gete	U	2	ц	61.2	46	HNU						
2	Alex	Gete	ပ	~	Ц	61.2	46	TVA 1000 (FID)	4	8004	0006	1400	2800	
2	Alve	Gete	υ	2	3	61.2	46	TVA 1000 (PID)						
8	Alev	Gate	U	3	LL LL	62.6	11	OVA 108	S	ห	8	22	8	
18	valve	Gate	υ	3	IL	62.6	Ħ	TLV Shifter	8	83	B	52	52	
8	vahe	Gate	U	3	ιr	62.6	11	INU						
8	valve	Gate	ပ	9	H	62.6	=	TVA 1000 (FID)	4	8	8	12	8	
8	Alle	Gate	v	-	Н	62.6	=	TVA 1000 (PID)						

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	Comments																															Plug No tags										
	Peek Bcreening et 1 cm (ppm)	006	600		100		110	40		+		8	¥		8		8	¥		8		8000	8005		Ş		8	₿		8		20	8		90		8	0		:		14
	Maxtmum Bustainable Bcreening at 1 cm (ppm)	300	450		8		8	Q.		1		25	¥		1		12	8		8		2000	000#		õ		₿	<del>5</del>		ę		8	8		8		-	0		6		7
ening Dete	Peak Bereening at Burface (ppm)	1100	360		808		120	8		200		18	8		8		8	72		8		10000			150000		250	175		250		1200	525		3000		R	0		8		8
Scr	Maximen Besteinebie Bertening et Burhece (ppm)	200	99C		300		120	8		150		R	8		ଛ		ន	22		30		00009	×10000		10000		80	175		80		1200 1	525		2500		8	0		8		8
	Background Bcreening Value (ppm)	2	12		•		5	20		*		ŧĵ	8		•		5	8		8		ŝ	2		9		5	0		4		ຄ	0		8		•	0		•		8
	Instrument Type	OVA 108	TLV Shifter	HNu	TVA 1000 (FID)	TVA 1000 (PID)	OVA 106	TLV Shifter	HNU	TVA 1000 (FID)	TVA 1000 [PID]	OVA 108	TLV Soffer	HNU	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Sniffer	HNN	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Soffer	Ĩ	TVA 1000 [FID)	TVA 1000 (PID)	OVA 108	TLV Shifler	HNU	TVA 1000 (FID)	TVA 1000 (PID)	OVA 106	TLV Shifter	HNU	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108	TLV Sniffer	HNU	TVA 1000 (FID)	TVA 1000 (PID)	OVA 108
onditions	Ambient Windspeed (R / min)	70	70	20	20	70	8	80	8	83	ខ	8	8	ន	8	8	0	10	9	10	10	8	8	8	8	8	8	8	8	8	R	43	4	Ş	<b>t</b> 3	8	24	24	24	24	~	221
Amblent C	Ambient Temp. (Fehrenheit)	5	2	2	5	5	64.1	64.1	64.1	64.1	64.1	66.6	66 G	888	866	<u>88.6</u>	836	806	83.6	63.6	8.6	832	832	832	802	80.2	62.7	62.7	82.7	52.7	62.7	80.7	60.7	60.7	60.7	60.7	615	61.5	61.5	61.5	61.5	808
	Bervice	r	Ľ	Ц	E	н	L	Ľ	H	1	E	Ц	H	Ε	3	Ξ	3	н	Н	н	Ц	Ħ	H	Ξ	H	Е	Е	Ξ	E	E	E	E	E	Ξ	Ξ	Е	E	Ę	비	E	╡	H
edon		£	3	C	£	e	£	£	£	3	9	•	•	-	+	-	2	2	2	2	2	30	8	8	8	ន្ល	4	4	◄	*	4	ž	1/4	1/4	14	M	7	~	~	2	2	4
ent inform	Actuation	c	С	с С	v	v	v	c	c	с С	U	X	N	Σ	¥	¥	ပ	ა	ပ	v	ပ				:	:	ပ	0	υ	0	0	:	:	:	:	:	ပ	J	ပ	0	v	0
Compon	Bub- category	Gate	Gate	Gate	Gate	Gate	Gate	Gate	Gate	Gate	Gate	Gate	Gate	Gate	Gale	Gate	Gate	Gate	Gate	Gate	Gate	ŧ	£	Ę	£	£	Gate	Gate Gate	Gate	Gate	Gate	f	£	Ē	£	£	Gate	Gate	Gate	Gate	9 Cete	Cate Cate
	Component Type	vahre	vaNe	vahe	wave	vahie	vahe	VENe	vahe	vahe	valve	vahe	vahe	Alle	valve	Alle	valve	Aller	vahe	valve	vahe	con-non	con-non	00-000	001-000	con-non	vahe	Seve	vave	vaNe	Alle	00-100	CON-NON	con-non	CON-RON	con-roo	Alle	vahe	Alle	Alte	Ň	A
Refinery	M Munder Number	8	88	98 98	98	8	87	67	67	87	87	88	98	88	96	88	8	68	68	68	60	96	8	8	8	8	91	91	9	91	91	8	8	6	26	8	8	ន	8	ន	8	2

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Refinery		Compone	nt inform	etion		Amblent C	onditions	والمراجع والمراجع		Scre	ming Date			
Runner Kunner Kunner	Component Type	Sut- category	Actuation		Bervice	Amblent Temp. (Fehrenheit)	Ambient Windspeed (R / min)	Instrument Type	Beckground Screening Velue (ppm)	Maximum Sustainable Screening at Surface (ppm)	Peak Borsening at Burbace (ppm)	Maxtmum Bustainebie Boreening af 1 cm (ppm)	Peek Bcreening et 1 cm (ppm)	Comments
9	saMay	Gate	U	ŀ	=	<b>8</b> 95	221	<b>TLV Sniffer</b>	0	0	0	0	0	
3	avev	Gate	U	•	E	808	221	NH						
3	aves	Gate	U	•	E	88	221	TVA 1000 (FID)	8	96	30	12	12	
3	eves	Gete	ပ	•	E	9 Q	221	TVA 1000 (PID)						
8	Alle	Gate Gate	U	~	E	49.6	83	OVA 108	6	100	<b>6</b>	8	8	
8	ever Nev	Gate	U	2	F	9.64	363	TLV Shiffer	0	75	75	0	0	
2 8	avay	Gate	0	~	1	49.6	88	HNN						
8		Gate	U	~	=	804	353	TVA 1000 (FID)	7	200	202	15	15	
8	ave.	Gate	υ	~	E	<b>9</b> 6¥	88	TVA 1000 (PID)						
8		ŧ	:	~	E	583	8	OVA 108	8	60	8	15	₽	
8		Ę	:	-	E	56.3	8	TLV Shiffer	0	20	8	0	0	
8 8		Ę	:	~	E	595	8	HNU						
8		ŧ	:	~	E	83	8	TVA 1000 (FID)	8	30	8	₽	2	
8		f	:	~	Ξ	56.3	8	TVA 1000 (PID)						
26		E	:	8	Ξ	582	47	OVA 108	4	8	65	04	8	
70 10		E	:	8	Ŀ	55.2	47	TLV Sniffer	0	30	30	22	22	
(s 01		E	:	8	=	56.2	41	HNU						
01 01		f	:	5	=	<u>55</u> 2	47	TVA 1000 (FID)	•	100	<b>1</b> 00	8	8	
60		Ē	:	5	F	55 Z	41	TVA 1000 (PID)						
5	valve	Gete	Ξ	•	F	54.4	3	OVA 108	8	8	8	-	22	
8	valve	Gete	3	•	T	54.4	3	TLV Shiffer	0	8	ŝ	0	٥	
5	vahe	Gate	Ξ	•	F	54.4	3	HNU						
8	valve	Gate	E	•	F	54.4	6	TVA 1000 (FID)	1	8	<b>6</b>	22	22	
8	valve	Gate	×	•	E	544	9	TVA 1000 (PID)						
8	Alve	Gate	E	6	E	565 565	100	OVA 108	9	ę	8	2	ຂ	
8	weve	Gate	Z		E	555	100	TLV Sniffer	0	Ð	8	٥	0	
8	Alle	Gete	¥	•	н	56.5	100	HNU						
6	vahe	Gate	Z	6	IL	565	100 1	TVA 1000 (FID)	ø	8	8	7	7	
8	valve	Gate	3	9	٦	<u>565</u>	<u>8</u>	TVA 1000 (PID)						
100 1	Aahe	Gate	Z	0	Е	8	6	OVA 108	-	8	¥	8	8	
<u>8</u>	valve	Gate	X	0	נו	8	3	TLV Sniffer	•	8	8	ŧ	15	
ĝ	valve	Gate	X	•	3	ß	C	HNU						
<u>8</u>	valve	Gate	X	9	H	8	6	TVA 1000 (FID)	•	ę	70	Ş	2	
<u>8</u>	vahe	Gate	X	9	H	R	9	TVA 1000 (PID)						
P004	valve	Gate	z	9	E	545	0	OVA 108	~	8	8	8	8	Dupticate
<u>8</u>	valve	Gate	X	С	H	545	0	TLV Shiffer	•	я	32	8	8	
100t	vahe	Gate	X	Ð	H	54.5	0	Ĩ						
<b>P00</b>	Alve	Gate	¥	9	IL	54.5	0	TVA 1000 (FID)	~	110	<b>2</b>	ę	\$3	
<b>P00</b>	valve	Gate	M	e	Ц	545	0	TVA 1000 (PID)						
101	vahe	Gate	Z	•	F	54.9	é	OVA 108	-	8	Ŧ	8	8	
101	vahe	Gate	W	•	Н	54.9	9	TLV Somer						

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W Ambient Ambient Ambient Ambient Ambient Ambient Ambient Sequencies Component Sub- Actuation Size Service Termp. Windspeed Instru Number Type cetagory (In.) 77	Amt Amt Ter Ter Ter Ter Ter Ter Ter Ter Ter Ter	Ment Amblent Trp. Windspeet Anheit) (fi / min)	Instrument						
	20 2 	4) 4)	adá	Bcreening Value (ppm)	Maximum Bustainable Screening at Surface (ppm)	Peak Borening at Surface (ppm)	Maximum Bustainable Borsening at 1 cm (ppm)	Peak Bcreening at 1 cm (ppm)	Commants
tot water Cate N 4 LL 549 16 HMU		2	HNU						
ini valve Gate M 4 LL 549 16 TVA 100	5	19 16	TVA 1000 (FID)	2	¥	8	8	ę	
tot whe Gate M 4 LL 54.9 16 TVA 100	2	1.9 16	TVA 1000 (PID)						
107 valve Gate M 6 LL 565 93 OVA 10	к к	55 93	OVA 108	•	25	8	8	8	
102 valve Gate M 6 LL 56.5 93 TLV Sni	ц 🕅	35 93	TLV Sniffer						Dead
102 valve Gate M 6 LL 56.5 93 HMU	נו צי	3.5 93	INU						
102 valve Gate M 6 LL 56.5 93 TVA 100	к П	<u>55</u> 93	TVA 1000 (FID)	~	8	8	₽	7	
102 valve Gate M 6 LL 565 93 TVA 100	א 	35 93	TVA 1000 (PID)						

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# APPENDIX B

# Statistical Analysis Details

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### B.1 Regression Analysis with Errors in Both X and Y

The fitting of a line to describe the relationship between two variables (X and Y) involves estimating a Y-intercept ( $\beta_0$ ) and a slope ( $\beta_1$ ). When both X and Y variables have measurement errors, measurement error methods (MEM), such as those described by Fuller (1987), can be used to determine the regression line. Whereas, in ordinary least squares (OLS) methods, one assumption is that there are no errors in X or that the errors in X are negligible when compared to the errors in Y, MEM techniques account for the errors in both the X and Y values. Thus, whereas, the OLS method chooses parameter estimates for  $\beta_0$  and  $\beta_1$  as those values which minimize the sum of squares of the <u>vertical</u> distances from the data points to the presumed regression line; MEM techniques involve minimizing the sum of the squares of the X values and Y values, for given estimates of the errors in X and Y.

The MEM technique detailed below is discussed by Fuller (1987) and Mandel (1964). All regression analyses performed for this study were done in log-space. Taking the natural logarithms of the screening values results in model errors that are normally distributed with constant variances. The use of natural logarithms (log base e), as opposed to common logarithms (log base 10), is the natural approach. If common logarithms are used, a correction factor of  $\log_e(10)$  is needed at various points throughout the analysis; this needless complication is avoided by using natural logarithms.

Let Y<sub>i</sub> = Log<sub>e</sub> (Screening value one for component i) = Log<sub>e</sub> (y<sub>i</sub>), and X<sub>i</sub> = Log<sub>e</sub> (Screening value two for component i).

=  $Log_{e}(x_{i})$ 

So that:

**B-1** 

$$Log_e$$
 (Screening value one) =  $\beta_0 + \beta_1 Log_e$  (Screening value two),

or

$$\mathbf{Y}_{i} = \mathbf{\beta}_{0} + \mathbf{B}_{1}\mathbf{X}_{i}$$

describes the regression line in log space.

In OLS regression analysis, the slope and intercept,  $\beta_0$  and  $\beta_1$ , are determined to minimize the following:

$$S = \sum_{i=1}^{n} (Y_i - \hat{Y}_i)^2$$

where

$$\hat{\mathbf{Y}}_{i} = \hat{\boldsymbol{\beta}}_{o} + \hat{\boldsymbol{\beta}}_{1} \hat{\mathbf{X}}_{i}$$

The "hat" notation has been used to indicate the estimate of a given quantity; e.g., â is an estimate of a.

This approach produces biased estimates of  $\beta_0$  and  $\beta_1$  when there is an error in X as well as Y. In this case, the correct approach is to determine the estimates of  $\beta_0$  and  $\beta_1$  using MEM techniques that minimize the following:

$$S' = \sum_{i=1}^{n} \frac{(X_i - \hat{X}_i)^2}{\sigma_{\chi}^2} + \sum_{i=1}^{n} \frac{(Y_i - \hat{Y}_i)^2}{\sigma_{\gamma}^2}$$

The quantities  $X_i - \hat{X}_i$  and  $Y_i - \hat{Y}_i$  are estimates of the model errors in  $X_i$  and  $Y_i$ , respectively. The values  $\sigma_x^2$  and  $\sigma_y^2$  are the <u>measurement</u> errors in X and Y, respectively.

**B-2** 

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We define the variable  $\lambda$  as:

$$\lambda = \frac{\sigma_{\chi}^2}{\sigma_{\chi}^2}$$

In the development here,  $\lambda$  is assumed known. (For the regression analyses performed  $\lambda$  was assumed equal to 1. Thus, the measurement errors in the X values were assumed equal to the measurement errors in the Y values. Duplicate screening value measurements were collected to test this assumption. Results of the analysis of the duplicate screening measurements are discussed in Section B.4 of this appendix).

Minimizing S' is equivalent to minimizing S':

$$S'' = \sum_{i=1}^{n} [(X_i - \hat{X}_i)^2 + \lambda (Y_i - \hat{Y}_i)^2]$$
  
= 
$$\sum_{i=1}^{n} [(X_i - \hat{X}_i)^2 + \lambda (Y_i - (\hat{\beta}_o + \hat{\beta}_1 \hat{X}_i))^2]$$

While the  $\tilde{X}_i$  values come into play in the optimization process, their values are not of primary interest here. Expressions for the estimates of the slope and intercept, which are of primary interest, are available in closed form.

Define

$$v = n \sum_{i=1}^{n} (X_i - \overline{X})^2$$
$$w = n \sum_{i=1}^{n} (Y_i - \overline{Y})^2$$
$$p = n \sum_{i=1}^{n} (X_i - \overline{X})(Y_i - \overline{Y})$$

where,

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$$\overline{X} = \frac{\sum_{i=1}^{n} X_{i}}{n}, \text{ and}$$
$$\overline{Y} = \frac{\sum_{i=1}^{n} Y_{i}}{n}$$

Then the estimates of the slope and intercept are as follows:

$$\hat{B}_{1} = \frac{\lambda w - v + \sqrt{(v - \lambda w)^{2} + 4\lambda p^{2}}}{2\lambda p}$$
$$\hat{B}_{0} = \bar{Y} - \hat{B}_{1} \bar{X}$$

Finally, estimates of  $\sigma_X^2$  and  $\sigma_Y^2$  are given by the formulas:

$$\hat{\sigma}_{x}^{2} = \frac{\lambda \sum d_{i}^{2}}{\left(1 + \lambda \hat{\beta}^{2}\right)(N - 2)}$$
$$\hat{\sigma}_{y}^{2} = \frac{\sum d_{i}^{2}}{\left(1 + \lambda \hat{\beta}^{2}\right)(N - 2)}$$

Where,

$$\sum d_i^2 = \frac{w - 2\hat{\beta} p + \hat{\beta}^2 u}{N}$$

The estimates of  $\sigma_x^2$  and  $\sigma_y^2$  given above are needed to calculate the scale bias correction factor (SBCF) as discussed in Section B.2 of this appendix. The estimates of  $\sigma_x^2$  and  $\sigma_y^2$  are also used in the calculation of confidence intervals for the regression.

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Confidence intervals were not calculated for this study; however, the methods for calculating confidence intervals for the MEM regression are described in Appendix D of the 1993 Refinery Study Report (Radian, 1993).

## **B.2** SCALE BIAS CORRECTION FACTOR

In order to predict the mean y value for a given x value (in linear space), one must first transform the results of the regression from log-log space back to arithmetic scales. To do this, a scale bias correction factor (SBCF) is required to obtain the following predictive equation:

$$\hat{y} = SBCF \times e^{(\hat{\beta}_0)} \times (x)^{\hat{\beta}_1}$$

or,

 $\hat{y} = SBCF \times e^{\hat{Y}}$ 

The SBCF is needed to account for the fact that a nonlinear transformation is being performed on the means. A SBCF was developed specifically for this application. The derivation of this SBCF is described in Appendix D of 1993 Refinery Study report (Radian, 1993).

The SBCF is defined as follows:

SBCF =  $e^{(\hat{\sigma}_Y^2 - \beta_1^2 \hat{\sigma}_X^2)/2}$ 

### **B.3** CORRELATION COEFFICIENT

The sample correlation coefficient is a statistical measure of the linear relationship between two variables. The correlation between two variables, X and Y, is computed as:

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$$r_{XY} = \frac{\sum (X_i - \bar{X}) \cdot (Y_i - \bar{Y})}{\sqrt{\sum (X_i - \bar{X})^2 \cdot \sum (Y_I - \bar{Y})^2}}$$
$$-1 \le r_{XY} \le 1$$

and is bounded:

The correlation coefficient squared  $(r_{XY}^2)$  can be interpreted as the fraction of the total variance of one variable that can be explained in terms of the other variable. In other words,  $r_{XY}$  measures how closely the two variables are related. If the total variation is all explained by the regression line, i.e., if  $r_{XY}^2 = 1$  or  $r_{XY} = \pm 1$ , we say there is a perfect linear correlation. On the other hand, if there is no linear relationship between sample values of X and Y, then  $r_{XY}$  will have a value near zero. In addition, if  $r_{XY} > 0$ , then the response variable (Y) increases as the independent variable (X) does. If  $r_{XY} < 0$ , the response decreases as the independent variable increases.

## **B.4** ANALYSIS OF DUPLICATE SCREENING DATA TO ESTIMATE $\lambda$

Duplicate screening data were collected on twelve components. An evaluation of the duplicate data was performed to determine whether or not the assumption of  $\lambda = 1$  (i.e., that the variability in the X value was equal to the variability in the Y value) was false. Ideally, it would be desirable to collect a very large number of replicate results, so that  $\lambda$  could be estimated with sufficient accuracy. However, this was not feasible within the confines of the current study. It was hypothesized, however, that the measurement variability for different types of screening value measurements would be comparable. In general, sufficient data were collected to test this hypothesis.

Attachment B.1 to this appendix shows the duplicate results that were collected for the twelve components, for each of the five instrument types. Given in Attachment B.1 is the sample id, the sample type (normal or duplicate), and the maximum sustainable

screening values at the surface and at 1 cm. The duplicate analysis was only performed on the maximum sustainable screening values (instead of the peak screening values), since this is the type of screening value measurement specified in Method 21 and the type of measurement typically collected by refineries. The screening values given in Attachment B.1 have been adjusted for background (i.e., the background screening values have been subtracted from the component screening values). As shown in Attachment B.1 duplicate screening measurements were not always obtained for every type of screening value, for every instrument. Thus, for example, there were usually 12 or close to 12 duplicate pairs for the OVA and TLV instruments, but fewer for the HNu and TVA instruments.

Table B-1 shows the variability estimates for screening values obtained at the surface and at 1 cm for the maximum sustainable screening values. Given in Table B-1 is the instrument type, the number of duplicate pairs used to develop the variability estimate, the pooled standard deviation (in ppm), and the pooled coefficient of variation (in percent). The coefficient of variation (CV) is calculated as the standard deviation divided by the mean, and is pooled in the same way standard deviations are pooled. Whereas the standard deviation shows the *absolute* variability and is expected to increase as screening values increase, the CV is a measure of *relative* variability and is not expected to vary as much for different ranges of screening values.

As shown in Table B-1 the standard deviations appear to be fairly similar when comparing the standard deviation at the surface versus the standard deviation at 1 cm for a given component. If fact, it was speculated that if there were differences between the variability estimates, that the variability at 1 cm would be larger that the variability at the surface, since measurements obtained at 1 cm are more subject to ambient conditions (e.g., windspeed, temperature, etc.). However, this is not supported by the data shown in Table B-1.

**B-7** 

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Table B-1

 Analysis of Screening Value Variability in Linear Space

Instrument	Variabili Values	ty Estimates for Sc Obtained at the Sc	creening urface	Variabilit Valu	y Estimates for Sci es Obtained at 1 c	reening m
Type	Number of Duplicate Pairs	Standard Deviation (ppm)	Coefficient of Variation (%)	Number of Duplicate Pairs	Standard Deviation (ppm)	Coefficient of Variation (%)
OVA 108	11	9657.05	44.0	12	11132.27	69.3
TLV Sniffer	10	248.80	45.4	10	246.97	60.6
HNu	8	32.57	31.7	7	3.00	59.1
TVA 1000 FID	2	103.76	55.1	2	40.00	50.0
TVA 1000 PID	0	- 3.	- -	0	3.	a.

Insufficient data to evaluate variability.

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Table B-1 also shows the standard deviations obtained for different instruments. As shown in the table, the standard deviations vary considerably for different instrument types, with the OVA instrument showing the largest standard deviations and the HNu instrument showing the smallest standard deviations. However, there were also higher screening values recorded for the OVA instrument, whereas no screening values greater than 5,000 ppm were recorded for the HNu instrument. The CV provides a more representative measure of how the variability within instruments differs from instrument to instrument in this case, since it is a measure of the relative variability. The CVs shown in Table B-1 do not vary considerable between instruments. The CVs vary from 31.7% to 55.1% for screening values obtained at the surface, and from 50.0% to 69.3% for screening values obtained at 1 cm.

Table B-2 shows the same types of variability estimates presented in Table B-1, except the analysis of the duplicate data was performed on the natural logarithms of the data. Statistical tests to test for the equivalence of variability estimates were only performed on the variability estimates presented in Table B-2. Since the correlation and regression analysis was performed on the logarithms of the data, it follows that the analysis of the variability results should be done in log-space. Furthermore, for this study,  $\lambda$  is the ratio of the variances of X and Y in log-space.

F-tests (Snedecor and Cochran, 1989) were performed to test whether there was a difference between the variances at the surface versus the variances at 1 cm, for each instrument type. The result of the F-tests are shown in the last two columns of Table B-2. There was only one instance (for the TLV instrument) where the F-test indicated a significant difference between the variances at the surface versus 1 cm. No statistically significant differences were indicated for the other instrument types tested ( $\alpha = 0.05$ ).

Bartlett's test (Snedecor and Cochran, 1989) was used to test the equality of variances when more than two variances were being compared (i.e., when comparing variances across different instrument types). The result of Bartlett's test are shown in the last row

**B-8** 

Screen		of
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Instrument Type	Variabilit; Values (	y Estimates f Obtained at ti	or Screening he Surface	Variabilit Valu	y Estimates f ies Obtained	or Screening at 1 cm	L L L L	Conclusions or the F-Test Equal Variances
	Number of Duplicate Pairs	Standard Deviation (ppm)	Coefficient of Variation (%)	Number of Duplicate Pairs	Standard Deviation (ppm)	Coefficient of Variation (%)	P-value	Variance at Surface Significantly Dlfferent From Variance at 1 cm?
A 108	Ξ	0.52	5.9	12	0.88	18.6	0.0949	No
Sniffer	6	1.13	29.9	8	0.53	21.0	0.0440	Yes
INu	5	0.44	11.4	3	0.40	18.0	0.9184	No
1000 FID	2	0.61	14.7	2	0.55	13.0	0.8998	Ŷ
1000 PID	0	2.	a.	0	a.	a.	3.	3.
c Conclusions rtlett's Test I Variances	Conclusio varianc diffe	p-value = 0.0 on: the measu ces are not sig rent for the d instrument ty	695 rement error inificantly lifferent pes	Conclusic varianc diffe	p-value = 0.3 m: the measu ces are not sig rent for the d instrument ty	986 rement error snificantly ifferent pes	Conclu measurem not signi the differ	sion: In general, the nent error variances are ificantly different for ent screening distances

<sup>a.</sup> Insufficient data to evaluate variability.

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of the table. As shown in the table, the Bartlett's test results did not indicate that the measurement errors variances were significantly different for the different instrument types tested ( $\alpha = 0.05$ ).

In summary, there were six separate tests for equality of variances in all. If the unknown, true variances being tested were equal in a given test, there would be a 95% probability that the test would indicate that there was no significant difference. That is, there is a 5% chance of erroneously concluding that there was a difference because of random effects in the data.

When six tests are performed, the probability of occurrence of at least one false conclusion of inequality of variances is higher than 5%. If the six tests were independent, and if all sets of true variances tested were in fact equal, then the probability that there would be no false conclusions at all would be  $0.95^6 = 0.735$ . Thus, there would be more than one chance in four that at least one test would falsely indicate that the variances tested were unequal.

The six tests are not strictly independent, since each variance is used in two of the tests. Nevertheless, the point has been made, that one result out of six that is barely statistically significant at the 5% level does not strongly indicate that the assumption of equal variances should be abandoned.

In conclusion, the duplicate data evaluated did not suggest that there were significant differences between measurement errors across different instrument types, for measurements obtained at the surface or at 1 cm. Also, in general, for a given instrument, significant differences were not found between measurement errors for screening values obtained at the surface versus screening values obtained at 1 cm (the only exception was for the TLV instrument). Thus, the assumption that  $\lambda$  is equal to 1 when using the measurement error method to develop regression equations appears to be a reasonable assumption for this study.

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- Radian Corporation, 1993 Study of Refinery Fugitive Emission from Equipment Leaks. Prepared for Western State Petroleum Association. Glendale, CA. February 1994.
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Attachment B.1

**Duplicate Screening Value Measurements** 

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WSPA Screening Study Duplicate Data

----- INSTR=OVA 108 ------

	Sample	Sample Type	_		Max.Sus. SV	Peak SV	Max.Sus. SV	Peak SV
Refinery	ID	(N or D)	Туре	Phase	0 Surface	@ Surface	at 1 cm	at 1 cm
M	20	N	valve	$\mathbf{L}\mathbf{L}$	24	24	10	16
M	20	D	valve	$\mathbf{LL}$	21	21	6	12
M	40	N	valve	GAS	192	242	32	62
M	40	D	valve	GAS	114	114	6	19
М	60	Ň	valve	$\mathbf{L}\mathbf{L}$	440	590	190	290
M	60	D	valve	$\mathbf{L}\mathbf{L}$	390	440	110	150
М	80	N	con-non	$\mathbf{L}\mathbf{L}$	184	184	44	64
М	80	D	con-non	$\mathbf{L}\mathbf{L}$	144	144	- 29	34
M	100	N	valve	LL	83	133	53	83
M	100	D	valve	$\mathbf{L}\mathbf{L}$	78	78	83	83
Ĺ	125	N	valve	GAS	•	•	49980	49980
L	125	D	valve	GAS	•	•	89980	89980
Ĺ	140	N	valve	HL	1192	1192	1292	1592
Ĺ	140	D	valve	HL	1692	2392	1092	1092
L	144	N	valve	HL	992	992	992	992
L	144	D	valve	HL	1042	1042	92	142
L	147	N	valve	HL	3492	4992	2392	2992
L	147	D	valve	HL	2193	2193	293	293
L	153	N	valve	GAS	8992	9992	9992	9992
L	153	D	valve	GAS	39993	39993	44993	44993
L	159	N	valve	GAS	6993	6993	3993	3993
L	159	D	valve	GAS	39988	39988	15988	19988
L	164	N	con-non	GAS	1180	1180	480	680
L	164	D	con-non	GAS	1093	1093	693	693

N = 24

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Duplicate Data

----- INSTR=TLV Sniffer ------

	Sample	Sample Type			Max.Sus. SV	Peak SV	Max.Sus. SV	Peak SV
Refinery	ID	(N or D)	Type	Phase	<pre>@ Surface</pre>	<pre>@ Surface</pre>	at 1 cm	at 1 cm
м	20	N	valve	$\mathbf{L}\mathbf{L}$			•	
M	20	D	valve	LL	•	•		
M	40	N	valve	GAS	Ō	0	0	Ō
M	40	D	valve	GAS	Ō	Ō	Ō	Ō
M	60	N	valve	LL	100	100	30	30
M	60	D	valve	LL	100	100	16	16
M	80	N	con-non	LL	92	92	45	45
M	80	D	con-non	LL	108	108	33	33
M	100	Ň	valve	$\mathbf{L}\mathbf{L}$	30	30	15	15
M	100	D	valve	$\mathbf{LL}$	32	32	30	30
L	125	Ň	valve	GAS	•	•	•	•
Ē	125	D	valve	GAS	•	•	•	•
Ē	140	Ň	valve	HL	992	992	792	792
Ĺ	140	D	valve	HL	992	992	772	772
Ĺ	144	N	valve	HL	642	642	372	372
L	144	D	valve	HL	538	538	338	338
L	147	N	valve	HL	480	480	23	23
L	147	D	valve	HL	4	4	4	4
L	153	N	valve	GAS	3430	3430	3130	3130
L	153	D	valve	GAS	4030	4030	3130	3130
L	159	N	valve	GAS	2000	2000	1100	1100
L	159	D	valve	GAS	2800	2800	2200	2200
L	164	N	con-non	GAS	80	80	0	0
L	164	D	con-non	GAS	100	100	86	86

N = 24

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# WSPA Screening Study Duplicate Data

				INSTR=	=HNu -							
		Sample			Max.	Sus.		Peak	Max.	Sus.	P	eak
	Sample	Type			S	v		sv	S	v		SV
Refinery	ID	(N or D)	Type	Phase	e Sur	face	6	Surface	at	1 CM	at	1 cm
м	20	N	valve	LL	1	.1		16		1		2
M	20	D	valve	$\mathbf{L}\mathbf{L}$	1	.6		16		0		2
M	40	N	valve	GAS	18	0		180	2	0		40
M	40	D	valve	GAS	5	0		70	1	0		10
M	60	N	valve	LL				•		•		•
M	60	D	valve	LL				•		•		•
M	80	N	con-non	LL		•		•		•		•
M	80	D	con-non	LL		•		•		•		•
M	100	N	valve	LL		•		•		•		•
M	100	D	valve	LL		•		•		•		•
L	125	Ň	valve	GAS	4	5		•				
L	125	D	valve	GAS	4	8		48	4	3		43
L	140	Ň	valve	HL	1	.5		15	1	0		10
L	140	D	valve	HL	1	0		10		5		5
L	144	N	valve	HL	1	.6		16		3		3
L	144	D	valve	HL	1	.9		19		3		3
L	147	Ň	valve	HL	_	0		0		0		0
L	147	D	valve	HL		0		0		0		0
Ĺ	153	Ň	valve	GAS	1	.9		19	1	9		19
L	153	D	valve	GAS		•		•		•		•
L	159	Ň	valve	GAS		0		Ō		0		0
L	159	D	valve	GAS		0		0		0		0
Ē	164	Ň	con-non	GAS		0		0		0		0
T.	164	D	con-non	GAS		0		Ō		0		0

N = 24

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## WSPA Screening Study Duplicate Data

			INSTR	=TVA 10	000 (FTD)			
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		Sample			Max.Sus.	Peak	Max.Sus.	Peak
	Sample	Type			SV	SV	SV	SV
Refinery	ID	(N or D)	Type	Phase	@ Surface	9 Surface	at 1 cm	at 1 cm
		(	- 4 1		-			
M	20	N	valve	$\mathbf{LL}$	•	•	•	•
M	20	D	valve	$\mathbf{L}\mathbf{L}$	•	•	•	•
М	40	N	valve	GAS	•	•	•	•
M	40	D	valve	GAS	•	•	•	
M	60	N	valve	$\mathbf{L}\mathbf{L}$	•	•	•	•
М	60	D	valve	$\mathbf{L}\mathbf{L}$	•	•	•	•
М	80	N	con-non	$\mathbf{L}\mathbf{L}$	690	700	40	100
M	80	D	con-non	$\mathbf{L}\mathbf{L}$	495	595	120	125
M	100	N	valve	$\mathbf{L}\mathbf{L}$	32	62	32	62
M	100	D	valve	$\mathbf{L}\mathbf{L}$	103	173	33	38
L	125	N	valve	GAS	•	179848	•	98654
L	125	D	valve	GAS	•	132978	•	136248
L	140	N	valve	HL	•	1688	•	1751
L	140	D	valve	HL	•	3627		3860
L	144	Ň	valve	HL	•	2395	•	222
L	144	D	valve	HL	•	519	•	3330
L	147	N	valve	HL	•	5981	•	12
L	147	D	valve	HL	•	3636	•	51
L	153	N	valve	GAS	•	29096	•	12996
L	153	D	valve	GAS	•	18296	•	18296
L	159	N	valve	GAS	•	17093	•	7339
$\mathbf{L}$	159	D	valve	GAS	•	56083	•	20352
L	164	N	con-non	GAS	. •	331	•	167
L	164	D	con-non	GAS	•	709	•	225

N = 24

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# API PUBL\*332 95 WSPA Screening Study Duplicate Data

			INSTR=	=TVA 1(	000 (PID) -			
	Sample	Sample Type			Max.Sus. SV	Peak SV	Max.Sus. SV	Peak SV
Refinery	ID	(N or D)	Туре	Phase	<pre>@ Surface</pre>	<pre>@ Surface</pre>	at 1 cm	at 1 cm
М	20	N	valve	LL	•	•	•	•
M	20	D	valve	$\mathbf{L}\mathbf{L}$	•	•	•	•
M	40	N	valve	GAS	•	•	•	•
Μ	40	D	valve	GAS	•	•	•	•
M	60	N	valve	$\mathbf{L}\mathbf{L}$	•	•	•	•
M	60	D	valve	$\mathbf{L}\mathbf{L}$	•	•	•	•
М	80	N	con-non	$\mathbf{L}\mathbf{L}$	•	•	•	•
М	80	D	con-non	LL	•	•	•	•
M	100	N	valve	$\mathbf{L}\mathbf{L}$	•	•	•	•
M	100	D	valve	$\mathbf{LL}$	•	•	•	•
L	125	N	valve	GAS	•	128	•	120
L	125	D	valve	GAS	•	115	•	105
L	140	N	valve	HL	•	14	•	14
L	140	D	valve	HL	•	21	•	23
L	144	N	valve	HL	•	16	•	3
L	144	D	valve	HL	•	9	•	24
L	147	N	valve	HL	•	25	•	0
L	147	D	valve	HL	•	20	•	0
L	153	N	valve	GAS	•	39	•	34
L	153	D	valve	GAS	•	43	•	42
L	159	N	valve	GAS	•	1	•	1
L	159	D	valve	GAS	•	2	•	6
L	164	N	con-non	GAS	•	1	•	1
L	164	D	con-non	GAS	•	1	•	1

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